

E.I. DUPONT DE NEMOURS PONTCHARTRAIN SITE NEOPRENE UNIT

APPLICATION FOR RENEWAL OF PERMIT NUMBER 2249-V6

LAPLACE, LOUISIANA ST. JOHN THE BAPTIST PARISH

AGENCY INTEREST NUMBER 38806

DECEMBER 4, 2013

MAINFILE



DuPont Performance Polymers Pontchartrain Site 560 Highway 44 LaPlace, LA 70068-6908

December 4, 2013

Mr. Sanford Phillips
Assistant Secretary, Environmental Services
Department of Environmental Quality
602 N. Fifth Street
Baton Rouge, LA 70802

original to JOH Con to Petro 162 Laylon

Dear Mr. Phillips:

Re: Title V Permit Renewal Application, Al No. 38806 - Permit No. 2249-V6

Enclosed are three copies of the Title V permit renewal application for DuPont's Neoprene Unit located in LaPlace, Louisiana. This application includes revised emission calculations and the addition of four new sources.

The table below shows a summary of the permitted limits and the proposed limits due to the revisions and new sources.

Pollutant	Current Permit (tpy)	Proposed Permit (tpy)	Change (tpy)
Chloroprene	173.48	174.3	+0.82
Toluene	33.81	33.14	-0.67
VOC	210.68	206.35	-4.33
Ammonia	10.51	5.27	-5.24
Particulates	0.15	0.19	+0.04

Enclosed is a check for \$1,866.00 to cover the cost of the minor modification. If you need additional information or have any questions you can contact me at 985-536-5437 or at Doris.B.Grego@usa.dupont.com.

Sincerely,

Doris B. Grego, P.E.

Nois B. Lego

Senior Environmental Consultant

Enclosures

cc: EPA Region VI

RECEIPT OF CHECK

Master AI #: 38806

Name on Check: El Dupont De Nemours & Company

Master File Name: E I DuPont de Nemours & Co - Pontchartrain Site

Check Received Date: 12/5/2013

Check Date: 11/20/2013

Check Number: 3000144100

Check Amount (\$): \$1,866.00

Staff Entry: SUNSHINEM

Date data entered: 12/5/2013

Media: AIR

Reason: Renewal w/a Mod.

Comments:



E.I. DUPONT DE NEMOURS PONTCHARTRAIN SITE NEOPRENE UNIT

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DECEMBER 4, 2013

TABLE OF CONTENTS

1.0 INTRODUCTION

- 1.1 Process Description
- 1.2 Emission Sources
- 1.3 Emission Calculation Methodology
- 1.4 Consolidation of Fugitive Emissions

2.0 REGULATORY APPLICABILITY

- 2.1 Federal and State Regulations
- 2.2 Prevention of Significant Deterioration (PSD) Regulations
- 2.3 Nonattainment New Source Review (NNSR)
- 2.4 New Source Performance Standards (NSPS)
- 2.5 National Emission Standards for Hazardous Air Pollutants
- 2.6 Louisiana Air Toxics Program LAC 33:III.Chapter 51 (State Only Requirements)
- 2.7 Insignificant Activities
- 2.8 General Condition XVII Activities

3.0 APPLICATION FOR APPROVAL OF EMISSIONS OF AIR POLLUTANTS FROM PART 70 SOURCES

FIGURES

Figure 1 Site Location Map

Figure 2 Neoprene Unit Process Diagram

APPENDICES

Appendix A Air Emission Calculations

Appendix B Certificate of Good Standing

Appendix C Fugitive Emissions Program Consolidation Notice

SECTION 1.0 INTRODUCTION

1.0 INTRODUCTION

E.I. DuPont de Nemours & Co., Inc. (DuPont) owns and operates a chemical manufacturing facility near LaPlace, Louisiana referred to as the Pontchartrain Site. The Site Location Map is provided in Figure 1.

Pontchartrain Site is a major source with respect to LAC 33:III.507 and 40 CFR 70 (i.e., a major source under the Part 70 Operating Permit program), a major stationary source with respect to LAC 33:III.509 and 40 CFR 51.166 (i.e., a major source under the Prevention of significant Deterioration [PSD] subprogram of the New Source Review [NSR] program) and a major source of toxic/hazardous air pollutants with respect to LAC 33:III.Chapter 51 and 40 CFR 63.

The site operates under several Part 70 operating permits for the following units: Neoprene Unit, Chloroprene Unit, HCl Recovery Unit, Diamines Unit and the Power Unit. The Neoprene Unit is permitted under permit number 2249-V6. This permit expires on June 16, 2014 unless a timely and complete renewal application has been submitted six months prior to expiration. This application is being submitted for the purpose of requesting a renewal to the existing Part 70 permit for the Neoprene Unit. This application also includes updates to the emissions calculations.

1.1 Process Description

The Neoprene Unit belongs to the Polymer and Resins I MACT Group. Neoprene is a synthetic rubber, which is a product of the polymerization of chloroprene. Chloroprene is manufactured at the Pontchartrain Site in the Chloroprene Unit. Prior to polymerization, refined chloroprene is stored in brine cooled tanks. From the tanks, the chloroprene is pumped to a make up area where various viscosity modifiers and emulsification agents are added to create a chloroprene emulsion. The emulsion is then transferred to one of the poly kettles (PKs), where polymerization occurs in the presence of a catalyst to form neoprene. Once the emulsion reaches the desired specific gravity, stabilizers are added to stop the reaction. The emulsion is then cooled and pumped to the unstripped emulsion tanks. From the tanks the emulsion is sent to the steam stripers to recover unreacted chloroprene. The chloroprene vapor is sent to condensers for recovery and the stripped emulsion is sent to storage. From storage, the emulsion is fed to the freeze roll pan. Acetic acid is added to help isolate the neoprene in the pan. As the freeze roll rotates, a film of neoprene and ice is formed on the surface and removed in a continuous sheet. The film is sent to the wash belt where it is washed with filtered water. From the wash belt, the film goes to squeeze rolls to remove excess water. The film is then sent to the air dryers where steam heated air is forced across the film. From the dryers, the film passes over a cooling roll and is gathered into a rope. The rope is fed to a cutter where the neoprene is cut into small chips. Tale is added to prevent chips from sticking together. The chips are sent through a conveyor where they are weighed and packaged in 55 pound bags.

Emissions at the facility are from the poly kettles, tanks, dryers and fugitive emissions.

ACR (2,3-dichloro-1,3-butadiene) manufactured at the Chloroprene Unit is sent to the Neoprene Unit via pipeline to be refined and stored until needed to manufacture certain neoprene types. A Process Flow Diagram of the Neoprene Unit is included as Figure 2.

1.2 Emission Sources

The following table (Table 1.1) provides a list of all the emission sources at the Neoprene Unit.

TABLE 1.1 EMISSION SOURCE SUMMARY DUPONT – NEOPRENE UNIT				
Number	EQT	Equipment Description		
1700-1	134	No. 7, 8, 10, 13, 14 Emulsion Storage Tanks Manhole and Exhaust Blower		
1700-2	RLP0014	Strippers Condenser Vent		
1700-2A	219	Stripper No. 1		
1700-2B	220	Stripper No. 2		
1700-2C	221	Stripper No. 3		
1700-3	RLP0015	Poly Kettles Vent Condenser		
1700-3A	222	Poly Kettle No. 1		
1700-3B	223	Poly Kettle No. 2		
1700-3C	224	Poly Kettle No. 3		
1700-3D	225	Poly Kettle No. 4		
1700-3E	226	Poly Kettle No. 5		
1700-5	GRP0008	Unstripped Emulsion Storage Tanks Common Vent (CAP)		
1700-5.3	150	Unstripped Emulsion Storage Tank. No. 6		
1700-5.4	151	Unstripped Emulsion Storage Tank. No. 7		
1700-5.5	152	Unstripped Emulsion Storage Tank. No. 8		
1700-5.6	153	Unstripped Emulsion Storage Tank. No. 10		
1700-5.7	154	Unstripped Emulsion Storage Tank. No. 13		
1700-5.8	155	Unstripped Emulsion Storage Tank. No. 14		
1700-5A	167	No. 6 Emulsion Storage Tank Manhole		
1700-13	135	Poly Kettles Manholes/Strainers (1 and 2) Common Vent		
1700-13A	136	Poly Kettles Manholes/Strainers (3, 4 and 5) Common Vent		
1700-14B.3	RLP0013	Stabilizer and Catalyst Tanks Manhole Vent		
1700-14B	GRP0006	Solution Make up Manhole Common Vent		
1700-14B.1	137	Acetic Acid Make-up Tank		
1700-14B.2	138	Acetic Acid Hold-up Tank		
1700-20	139	CD Refining Column Jet		

<u></u>	TABLE 1.1					
	EMISSION SOURCE SUMMARY					
	DUPONT - NEOPRENE UNIT					
Number	EQT	Equipment Description				
1700-20A	140	CD Refining Column Jet (Spare)				
1700-21A	141	2MM Pound CD Storage Tank				
1700-25A	GRP0007	Product Drying CAP				
1700-25	142	East Wash Belt Dryer				
1700-26	143	West Wash Belt Dryer				
1700-27	144	East Hot Dryer Exhaust				
1700-28	145	West Hot Dryer Exhaust				
1700-45	146	No. 1 East Dryer Cooling Compartment				
1700-46	147	No. 1 West Dryer Cooling Compartment				
1700-47	148	No. 2 East Dryer Cooling Compartment				
1700-48	149	No. 2 West Dryer Cooling Compartment				
1700-50	GRP0009	Stabilizer Tanks Common Vent (CAP)				
1700-50.1	156	Stabilizer Tank No. 1				
1700-50.2	157	Stabilizer Tank No. 2				
1700-50.3	158	Stabilizer Tank No. 3				
1700-50.4	159	Stabilizer Tank No. 4				
1700-50.5	160	Stabilizer Tank No. 5				
1700-50.6	161	Stabilizer Tank – LD750				
1700-51	162	Inhibitor Mix Tank				
1700-53	163	Stripped Emulsion Tank No. 1				
1700-54	164	Stripped Emulsion Tank No. 2				
1700-55	165	Stripped Emulsion Tank No. 3				
1700-56	RLP0016	No. 6, 7, 8, 10, 13 and 14 Unstripped Storage Tanks				
		Depressure Vent				
1700-57	166	Diisobutylene (DIB) Storage Tank				
1700-60	168	Diisobutylene Nitrosate (DIBN) Storage Tank No. 3				
1700-61	169	Diisobutylene Nitrosate (DIBN) Storage Tank No. 4				
1700-62	170	Diisobutylene Nitrosate (DIBN) Storage Tank No. 5				
1700-63	GRP0010	Vent Header System (CAP)				
1700-63.1	171	No. 1 CD Solution Tank				
1700-63.2	175	No. 2 CD Solution Tank				
1700-63.3	176	Recovered CD Storage Tank No. 1				
1700-63.4	177	Recovered CD Storage Tank No. 2				
1700-63.5	178	CD Heels Tank				
1700-63.8	181	Crude CD Storage Tank No. 3				
1700-63.9	182	Refined CD Storage Tank				
1700-63.10	172	Inhibitor Final Make-up Tank				
1700-63.11	173	Inhibitor Hold-up Tank				
1700-64	183	Water Solution Exhaust Fan				

C

	TABLE 1.1					
	EMISSION SOURCE SUMMARY					
	_	DUPONT – NEOPRENE UNIT				
Number	EQT	Equipment Description				
1700-66	185	Poly Building Wall Fans				
1700-67	186	Stripped Emulsion Tank No. 4				
1700-68	187	Stripped Emulsion Tank No. 5				
1700-69	188	Stripped Emulsion Tank No. 9				
1700-70	189	Stripped Emulsion Tank No. 11				
1700-71	190	Stripped Emulsion Tank No. 12				
1700-72	191	Stripped Emulsion Tank No. 15				
1700-73	192	Stripped Emulsion Tank No. 16				
1700-74	193	Finishing Stabilizer Makeup Bag Filter				
1700-75	194	Resin 90 Railcar				
1700-76	195	Rosin S Railcar				
1700-77	196	Octopol Storage Tank				
1700-79	198	Emergency Stablizer Drumming				
1700-80	RLP017	ACR Storage Common Vent Header				
1700-80.1	199	Refined ACR Storage Tank				
1700-80.2	200	Chlorinated ACR Storage Tank				
1700-81	RLP018	ACR Refining Vent				
1700-81.1	205	NMP/PTZ Tote				
1700-81.2	206	Aqueous Actrene Tote				
1700-81.3	207	Recovery Column Heels Tote				
1700-81.4	208	TBC Tote				
1700-81.5	209	ACR Refining Column				
1700-81.6	210	ACR RC Condenser				
1700-81.7	211	ACR RC Reboiler				
1700-82	201	ACR/Solvent Blend Tank				
1700-83	RLP019	ACR Drumming Vent				
1 - 93	FUG0004	Fugitive Emissions - Neoprene Unit				
3 - 95	202	Diversion Tank				
4 - 95	203	Surge Tank				
5 - 95	204	Aeration Tank				
1700-84A	212	Advanced Fibres System (AFS) Emulsion Shipping (Emulsion Blend Tank)				
1700-84B	213	Advanced Fibres System (AFS) Emulsion Shipping (Tote Loading)				
1700-85	214	Liquid Dispersion Loading Emissions (Truck, Tote, Railcar)				
1700-86	215	Rosin S Storage Tank				
6-95	New	Clarifier				
1700-87	New	No. 10 Emulsion Storage Tank Manway				
1700-88	New	No. 13 Emulsion Storage Tank Manway				
1700-89	New	No. 14 Emulsion Storage Tank Manway				

1.3 Emissions Calculation Methodology

Potential emissions from poly kettles, tanks, dryers and fugitive emissions are based on material balance, stack testing, and engineering calculations. Where appropriate, the latest version of USEPA emission factors and the Tanks program are used to calculate emissions. Emission calculations are presented in Appendix A.

Calculations were updated to reflect current operations; also four new sources were added. Below is a comparison of the current permitted limits and the proposed limits.

Pollutant	Current Permit (tpy)	Proposed Permit (tpy)	Change (tpy)
Chloroprene	173.48	174.3	+0.82
Toluene	33.81	33.14	-0.67
VOC	210.68	206.35	-4.33
Ammonia	10.51	5.27	-5.24
Particulates	0.15	0.19	+0.04

1.4 Consolidation of Fugitive Emissions

On November 18, 2013, DuPont submitted a site wide Fugitive Emissions Program Consolidation Notice. A copy of this document is included in Appendix C. DuPont is requesting to incorporate this program with the permit renewal.

SECTION 2.0 REGULATORY APPLICABILITY

2.0 REGULATORY APPLICABILITY

2.1 Federal and State Regulations

The Pontchartrain Site is subject to a variety of federal and state air quality regulations. State requirements are outlined in Chapters 9, 11, 13, 21, 51, 56 and 59 of the Louisiana Air Quality Regulations. In accordance with LAC 33:III.517.D.10, state and federal requirements have been identified in a matrix on Table 1 contained in Item 22 of the Application for Approval of Emissions of Air Pollutants from Part 70 Sources (Section 3.0 of this document). Table 2 of Item 22 clearly identifies potentially applicable state and federal requirements for the facility. Table 2 also contains a description and reference to compliance methods/provisions required by regulations and/or current permit. Table 3, also contained in Item 22, indicates exempt status or non-applicability for emission sources.

2.2 Prevention of Significant Deterioration (PSD) Regulations

This application does not include a significant modification; therefore, a PSD review is not required.

2.3 Nonattainment New Source Review (NNSR)

St. John the Baptist Parish, in which the DuPont, Neoprene facility is located, is designated as an attainment area for all criteria pollutants. Therefore, NNSR does not apply.

2.4 New Source Performance Standards (NSPS)

Certain units or equipment items at the Neoprene Unit are designated as affected facilities under 40 CFR 60, Subpart Kb.

2.5 National Emission Standards for Hazardous Air Pollutants (40 CFR 61 AND 63)

The Pontchartrain Site is a major source of hazardous air pollutants (HAPs). The facility is subject to certain provisions of 40 CFR 61 and 63, which are stated in the applicability matrices of the permit application form, Item 22 in Section 3.0 of this document.

2.6 Louisiana Air Toxics Program - LAC 33:III.Chapter 51 (State Only Requirements)

The Pontchartrain Site is a major source of toxic air pollutants (TAPs). The facility is subject to certain provisions of LAC 33:III. Chapter 51, which are stated in the

applicability matrices of the permit application form, Item 22 in Section 3.0 of this document.

2.7 Insignificant Activities

The Neoprene facility engages in a variety of activities which are defined as insignificant under LAC 33:III.501.B.5. Activities exempt based on size or emission rate are addressed in Item 20 of The Application for Approval of Emissions from Part 70 Sources, Section 3.0 of this document.

2.8 General Condition XVII Activities

The Neoprene facility performs various activities which are authorized under LDEQ General Permit Condition XVII which are included in the current Air Permit No. 2249-V6. These activities are listed in Item 19 of the Application for Approval of Emissions from Part 70 Sources, Section 3.0 of this document.

SECTION 3.0

APPLICATION FOR APPROVAL OF EMISSIONS OF AIR POLLUTANTS FROM PART 70 SOURCES

Department of Environmental Quality
Office of Environmental Services
Air Permits Division
P.O. Box 4313
Baton Rouge, LA 70821-4313
(225) 219-3181

LOUISIANA

Application for Approval of Emissions of Air Pollutants from Part 70 Sources



PLEASE TYPE OR PRINT

1.	Facility	Information	[LAC 33:III.517.D	.1]
			, [,

Facility Name or Process Unit Name (if any	7)		. —	cess Units
Pontchartrain Works, Neoprene Unit	Pontchartrain Works, Neoprene Unit			Unit-specific Permit
Agency Interest Number (A.I. Number)		Currently Effective Permit Number(s)		
38806		2249-V6		1
Company - Name of Owner				
E.I. DuPont de Nemours and Co., Inc. (Du	<u> </u>			
Company - Name of Operator (if different	from Owner)			
Parent Company (if Company - Name of C	wner given a	bove is a division	on)	
Ownership: Check the appropriate box.		 _		
orporation, partnership, or sole proprietors	hip 🔲 reg	ulated utility	municipal go	overnment
state government	☐ fed	eral government	other, specif	y
[LAC 33:III.517.D.18, unless otherw What does this facility produce? Add more roo This unit manufactures, neoprene, which What modifications/changes are proposed in a This is the five year renewal application for	ws as necessalis a synthetic	n? Add more ro		of chloroprene.
Nearest town (in the same parish as the fact LaPlace	ility):	Parish(es) s	where facility is locate Baptist	d:
Distance To (mi): 194	Texas <u>2</u>	10 Arkansas	56 Mississippi	131 Alabama
Latitude of Facility Front Gate: 30 D	eg <u>0</u> :	3 Min	<u>14</u> Sec	Hundredths
Longitude of Facility Front Gate: 90 D	eg <u>3</u>	<u>l</u> Min	<u>29</u> Sec	Hundredths
Distance from nearest Class I Area:	<u>113</u> ki	lometers		
Add physical address and description of locati directions. Add more rows as necessary. The facility is located at 586 Highway 44, Mississippi River, to the North by John L.	LaPlace, Lou	uisiana. The fa	cility is bordered on th	ne south by the
facility to the east and the west.		·		

- Map attached (required per LAC 33:Ⅲ.517.D.1)
- ☑ Description of processes and products attached (required per LAC 33:III.517.D.2)
- ☑ Introduction/Description of the proposed project attached (required per LAC 33:III.517.D.5)

3. Conf	idential	ity [LAC 33.I.	Chapter 5]				•	
Are you req	questing co	onfidentiality for a	ny information <u>except a</u>	<u>ir pollutant emissi</u>	on rates?	☐ Yes	⊠ No	
require a s	submittal ti		onfidentiality is reques m this application. In t instructions.					
							<u>.</u>	
4. Type	of Appl	lication [LAC	33:III.517.D]					
Complete t		-	2) that corresponds to	the type of permit	being sou	ight. Ch	eck all that a	apply within
Column 1				Column 2				•
Part 70	General	<u> </u>		Part 70 Regul	ar	_		
Renewa	al			Renewal			:	
Select one,	if applical	ole:		Select one, if app	licable:			
☐ Entirely				Entirely new				
☐ Modifice	cation or ex reconcilia	xpansion of existin	g facility (may also	Significant m	odificatio			
Reconc	iliation on	ly		Minor modifi				•
🔲 Individ	ual emissio	ons unit(s) addition	1	also include r	econcilia	tions) (L	.AC 33:Щ.52	25]
				Reconciliatio	n only	<u> </u>		
				NSR Analysis:			•	
					_			
				PSD NNSR	<u>⊔</u>			
								•
Does this s	ubmittal uj	pdate or replace a	n application currently	under review? 🗌	Yes 🛚	No		
If yes, prov	ide date th	at the prior applic	ation was submitted: _					
			isting facility that does	not have an air ou	ality nam	nit:	• •	
Scient One	ու ասե գրիւ 7		ndfathered (LAC 33:III	-	anty pern	ut.		•
	Ī		mpted (e.g., Small Sou	•	C 33:III ⁴	501.B.2	ժ) ;	
	Ĭ	Previously Unp		2p.10, 2				•
	•	_		•				
5. Fee I	Informa	tion [LAC 33	:III.517.D.17]				•	•
		e fee code is based	on an operational para	meter (such as nun	nber of er	nployee	s or capital c	ost), enter that
parameter l	here	Enter the Standa	rd Industrial Classificat		h Amoria	on Indu	cter Classific	nation
		apply to the facility		ion (SIC) and Non	ui Aineric	STILL LINGU	SILY CIASSILI	cauon
Primary S		2822		<u>325</u>	<u>212</u>			
Secondary	SICC(s):						•	•
	220(0).			<u> </u>				 .
Project Fa	ee Calcula	ition: Enter fee co	ode, permit type, produ	action canacity/thr	nughnut	and fee	amount nur	suant to LAC
			as needed. Include w					
permit app		<u>. </u>						
FEE]	EXISTING	INCREMENTAL			JRCHA.		
CODE	TYPE	CAPACITY	CAPACITY	MULTIPLIER	<u>NSPS</u>	<u>PSD</u>	AIR	TOTAL
0500	 	 	INCREASE				TOXICS	AMOUNT
0580	ľ		ì	l		ı	l Ll	\$1,866.00

\$

\$

GRAND TOTAL

Optional Fee Explanation: Use the space Using this area will help to avoid confusion.	ce provided to giv	ve an explanation o	of the fee determination display	yed above.
Electronic Fund Transfer (EFT): If paying include the EFT Transaction Number, the Dat If not paying the permit application fee using I EFT Transaction Number	te that the EFT v	vas made, and the		in the EFT.
6. Key Dates Estimated date construction will commence:	NA	Estimated date	operation will commence:	NA NA
7. Pending Permit Applications [LAC 33:III.517.D.18] List all other process units at this facility for acted upon by LDEQ as of the date of submitt to update this table during the permit review	which Part 70 al of this applica	permit application	is have been submitted, but he "none" in the table. ***It is n	
Process Unit Name	Permit N		Date Submitted]
8. LAC 33:I.1701 Requirements renewals - Yes No	- Answer al	l below for n	ew sources and perm	it
Does the company or owner have federal or s for which you are applying in Louisiana or of corporations, or other entities who own a conenvironmental management of the facility for Yes No	ther states? (This strolling interest	s requirement app of 50% or more i	lies to all individuals, partner 1 your company, or who parti	ships, cipate in the
If yes, list States:		<u> </u>		
Do you owe any outstanding fees or final pen- lf yes, explain below. Add rows if necessary.	alties to the Dep	artment? 🗌 Yes	⊠ No	
Is your company a corporation or limited liab If yes, attach a copy of your company's Cer Secretary of State. The appropriate certific	rtificate of Regi	stration and/or C		

type of permit shield being soug	the Include the specific regulato	7
. If additional pages are used, attac	nstances that will justify the pern	nit -
oly):		
Specific Citation(s)	Explanation	\exists
	·	
Specific Citation(s)	Explanation	
	oly): Specific Citation(s)	Specific Citation(s) Explanation

10. Certification of Compliance With Applicable Requirements

Statement for Applicable Requirements for Which the Company and Facility Referenced In This Application Is In Compliance

Based on information and belief, formed after reasonable inquiry, the company and facility referenced in this application is in compliance with and will continue to comply with all applicable requirements pertaining to the sources covered by the permit application, as outlined in Tables 1 and 2 in the permit application. For requirements promulgated as of the date of this certification with compliance dates effective during the permit term, I further certify that the company and facility referenced in this application will comply with such requirements on a timely basis and will continue to comply with such requirements.

For corporations only: By signing this form, I certify that, in accordance with the definition of Responsible Official found in LAC 33:III.502, (1) I am a president, secretary, treasurer, or vice-president in charge of a principal business function, or other person who performs similar policy or decision-making functions; or (2) I am a duly authorized representative of such person; am responsible for the overall operation of one or more manufacturing, production, or operating facilities addressed in this permit application; and either the facilities employ more than 250 persons or have gross annual sales or expenditures exceeding \$25 million (in second quarter 1980 dollars); or the delegation of authority has been approved by LDEQ prior to this certification.*

CERTIFICATION: I certify, under provisions in Louisiana and United States law which provide criminal penalties for false statements, that based on information and belief formed after reasonable inquiry, the statements and information contained in this Application for Approval of Emissions of Air Pollutants from Part 70 Sources, including all attachments thereto and the compliance statement above, are true, accurate, and complete.

CERTIFICATION: I certify that the engineering calculations, drawings, and design are true and accurate to the best of my knowledge.

a. Responsible Official		
Name		
Walter L. Glenn		
Title		
Plant Manager		
Сотралу		
E.I. DuPont de Nemours and	Company	
Suite, mail drop, or division		
Street or P.O. Box		
586 Highway 44		
City	State	Zip
LaPlace	LA	70068
Business phone		
985-536-5129		
Email Address		
walter.l.glenn@usa.dupont.co	<u>m</u>	
 :		-

b. Protessional Engineer		
Name		
Doris B. Grego		
Title		
Senior Environmental Consultan	t	
Company		
E.I. DuPont de Nemours and Co	mpany	
Suite, mail drop, or division	•	
Street or P.O. Box		
586 Highway 44		
City	State	Zip
LaPlace	LA	70068
Business phone		
985-536-5437		
Email Address		
doris h grego@usa dunont.com		

Signature of responsible official (See 40 CFR 70.2):

Date:

12-3-13

*Approval of a delegation of authority can be requested by completing a Duly Authorized Representative Designation Form (Form_7218) available on LDEQ's website at http://www.deq.louisiana.gov/ponal/tabid/2758/Default.aspx

Date: 12 / Date:

Signature of Professional Engineer:

Louisiana Registration No.

33930

DORIS B. GREGO
License No. 33930
PROFESSIONAL ENGINEER
IN

11. Personnel [LAC 33:III.517.D.1]

a. Manager of Facility	who is located :	et plant site		b. On-site contact regardin	e air pollu	tion control
Name				Name		
Walter L. Glenn	∐Primar	y contact		Doris B. Grego	⊠Pn	mary contact
Title	<u> </u>		-	Title		
Plant Manager	alter L. Glenn tile ant Manager ompany b. DuPont de Nemours and Company ite, mail drop, or division reet or P.O. Box 6 Highway 44 ty State Zip Place LA 70068 ssiness phone 5-536-5129 nail address alter.l.glenn@usa.dupont.com Person to contact with written correspondence ame Primary contact tile ampany ite, mail drop, or division reet or P.O. Box ty State Zip ssiness phone anil address Person to contact about Annual Maintenance Ferme Primary contact			Senior Environmental Cor	s <u>ulta</u> nt	
Company	-			Company		
E.I. DuPont de Nemour	rs and Company	j		E.I. DuPont de Nemours and	Company	
Suite, mail drop, or d	ivision			Suite, mail drop, or division	1	
Street or P.O. Box				Street or P.O. Box		
586 Highway 44		,		586 Highway 44		
City	State	Zip		City	State	Zip
LaPlace	l = -			LaPlace	LA	70068
Business phone	<u> </u>			Business phone		
985-536-5129		1	:	985-536-5437		
Email address	Fitle Plant Manager Company E.I. DuPont de Nemours and Company Suite, mail drop, or division Street or P.O. Box S86 Highway 44 City State Zip APlace LA 70068 Business phone S85-536-5129 Email address valter.l.glenn@usa.dupont.com C. Person to contact with written correspondence Name Primary contact Citle Company Suite, mail drop, or division Street or P.O. Box City State Zip			Email address		
I	lupont com			doris.b.grego@usa.dupont.co	om	
			Ī			
			,	г		
c. Person to contact w	ith written corre	spondence		d. Person who prepared thi	s report	
Name	Prim	ary contact		Name		Primary contact
Title				Title		
Company				Company		
Suite, mail drop, or di	vision			Suite, mail drop, or division		
Street or P.O. Box				Street or P.O. Box		·
City	State	Zip		City	State	Zip
Business phone		' .		Business phone		
Email address	-			Email address		
			, ,	L		
	Iter L. Glenn			a b c d	ouner (sp	ecify below)
Name	□P	rimary contact		ite, mail drop, or division		
Title			Str	reet or P.O. Box		
Company			Cit	ty	State	Zip
Business Phone			En	nail Address		

12. Proposed Project Emissions [LAC 33:III.517.D.3]

List the total emissions following the proposed project for this facility or process unit (for process unit-specific permits).

Speciate all criteria pollutants, TAP, and HAP for the proposed project.

Pollutant	Proposed Emission Rate (tons/yr)
PM2.5	0.19
NOx	3.30
VOC	206.35
Ammonia	5.27
Chloroprene	174.30
Hydrochloric Acid	0.07
Methylene Chloride (Dichloromethane)	0.06
Tetrachloroethylene	0.04
Toluene	33.14
Xylene	0.02
	
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13. History of Permitted Emissions [LAC 33:III.517.D.18]

List each of the following in chronological order:

- The Permit Number and Date Action Issued for each air quality permit that has been issued to this facility or
 process unit (for process unit-specific permits) within the last ten (10) years.
- All small source exemptions, authorizations to construct, administrative amendments, case-by-case insignificant
 activities, and changes of tank service that have been approved since the currently effective Title V Operating
 Permit or State Operating Permit was issued to this facility or process unit (for process unit-specific permits). It
 is not necessary to list any such activities issued prior to the issuance of the currently effective Title V Operating
 Permit or State Operating Permit, if one exists.

Permit Number	Date Action Issued
	·
2249-V2	December 19, 2003
2249-V3	August 9, 2004
2249-V4	November 28, 2007
2249-V5	December 18, 2008
2249-V6	June 16, 2009
	<u> </u>
	·
	
	
	
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	<u> </u>
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If yes, list all federal and a this facility and/or process Operating Permit or State regulatory authority or au conditions imposed by the	state air quality enforcements unit (for process unit-spectoperating Permit. For eacthorities that issued the action settless	III.517.D.18] - Yes At actions, settlement agreements, iffic permits) since the issuance of action, list the type of action (or on, and the date that the action warment agreement, and consent decrease.	and consent decrees received for the currently effective Title V its tracking number), the
Type of Action or Tracking Numbe	Issuing Authorit	y Date Action Issued	Summary of Conditions Included?
			☐ Yeş ☐ No
			☐ Yes ☐ No
If yes, list all correspond alternate methods of cor specific permits). List the appendix a copy of all the specific permits are specific permits.	dence with LDEQ, EPA, or npliance with any applicable date of issuance of the le	e Methods of Complian other regulatory bodies that provi e regulations for this facility or pi tter and the regulation referenced this table. Letters that are not inc	ides for or supports a request for rocess unit (for process unitby the letter. Attach as an
Date Letter Issued	Issuing Authority	Referenced Regulation(s)	Copy of Letter Attached?
1997	LDEQ	40 CFR 63.114(b)(2)	☐ Yes ☑ No ☐ Yes ☐ No ☐ Yes ☐ No ☐ Yes ☐ No
If yes, list any initial no for this facility or proce Operating Permit or Sta time performance test re	tifications that have been so ss unit (for process unit-spe te Operating Permit in orde equirements that have not b	een satisfied should be listed in S	e tests that have been performed of the currently effective Title V nts. Any initial notification or one-

Initial Notification or

One-time Performance Test?

Table 2 of this application. Add rows to table as necessary.

Regulatory Citation Satisfied

Date

Completed/Approved

Applicable Source(s)

☐ Yes 🗵 No		•	·			under one or more NSA table as necessary. Bo
	Date			s) in Sections 12 ar BACT/LAER Limit ¹		
¹ For example, lb	/MM Btu, ppm	ıvd @ 15%	O ₂ , lb/ton, lb	h/hr		
Was Air Quality	Dispersion Mod	deling as re	equired by LA		l in support of thi	is permit application? sted by LDEQ.)
Was Air Quality Quality Dispersi ☐ Yes ⊠ No Has Air Quality	Dispersion Modeling is Dispersion Modeling is	deling as re only requir deling comp	equired by LA red when appo	AC 33:III performed lying for PSD perm ordance with LAC 3	l in support of thi its and as reques 3:III ever been p	sted by LDEQ.) erformed for this facil
Was Air Quality Quality Dispersi ☐ Yes ⊠ No Has Air Quality	Dispersion Mod on Modeling is Dispersion Mod permit applicati	deling as re only requir deling comp ion previou	equired by LA red when appo pleted in acco sly submitted	AC 33:III performed lying for PSD perm ordance with LAC 3 for this facility or p	l in support of thi its and as reques 3:III ever been p	sted by LDEQ.)
Was Air Quality Quality Dispersi ☐ Yes	Dispersion Modeling is Dispersion Modeling is Dispersion Modeling is Dispersion Modeling is	deling as re only requir deling comp ion previous s AND appi	equired by LA red when appo pleted in acco sly submitted roved by LDE	AC 33:III performed lying for PSD perm ordance with LAC 3 for this facility or p SQ?	l in support of thi its and as reques 3:III ever been p process unit (for	sted by LDEQ.) erformed for this facil
Was Air Quality Quality Dispersi Yes No Has Air Quality support of a air pas required by of Yes No If yes, enter the confirman	Dispersion Modeling is	deling as re only requir deling comp ion previous s AND appo ecent Air Qu above is "ye	equired by LA red when apport coleted in according sty submitted roved by LDE mality Dispers	AC 33:III performed lying for PSD perm ordance with LAC 3 for this facility or p EQ?	I in support of the its and as reques 3:III ever been p process unit (for ts as required by	ited by LDEQ.) performed for this facil process unit-specific p
Was Air Quality Quality Dispersi Yes No Has Air Quality support of a air pas required by of Yes No If yes, enter the confirman	Dispersion Modeling is Dispersion Modeling is Dispersion Modeling is Dispersion Modeling is ther regulations late the most reconstitute the most reconstitute is "no."	deling as re only requir deling comp ion previous s AND appo ecent Air Qu above is "ye	equired by LA red when appointed in according submitted roved by LDE mality Dispers res," enter a su re" in the tab	AC 33:III performed lying for PSD permordance with LAC 3 for this facility or page 202.	in support of the its and as reques 3:III ever been process unit (for process unit (for process unit as required by the recent results in the le as necessary. Lou Ambie	eted by LDEQ.) nerformed for this facil process unit-specific p LAC 33:III were subn

19. General Condition XVII Activities- ✓ Yes ✓ No

Enter all activities that qualify as Louisiana Air Emissions Permit General Condition XVII Activities.

- Expand this table as necessary to include all such activities.
- See instructions to determine what qualifies as a General Condition XVII Activity.
- Do not include emissions from General Condition XVII Activities in the proposed emissions totals for the permit application.

				Emission	Rates - 1	ГРҮ	<u> </u>
Work Activity	Schedule	PM ₁₀	SO ₂	NO _x	co	voc	Other
Inhibitor Mix Tank Cleaning	1 time/yr					0.003	
Refining Column Cleaning	9 times/yr					0.11	
Acetic Acid Rail Car	1 time/yr				1	0.02	
Routine Maintenance Activities	NA					1.75	
Railcars During Shutdown (20 Loading/Steaming)	2 times/yr		 -			0.17	· · · · · · · · · · · · · · · · · · ·
ACR Refining Column and Tanks Cleaning	25 times/yr					0.25	'

20. Insignificant Activities [LAC 33:III.501.B.5] - Yes No

Enter all activities that qualify as Insignificant Activities.

- Expand this table as necessary to include all such activities.
- For sources claimed to be insignificant based on size or emission rate (LAC 33:III.501.B.5.A), information must be supplied to verify each claim. This may include but is not limited to operating hours, volumes, and heat input ratings.
- If aggregate emissions from all similar pieces of equipment (i.e. all LAC 33:III.501.B.5.A.1 activities) claimed to be insignificant are greater than 5 tons per year for any pollutant, then the activities can not be claimed as insignificant and must be represented as permitted emission sources. Consult instructions.

Emission Point ID No.	Description	Physical/Operating Data	Citation
	No. 1 Blend Tank		LAC 33:III.501.B.5.A.3
	No. 2 Blend Tank		LAC 33:III.501.B.5.A.3
	Precondenser Rundown Tank		LAC 33:III.501.B.5.A.3
	EDMA Tote		LAC 33:III.501.B.5.A.3
<u></u>	Calight RPO Tote		LAC 33:III.501.B.5.A.3
	DAXAD Tote		LAC 33:III.501.B.5.A.3
	Dresinate Tote		LAC 33:III.501.B.5.A.3
	Poly Witcolake Tote		LAC 33:III.501.B.5.A.3
	Finishing Witcolake Tote		LAC 33:III.501.B.5.A.3
	DEA Tote		LAC 33:III.501.B.5.A.3
<u></u>	Keltrol Solution Tank		LAC 33:III.501.B.5.A.3
	Sulfur Slurry Batch Tank No. 1		LAC 33:III.501.B.5.A.3
	Sulfur Slurry Batch Tank No. 2		LAC 33:III.501.B.5.A.3

Emission Point ID No.	Description	Physical/Operating Data	Citation
	Finishing Stabilizer M/U Tank		LAC 33:III.501.B.5.A.3
	Finishing Stabilizer Hold Tank		LAC 33:ПІ.501.В.5.А.3
	Finishing Stabilizer Batch Scale Tank		LAC 33:III.501.B.5.A.3
	Lomar Head Tank		LAC 33:III.501.B.5.A.3
	KOH Tote		LAC 33:UI.501.B.5.A.4
	KOH Storage Tank		LAC 33:III.501.B.5.A.4
	DDM Storage Tank		LAC 33:III.501.B.5.A.3
	No. 1 Vent Hood (ACR Lab)		LAC 33:III.501.B.5.A.6
	No. 2 Vent Hood (Neoprene Lab)		LAC 33:III.501.B.5.A.6
	ACR Refining Decanter, Emergency Vent		LAC 33:III.501.B.5.A.6

21. Regulatory Applicability for Commonly Applicable Regulations – Answer all below [LAC 33:III.517.D.10]
Does this facility contain asbestos or asbestos containing materials? Yes No If "yes," the facility or any portion thereof may be subject to 40 CFR 61, Subpart M, LAC 33:III. Chapter 27, and/or LAC 33:III.5151 and this application must address compliance as stated in Section 22 of this application
Is the facility or process unit represented in this permit subject to 40 CFR 68, or is any other process unit located at the same facility as the process unit represented in this application subject to 40 CFR 68? Yes No If "yes," the entire facility is subject to 40 CFR 68 and LAC 33:III. Chapter 59 and this application must address compliance as stated in Section 22 of this application.
Is the facility listed in LAC 33:111.5611
Table 5 \(\sum \text{Yes} \) \(\sum \text{No} \)
Table 6 X Yes No
Table 7 🛛 Yes 🗌 No
Does the applicant own or operate commercial refrigeration equipment normally containing more than 50 pounds of refrigerant at this facility or process unit? Yes No If "yes," the entire facility is subject to 40 CFR 82, Subpart F and this application must address compliance as stated in Section 22 of this application.

22. Applicable Regulations, Air Pollution Control Measures, Monitoring, and Recordkeeping

Important points for Table 1 [LAC 33:III.517.D.10]:

- List in Table 1, by Emission Point ID Number and Descriptive Name of the Equipment, state and federal
 pollution abatement programs and note the applicability or non-applicability of the regulations to each
 source
- Adjust the headings for the columns in Table 1 as necessary to reflect all applicable regulations, in addition to any regulations that do not apply but need an applicability determination to verify this fact.
- For each piece of equipment, enter "1" for each regulation that applies. Enter "2" for each regulation that applies to this type of source, but from which this source of emissions is exempt. Enter "3" for equipment that is subject to a regulation, but does not have any applicable requirements. Also, enter "3" for each regulation that have applicable requirements that apply to the particular emission source but the regulations currently do not apply due to meeting a specific criterion, such as it has not been constructed, modified or reconstructed since the regulations have been in place.
- Leave the spaces blank when the regulations clearly would not apply under any circumstances to the source.
 For example, LAC 33:III.2103 Storage of Volatile Organic Compounds would never apply to a steam generating boiler, no matter the circumstances.
- Consult instructions.

Important points for Table 2 [LAC 33:III.517.D.4; LAC 33:III.517.D.7; LAC 33:III.517.D.10]:

- For each piece of equipment listed in Table 2, include all applicable limitation, recordkeeping, reporting, monitoring, and testing requirements. Also include any one-time notification or one-time tests performance test requirements that have not been fulfilled.
- Each of these regulatory aspects (limitation, recordkeeping, reporting, etc.) should be addressed for each regulation that is applicable to each emissions source or emissions point.
- For each regulation that provides a choice regarding the method of compliance, indicate the method of
 compliance that will be employed. It is not sufficient to state that all compliance options will be employed,
 though multiple compliance options may be approved as alternative operating scenarios.
- Consult instructions.

Important points for Table 3 [LAC 33:III.517.D.16]:

- Each time a 2 or a 3 is used to describe applicability of a source in Table 1, an entry should be made in Table 3 that explains the exemption or non-applicability status of the regulation to that source.
- Fill in all requested information in the table.
- The exact regulatory citation that provides for the specific exemption or non-applicability determination should be entered into the Citation Providing for Exemption or Non-applicability column.
- Consult Instructions.

Important points for Table 4 [LAC 33:III.517.D.18]

- List any single emission source that routes its emissions to another point where these emissions are commingled with the emissions of other sources before being released to the atmosphere. Do not list any single emission source in this table that does not route its emissions in this manner.
- List any and all emission sources that are routed as described above. This includes emission sources that do
 not otherwise appear in this permit application.
- Consult instructions.

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address <u>ALL</u> potentially applicable requirements.

Source	Descriptive Name of the Source				LAC	33:III		<u>-</u> -					LA	AC 3:	3:III.0	Chap	ter		_	
ID No.:	Descriptive Name of the Source	509	2103	2104	2107	2111	2113	2115	2121	5	9	11	13	15	22	29	51	53	56	59
UNF001	Plant Wide					1	1			1	1	1	1	1			1		1	1
EQT134	1700-1 No. 7, 8, 10, 13, 14 Emulsion Storage Tanks Manhole and Exhaust Blower							2					_				3			
EQT135	1700-13 Poly Kettles Manholes/Strainers (1 and 2)							2									3			
EQT136	1700-13A Poly Kettles Manholes/Strainers (3, 4 and 5)							2								l	3			
EQT137	1700-14B.1 Acetic Acid Make-up Tank		3														3			
EQT138	1700-14B.2 Acetic Acid Hold-up Tank		3														3			
EQT139	1700-20 CD Refining Column Jet							1									1			
EQT140	1700-20A CD Refining Column Jet (Spare)							1									1			
EQT141	1700-21A 2MM Pound CD Storage Tank		3														1			
EQT142	1700-25 East Wash Belt Dryer							2									1			
EQT143	1700-26 West Wash Belt Dryer							2	Ì								1			
EQT144	1700-27 East Hot Dryer Exhaust							2									1			
EQT145	1700-28 West Hot Dryer Exhaust							2									1			
EQT146	1700-45 No. I East Dryer Cooling Compt.							2									1			
EQT147	1700-46 No. 1 West Dryer Cooling Compt.							2									1			
EQT148	1700-47 No. 2 East Dryer Cooling Compt.							2									1			
EQT149	1700-48 No. 2 West Dryer Cooling Compt.	_						2									1			
EQT150	1700-5.3 Unstripped Emulsion Storage Tank. No. 6		1						·								1			
EQT151	1700-5.4 Unstripped Emulsion Storage Tank. No. 7		i												,		1			

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address <u>ALL</u> potentially applicable requirements.

Source	Descriptive Name of the Spures				LAC	33:III							LA	AC 3	3:111.0	Chap	ter	•		
ID No.:	Descriptive Name of the Source	509	2103	2104	2107	2111	2113	2115	2121	5	9	11	13	15	22	29	51	53	56	59
EQT152	1700-5.5 Unstripped Emulsion Storage Tank. No. 8		1														1			
EQT153	1700-5.6 Unstripped Emulsion Storage Tank. No. 10		1					,									1			
EQT154	1700-5.7 Unstripped Emulsion Storage Tank. No. 13		1		1		ļ										1_	:		
EQT155	1700-5.8 Unstripped Emulsion Storage Tank. No. 14		1														1_			
EQT156	1700-50.1 Stabilizer Tank No. 1		3														1			
EQT157	1700-50.2 Stabilizer Tank No. 2		3														1			
EQT158	1700-50.3 Stabilizer Tank No. 3		3														1_	<u>.</u>		
EQT159	1700-50.4 Stabilizer Tank No. 4		3														1			
EQT160	1700-50.5 Stabilizer Tank No. 5		3		_							_					1			
EQT161	1700-50.6 Stabilizer Tank - LD750		3													<u> </u>	1			
EQT162	1700-51 Inhibitor Mix Tank		3												Ĺ <u> </u>	<u> </u>	1			
EQT163	1700-53 Stripped Emulsion Tank No. 1		3														1			ļ
EQT164	1700-54 Stripped Emulsion Tank No. 2		3													_	1_			
EQT165	1700-55 Stripped Emulsion Tank No. 3		3														1			
EQT166	1700-57 Diisobutylene (DIB) Storage Tank		3														3			
EQT167	1700-5A No. 6 Emulsion Storage Tank Manhole	.,.					·	2									3			
EQT168	1700-60 Diisobutylene Nitrosate (DIBN) Storage Tank No. 3		3														3			
EQT169	1700-61 Diisobutylene Nitrosate (DIBN) Storage Tank No. 4		3														3			-

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

Source	Descriptive Name of the Source				LAC	33:111							LA	AC 3	3:LII.C	Chap	ter			
ID No.:	Descriptive Name of the Source	509	2103	2104	2107	2111	2113	2115	2121	5	9	11	13	15	22	29	51	53	56	59
EQT170	1700-62 Diisobutylene Nitrosate (DIBN) Storage Tank No. 5		3							}							3			
EQT171	1700-63.1 No. I CD Solution Tank		3														1			
EQT172	1700-63.10 Inhibitor Final Make-up Tank		3														1			
EQT173	1700-63.11 Inhibitor Hold-up Tank		3									·					1			
EQT175	1700-63.2 No. 2 CD Solution Tank		3														1			
EQT176	1700-63.3 Recovered CD Storage Tank No. 1		3														1	,		
EQT177	1700-63.4 Recovered CD Storage Tank No. 2		3														1		·	
EQT178	1700-63.5 CD Heels Tank		_ 1														1			
EQT181	1700-63.8 Crude CD Storage Tank No. 3		_ 3										·				1			
EQT182	1700-63.9 Refined CD Storage Tank		1														1			
EQT183	1700-64 Water Solution Exhaust Fan							2								·	3			
EQT185	1700-66 Poly Building Wall Fans							2						•			3			
EQT186	1700-67 Stripped Emulsion Tank No. 4		3														1			
EQT187	1700-68 Stripped Emulsion Tank No. 5		3														1			
EQT188	1700-69 Stripped Emulsion Tank No. 9		3														1			
EQT189	1700-70 Stripped Emulsion Tank No. 11		3														1			
EQT190	1700-71 Stripped Emulsion Tank No. 12		3														1			
EQT191	1700-72 Stripped Emulsion Tank No. 15		3														1			
EQT192	1700-73 Stripped Emulsion Tank No. 16		3														1			
EQT193	1700-74 Finishing Stabilizer Makeup Bag Filter												1							

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

Source	Descriptive Name of the Source				LAC	33:П		·		LAC 33:III.Chapter										
ID No.:	:: Descriptive realite of the source	509	2103	2104	2107	2111	2113	2115	2121	5	9	11	13	15	22	29	51	53	56	59
EQT194	1700-75 Resin 90 Railcar		3_														3			
EQT195	1700-76 Rosin S Railcar		3														3			
EQT196	1700-77 Octopol StorageTank		3														3			
EQT198	1700-79 Emergency Stablizer Drumming							2									3			
EQT199	1700-80.1 Refined ACR Storage Tank		3										-				3			
EQT200	1700-80.2 Chlorinated ACR Storage Tank		3														3			
EQT201	1700-82 ACR/Solvent Blend Tank		1														2			
EQT202	3-95 Diversion Tank		3														1			
EQT203	4-95 Surge Tank		3														1			
EQT204	5-95 Aeration Tank		3			1											1			
EQT205	1700-81.1 NMP/PTZ Tote		3														3			
EQT206	1700-81.2 Aqueous Actrene Tote		3														3			
EQT207	1700-81.3 Recovery Column Heels Tote		3							Ì							3			
EQT208	1700-81.4 TBC Tote		3														3			
EQT209	1700-81.5 ACR Refining Column		3														3			
EQT210	1700-81.6 ACR RC Condenser		3			<u> </u>											3			
EQT211	1700-81.7 ACR RC Reboiler		3														3			
EQT212	1700-84A Advance Fibres System (AFS) Emulsion Shipping (Emulsion Blend Tank)		2		-			-	·											
EQT213	1700-84B Advance Fibres System (AFS) Emulsion Shipping (Tote Loading)				2 .															
EQT214	1700-85 Liquid Dispersion Loading Emissions		1 '		2					•							·	-		

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. After the headings of this table as necessary in order to address <u>ALL</u> potentially applicable requirements.

Source	Descriptive Name of the Source				LAC	33:Ш	LAC 33:III.Chapter													
ID No.:	Descriptive Name of the Source	509	2103	2104	2107	2111	2113	2115	2121	5	9	11	13	15	22	29	51	53	56	59
EQT215	1700-86 Rosin S Storage Tank		2																	
FUG004	1-93 Fugitive Emissions - Neoprene Unit			,					1			Ì					1			
RLP013	1700-14B.3 Stabilizer & Catalyst Yanks Manhole Vent		2										1				3			
RLP014	1700-2 Strippers Condenser Vent							1	,				İ				1			
RLP015	1700-3 Poly Kettles Vent Condenser							1									1			
RLP016	1700-56 No. 6, 7, 8, 10, 13 and 14 Unstripped Storage Tanks Depressure Vent				-			2									1			
RLP017	1700-80 ACR Storage Vent Header					ļ					_			<u> </u>			3			
RLP018	1700-81 ACR Refining Vent																3			
RLP019	1700-83 ACR Drumming Vent							2							•		2			
UNF001	Plant Wide					1	1			1	1	1	1				1		1	1
	6-95 Clarifier		3														1			
·	1700-87, 1700-88, 1700-89 No. 10, No. 13 & No. 14 Emulsion Storage Tank Manway							2									3			

KEY TO MATRIX

- 1 (Applicable) The regulations have applicable requirements that apply to this particular emissions source. This includes any monitoring, recordkeeping, or reporting requirements.
- 2 (Exempt) The regulations apply to this general type of emission source (i.e. vents, furnaces, towers, and fugitives) but do not apply to this particular emission source.
- 3 (Does Not Apply) The regulations do not apply to this emissions source. The regulations may have applicable requirements that could apply to this emissions source but the requirements do not currently apply to the source due to meeting a specific criterion, such as it has not been constructed, modified or reconstructed since the regulations have been in place.

Blank - The regulations clearly do not apply to this type of emission source.

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

Source	Descriptive Name of the Course			40 (CFR (60 NS	SPS		4	0 CFR	R 61	40	CFR (63 NES	HAP	40 CFR				
ID No.:	Descriptive Name of the Source	Α	Ka	Kb	Dъ	Dc	GG	ккк	Α	M	FF	Α	Н	FFFF	U	60	64	68	70	
UNF001	Plant Wide	1							1	1	1			1	1		: 1	1		
EQT134	1700-1 No. 7, 8, 10, 13, 14 Emulsion Storage Tanks Manhole and Exhaust Blower	_			-										3					
EQT135	1700-13 Poly Kettles Manholes/Strainers (1 and 2)														3					
EQT136	1700-13A Poly Kettles Manholes/Strainers (3, 4 and 5)														3					
EQT137	1700-14B.1 Acetic Acid Make-up Tank			3_				<u> </u>				<u> </u>			2]	<u></u>	<u> </u>		
EQT138	1700-14B.2 Acetic Acid Hold-up Tank	_		3											2					
EQT139	1700-20 CD Refining Column Jet	١)	<u> </u>								1	-				
EQT140	1700-20A CD Refining Column Jet (Spare)										-				1					
EQT141	1700-21A 2MM Pound CD Storage Tank			3							["				1					
EQT142	1700-25 East Wash Belt Dryer														2					
EQT143	1700-26 West Wash Belt Dryer									_					2					
EQT144	1700-27 East Hot Dryer Exhaust									_					2					
EQT145	1700-28 West Hot Dryer Exhaust														2					
EQT146	1700-45 No. 1 East Dryer Cooling Compt.														2					
EQT147	1700-46 No. 1 West Dryer Cooling Compt.														2					
EQT148	1700-47 No. 2 East Dryer Cooling Compt.									-					2					
EQT149	1700-48 No. 2 West Dryer Cooling Compt.														2					
EQT150	1700-5.3 Unstripped Emulsion Storage Tank. No. 6			2									2		1	-				

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address <u>ALL</u> potentially applicable requirements.

Source	Descriptive Name of the Source			40 0	CFR (50 NS	SPS		. 4	0 CFR	61	40	CFR (53 NES	HAP	40 CFR				
ID No.:	:	Α	Ka	Kb	Dь	Dc	GG	ккк	Α	М	FF	Α	Н	FFFF	U	60	64	68	70	
EQT151	1700-5.4 Unstripped Emulsion Storage Tank. No. 7			2							ļ		2		1					
EQT152	1700-5.5 Unstripped Emulsion Storage Tank. No. 8			2						_			2		1					
EQT153	1700-5.6 Unstripped Emulsion Storage Tank. No. 10] 									2		1					
EQT154	1700-5.7 Unstripped Emulsion Storage Tank. No. 13												2		1					
EQT155	1700-5.8 Unstripped Emulsion Storage Tank. No. 14					ļ							2		1 ·					
EQT156	1700-50.1 Stabilizer Tank No. 1			3									2		1					
EQT157	1700-50.1 Stabilizer Tank No. 2			3						_			2		1					
EQT158	1700-50.3 Stabilizer Tank No. 3			3									2		1			l		
EQT159	1700-50.4 Stabilizer Tank No. 4			3									2		1					
EQT160	1700-50.5 Stabilizer Tank No. 5			3									2		1					
EQT161	1700-50.6 Stabilizer Tank – LD750			3									· 2		1					
EQT162	1700-51 Inhibitor Mix Tank			3									2		1					
EQT163	1700-53 Stripped Emulsion Tank No. 1			3											2					
EQT164	1700-54 Stripped Emulsion Tank No. 2			3											· 2					
EQT165	1700-55 Stripped Emulsion Tank No. 3			3											2					
EQT166	1700-57 Diisobutylene (DIB) Storage Tank			3											2					
EQT167	1700-5A No. 6 Emulsion Storage Tank Manhole														3					
EQT168	1700-60 Diisobutylene Nitrosate (DIBN) Storage Tank No. 3			3			<u> </u>								3					

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. After the headings of this table as necessary in order to address <u>ALL</u> potentially applicable requirements.

Source	Descriptive Name of the Source			40 C	CFR (60 NS	SPS		4	0 CFF	R 61	40	CFR (63 NES	HAP	40 CFR			
ID No.:	Descriptive Name of the Source	A	Ka	Kb	Db	Dc	GG	KKK	Α	M	FF	Α	Н	FFFF	U	60	64	68	70
EQT169	1700-61 Diisobutylene Nitrosate (DIBN) Storage Tank No. 4			3											3				
EQT170	1700-62 Diisobutylene Nitrosate (DIBN) Storage Tank No. 5			3											3				
EQT171	1700-63.1 No. 1 CD Solution Tank			3									2		1				
EQT172	1700-63.10 Inhibitor Final Make-up Tank			3									2		1				
EQT173	1700-63.11 Inhibitor Hold-up Tank			3									2		1				
EQT175	1700-63.2 No. 2 CD Solution Tank			3									2		1				
ЕСТ176	1700-63.3 Recovered CD Storage Tank No. 1			3									2		1				
EQT177	1700-63.4 Recovered CD Storage Tank No. 2			3									2		1				
EQT178	1700-63.5 CD Heels Tank			2			 			<u></u> .	<u> </u>		2		1	ļ			
EQT181	1700-63.8 Crude CD Storage Tank No. 3			3						<u></u>	<u> </u>	<u> </u>	<u> </u>		1	<u> </u>	<u>]</u>		
EQT182	1700-63.9 Refined CD Storage Tank			3											1		<u> </u>		<u> </u>
EQT183	1700-64 Water Solution Exhaust Fan														3				
EQT185	1700-66 Poly Building Wall Fans					l									3_				
EQT186	1700-67 Stripped Emulsion Tank No. 4			3											2_				
EQT187	1700-68 Stripped Emulsion Tank No. 5			3											2				
EQT188	1700-69 Stripped Emulsion Tank No. 9			3											2				
EQT189	1700-70 Stripped Emulsion Tank No. 11			3											2				
EQT190	1700-71 Stripped Emulsion Tank No. 12		<u> </u>	3											2				
EQT191	1700-72 Stripped Emulsion Tank No. 15			3							·				2				

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address ALL potentially applicable requirements.

Source	Description Name of the Course			40 (CFR (60 NS	SPS		4	0 CFF	R 61	40 (CFR (63 NES	HAP		40 Cl	FR	
ID No.:	Descriptive Name of the Source	Α	Ka	Kb	Db	Dc	GG	ккк	Α	М	FF	Α	H	FFFF	U	60	64	68	70
EQT192	1700-73 Stripped Emulsion Tank No. 16			3											2		-		
EQT193	1700-74 Finishing Stabilizer Makeup Bag Filter																		
EQT194	1700-75 Resin 90 Railcar			2											2.				
EQT195	1700-76 Rosin S Railcar			2											2				
EQT196	1700-77 Octopol StorageTank			2											2				
EQT198	1700-79 Emergency Stablizer Drumming														3				
EQT199	1700-80.1 Refined ACR Storage Tank			3										3	3				
EQT200	1700-80.2 Chlorinated ACR Storage Tank			3										3	3				
EQT201	1700-82 ACR/Solvent Blend Tank			3										3					
EQT202	3-95 Diversion Tank			3]		1				
EQT203	4-95 Surge Tank			3											1				
EQT204	· 5-95 Aeration Tank			3											1	l:			
EQT205	. 1700-81.1 NMP/PTZ Tote			3										3				ļ <u>-</u>	
EQT206	1700-81.2 Aqueous Actrene Tote			3										3					
EQT207	1700-81.3 Recovery Column Heels Tote			3			ļ							3		·			
EQT208	1700-81.4 TBC Tote			3										3					
EQT209	1700-81.5 ACR Refining Column								1					3	3		,		
EQT210	1700-81.6 ACR RC Condenser													3	3				
EQT211	1700-81.7 ACR RC Reboiler				1						1		<u> </u>	3	3				
EQT212	1700-84A Advance Fibers System (AFS) Emulsion Shipping (Emulsion Blend Tank)			3										2	3		_		

TABLE 1: APPLICABLE LOUISIANA AND FEDERAL AIR QUALITY REQUIREMENTS

Note: This table lists regulations that are commonly applicable to many sources, but is not intended to be an all inclusive list. Alter the headings of this table as necessary in order to address <u>ALL</u> potentially applicable requirements.

Source	Descriptive Name of the Source		•	40 C	FR (50 NS	PS		4	0 CFR	61	40	CFR (53 NES	HAP		40 C	FR	
ID No.:	Descriptive Name of the Source	Α	Ka	Kb	Db	Dc	GG	KKK	Α	М	FF	Α	Н	FFFF	U	60	64	68	70
EQT213	1700-84B Advance Fibers System (AFS) Emulsion Shipping (Tote Loading)	_												2	3				
EQT214	1700-85 Liquid Dispersion Loading Emissions													2	3				
EQT215	1700-86 Rosin S Storage Tank		3	<u> </u>										2	3	<u> </u>			
FUG004	1-93 Fugitive Emissions - Neoprene Unit			}		_		_							1_				
RLP013	1700-14B.3 Stabilizer & Catalyst Yanks Manhole Vent														3				
RLP014	1700-2 Strippers Condenser Vent														1				
RLP015	1700-3 Poly Kettles Vent Condenser													<u> </u>	1				
RLP016	1700-56 No. 6, 7, 8, 10, 13 and 14 Unstripped Storage Tanks Depressure Vent							_							1				
RLP017	1700-80 ACR Storage Vent Header													3	3				
RLP018	1700-81 ACR Refining Vent					-							-	3	3				
RLP019	1700-83 ACR Drumming Vent						-							2	3				
	6-95 Clarifier			3											1				
	1700-87, 1700-88, 1700-89 No. 10, No. 13 & No. 14 Emulsion Storage Tank Manway														3				

KEY TO MATRIX

- 1 (Applicable) The regulations have applicable requirements that apply to this particular emissions source. This includes any monitoring, recordkeeping, or reporting requirements.
- 2 (Exempt) The regulations apply to this general type of emission source (i.e. vents, furnaces, towers, and fugitives) but do not apply to this particular emission source.
- 3 (Does Not Apply) The regulations do not apply to this emissions source. The regulations may have applicable requirements that could apply to this emissions source but the requirements do not currently apply to the source due to meeting a specific criterion, such as it has not been constructed, modified or reconstructed since the regulations have been in place.

Blank - The regulations clearly do not apply to this type of emission source.

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement	
		Requirements that limit emissions or operations -				
		N/A	N/A	N/A		
	Subpart U: National	Requirements that specify monitoring -	-			
1700-21A	Emission Standards for	N/A	N/A	N/A		
2 MM Pound CD Storage Tank EQT 0141	Emissions: Group 1	Hazardous Air Pollutant Emissions: Group 1 Polymers and Resins	Requirements that specify records to be kept and requirements that specify record retention time -			
	1 Glymons and Account	Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR 63.484(a)]. This Tank is Group 2.	40 CFR 63.484(a)	N/A		
		Requirements that specify reports to be submitted -			-	
		N/A	N/A	N/A		
		Requirements that specify performance testing -				
		N/A	N/A	N/A		
		Requirements that limit emissions or operations -				
1700-21A 2 MM Pound CD Storage Tank	Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program:	Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U as applicable determined as MACT.	LAC 33:III.5109.A	N/A		
EQT 0141	Emission Control and Reduction	Requirements that specify monitoring -				
	Requirements and	N/A	N/A	N/A		
	Standards	Requirements that specify records to be kept and requirements that specify record retention time -				
		N/A	N/A	N/A	1	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement						
		Requirements that specify reports to be submitted -									
1700-21A	Title 33 Chapter 51:	N/A	N/A	N/A							
2 MM Pound CD Storage Tank	(Continued)	Requirements that specify performance testing -									
EQT 0141	N/A N/A		N/A	N/A							
<u> </u>		Requirements that limit emissions or operations -	<u> </u>								
1700-25: East Wash Belt Dryer 1700-26: West Wash Belt Dryer 1700-27: East Hot Dryer Exhaust	C th	Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U as applicable determined as MACT.	LAC 33:III.5109.A	N/A							
1700-28: West Hot Dryer Exhaust	Title 33 Chapter 51:	Requirements that specify monitoring -		 -							
1700-45: No. 1 East Dryer	Comprehensive Toxic Air Pollutant Emission	Air Pollutant Emission	Air Pollutant Emission	Air Pollutant Emission	Air Pollutant Emission	Air Pollutant Emission		N/A	N/A	N/A	
Cooling Compartment 1700-46: No: 1 West Dryer	Emission Control and Reduction	Requirements that specify records to be kept and requirements that specify record retention time -									
Cooling Compartment	Requirements and	N/A	N/A	N/A							
1700-47: No. 2 East Dryer Cooling Compartment	Standards	Standards	Requirements that specify reports to be submitted -								
1700-48: No. 2 West Dryer		N/A	N/A	N/A	1.						
Cooling Compartment EQT 0142-0149		Requirements that specify performance testing -									
		N/A	N/A	N/A							

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
1700-5.3: Unstripped Emulsion Storage Tank No. 6		Equip with a submerged fill pipe.	LAC 33:III.2103.A	N/A	
1700-5.4: Unstripped Emulsion Storage Tank No. 7		Determine VOC maximum true vapor pressure using the methods in LAC 33:III.2103.H.3.a-e.	LAC 33:III.2103.H.3	N/A	
1700-5.5: Unstripped Emulsion		Requirements that specify monitoring -			
Storage Tank No. 8		N/A	N/A	N/A	
1700-5.6: Unstripped Emulsion Storage Tank No. 10	Title 33 Chapter 21: Control of Emission of	Requirements that specify records to be kept and requirements that specify record retention time -			
1700-5.7: Unstripped Emulsion Storage Tank No. 13	Organic Compounds	N/A	N/A	N/A	
1700-5.8: Unstripped Emulsion		Requirements that specify reports to be submitted -			
Storage Tank No. 14		N/A	N/A	N/A	
EQT 0150 - 0155		Requirements that specify performance testing -			
<u> </u>	,	N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
1700-5.3: Unstripped Emulsion Storage Tank No. 6 1700-5.4: Unstripped Emulsion Storage Tank No. 7	Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission	Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT.	LAC 33:III.5109.A	N/A	
1700-5.5: Unstripped Emulsion	Control Program: Emission Control and	Requirements that specify monitoring -			
Storage Tank No. 8 1700-5.6: Unstripped Emulsion	Reduction Requirements and	N/A	N/A	N/A	
Storage Tank No. 10 1700-5.7: Unstripped Emulsion	Standards	Requirements that specify records to be kept and requirements that specify record retention time -			
Storage Tank No. 13		N/A	N/A	N/A	
1700-5.8: Unstripped Emulsion Storage Tank No. 14		Requirements that specify reports to be submitted -			
1700-5.3 to 1700-5.8 EQT 0150 - 0155		N/A	N/A	N/A	
1561 0120 - 0133		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -		T	
1700-5.3: Unstripped Emulsion Storage Tank No. 6		Comply with the requirements of 40 CFR 63 Subpart H, except as specified in 40 CFR 63.502(b) through (m). Subpart U.	40 CFR 63.502(a)	N/A	
1700-5.4: Unstripped Emulsion Storage Tank No. 7	Subpart U: National	Requirements that specify monitoring -			-
1700-5.5: Unstripped Emulsion Storage Tank No. 8	Emission Standards for Hazardous Air Pollutant	N/A	N/A	N/A	
1700-5.6: Unstripped Emulsion Storage Tank No. 10	Emissions: Group I Polymers and Resins	Requirements that specify records to be kept and requirements that specify record retention time -			
1700-5.7: Unstripped Emulsion Storage Tank No. 13		N/A	N/A	N/A	
1700-5.8: Unstripped Emulsion]	Requirements that specify reports to be submitted -			
Storage Tank No. 14 1700-5.3 to 1700-5.8		N/A	N/A	N/A	
EQT 0150 - 0155		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		N/A	N/A	N/A	
		Requirements that specify monitoring -			
1700-50.1: Stabilizer Tank No. 1		N/A	N/A	N/A	
1700-50.2: Stabilizer Tank No. 2 1700-50.3: Stabilizer Tank No. 3	Subpart U: National	Requirements that specify records to be kept and requirements that specify record retention time -			
1700-50.4: Stabilizer Tank No. 4 1700-50.5: Stabilizer Tank No. 5 1700-50.6: Stabilizer Tank No. 6	Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins	Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR 63.484(a)] These tanks are Group 2.	40 CFR 63.484(a)	N/A	
EQT 0156 - 0161		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -		1	
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		N/A	N/A	N/A	
		Requirements that specify monitoring -			
		N/A	N/A	N/A	
1700-51 Inhibitor Mix Tank EQT 0162	Subpart U: National	Requirements that specify records to be kept and requirements that specify record retention time -			
	Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins	Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR 63.484(a)] This tank is Group 2.	40 CFR 63.484(a)	N/A	
		Requirements that specify reports to be submitted -			
		N/A N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
1700-51: Inhibitor Mix Tank EQT 0162	Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and	Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT	LAC 33:III.5109.A	N/A	
EQ1 0102	Reduction	Requirements that specify monitoring -			
	Requirements and Standards	N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement	
1700-51: Inhibitor Mix Tank		Requirements that specify reports to be submitted -				
EQT 0162	Title 33 Chapter 51 (Continued)	- 13//% 137/A	N/A	N/A		
	}	Requirements that specify performance testing -				
		N/A	N/A	N/A		
1700-53: Stripped Emulsion Tank No. 1		Requirements that limit emissions or operations -				
1700-54: Stripped Emulsion Tank No. 2		Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. No	LAC 33:III.5109.A	N/A		
1700-55: Stripped Emulsion Tank No. 3		additional controls determined as MACT.				
1700-67: Stripped Emulsion				Requirements that specify monitoring -		
Tank No. 4	Title 33 Chapter 51:	N/A	N/A	N/A		
1700-68: Stripped Emulsion Tank No. 5	Comprehensive Toxic	Requirements that specify records to be kept and				
1700-69: Stripped Emulsion	Air Pollutant Emission Control Program:	requirements that specify records to be kept and requirements that specify record retention time -				
Tank No. 9	Emission Control and Reduction	N/A	N/A	N/A		
1700-70: Stripped Emulsion Tank No. 11	Requirements and	D				
·	Standards	Requirements that specify reports to be submitted -	İ	ł	}	
1700-71: Stripped Emulsion Tank No. 12	}	N/A	N/A	N/A		
1700-72: Stripped Emulsion			17/23	IVA		
Tank No. 15	1	Requirements that specify performance testing -				
1700-73: Stripped Emulsion Tank No. 16		N/A		<u> </u>	<u> </u>	
EQT 0163 to 0165;0186 to 0192		N/A	N/A	N/A		

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
1700-63.1: No. 1 CD Solution Tank		N/A	N/A	N/A	
1700-63.2: No. 2 CD Solution Tank		Requirements that specify monitoring -			
1700-63.3: Recovered CD		N/A	N/A	N/A]
Storage Tank No. 1		Requirements that specify records to be kept and			
1700-63.4: Recovered CD	Subpart U: National Emission Standards for	requirements that specify record retention time -		ļ —— <u>——</u>	
Storage Tank No. 2 1700-63.8 Crude CD Storage Tank No. 3	Hazardous Air Pollutant Emissions: Group I Polymers and Resins	Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR	40 CFR 63.484(a)	N/A	
1700-63.10: Inhibitor Final Make-Up Tank		63.484(a)] These tanks are Group 2. Requirements that specify reports to be submitted -		 -	
1700-63.11: Inhibitor Hold-up Tank		N/A	N/A	N/A	
EQT 0171 to 0173, 0175 to		Requirements that specify performance testing -			
0177 and 0181		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
1700-63.1: No. 1 CD Solution Tank 1700-63.2: No. 2 CD Solution Tank	Title 22 Chantag 51.	Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT.	LAC 33:III.5109.A	N/A	
1700-63.3: Recovered CD Storage Tank No. 1	Title 33 Chapter 51:	Requirements that specify monitoring -			
1700-63.4: Recovered CD Storage Tank No. 2	Comprehensive Toxic Air Pollutant Emission Control Program:	N/A	N/A	N/A	
1700-63.8 Crude CD Storage Tank No. 3	Emission Control and Reduction	Requirements that specify records to be kept and requirements that specify record retention time -			
1700-63.10: Inhibitor Final	Requirements and Standards	N/A	N/A	N/A	
Make-Up Tank	Standards	Requirements that specify reports to be submitted -			
1700-63.11: Inhibitor Hold-up Tank		N/A	N/A	N/A	
EQT 0171 to 0173, 0175 to 0177 and 0181		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			_
1700-63.5 CD Heels Tank	Title 33 Chapter 21:	Equip with a submerged fill pipe.	LAC 33:III.2103.A	N/A	
1700-63.9 Refined CD Storage Tank	Control of Emission of Organic Compounds	Determine VOC maximum true vapor pressure using the methods in LAC 33:III.2103.H.3.a-e.	LAC 33:ПП.2103.Н.3	N/A	
EQT 0178 and 0182	·	Requirements that specify monitoring -			
		N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
1700-63.5 CD Heels Tank 1700-63.9 Refined CD Storage Tank	Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission	Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT.	LAC 33:111.5109.A	N/A	
EQT 0178 and 0182	Control Program: Emission Control and	Requirements that specify monitoring -			
	Reduction Requirements and	N/A	N/A	N/A	
	Standards	Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that specify reports to be submitted -		T	
1700-63.5 CD Heels Tank	Title 33 Chapter 51: (Continued)	N/A	N/A	N/A	
1700-63.9 Refined CD Storage Tank	(**************************************	Requirements that specify performance testing -			
EQT 0178 and 0182		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
		N/A	N/A	N/A	
		Requirements that specify monitoring -			
		N/A	N/A	N/A	
1700-63.5 CD Heels Tank	Subpart U: National	Requirements that specify records to be kept and requirements that specify record retention time -			
1700-63.9 Refined CD Storage Tank EQT 0178 and 0182	Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins	Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR 63.484(a)] This tank is Group 2.	40 CFR 63.484(a)	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
Tiple 22 Ch		Prevent particulate matter from becoming airborne by taking all reasonable precautions. These precautions shall include, but not be limited to, those specified in LAC 33:III.1305.A.1-7.	LAC 33:III.1305	N/A	
	Title 33 Chapter 13:	Opacity ≤ 20 percent; except emissions may have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive minutes.	LAC 33.III.1311.C	N/A	
1700-74: Finishing Stabilizer	Emission Standards for	Requirements that specify monitoring -			
Makeup Bag Filter	Particulate Matter (Including Standards for	N/A	N/A	N/A	
EQT 0193	Some Specific Facilities)	Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
	:	Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with LAC 33:III.2103 determined as MACT.	LAC 33:III.5109.A	N/A	
	Title 33 Chapter 51: Comprehensive Toxic	Requirements that specify monitoring -			
1700-82: ACR/Solvent Blend	Air Pollutant Emission	N/A	N/A	N/A	
Tank EQT 0201	Control Program: Emission Control and Reduction	Requirements that specify records to be kept and requirements that specify record retention time -			
	Requirements and Standards	N/A	N/A	N/A	
		Requirements that specify reports to be submitted -	1		
		N/A	N/A	N/A	<u></u>
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
		Equip with a submerged fill pipe.	LAC 33:III.2103.A	N/A	
1700-82: ACR/Solvent Blend	Tr. 1 22 Cl	Determine VOC maximum true vapor pressure using the methods in LAC 33:III.2103.H.3.a-e.	LAC 33:Ш.2103.Н.3	N/A	
Tank	Title 33 Chapter 21: Control of Emission of	Requirements that specify monitoring -			
EQT 0201	Organic Compounds	N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
1700-82: ACR/Solvent Blend	Title 33 Chapter 21:	Requirements that specify reports to be submitted -			
Tank	Control of Emission of Organic Compounds	N/A	N/A	N/A	
EQT 0201	Organic Compounds	Requirements that specify performance testing -		_	
,		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
3-95 Diversion Tank	Subpart G - National Emission Standards For	N/A	N/A	N/A	
4-95 Surge Tank 5-95 Aeration Tank	Organic Hazardous Air Pollutants From The	Requirements that specify monitoring -			
6-95 Clarifier	Synthetic Organic	N/A	N/A	N/A	
EQT 0202 to 0204	Chemical Manufacturing Industry	Requirements that specify records to be kept and requirements that specify record retention time -			
Storage Vessels,	Transfer Operations,	Equipment/operational data recordkeeping by electronic or hard copy at the regulation's specified frequency. Maintain records specified in 40 CFR 63.147(a) through (f), as applicable. Subpart G.	40 CFR 63.147	N/A	
	And Wastewater	Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			<u> </u>
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
3-95 Diversion Tank 4-95 Surge Tank	Subpart U: National Emission Standards for	Comply with the requirements of 40 CFR 63.132 through 63.148, except as specified in 40 CFR 63.501(a)(1) through (a)(23) and (c). Subpar U [40 CFR 63.501(a)]	40 CFR 63.501(a)	N/A	
5-95 Aeration Tank	Hazardous Air Pollutant Emissions: Group I	Requirements that specify monitoring -		T	
EQT 0202 to 0204	Polymers and Resins	N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
3-95 Diversion Tank 4-95 Surge Tank 5-95 Aeration Tank	Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission	Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT.	LAC 33:111.5109.A	N/A	
EQT 0202 to 0204	Control Program: Emission Control and	Requirements that specify monitoring -			
	Reduction Requirements and	N/A	N/A	N/A	
	Standards	Requirements that specify records to be kept and ' requirements that specify record retention time -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
3-95 Diversion Tank	Title 33 Chapter 51:	Requirements that specify reports to be submitted -			
4-95 Surge Tank	(Continued)	N/A	N/A	N/A	-
5-95 Aeration Tank		Requirements that specify performance testing -			_
EQT 0202 to 0204		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
		Determine VOC maximum true vapor pressure using the methods in LAC 33:III.2103.H.3.a-e.	LAC 33:III.2103.H.3	N/A	
,	Title 33 Chapter 21: Control of Emission of Organic Compounds	Requirements that specify monitoring -			
		N/A	N/A	N/A	
1700-84A: Advance Fibers System (AFS) – Emulsion Shipping (Blend Tank)		Requirements that specify records to be kept and requirements that specify record retention time -			
EQT 0212		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
	Title 33 Chapter 51:	Requirements that limit emissions or operations -			
1700-84A: Advance Fibers System (AFS) – Emulsion Shipping (Blend Tank) EQT 0212	Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards	Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with LAC 33:III.2103 determined as MACT.	LAC 33:III.5109.A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
1700-84A: Advance Fibers	Title 33 Chapter 51:	Requirements that specify monitoring -			
System (AFS) – Emulsion Shipping (Blend Tank)	(Continued)	N/A	N/A	N/A	
EQT 0212		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
		N/A	N/A	N/A	
		Requirements that specify monitoring -			
1700-84B: Advance Fibers	Subpart FFFF - National Emission	N/A	N/A	N/A	
System (AFS) – Emulsion Shipping (Tote Loading)	Standards For Hazardous Air	Requirements that specify records to be kept and requirements that specify record retention time -			
1700-85 Liquid Dispersion Loading EQT 0213 and 0214	Pollutants: Miscellaneous Organic Chemical Manufacturing	Equipment/operational data recordkeeping by electronic or hard copy annually. Keep records of the information specified in 40 CFR 63.130(f)(1) through (f)(3) (as per Subpart FFFF). Subpart G [40 CFR 63.130(f)]	40 CFR 63.130(f)	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
1700-84B and 1700-85	Subpart FFFF	Requirements that specify performance testing -			
EQT 0213 and 0214	(Continued)	N/A	N/A	N/A	
		Requirements that limit emissions or operations -			-
		Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with 40 CFR 63 Subpart FFFF determined as MACT.	LAC 33:III.5109.A	N/A	
1700-84B: Advance Fibers	Title 33 Chapter 51: Comprehensive Toxic	Requirements that specify monitoring -			
System (AFS) – Emulsion Shipping (Tote Loading)	Air Pollutant Emission	N/A	N/A	N/A	
1700-85 Liquid Dispersion Loading	Control Program: Emission Control and Reduction	Requirements that specify records to be kept and requirements that specify record retention time -			
EQT 0213 and 0214	Requirements and	N/A	N/A	N/A	
	Standards	Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
1-93: Fugitive Emissions –	Subpart U: National Emission Standards for	Comply with the requirements of 40 CFR 63 Subpart H, except as specified in 40 CFR 63.502(b) through (m). Subpart U.	40 CFR 63.502(a)	N/A	
Neoprene Unit FUG 0004	Hazardous Air Pollutant Emissions: Group I	N/A	N/A	N/A	
FUG 0004	Polymers and Resins	Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
		Repair according to LAC 33:III.2121.B.3 any regulated component observed leaking by sight, sound, or smell, regardless of the leak's concentration.	LAC 33:ΠΠ.2121.B.1		
1-93: Fugitive Emissions – Neoprene Unit FUG 0004	Title 33 Chapter 21: Control of Emission of Organic Compounds	Do not locate any valve, except safety pressure relief valves, valves on sample lines, valves on drain lines and valves that can be removed and replaced without a shutdown, at the end of a pipe or line containing VOC unless the end of such line is sealed with a second valve, a blind flange, a plug, or a cap. Remove such sealing devices only when the line is in use, for example, when a sample is being taken. When the line has been used and is subsequently resealed, close the upstream valve first, followed by the sealing device.	LAC 33:III.2121.B.2	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Make every reasonable effort to repair a leaking component, as described in LAC 33:III.2121.B, within 15 days, except as provided.	LAC 33:III.2121.B.3	N/A	
	}	Requirements that specify monitoring -			
		N/A	N/A	N/A	
1-93: Fugitive Emissions -	Title 33 Chapter 21:	Requirements that specify records to be kept and requirements that specify record retention time -			
Neoprene Unit	Control of Emission of	N/A	N/A	N/A	
FUG 0004	Organic Compounds	Requirements that specify reports to be submitted -			
(Continued)		Submit report: Due semiannually, by the 31st of January and July, to the Office of Environmental Assessment, Air Quality Assessment Division. Include the information specified in LAC 33:III.2121.F.1 through 4 for each calendar quarter during the reporting period.	LAC 33:Ш.2121.F	Semiannually	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		VOC, Total <= 0.72 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period.	LAC 33:III.501.C.6	N/A	State Only
		Requirements that specify monitoring -			
	Title 33 Chapter 51:	VOC, Total monitored by technically sound method as needed, (when source is venting).	LAC 33:III.501.C.6	N/A	State Only
1700-14B - Solution Make Up Manhole Common Vent	Comprehensive Toxic Air Pollutant Emission Control Program:	Requirements that specify records to be kept and requirements that specify record retention time -			
GRP 0006	Emission Control and Reduction Requirements and Standards	VOC. Total recordkeeping by electronic or hard copy monthly. Keep records of the total VOC emissions each month, as well as the total VOC emissions for the last twelve months. Make records available for inspection by DEQ personnel.	LAC 33:III.501.C.6	N/A	State Only
		Requirements that specify reports to be submitted -			
		Submit report: Due annually, by the 31st of March. Report the total VOC emissions for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division.	LAC 33:Ш.501.С.6	Annually	State Only
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			1
		VOC, Total <= 69.17 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period. The VOC emissions shall be calculated based on operation and throughput.	LAC 33:III.501.C.6	N/A	State Only
		Requirements that specify monitoring -			
	Title 33 Chapter 51: Comprehensive Toxic	VOC, Total monitored by technically sound method daily.	LAC 33:III.501.C.6	N/A	State Only
1700-25A – Product Drying CAP GRP 0007	Air Pollutant Emission Control Program:	Requirements that specify records to be kept and requirements that specify record retention time -			
	Emission Control and Reduction Requirements and Standards	VOC, Total recordkeeping by electronic or hard copy monthly. Keep records of the total VOC emissions each month, as well as the total VOC emissions for the last twelve months, (VOC emissions calculated based on operation and throughput). Make records available for inspection by DEQ personnel.	LAC 33:III.501.C.6	N/A	State Only
		Requirements that specify reports to be submitted -			
	Re ca	Submit report: Due annually, by the 31st of March. Report the total VOC emissions for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division.	LAC 33:III.501.C.6	Annually	State Only
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		VOC, Total <= 2.77 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period. VOC emissions shall be calculated based on operation and throughput.	LAC 33:III.501.C.6	N/A	State Only
		Requirements that specify monitoring -			
1700- 5 Unstripped Emulsion	Title 33 Chapter 51: Comprehensive Toxic	VOC, Total monitored by technically sound method daily.	LAC 33:III.501.C.6	N/A	State Only
Storage Yanks Common Vent & CAP	Air Pollutant Emission Control Program:	Requirements that specify records to be kept and requirements that specify record retention time -			
GRP 0008	Emission Control and Reduction Requirements and Standards	VOC, Total recordkeeping by electronic or hard copy monthly. Keep records of the total VOC emissions each month, as well as the total VOC emissions for the last twelve months, (VOC emissions calculated based on operation and throughput). Make records available for inspection by DEQ personnel.	LAC 33:III.501.C.6	N/A	State Only
		Requirements that specify reports to be submitted -			
		Submit report: Due annually, by the 31st of March. Report the total VOC emissions for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division.	LAC 33:III.501.C.6	LAC 33:III.501.C.6 Annually	State Only
		Requirements that specify performance testing -			Ţ · · - ·
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		VOC, Total <= 0.59 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period. VOC emissions shall be calculated based on operation and throughput.	LAC 33:ПІ.501.С.6	N/A	State Only
		Requirements that specify monitoring -	-1.		
	Title 33 Chapter 51: Comprehensive Toxic	VOC, Total monitored by technically sound method daily.	LAC 33:III.501.C.6	N/A	State Only
1700- 50 Stabilizer tanks Common Vent & CAP	Air Pollutant Emission Control Program:	Requirements that specify records to be kept and requirements that specify record retention time -			
GRP 0009 Emission Control and Reduction Requirements and Standards	Reduction Requirements and	VOC, Total recordkeeping by electronic or hard copy monthly. Keep records of the total VOC emissions each month, as well as the total VOC emissions for the last twelve months, (VOC emissions based on operation and throughput). Make records available for inspection by DEQ personnel.	LAC 33:III.501.C.6	N/A	State Only
		Requirements that specify reports to be submitted -			
		Submit report: Due annually, by the 31st of March. Report the total VOC emissions for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division.	LAC 33:III.501.C.6	Annually	State Only
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		VOC, Total <= 2.18 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period. VOC emissions shall be calculated based on operation and throughput.	LAC 33:III.501.C.6	N/A	State Only
		Requirements that specify monitoring -			
	Title 33 Chapter 51: Comprehensive Toxic	VOC, Total monitored by technically sound method daily.	LAC 33:III.501.C.6	N/A	State Only
1700- 63 Vent Header System CAP	Air Pollutant Emission Control Program:	Requirements that specify records to be kept and requirements that specify record retention time -			
GRP 0010	Emission Control and Reduction Requirements and Standards	VOC, Total recordkeeping by electronic or hard copy monthly. Keep records of the total VOC emissions each month, as well as the total VOC emissions for the last twelve months, (VOC emissions based on operation and throughput). Make records available for inspection by DEQ personnel.	LAC 33:III.501.C.6	N/A	State Only
		Requirements that specify reports to be submitted -			
		Submit report: Due annually, by the 31st of March. Report the total VOC emissions for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division.	LAC 33:III.501.C.6	Annually	State Only
		Requirements that specify performance testing -			
	<u> </u>	N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		Neoprene Types: Production rate <= 98 MM lbs/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if total Neoprene Types produced exceeds the maximum listed in this specific condition for any twelve consecutive month period.	LAC 33:III.501.C.6	N/A	State Only
		Requirements that specify monitoring -			
	Title 33 Chapter 51:	Neoprene Types: Production rate monitored by technically sound method daily.	LAC 33:III.501.C.6	N/A	State Only
Facility Wide CAP - Neoprene Types Production CAP	Comprehensive Toxic Air Pollutant Emission Control Program:	Requirements that specify records to be kept and requirements that specify record retention time -			
GRP 0011 E	Emission Control and Reduction Requirements and Standards	Neoprene Types: Production rate recordkeeping by electronic or hard copy monthly. Keep records of the total Neoprene Products production each month, as well as the total Neoprene Products production for the last twelve months. Make records available for inspection by DEQ personnel.	LAC 33:Ш.501.С.6	N/A	State Only
		Requirements that specify reports to be submitted -			
		Submit report: Due annually, by the 31st of March. Report the Total Neoprene Types produced for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division.	LAC 33:III.501.C.6	Annually	State Only
		Requirements that specify performance testing -			
	N/A	N/A	N/A		

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations - Comply with the requirements of 40 CFR 63.113 through 63. 118, except as provided in 40 CFR 63.485(b) through (v). Subpart U. [40 CFR 63.485(a)]	40 CFR 63.485(a)	N/A	
1700-20: CD Refining Column Jets Emissions CAP GRP 0012	Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I	Requirements that specify monitoring - N/A Requirements that specify records to be kept and requirements that specify record retention time -	N/A	N/A	
	Polymers and Resins	N/A Requirements that specify reports to be submitted -	N/A	N/A	
	·	Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent to become a Group 1 continuous front-end process vent, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the Group 1 provisions in 40 CFR 63.113 through 63.118 in accordance with 40 CFR 63.480(i)(2)(ii) or (i)(2)(iii), as applicable. Subpart U. [40 CFR 63.485(l)(1)]	40 CFR 63.485(I)(1)	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that specify reports to be submitted	· · · · · · · · · · · · · · · · · · ·		
1700-20: CD Refining Column Jets Emissions CAP (Continued) GRP 0012	Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins	Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with a TRE greater than 4.0 to become a Group 2 continuous front-end process vent with a TRE less than 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(1)(2)]	40 CFR 63.485(1)(2)	N/A	
	·	Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with a flow rate less than 0.005 standard cubic meter per minute (scmm) to become a Group 2 continuous front-end process vent with a flow rate of 0.005 scmm or greater and a TRE index value less than or equal to 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(l)(3)]	40 CFR 63.485(1)(3)	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that specify reports to be submitted			
1700-20: CD Refining Column Jets Emissions CAP (Continued) GRP 0012	Jets Emissions CAP (Continued) Emission Standards for Hazardous Air Pollutant	Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with an organic HAP concentration less than 50 parts per million by volume (ppmv) to become a Group 2 continuous frontend process vent with an organic HAP concentration of 50 ppmv or greater and a TRE index value less than or equal to 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(l)(4)]	40 CFR 63.485(1)(4)	N/A	
		Requirements that specify performance testing -			i _
		Conduct performance testing in accordance with 40 CFR 63.7(a)(1), (a)(3), (d), (e)(1), (e)(2), (e)(4), (g), and (h), with the exceptions specified in 40 CFR 63.504(a)(1) through (a)(5) and the additions specified in 40 CFR 63.504(b). Subpart U. [40 CFR 63.504(a)]	40 CFR 63.504(a)	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
1700-20: CD Refining Column Jets Emissions CAP (Continued) GRP 0012	Title 33 Chapter 21: Control of Emission of Organic Compounds: Waste Gas Disposal	Halogenated hydrocarbons, total >= 95 % removal efficiency as determined in accordance with LAC 33:III.2115.J.1, by combustion or other methods specified in LAC 33:III.2115.G. If combusted, reduce the halogenated products of combustion to an emission level acceptable to DEQ.	LAC 33:III.2115.F	N/A	
		Alternative Control Requirements. Other methods of control (such as, but not limited to, carbon adsorption, refrigeration, catalytic and/or thermal reaction, secondary steam stripping, recycling, or vapor recovery system) may be substituted for burning provided the substitute is acceptable to the administrative authority* and it achieves the same removal efficiency as required by this Section and determined in accordance with Paragraph J.1 of this Section or it achieves a degree of control not practically or safely achieved by other means. Permittee is using a condenser as control device.	LAC 33:III.2115.G		
		Requirements that specify monitoring -			
		N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
·		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
	·	N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ.	LAC 33:III.5109.A	N/A	
		Operating time <= 8760 hr/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if total Neoprene Types produced exceeds the maximum listed in this specific condition for any twelve consecutive month period. Only one vacuum jet shall operate at a time.	LAC 33:III.501.C.6	N/A	State Only
1700-20: CD Refining Column Jets Emissions CAP (Continued) GRP 0012	Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and	VOC, Total <= 12.40 tons/yr. Noncompliance with this limitation is a reportable violation of the permit. Notify the Office of Environmental Compliance, Enforcement Division if Total VOC emissions exceeds the maximum listed in this specific condition for any twelve consecutive month period.	LAC 33:III.501.C.6	N/A	State Only
<u> </u>	Reduction Requirements and	Requirements that specify monitoring -			
	Standards	Operating time monitored by technically sound method daily. Only one vacuum jet shall operate at a time.	LAC 33:Ш.501.С.6	N/A	State Only
		Requirements that specify records to be kept and requirements that specify record retention time -			
		Operating time recordkeeping by electronic or hard copy monthly. Keep records of the total operating time and total VOC emissions each month, as well as the total operating time and total VOC emissions for the last twelve months, (VOC emissions based on operation and throughput). Make records available for inspection by DEQ personnel. Only one vacuum jet shall operate at a time.	LAC 33:III.501.C.6	N/A	State Only

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
	Title 33 Chapter 51:	Requirements that specify reports to be submitted -			
1700-20: CD Refining Column Jets Emission's CAP (Continued) GRP 0012	Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and	Submit report: Due annually, by the 31st of March. Report the Total operating time and Total VOC emissions for the preceding calendar year to the Office of Env. Compliance, Enforcement Division.	LAC 33:ΠΙ.501.C.6	Annually	State Only
	Reduction Requirements and	Requirements that specify performance testing -			
	Standards	N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
1700-14B.3 Stabilizer & Catalyst Tanks Manhole Vent	Title 33 Chapter 13: Emission Standards for Particulate Matter (Including Standards for	Prevent particulate matter from becoming airborne by taking all reasonable precautions. These precautions shall include, but not be limited to, hose specified in LAC 33:III.1305.A.1-7.	LAC 33:III.1305	N/A	
RLP 0013	Some Specific Facilities)	Total suspended particulate <= 11.22 lb/hr. The rate of emission shall be the total of all emission points from the source.	LAC 33.III.1311.B	N/A	
		Opacity <= 20 percent; except emissions may have an average opacity in excess of 20 percent for not more than one six-minute period in any 60 consecutive min.	LAC 33.III.1311.C	N/A	
		Requirements that specify monitoring -			
		N/A	N/A	N/A	1
	·	Requirements that specify records to be kept and requirements that specify record retention time -			
1		N/A	N/A	N/A	1
		Requirements that specify reports to be submitted -		1	
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
	Ţ	Requirements that limit emissions or operations -			
		Comply with the requirements of 40 CFR 63.113 through 63. 118, except as provided in 40 CFR 63.485(b) through (v). Subpart U. [40 CFR 63.485(a)]	40 CFR 63.485(a)	N/A	
		Requirements that specify monitoring -			
1700-2: Strippers Condenser Vent RLP0014	Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins	The owner or operator of a Group 2 process vent having a flow rate greater than or equal to 0.005 standard cubic meter per minute, a HAP concentration greater than or equal to 50 parts per million by volume, and a TRE index value greater than 1.0 but less than or equal to 4.0 shall maintain a TRE index value greater than 1.0 and shall comply with the monitoring of recovery device parameters in §63.114(b) or (c) of this subpart, the TRE index calculations of §63.115 of this subpart, and the applicable reporting and recordkeeping provisions of §863.117 and 63.118 of this subpart. Such owner or operator is not subject to any other provisions of §863.114 through 63.118 of this subpart. [40 CFR 63.113(d)]	40 CFR 63.113(d)	N/A	
		Temperature monitored by temperature monitoring device continuously. Equip the temperature monitoring device with a continuous recorder. Monitor the exit (product side) temperature. Subpart G As allowed by 40 CFR 63.114 (c), DPP uses an alternate method due to low flow on the process side of the condenser. [40 CFR 63.114(b)(2)]	40 CFR 63.114(b)(2)	Continuously	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
1700-2: Strippers Condenser Vent RLP0014 (Continued)	Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins	An owner or operator of a process vent may request approval to monitor parameters other than those listed in paragraph (a) or (b) of this section. The request shall be submitted according to the procedures specified in 40 CFR 63.151(f) or 40 CFR 63.152(e) of this subpart. Approval shall be requested if the owner or operator uses one of the combustion or recovery or recapture devices listed in paragraphs (a) and (b) of this section, but seeks to monitor a parameter other than those specified in paragraphs (a) and (b) of this section. DPP monitors the cooling media temperature for each condenser. The daily average cooling media should not exceed the following limits: Cooling Water Loop on Water Condenser: 50 degrees Centigrade at Cooling Water Loop Sample Point Cooling Brine Loop on CD Condenser: 5 degrees Centigrade at Cooling Brine Loop Sample Point Condenser Brine Inlet on Common Condenser: (Negative) - 15 degrees Centigrade at Condenser Brine Inlet Sample Point. [40 CFR 63.114(c)(3)]	40 CFR 63.114(c)(3)	Continuously	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that specify records to be kept and requirements that specify record retention time -			
		Equipment/operational data recordkeeping by electronic or hard copy at the regulation's specified frequency. Keep up-to-date, readily accessible records of the data specified in 40 CFR 63.118(b)(1) and (b)(2). Subpart G. [40 CFR 63.118(b)]	40 CFR 63.118(b)	N/A	
4		Requirements that specify reports to be submitted -			
1700-2: Strippers Condenser Vent RLP0014 (Continued)	Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins	Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent to become a Group 1 continuous front-end process vent, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the Group 1 provisions in 40 CFR 63.113 through 63.118 in accordance with 40 CFR 63.480(i)(2)(ii) or (i)(2)(iii), as applicable. Subpart U. [40 CFR 63.485(l)(1)]	40 CFR 63.485(1)(1)	N/A	
		Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with a TRE greater than 4.0 to become a Group 2 continuous front-end process vent with a TRE less than 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(1)(2)]	40 CFR 63.485(1)(2)	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
1700-2: Strippers Condenser Vent RLP0014 (Continued)	Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins	Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with a flow rate less than 0.005 standard cubic meter per minute (scmm) to become a Group 2 continuous front-end process vent with a flow rate of 0.005 scmm or greater and a TRE index value less than or equal to 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(l)(3)] Submit report: Due within 180 days after a process change, as defined in 40 CFR 63.115(e), is made that causes a Group 2 continuous frontend process vent with an organic HAP concentration less than 50 parts per million by volume (ppmv) to become a Group 2 continuous frontend process vent with an organic HAP concentration of 50 ppmv or greater and a TRE index value less than or equal to 4.0, or with the next Periodic Report, whichever is later. Submit a description of the process change with the report of the process change, and comply with the provisions in 40 CFR 63.113(d) by the dates specified in 40 CFR 63.481. Subpart U. [40 CFR 63.485(l)(4)] Requirements that specify performance testing -	40 CFR 63.485(1)(3) 40 CFR 63.485(1)(4)	N/A	
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ Compliance with 40 CFR 63 Subpart U determined as MACT.	LAC 33:UI.5109.A	N/A	
	Title 33 Chapter 51: Comprehensive Toxic	Requirements that specify monitoring -			
1700-2: Strippers Condenser Vent	Air Pollutant Emission	N/A	N/A	N/A	
RLP0014	Control Program: Emission Control and Reduction Requirements and Standards	Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
1700-2: Strippers Condenser Vent RLP0014	Title 33 Chapter 21: Control of Emission of Organic Compounds: Waste Gas Disposal	Halogenated hydrocarbons, total >= 95 % removal efficiency as determined in accordance with LAC 33:III.2115.J.1, by combustion or other methods specified in LAC 33:III.2115.G. If combusted, reduce the halogenated products of combustion to an emission level acceptable to DEQ. Permittee uses an alternate compliance method for control (condenser) as per LAC 33:III.2115.G.	LAC 33:111.2115.F	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
1700-2: Strippers Condenser Vent RLP0014 Title 33 Chapter 21: Control of Emission of		Alternative Control Requirements. Other methods of control (such as, but not limited to, carbon adsorption, refrigeration, catalytic and/or thermal reaction, secondary steam stripping, recycling, or vapor recovery system) may be substituted for burning provided the substitute is acceptable to the administrative authority* and it achieves the same removal efficiency as required by this Section and determined in accordance with Paragraph J.1 of this Section or it achieves a degree of control not practically or safely achieved by other means. Permittee is using a condenser as a control device.	LAC 33:III.2115.G		
(Continued)	Waste Gas Disposal	Demonstrate compliance with LAC 33:III.2115 as requested by DEQ.	LAC 33:III.2115.J.1		
		Requirements that specify monitoring -			
		N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			,
•	N/Ā	N/A	N/A		
	Requirements that specify reports to be submitted -				
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		N/A	N/A	N/A	
		Requirements that specify monitoring -			
1700-3: Poly Kettles Vent Condenser RLP 0015	Subpart U: National Emission Standards for Hazardous Air Pollutant Emissions: Group I	Organic HAP >= 90 % reduction by weight using a control device. Subpart U To ensure that the Poly Kettles maintain the status of Group 2, the temperature of the condenser brine outlet is monitored to ensure it is below 5 degrees Centigrade. [40 CFR 63.487(a)(2)]	40 CFR 63.487(a)(2)	N/A	
	Polymers and Resins	Requirements that specify records to be kept and requirements that specify record retention time -			
		Equipment/operational data recordkeeping by electronic or hard copy at the regulation's specified frequency. Keep records of the information specified in 40 CFR 63.491(a) through (g), as applicable. Subpart U.	40 CFR 63.491	N/A	
	· [Requirements that specify reports to be submitted -			
-		Submit Notification: Due within 180 days after a process change, as defined in 40 CFR 63.488(i)(1), is made that causes a Group 2 batch front-end process vent to become a Group 1 batch front-end process vent, or with the next Periodic Report, whichever is later. Submit a description of the process change. Comply with the Group 1 batch front-end process vent provisions in 40 CFR 63.486 through 63.492 in accordance with 40 CFR 63.480(i)(2)(ii). Subpart U. [40 CFR 63.492(b)] Requirements that specify performance testing -	40 CFR 63.492(b)	N/A	
					<u> </u>
	1	N/A	N/A	N/A	1

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
1700-3: Poly Kettles Vent	Title 33 Chapter 21:	Halogenated hydrocarbons, total >= 95 % removal efficiency as determined in accordance with LAC 33:III.2115.J.1, by combustion or other methods specified in LAC 33:III.2115.G. If combusted, reduce the halogenated products of combustion to an emission level acceptable to DEQ. Permittee uses an alternate compliance method for control (condenser) as per LAC 33:III.2115.G.	LAC 33:ΙΠ.2115.F	N/A	
Condenser RLP 0015	Control of Emission of Organic Compounds: Waste Gas Disposal	Alternative Control Requirements. Other methods of control (such as, but not limited to, carbon adsorption, refrigeration, catalytic and/or thermal reaction, secondary steam stripping, recycling, or vapor recovery system) may be substituted for burning provided the substitute is acceptable to the administrative authority* and it achieves the same removal efficiency as required by this Section and determined in accordance with Paragraph J.1 of this Section or it achieves a degree of control not practically or safely achieved by other means.	LAC 33:III.2115.G		
		Demonstrate compliance with LAC 33:III.2115 as requested by DEQ.	LAC 33:Ш.2115.J.1	N/A	
		Requirements that specify monitoring -			
		N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
1700-3: Poly Kettles Vent Condenser RLP 0015	Title 33 Chapter 21:	Requirements that specify performance testing -			
(Continued)	(Continued)	N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
		Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ Compliance with 40 CFR 63 Subpart U and LAC 33:III.2115 determined as MACT.	LAC 33:III.5109.A	N/A	
		Requirements that specify monitoring -	1		
	Title 33 Chapter 51: Comprehensive Toxic	Monitor the temperature of the Condenser Brine Outlet to ensure it is below 5 degrees Centigrade.	LAC 33:III.501.C.6	N/A	State Only
1700-3: Poly Kettles Vent Condenser	Air Pollutant Emission Control Program: Emission Control and	Requirements that specify records to be kept and requirements that specify record retention time -			
RLP 0015	Reduction Requirements and Standards	Daily records of cooling temperature and valve monitoring shall be kept on site and available for inspection DEQ personnel.	LAC 33:III.501.C.6	N/A	State Only
		Requirements that specify reports to be submitted -			
		Submit report: Due annually, by the 31st of March. Report the cooling media temperature showing the total number of hours during which the maximum temperature was exceeded for the preceding calendar year to the Office of Environmental Compliance, Enforcement Division.	LAC 33:III.501.C.6	Annually	State Only
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		N/A	N/A	N/A	
		Requirements that specify monitoring -			
		N/A	N/A	N/A	
1700-56: No. 6, 7, 8, 10, 13 & 14 Unstripped Storage Tanks	Subpart U: National Emission Standards for	Requirements that specify records to be kept and requirements that specify record retention time -			
Depressure Vent RLP 0016	Hazardous Air Pollutant Emissions: Group I Polymers and Resins	Comply with the requirements of 40 CFR 63.119 through 63.123 and 63.148, with the differences noted in 40 CFR 63.484(b) through (s). Subpart U. [40 CFR 63.484(a)] This tank is Group 2.	40 CFR 63.484(a)	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		Control emissions of toxic air pollutants to a degree that constitutes Maximum Achievable Control Technology (MACT) as approved by DEQ. Compliance with NESHAP Subpart U determined as MACT.	LAC 33:III.5109.A	N/A	
1700-56: No. 6, 7, 8, 10, 13 &	Title 33 Chapter 51: Comprehensive Toxic	Requirements that specify monitoring -			
14 Unstripped Storage Tanks	Air Pollutant Emission	N/A	N/A	N/A	
Depressure Vent RLP 0016	Control Program: Emission Control and Reduction	Requirements that specify records to be kept and requirements that specify record retention time -			
	Requirements and Standards	N/A	N/A	N/A	
	Standards	Requirements that specify reports to be submitted -			
	N/A	N/A	N/A		
	Requirements that specify performance testing -				
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -	<u> </u>		
		All affected facilities shall comply with all applicable provisions in 40 CFR 60 Subpart A.	40 CFR 60	N/A	
		Requirements that specify monitoring -			
	Process of the second	N/A	N/A	N/A_	
Facility Wide - DuPont - Pontchartrain Site - Facility Wide Emissions	Part 60 - Standards of Performance for New Stationary Sources.	Requirements that specify records to be kept and requirements that specify record retention time -			
UNF 0001	Subpart A: General Provisions	N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
	1	Requirements that specify performance testing -		1	
		N/A	N/A	N/A	-
——————————————————————————————————————		Requirements that limit emissions or operations -			
		All affected facilities shall comply with all applicable provisions in 40 CFR 61 Subpart A.	40 CFR 61	N/A	
	 Part 61 – National	Requirements that specify monitoring -		<u> </u>	
Facility Wide - DuPont -	Emission Standards for	N/A	N/A	N/A	
Pontchartrain Site – Facility Wide Emissions UNF 0001	Hazardous Air Pollutants Subpart A: General Provisions	Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
Facility Wide – UNF 0001	Part 61 -	Requirements that specify performance testing -		T	
(Continued)	(Continued)	N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
Facility Wide - DuPont - Pontchartrain Site - Facility Wide Emissions	Subpart M: National Emission Standards for Asbestos	Do not install or reinstall on a facility component any insulating materials that contain commercial asbestos if the materials are either molded and friable or wetapplied and friable after drying. Subpart M.	40 CFR 61.148	N/A	
UNF 0001		Requirements that specify monitoring -			
		N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		Provide DEQ with written notice of intention to demolish or renovate prior to performing activities to which 40 CFR 61 Subpart M applies. Delivery of the notice by U.S. Postal Service, commercial delivery service, or hand delivery is acceptable. Subpart M. [40 CFR 61.145(b)(1)]	40 CFR 61.145(b)(1)	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
	·	Requirements that limit emissions or operations -			
Facility Wide - DuPont -	Subpart FF: National	Benzene < 1 Mg/yr (1.1 ton/yr) total quantity. Subpart FF. [40 CFR 61.342(d)(2)(i)]	40 CFR 61.342(d)(2)(i)	N/A	
Pontchartrain Site - Facility Wide Emissions	Emission Standards for Benzene Waste	Requirements that specify monitoring -		1	
UNF 0001	Operations	Determine compliance with 40 CFR 61 Subpart FF using the test methods and procedures specified in 40 CFR 61.355(a) through (i), as applicable. Subpart FF.	40 CFR 61.355	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		Equipment/operational data recordkeeping by electronic or hard copy at the regulation's specified frequency Maintain records as specified in 40 CFR 61.356(a) through (n), as applicable. Maintain each record in a readily accessible location at the facility site for a period not less than two years from the date the information is recorded unless otherwise specified. Subpart FF.	40 CFR 61.356	N/A	
	\	Requirements that specify reports to be submitted -			
	Submit report: Due whenever there is a change in the process generating the waste stream that could cause the total annual benzene quantity from facility waste to increase to 1 Mg/yr (1.1 ton/yr) or more. Submit updates to the information listed in 40 CFR 61.357(a)(1) through (a)(3). Subpart FF. [40 CFR 61.357(b)]	40 CFR 61.357(b)	N/A		
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
Facility Wide - DuPont -	Subpart U: National Emission Standards for	N/A	N/A	N/A	
Pontchartrain Site - Facility Wide Emissions	Hazardous Air Pollutant	Requirements that specify monitoring -	-:-	-	
UNF 0001	Emissions: Group I Polymers and Resins	N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		Keep copies of all applicable records and reports required by 40 CFR 63 Subpart U for at least 5 years, as specified in 40 CFR 63.506(a)(1), with the exception listed in 40 CFR 63.506(a)(2). Subpart U. [40 CFR 63.506(a)]	40 CFR 63.506(a)	N/A	
		Comply with the applicable recordkeeping and reporting requirements in 40 CFR 63 Subpart A, as specified in 40 CFR 63 Subpart U Table 1. Subpart U. [40 CFR 63.506(b)]	40 CFR 63.506(b)	N/A	
	Equipment/operational data recordkeeping by electronic or hard copy continuously. Keep records of the information specified in 40 CFR 63.506(d)(1) through (d)(9), unless an alternative recordkeeping system has been requested and approved as specified in 40 CFR 63.506(g), and except as provided in 40 CFR 63.506(h). Subpart U. [40 CFR 63.506(d)]	40 CFR 63.506(d)	Continuously		

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
	Subpart U: National	Requirements that specify reports to be submitted -			
Pontchartrain Site – Facility Wide Emissions	Emission Standards for Hazardous Air Pollutant Emissions: Group I Polymers and Resins	Submit Notification of Compliance Status: Due no later than 150 days after the compliance dates specified in 40 CFR 63 Subpart U. Submit the information specified in 40 CFR 63.506(e)(5)(i) through (e)(5)(xii), as applicable. Subpart U. [40 CFR 63.506(e)(5)	40 CFR 63.506(e)(5)	N/A	
		Submit Periodic Report: Due semiannually no later than 60 days after the end of each 6-month period. Submit the first report no later than 240 days after the date the Notification of Compliance Status is due, covering the 6-month period beginning on the date the Notification of Compliance Status is due. Submit the information specified in 40 CFR 63.506(e)(6)(i) through (e)(6)(xii). Subpart U. [40 CFR 63.506(e)(6)]	40 CFR 63.506(e)(6)	Semiannually	
		Requirements that specify performance testing -			
		Conduct performance testing in accordance with 40 CFR 63.7(a)(1), (a)(3), (d), (e)(1), (e)(2), (e)(4), (g), and (h), with the exceptions specified in 40 CFR 63.504(a)(1) through (a)(5) and the additions specified in 40 CFR 63.504(b). Subpart U. [40 CFR 63.504(a)]	40 CFR 63.504(a)	N/A	
D. W. Will D. D.		Requirements that limit emissions or operations -			
Wide Emissions	Part 63 – National Emission Standards for	All affected facilities shall comply with all applicable provisions in 40 CFR 63 Subpart A.	40 CFR 63	N/A	
UNF 0001	Hazardous Air	Requirements that specify monitoring -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
Facility Wide - DuPont -		Requirements that specify records to be kept and requirements that specify record retention time -			
Pontchartrain Site - Facility Wide Emissions	Part 63 – National Emission Standards for	N/A	N/A	N/A	
UNF 0001	Hazardous Air	Requirements that specify reports to be submitted -			
(Continued)		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
		Shall comply with all the applicable requirements of 40 CFR 63 Subpart FFFF - Miscellaneous Organic Chemical Manufacturing.	40 CFR 63.2430	N/A	
		Requirements that specify monitoring -			
Facility Wide – DuPont – Pontchartrain Site – Facility	Subpart FFFF: National Emission Standards for	N/A	N/A	N/A	
Wide Emissions UNF 0001	Hazardous Air Pollutants:	Requirements that specify records to be kept and requirements that specify record retention time -			
	Miscellaneous Organic Chemical	N/A	N/A	N/A	
	Manufacturing	Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
Facility Wide - DuPont - Pontchartrain Site - Facility Wide Emissions UNF 0001	Part 68 – Chemical Accident Prevention Provisions. Subpart A:	Ensure that response actions have been coordinated with local emergency planning and response agencies. [40 CFR 68.12(b)(3)]	40 CFR 68.12(b)(3)	N/A	
0111 0001	General Provisions	Include in the RMP the certification specified in 68.12(b)(4). [40 CFR 68.12(b)(4)]	40 CFR 68.12(b)(4)	N/A	
1		Requirements that specify monitoring -		<u> </u>	
		N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		Equipment/operational data recordkeeping by electronic or hard copy continuously. Document that the nearest public receptor is beyond the distance to a toxic or flammable endpoint defined in 68.22. [40 CFR 68.12(b)(1)]	40 CFR 68.12(b)(1)	Continuously	
		Complete the five-year accident history for the process as provided in 68.42. [40 CFR 68.12(b)(2)]	40 CFR 68.12(b)(2)	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
	}	N/A	N/A	N/A	

Emíssion Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		Use the endpoints specified in 68.22(a) through (g) for analyses of offsite consequences.	40 CFR 68.22	N/A	
Facilia, Wide D. D. A	Port 49 Chamian	Analyze the release scenarios in 68.25, as specified in 68.25(a) through (h).	40 CFR 68.25	N/A	
Pontchartrain Site - Facility Wide Emissions UNF 0001	Vide Emissions Provisions. Subpart B:	Identify and analyze at least one alternative release scenario for each regulated toxic substance held in a covered process(es) and at least one alternative release scenario to represent all flammable substances held in covered processes, as specified in 68.28(b) through (e).	40 CFR 68.28	N/A	
		Estimate in the RMP the population within a circle with its center at the point of the release and a radius determined by the distance to the endpoint defined in 68.22(a).	40 CFR 68.30	N/A	
		List in the RMP environmental receptors within a circle with its center at the point of the release and a radius determined by the distance to the endpoint defined in 68.22(a).	40 CFR 68.33	N/A	
		Review and update the offsite consequence analyses at least once every five years. Complete a revised analysis within six months if changes in processes, quantities stored or handled, or any other aspect of the stationary source might reasonably be expected to increase or decrease the distance to the endpoint by a factor of two or more.	40 CFR 68.36	Every 5 Years	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Include in the five-year accident history all accidental releases from covered processes that resulted in deaths, injuries, or significant property damage on site, or known offsite deaths, injuries, evacuations, sheltering in place, property damage, or environmental damage. Include the information specified in 68.42(b)(1) through (10) for each accidental release.	40 CFR 68.42	N/A	
		Requirements that specify monitoring -			
Facility Wide - DuPont - Pontchartrain Site - Facility	Part 68 – Chemical Accident Prevention	N/A	N/A	N/A	
Wide Emissions UNF 0001	Provisions. Subpart B: Hazard Assessment	Requirements that specify records to be kept and requirements that specify record retention time -			
(Continued)	(Continued)	Equipment/operational data recordkeeping by electronic or hard copy continuously. Maintain the records specified in 68.39(a) through (e) on the offsite consequence analyses.	40 CFR 68.39	Continuously	
		Requirements that specify reports to be submitted -			
		Submit revised RMP: Due within six months after changes in processes, quantities stored or handled, or any other aspect of the stationary source increase or decrease the distance to the endpoint by a factor of two or more. [40 CFR 68.36(b)]	40 CFR 68.36(b)	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -		T	
		N/A	N/A	N/A	
		Requirements that specify monitoring -			
		. N/A	N/A	N/A	-
Facility Wide - DuPont -	Part 68 – Chemical	Requirements that specify records to be kept and requirements that specify record retention time -			
Pontchartrain Site - Facility	Accident Prevention Provisions. Subpart G:	N/A	N/A	N/A	
Wide Emissions UNF 0001	Risk Management Plan	Requirements that specify reports to be submitted -			
		Provide in the RMP an executive summary that includes a brief description of the elements listed in 68.155(a) through (g)	40 CFR 68.155	N/A	
		Submit in the RMP information one worst-case release scenario for each Program 1 process. Include the data specified in 68.165(b)(1) through (13).	40 CFR 68.165	N/A	
		Submit in the RMP the information provided in 68.42(b) on each accident covered by 68.42(a).	40 CFR 68.168	N/A	
		Provide in the RMP the emergency response information listed in 68.180(a) through (c).	40 CFR 68.180	N/A	
	•	Submit Risk Management Plan (RMP): Due no later than June 21, 1999, or three years after the date on which a regulated substance is first listed under 68.130, or the date on which a regulated substance is first present above a threshold quantity in a process. Submit in a method and format to a central point as specified by EPA prior to June 21, 1999.	40 CFR 68.150	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Complete a single registration form and include in the RMP. Cover all regulated substances handled in covered processes. Include in the registration the information specified in 68.160(b)(1) through (13).	40 CFR 68.160	N/A	
Facility Wide DuPont Pontchartrain Site Facility Wide Emissions UNF 0001	Part 68 – Chemical Accident Prevention Provisions. Subpart G:	Submit revised registration to EPA: Due within six months after a stationary source is no longer subject to 40 CFR 68. Indicate that the stationary source is no longer covered. [40 CFR 68.190(c)]	40 CFR 68.190(c)	N/A	
(Continued)	Risk Management Plan (Continued)	Review and update the RMP as specified in 68.190(b) and submit it in a method and format to a central point specified by EPA prior to June 21, 1999.	40 CFR 68.190	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -		1	
Facility Wide - DuPont -	Part 68 - Chemical	N/A	N/A	N/A	
Pontchartrain Site - Facility Wide Emissions	Accident Prevention Provisions. Subpart H:	Requirements that specify monitoring -			
UNF 0001	Other Requirements	N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
	1	Maintain records supporting the implementation of 40 CFR 68 for five years unless otherwise provided.	40 CFR 68.200	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
}		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -			
		N/A	N/A	N/A	
		Requirements that specify monitoring -			
Facility Wide DuPont		N/A	N/A	N/A	
Pontchartrain Site - Facility Wide Emissions	Part 70 – State Operating Permit	Requirements that specify records to be kept and requirements that specify record retention time -			
UNF 0001	Programs	N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			1
		Submit Title V permit application for renewal: Due 6 months before permit expiration date. [40 CFR 70.5(a)(1)(iii)]	40 CFR 70.5(a)(1)(iii)	N/A	
		Submit Title V monitoring results report: Due semiannually, by March 31st and September 30th for the preceding periods encompassing July through December and January through June, respectively. Submit reports to the Office of Environmental Compliance, Surveillance Division. Certify reports by a responsible company official. Clearly identify all instances of deviations from permitted monitoring requirements. For previously reported deviations, in lieu of attaching the individual deviation reports, clearly reference the communication(s)/correspondence(s) constituting the prior report, including the date the prior report was submitted. [40 CFR 70.6(a)(3)(iii)(A)]	40 CFR 70.6(a)(3)(iii)(A)	Semiannually	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued)	Part 70 – State Operating Permit Programs (Continued)	Submit Title V excess emissions report: Due quarterly, by June 30, September 30, December 31, March 31. Submit reports of all permit deviations to the Office of Environmental Compliance, Surveillance Division. Certify all reports by a responsible official in accordance with 40 CFR 70.5(d). The reports submitted on March 31 and September 30 may be consolidated with the semi-annual reports required by 40 CFR 70.6(a)(3)(iii)(A) as long as the report clearly indicates this and all required information is included and clearly delineated in the consolidated report. Unless required by an applicable reporting requirement, a written report is not required during periods in which there is no deviation. [40 CFR 70.6(a)(3)(iii)(B)] Submit Title V compliance certification: Due annually, by the 31st of March. Submit to the Office of Environmental Compliance, Surveillance Division. [40 CFR 70.6(c)(5)(iv)] Requirements that specify performance testing -	40 CFR 70.6(a)(3)(iii)(B) 40 CFR 70.6(c)(5)(iv)	Quarterly Annually	
·		N/A .	N/A	N/A	
Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001	Title 33 Chapter 11: Control of Emission of Smoke – Impairment of Visibility on Public Roads Prohibited	Requirements that limit emissions or operations - Emissions of smoke which pass onto or across a public road and create a traffic hazard by impairment of visibility as defined in LAC 33:III.111 or intensify an existing traffic hazard condition are prohibited. Requirements that specify monitoring - N/A Requirements that specify records to be kept and requirements that specify record retention time -	LAC 33:III.1103	N/A N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		N/A	N/A	N/A	
	Title 33 Chapter 11:	Requirements that specify reports to be submitted -			
Facility Wide - DuPont - Pontchartrain Site - Facility	Control of Emission of Smoke – Impairment of	N/A	N/A	N/A	
Wide Emissions	Visibility on Public Roads Prohibited	Requirements that specify performance testing -			
UNF 0001 (Continued)	Roads I followed	N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
		Emissions of particulate matter which pass onto or across a public road and create a traffic hazard by impairment of visibility or intensify an existing traffic hazard condition are prohibited.	LAC 33:III.1303.B	N/A	
	Title 33 Chapter 13:	Requirements that specify monitoring -			
Facility Wide - DuPont - Pontchartrain Site - Facility	Emission Standards for Particulate Matter	N/A	N/A	N/A	
Wide Emissions UNF 0001	(Including Standards for Some Specific	Requirements that specify records to be kept and requirements that specify record retention time -			
_	Facilities) – Provisions Governing Specific	N/A	N/A	N/A	
	Activities	Requirements that specify reports to be submitted -	· · · · ·		
		N/A	N/A	N/A	
		Requirements that specify performance testing -	· · · · · · · · · · · · · ·		
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -		Ī	
Facility Wide – DuPont –	Title 33 Chapter 21:	Equip all rotary pumps and compressors handling volatile organic compounds having a true vapor pressure of 1.5 psia or greater at handling conditions with mechanical seals or other equivalent equipment.	LAC 33:III.2111	N/A	
Pontchartrain Site – Facility Wide Emissions UNF 0001	Control of Emission of Organic Compounds	Maintain best practical housekeeping and maintenance practices at the highest possible standards to reduce the quantity of organic compounds emissions. Good housekeeping shall include, but not be limited to, the practices listed in LAC 33:III.2113.A.1-5.	LAC 33:III.2113.A	N/A	
		Requirements that specify monitoring -			
		N/A	N/A	N/A	
·		Requirements that specify records to be kept and requirements that specify record retention time -			
	·	N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	<u>† </u>
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -		T	
Facility Wide - DuPont - Rontchartrain Site - Facility Wide Emissions	Title 33 Chapter 2: Rules and Regulations for the Fee System of the Air Quality Control Programs	Failure to pay the prescribed application fee or annual fee as provided herein, within 90 days after the due date, will constitute a violation of these regulations and shall subject the person to applicable enforcement actions under the Louisiana Environmental Quality Act including, but not limited to, revocation or suspension of the applicable permit, license, registration, or variance.	LAC 33:III.219	N/A	
		Requirements that specify monitoring -			_
		N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
Facility Wide – DuPont – Pontchartrain Site – Facility	Title 33 Chapter 5:	Requirements that limit emissions or operations - Permittee shall comply with the Part 70 General	LAC 33:III.535	N/A	
i vide Linasions	Permit Procedures	Conditions as set forth in LAC 33:III.535 and the Louisiana General Conditions as set forth in LAC 33:III.537. [LAC 33:III.535 and LAC 33:III.535	LAC 33.III.333	N/A	
		Requirements that specify monitoring -			
		N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -		Ţ	
Facility Wide – DuPont –	Title 33 Chapter 51:	Do not construct or modify any stationary source subject to any standard set forth in LAC 33:III.Chapter 51.Subchapter A without first obtaining written authorization from DEQ in accordance with LAC 33:III.Chapter 51.Subchapter A, after the effective date of the standard.	LAC 33:Ш.5105.A.1		
Pontchartrain Site – Facility Wide Emissions UNF 0001	Comprehensive Toxic Air Pollutant Emission Control Program: Prohibited Activities	Do not cause a violation of any ambient air standard listed in LAC 33:III.Table 51.2, unless operating in accordance with LAC 33:III.5109.B.	LAC 33:III.5105.A.2	N/A	
	and Special Provisions	Do not build, erect, install, or use any article, machine, equipment, process, or method, the use of which conceals an emission that would otherwise constitute a violation of an applicable standard.	LAC 33:III.5105.A.3		
·		Requirements that specify monitoring -			
		N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		Do not fail to keep records, notify, report or revise reports as required under LAC 33:III.Chapter 51.Subchapter A.	LAC 33:UI.5105.A.4	N/A	
		Requirements that specify reports to be submitted -			
		N/A	N/A	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that limit emissions or operations -]	
		N/A	N/A	N/A	
		Requirements that specify monitoring -		† · · · · · · · · · · · · · · · · · · ·	
Facility Wide - DuPont -	Title 33 Chapter 51:	N/A	N/A	N/A	
Pontchartrain Site - Facility Wide Emissions	Comprehensive Toxic Air Pollutant Emission Control Program:	Requirements that specify records to be kept and requirements that specify record retention time -			
UNF 0001	Reporting Requirements	N/A	N/A	N/A	
		Requirements that specify reports to be submitted -			
		Submit Annual Emissions Report (TEDI): Due annually, by the 31st of March unless otherwise directed by DEQ, to the Office of Environmental Assessment in a format specified by DEQ. Identify the quantity of emissions in the previous calendar year for any toxic air pollutant listed in Table 51.1 or Table 51.3.	LAC 33:III.5107.A	Annually	State Only
		Include a certification statement with the annual emission report and revisions to any emission report that attests that the information contained in the emission report is true, accurate, and complete, and that is signed by a responsible official, as defined in LAC 33:III.502. Include the full name of the responsible official, title, signature, date of signature and phone number of the responsible official.	LAC 33:III.5107.A.2	N/A	State Only

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001 (Continued)	Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program:	Submit notification: Due to the Department of Public Safety 24-hour Louisiana Emergency Hazardous Materials Hotline at (225) 925-6595 immediately, but in no case later than 1 hour, after any discharge of a toxic air pollutant into the atmosphere that results or threatens to result in an emergency condition (a condition which could reasonably be expected to endanger the health and safety of the public, cause significant adverse impact to the land, water or air environment, or cause severe damage to property).	LAC 33:III 5107.B.1	N/A	State Only
		Submit notification: Due to SPOC, except as provided in LAC 33:III.5107.B.6, no later than 24 hours after the beginning of any unauthorized discharge into the atmosphere of a toxic air pollutant as a result of bypassing an emission control device, when the emission control bypass was not the result of an upset, and the quantity of the unauthorized bypass is greater than or equal to the lower of the Minimum Emission Rate (MER) in LAC 33:III.5112, Table 51.1, or a reportable quantity (RQ) in LAC 33:I.3931, or the quantity of the unauthorized bypass is greater than one pound and there is no MER or RQ for the substance in question. Submit notification in the manner provided in LAC 33:I.3923.	LAC 33:III.5107.B.2	N/A	State Only
		Submit notification: Due to SPOC, except as provided in LAC 33:III.5107.B.6, immediately, but in no case later than 24 hours after any unauthorized discharge of a toxic air pollutant into the atmosphere that does not cause an emergency condition, the rate or quantity of which is in excess of that allowed by permit, compliance schedule, or variance, or for upset events that exceed the reportable quantity in LAC 33:I.3931. Submit notification in the manner provided in LAC 33:I.3923.	LAC 33:III.5107.B.3	N/A	State Only

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
Facility Wide - DuPont - Pontchartrain Site - Facility Wide Emissions UNF 0001 (Continued)	Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Reporting Requirements	Submit written report: Due by certified mail to SPOC within seven calendar days of learning of any such discharge or equipment bypass as referred to in LAC 33:III.5107.B.1 through B.3. Include the information specified in LAC 33:III.5107.B.4.a.i through B.4.a.viii.	LAC 33:III.5107.B.4	N/A	State Only
	Reporting Requirements	Report all discharges to the atmosphere of a toxic air pollutant from a safety relief device, a line or vessel rupture, a sudden equipment failure, or a bypass of an emission control device, regardless of quantity, IF THEY CAN BE MEASURED AND CAN BE RELIABLY QUANTIFIED USING GOOD ENGINEERING PRACTICES, to DEQ along with the annual emissions report and where otherwise specified. Include the identity of the source, the date and time of the discharge, and the approximate total loss during the discharge.	LAC 33:III.5107.B.5	N/A	State Only
		Requirements that specify performance testing -			
		N/A	N/A	N/A	_
Facility Wide - DuPont -		Requirements that limit emissions or operations -			,
Pontchartrain Site - Facility	Title 33 Chapter 51: Comprehensive Toxic	N/A	N/A	N/A	
Wide Emissions UNF 0001 Comprehensive Toxic Air Pollutant Emission Control Program:	Air Pollutant Emission	Requirements that specify monitoring -			
	N/A	N/A	N/A		
	,	Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that specify reports to be submitted -			
Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001	Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission Control Program: Emission Control and Reduction Requirements and Standards	Develop a standard operating procedure (SOP) within 120 days after achieving or demonstrating compliance with the standards specified in LAC 33:III.Chapter 51. Detail in the SOP all operating procedures or parameters established to ensure that compliance with the applicable standards is maintained and address operating procedures for any monitoring system in place, specifying procedures to ensure compliance with LAC 33:III.5113.C.5. Make a written copy of the SOP available on site or at an alternate approved location for inspection by DEQ. Provide a copy of the SOP within 30 days upon request by DEQ.	LAC 33:Ш.5109.C	N/A	State Only
		Requirements that specify performance testing -		<u> </u>	<u> </u>
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
Facility Wide - DuPont - Pontchartrain Site - Facility Wide Emissions UNF 0001	Title 33 Chapter 51: Comprehensive Toxic Air Pollutant Emission	An individual or company contracted to perform a demolition or renovation activity which disturbs RACM must be recognized by the Licensing Board for Contractors to perform asbestos abatement, and shall meet the requirements of LAC 33:III.5151.F.2 and F.3 for each demolition or renovation activity.	LAC 33:III.5151.F.1.f	N/A	State Only
	Control Program: Emission Standard for	Requirements that specify monitoring -		<u> </u>	<u> </u>
	Asbestos	N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			·
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that specify reports to be submitted -	-		
Facility Wide - DuPont - Pontchartrain Site - Facility	Title 33 Chapter 51: Comprehensive Toxic	Submit notification in writing: Due to SPOC not more than 60 days nor less than 30 days prior to initial start-up. Submit the anticipated date of the initial start-up.	LAC 33:III.5113.A.1	N/A	
Wide Emissions UNF 0001 (Continued)	Air Pollutant Emission Control Program: Emission Standard for Asbestos	Submit notification in writing: Due to SPOC within 10 working days after the actual date of initial start-up of the source. Submit the actual date of initial start-up of the source.	LAC 33:III.5113.A.2	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
		Activate the preplanned abatement strategy listed in LAC 33:III.5611.Table 5 when the administrative authority declares an Air Pollution Alert.	LAC 33:III.5609.A.1.b	N/A	
Facility Wide - DuPont -	Title 33 Chapter 56: Prevention of Air	Activate the preplanned strategy listed in LAC 33:III.5611.Table 6 when the administrative authority declares an Air Pollution Warning.	LAC 33:III.5609.A.2.b	N/A	
Pontchartrain Site – Facility Wide Emissions UNF 0001	Prevention of Air Pollution Emergency Episodes: Preplanned Strategies Required	Activate the preplanned abatement strategy listed in LAC 33:III.5611.Table 7 when the administrative authority declares an Air Pollution Emergency.	LAC 33:III.5609.A.3.b	N/A	
		Requirements that specify monitoring -			
		N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
<u></u>		Requirements that specify reports to be submitted -			
Facility Wide – DuPont – Pontchartrain Site – Facility Wide Emissions UNF 0001	Title 33 Chapter 56: Prevention of Air Pollution Emergency Episodes: Preplanned Strategies Required	Prepare standby plans for the reduction of emissions during periods of Air Pollution Alert, Air Pollution Warning and Air Pollution Emergency. Design standby plans to reduce or eliminate emissions in accordance with the objectives as set forth in LAC 33:III.5611.Tables 5, 6, and 7.	LAC 33:III.5609.A	N/A	
(Continued)	Judiogies Required	Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
		Comply with the provisions in 40 CFR 68, except as specified in LAC 33:III.5901.	LAC 33:III.5901.A	N/A	
Facility Wide - DuPont - Pontchartrain Site - Facility Wide Emissions UNF 0001	Title 33 Chapter 59: Chemical Accident Prevention and Minimization of Consequences	Identify hazards that may result from accidental releases of the substances listed in 40 CFR 68.130, Table 59.0 of LAC 33:III.5907, or Table 59.1 of LAC 33:III.5913 using appropriate hazard assessment techniques, design and maintain a safe facility, and minimize the off-site consequences of accidental releases of such substances that do occur.	LAC 33:III.5907	N/A	
		Requirements that specify monitoring -			
		N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that specify reports to be submitted -	-		
Facility Wide - DuPont - Pontchartrain Site - Facility Wide Emissions UNF 0001 (Continued)	Title 33 Chapter 59: Chemical Accident Prevention and Minimization of Consequences	Submit registration: Due January 31, 1998, or within 60 days after the source becomes subject to LAC 33:III.Chapter 59, whichever is later. Include the information listed in LAC 33:III.5911.B, and submit to the Department of Environmental Quality, Office of Environmental Compliance, Emergency and Radiological Services Division.	LAC 33:Ш.5911.A	N/A	
		Submit amended registration: Due to the Department of Environmental Quality, Office of Environmental Compliance, Emergency and Radiological Services Division, within 60 days after the information in the submitted registration is no longer accurate.	LAC 33:Ш.5911.C	N/A	
		Requirements that specify performance testing -			
		N/A	N/A	N/A	
		Requirements that limit emissions or operations -			
Parities Wide Dan		N/A	N/A	N/A	
Facility Wide - DuPont - Pontchartrain Site - Facility	Title 33 Chapter 9: General Regulations on	Requirements that specify monitoring -			
Wide Emissions UNF 0001	Control of Emissions and Emission Standards	N/A	N/A	N/A	
		Requirements that specify records to be kept and requirements that specify record retention time -			
		N/A	N/A	N/A	

TABLE 2: STATE AND FEDERAL AIR QUALITY REQUIREMENTS

Emission Point ID No.:	Applicable Requirement	Compliance Method/Provision	Compliance Citation	Averaging Period/ Frequency	State Only Requirement
		Requirements that specify reports to be submitted -			
Facility Wide DuPont Pontchartrain Site Facility Wide Emissions UNF 0001 (Continued)	Title 33 Chapter 9: General Regulations on Control of Emissions and Emission Standards	Submit Emission Inventory (EI)/Annual Emissions Statement: Due annually, by the 31st of March for the period January 1 to December 31 of the previous year unless otherwise directed. Submit emission inventory data in the format specified by the Office of Environmental Assessment, Air Quality Assessment Division. Include all data applicable to the emissions source(s), as specified in LAC 33:III.919.A-D. Report the unauthorized discharge of any air pollutant into the atmosphere in accordance with LAC	LAC:III.919.D	N/A	
·		33:I.Chapter 39, Notification Regulations and Procedures for Unauthorized Discharges. Submit written reports to the department pursuant to LAC 33:I.3925. Submit timely and appropriate follow-up reports detailing methods and procedures to be used to prevent similar atmospheric releases.			
		Requirements that specify performance testing -			
		N/A	N/A	N/A	

Emission Point ID No:	Requirement	Exempt or Does Not Apply	Explanation	Citation Providing for Exemption or Non-applicability
EQT150 thru EQT155	40 CFR 60.110b	Does Not Apply	Storage tanks have a capacity of less than 75 cubic meters (19,813 gallons).	40 CFR 60.110b(a)
1700-5.3 thru 5.8 EQT178 1700-63.5	40 CFR 63.160	Exempted	Exempt from controls as surge vessels do not meet the conditions specified in Table 2. Vessels have capacities less than 75 m ³ .	40 CFR 63.160
RLP016 1700-56	LAC 33:III.2115	Exempted	As per requirement of LAC 33:111.2115.H.1.c	LAC 33:III.2115.H.1.c
EQTs - 134, 167,	LAC 33:III.2115	Exempted	As per requirement of LAC 33:III.2115.H.2.b.	LAC 33:III.2115.H.2.b
135, 136, 183, 0185, 1 0198	LAC 33:III.5107 and 5109	Does Not Apply	Emissions are intermittent. Controlling these emissions is not practical or safe.	
1700-1, 5A, 13, 13A, 64, 66 and 79	40 CFR 63.480	Does Not Apply	Does not meet the definition of batch or continuous front-end process vent.	
EQT142 thru EQT149	LAC 33:III.2115.	Exempted	As per requirements of LAC 33:III.2115.H.2.b	LAC 33:III.2115.H.2.b
1700-25 thru 28, and 45 thru 48	40 CFR 63 Subpart U	Exempted	As per requirements of 40 CFR 63.494(a)(4). There are no process back end requirements for the Neoprene Units. These sources are exempted from Subpart U under the back-end process provisions.	40 CFR 63.494(a)(4)
EQT141	LAC 33:III.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
1700-21A	40 CFR 60.110b	Does Not Apply	No construction or modification after 7/23/84.	
	LAC 33:III.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
EQT137 & ETQ138	LAC 33:III.5107 and 5109	Does Not Apply	These vessels do not store TAP compounds.	
1700-14B.1 and 14B.2	40 CFR 60.110b	Does Not Apply	Tanks have a capacity of less than 75 cubic meters (19,813 gallons).	40 CFR 60.110b(a)
	40 CFR 63.480	Exempted	As per the requirements of 40 CFR 63.480(c)(1). These vessels do not store HAPs.	40 CFR 63.480(c)(1)

TABLE 3: EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

Emission Point ID No:	Requirement	Exempt or Does Not Apply	Explanation	Citation Providing for Exemption or Non-applicability
	LAC 33:III.2115	Exempled	As per the requirements of LAC 33:III.2115.H.4.	LAC 33:III.2115.H,4
RLP013 1700-14B.3	LAC 33:IJI.5107 and 5109	Does Not Apply	Emissions are intermittent. Controlling these emissions is not practical or safe	
	40 CFR 63.480	Does Not Apply	Does not meet the definition of batch or continuous front-end process vent.	
ETQ166, 168, 169, 170	LAC 33:111.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	_
1700-57	LAC 33:II.5107 and 5109	Does Not Apply	Does not store TAP compounds.	
1700-60 thru 62	40 CFR 60.110b	Does Not Apply	Tanks have a capacity of less than 75 cubic meters (19,813 gallons).	40 CFR 60.110b(a)
	40 CFR 63.480	Exempted	As per the requirements of 40 CFR 63.480(c)(1). These vessels do not store HAPs.	40 CFR 63.480(c)(1)
EQT163 thru EQT165	LAC 33:III.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
1700-53 thru 55	40 CFR 60.110b	Does Not Apply	Tanks have a capacity of less than 75 cubic meters (19,813 gallons).	40 CFR 60.110b(a)
	40 CFR 63 Subpart U 40 CFR 63.480	Exempted	As per requirements of 40 CFR 63.484(b)(2)	40 CFR 63.484(b)(2)
EQT156 thru EQT161, EQT171, EQT175 thru EQT177, and	LAC 33:III.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
EQT162 1700-50.1 thru 50.6, 63.1 thru 63.4 and 1700-51	40 CFR 60.110b	Does Not Apply	Tanks have a capacity of less than 75 cubic meters (19,813 gallons).	40 CFR 60.110b(a)

Emission Point ID No:	Requirement	Exempt or Does Not Apply	Explanation	Citation Providing for Exemption or Non-applicability
EQT172, EQT173, & EQT181 1700-63.8, 1700-	LAC 33:III.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
63.10 and 1700-63.11	40 CFR 60.110b	Exempted	As per the requirements of 40 CFR 110b(b), vapor pressure of contents is less than 2.1 psia (15 kpa).	40 CFR 60.110b(a)
EQT182 1700-63.9	40 CFR 60.110b	Does Not Apply	No Construction or modification after 7/23/84.	
EQT186 thru	40 CFR 63 Subpart U	Exempted	As per requirements of 40 CFR 63.484(b)(2)	40 CFR 63.484(b)(2)
EQT192 1700-67 thru 73	LAC 33:IΠ.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
	40 CFR 60.110b	Does Not Apply	Tanks have a capacity of less than 75 cubic meters (19,813 gallons). 40 CFR 60.110b(a)	40 CFR 60.110b(a)
	LAC 33:III.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
EQT194 thru	LAC 33:III. 5107, and 5109	Does Not Apply	Tanks do not store TAP compounds.	
EQT196 1700-75 thru 77	40 CFR 60.110b	Exempted	As per the requirements of 40 CFR 110b(b), vapor pressure of contents is less than 2.1 psia (15 kpa).	40 CFR 110b(b)
	40 CFR 63.480	Exempted	As per the requirements of 40 CFR 63.480(c)(1). These vessels do not store HAPs.	40 CFR 63.480(c)(1)
ET202 thru EQT204	40 CFR 60.110b	Does Not Apply	No Construction or modification after 7/23/84.	
3-95, 4-95, and 5-95	LAC 33:III.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	22222

TABLE 3: EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

Emission Point ID No:	Requirement	Exempt or Does Not Apply	Explanation	Citation Providing for Exemption or Non-applicability
FOTIO	LAC 33:Ш.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
EQT199 and EQT200	LAC 33:III. 5107 and 5109	Does Not Apply	Tanks do not store TAP compounds.	
1700-80.1 1700-80.2	40 CFR 60.110b	Exempted	As per the requirements of 40 CFR 110b(b), vapor pressure of contents is less than 2.1 psia (15 kpa).	40 CFR 110b(b)
1700-00.2	40 CFR 63.480	Does Not Apply	These tanks are associated with the ACR production Unit which is covered under Subpart FFFF	
	40 CFR 63.2470	Exempted	These vessels do not store organic HAPs.	
	LAC 33:III. 5107 and 5109	Does Not Apply	This header does not emit TAP compounds.	
RLP 017 1700-80	40 CFR 63.480	Does Not Apply	Sources venting thru this header are associated with the ACR production Unit which is covered under Subpart FFFF	
	40 CFR 63.2470	Exempted	This header does not emit organic HAPs.	
EQT205 thru EQT208	LAC 33:III.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
1700-81.1	LAC 33:IU. 5107 and 5109	Does Not Apply	Tanks do not store TAP compounds.	
1700-81.2 1700-81.3	40 CFR 60.110b	Does Not Apply	Tanks have a capacity of less than 75 cubic meters (19,813 gallons).	40 CFR 60.110h(a)
1700-81.4	40 CFR 63.2470	Exempted	These vessels do not store organic HAPs.	

Emission Point ID	Requirement	Requirement Exempt or Does Not Apply Explanation		Citation Providing for Exemption or Non-applicability
EQT209 thru	LAC 33:III.2115	Exempted	The waste gas stream has a combined weight of VOC of less than 100 pounds in any continuous 24-hour period.	LAC 33:III.2115.H.1.c
EQT211	LAC 33:III.5107 and 5109	Does Not Apply	Does not store TAP compounds.	
1700-81.5 1700-81.6 1700-81.7	40 CFR 63.480	Does Not Apply	These sources are associated with the ACR production Unit which is covered under Subpart FFFF.	
	40 CFR 63.2470	Does Not Apply	These sources do not emit TAP compounds.	
RLP018	LAC 33:III.2115	Exempted	The waste gas stream has a combined weight of VOC of less than 100 pounds in any continuous 24-hour period.	LAC 33:III.2115
1700-81	LAC 33:III.5107 and 5109	Does Not Apply	Does not store TAP compounds.	LAC 33:111.5107 and 5109
	40 CFR 63.480	Does Not Apply	This vent is associated with the ACR production Unit which is covered under Subpart FFFF.	40 CFR 63.480
	40 CFR 63.2470	Does Not Apply	This vent does not emit TAP compounds.	40 CFR 63.2470
	40 CFR 60.110b	Does Not Apply	This tank has a capacity of less than 75 cubic meters (19,813 gallons).	40 CFR 60.110b(a)
EQT201 1700-82	40 CFR 63.480	Does Not Apply	This tank is associated with the ACR production Unit which is covered under Subpart FFFF.	
	40 CFR 63.2470	Exempted	The volume of this tank is less than 10,000 gallons.	

TABLE 3: EXPLANATION FOR EXEMPTION STATUS OR NON-APPLICABILITY OF A SOURCE

Emission Point ID No:	Requirement	Exempt or Does Not Apply	Explanation	Citation Providing for Exemption or Non-applicability
	LAC 33:III.2115	Exempted	The waste gas stream has a combined weight of VOC of less than 100 pounds in any continuous 24-hour period.	LAC 33:III.2115.H.1.c
RLP019 1700-83	LAC 33:III.5107 and 5109	Does Not Apply	TAPs emissions from this source are emitted below their respective MER facility wide. No MACT required.	
1,00 05	40 CFR 63.480	Does Not Apply	This tank is associated with the ACR production Unit which is covered under Subpart FFFF.	
	40 CFR 63.2470	Exempted	This source does not meet the definition of process vent per 40 CFR 63.2455.	40 CFR 63.2455
	LAC 33:III.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
EQT212	40 CFR 60.110b	Does Not Apply	This tank has a capacity of less than 75 cubic meters (19,813 gallons).	
1700-84A	40 CFR 63.480	Does Not Apply	This tank is associated with the ACR production Unit which is covered under Subpart FFFF.	
	40 CFR 63.2470	Exempted	The volume of this tank is less than 10,000 gallons	
EQT213 1700-84B	LAC 33:III.2107	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
EQT214 1700-85	40 CFR 63.2470	Exempted	As per 63.2550 – definition of Group 1 transfer racks, since the vapor pressure of the liquid being loaded is less than 1.5 psia this facility is a Group 2 and there are no requirements othen than recordkeeping under 40 CFR 63.130(f)	40 CFR 63.130(f)

Emission Point ID No:	Requirement	Exempt or Does Not Apply	Explanation	Citation Providing for Exemption or Non-applicability
	LAC 33:III.2103	Does Not Apply	VOC total vapor pressure is less than the regulated threshold of 1.5 psia.	
EQT215 1700-86	LAC 33:III.5107 and 5109	Does Not Apply	Does not store TAP compounds	
	40 CFR 60.110b	Does Not Apply	Tank has a capacity of less than 75 cubic meters (19,813 gallons).	
	40 CFR 63.480	Exempted	As per the requirements of 40 CFR 63.480(c)(1). This vessel does not store HAHPs.	40 CFR 63.480(c)(1).
1700-87, 1700-88, 1700-89	LAC 33:ΠΙ.2115	Exempted	As per requirement of LAC 33:III.2115.H.2.b.	LAC 33:III.2115.H.2.b
No. 10, No. 13 & No. 14	LAC 33:III.5107 and 5109	Does Not Apply	Emissions are intermittent. Controlling these emissions is not practical or safe.	
Emulsion Storage Tank Manway	40 CFR 63.480	Does Not Apply	Does not meet the definition of batch or continuous front-end process vent.	

The above table provides explanation for either the exemption status or non-applicability of a source cited by 2 or 3 in the matrix presented in Table 1 of this application.

Enter each single emission point that routes its emissions to another source (i.e., a control device) or a common stack, or is part of an Emissions Cap. List the emissions source to which each single emission point is routed or the Cap of which the source is a member, if applicable. Consult instructions.

Emission Point ID No:	Description	Construction Date	Routes to:	Operating Rate/Volume	Applicable Requirement(s)?
1700-2 (RLP0014)	Strippers Condenser Vent				⊠ Yes □ No
1700-2A (EQT219)	No. 1 Stripper		1700-2 (RLP0014)	12,600 lb/hr	⊠ Yes □ No
1700-2B (EQT220)	No. 2 Stripper		1700-2 (RLP0014)	12,600 lb/hr	⊠ Yes □ No
1700-2C (EQT221)	No. 3 Stripper		1700-2 (RLP0014)	12,600 lb/hr	⊠ Yes □ No
1700-3 (RLP0015)	Poly Kettles Vent Condenser				⊠ Yes □ No
1700-3A (EQT222)	Poly Kettle No. 1		1700-3 (RLP0015)	1420 charges/yr	☑ Yes ☐ No
1700-3B (EQT223)	Poly Kettle No. 2		1700-3 (RLP0015)	1420 charges/yr	⊠ Yes □ No
1700-3C (EQT224)	Poly Kettle No. 3		1700-3 (RLP0015)	1420 charges/yr	⊠ Yes □ No
1700-3D (EQT225)	Poly Kettle No. 4		1700-3 (RLP0015)	1420 charges/yr	⊠ Yes □ No
1700-3E (EQT226)	Poly Kettle No. 5	·	1700-3 (RLP0015)	1420 charges/yr	⊠ Yes □ No
1700-5 (GRP0008)	Unstripped Emulsion Storage Tanks Vent	·			⊠ Yes □ No
1700-5.3 (EQT150)	Unstripped Emulsion Storage Tank. No. 6	7/1968	1700-5 (GRP0008)	11,622 gal	⊠ Yes □ No
1700-5.4 (EQT151)	Unstripped Emulsion Storage Tank. No. 7	8/1972	1700-5 (GRP0008)	14,950 gal	☑ Yes ☐ No
1700-5.5 (EQT152)	Unstripped Emulsion Storage Tank. No. 8	8/1972	1700-5 (GRP0008)	14,950 gal	⊠ Yes □ No

Emission Point ID No:	Description	Construction Date	Routes to:	Operating Rate/Volume	Applicable Requirement(s)?
1700-5.6 (EQT153)	Unstripped Emulsion Storage Tank. No. 10	9/2007	1700-5 (GRP0008)	16,000 gal	☐ Yes ☐ No
1700-5.7 (EQT154)	Unstripped Emulsion Storage Tank. No. 13	9/2007	1700-5 (GRP0008)	10,000 gal	⊠ Yes □ No
1700-5.8 (EQT155)	Unstripped Emulsion Storage Tank. No. 14	9/2007	1700-5 (GRP0008)	10,000 gal	⊠ Yes □ No
1700-14B (GRP0006)	Acetic Acid Tanks				☐ Yes ⊠ No
1700-14B.1 (EQT137)	· Acetic Acid Make-up Tank	1975	1700-14B (GRP0006)	1,590 gal	☐ Yes ⊠ No
1700-14B.2 (EQT138)	Acetic Acid Hold-up Tank	1975	1700-14B (GRP0006)	600 gal ´	☐ Yes ⊠ No
1700-25A (GRP0007)	Product Drying CAP				⊠ Yes □ No
1700-25 (EQT142)	East Wash Belt Dryer	1970	1700-25A (GRP0007)	30,000 lb/hr	⊠ Yes □ No
1700-26 (EQT143)	West Wash Belt Dryer	1970	1700-25A (GRP0007)	30,000 lb/hr	⊠ Yes □ No
1700-27 _(EQT144)	East Hot Dryer Exhaust	1970	1700-25A (GRP0007)	30,000 lb/hr	⊠ Yes □ No
1700-28 (EQT145)	West Hot Dryer Exhaust	1970	1700-25A (GRP0007)	30,000 lb/hr	⊠ Yes □ No
1700-45 (EQT146)	No. 1 East Dryer Cooling Compt.	1970	1700-25A (GRP0007)	30,000 lb/hr	⊠ Yes □ No
1700-46 (EQT147)	No. 1 West Dryer Cooling Compt.	1970	1700-25A (GRP0007)	30,000 lb/hr	⊠ Yes □ No
1700-47 (EQT148)	No. 2 East Dryer Cooling Compt.	1970	1700-25A (GRP0007)	30,000 lb/hr	⊠ Yes □ No
1700-48 (EQT149)	No. 2 West Dryer Cooling Compt.	1970	1700-25A (GRP0007)	30,000 lb/hr	⊠ Yes □ No

Emission Point ID No:	Description	Construction Date	Routes to:	Operating Rate/Volume	Applicable Requirement(s)?
1700-50 (GRP0009)	Stabilizer Tanks Vent				⊠ Yes □ No
1700-50.1 (EQT156)	Stabilizer Tank No. 1	10/1975	1700-50 (GRP0009)	1,070 gal	⊠ Yes □ No
1700-50.2 (EQT157)	Stabilizer Tank No. 2	10/1975	1700-50 (GRP0009)	1,070 gal	⊠ Yes □ No
1700-50.3 (EQT158)	Stabilizer Tank No. 3	7/1968	1700-50 (GRP0009)	1,070 gal	☑ Yes ☐ No
1700-50.4 (EQT159)	Stabilizer Tank No. 4	7/1968	1700-50 (GRP0009)	1,070 gal	⊠ Yes □ No
1700-50.5 (EQT160)	Stabilizer Tank No. 5	9/2007	1700-50 (GRP0009)	1,070 gal	⊠ Yes □ No
1700-50.6 (EQT161)	Stabilizer Tank - LD750	9/2007	1700-50 (GRP0009)	300 gal	⊠ Yes □ No
1700-63 (GRP0010)	Vent Header System				
1700-63.1 (EQT171)	No. 1 CD Solution Tank	8/1968	1700-63 (GRP0010)	3,690 gal	⊠ Yes □ No
1700-63.2 (EQT175)	No. 2 CD Solution Tank	7/1972	1700-63 (GRP0010)	3,690 gal	⊠ Yes □ No
1700-63.3 (EQT176)	Recovered CD Storage Tank No. 1	6/1968	1700-63 (GRP0010)	8,156 gal	⊠ Yes □ No
1700-63.4 (EQT177)	Recovered CD Storage Tank No. 2	6/1968	1700-63 (GRP0010)	8,156 gal	⊠ Yes □ No
1700-63.5 (EQT178)	CD Heels Tank	9/1990	1700-63 (GRP0010)	8,315 gal	⊠ Yes □ No
1700-63.8 (EQT181)	Crude CD Storage Tank No. 3	3/1971	1700-63 (GRP0010)	25,750 gal	⊠ Yes □ No

Emission Point ID No:	Description	Construction Date	Routes to:	Operating Rate/Volume	Applicable Requirement(s)?
1700-63.9 V182)	Refined CD Storage Tank	3/1971	1700-63 (GRP0010)	50,000 gal	⊠ Yes □ No
1700-63.10 (EQT172)	Inhibitor Final Make-up Tank	6/1968	1700-63 (GRP0010)	22,164 gal	⊠ Yes □ No
1700-63.11 (EQT173)	Inhibitor Hold-up Tank	6/1968	1700-63 (GRP0010)	22,164 gai	⊠ Yes □ No
1700-80 (RLP017)	ACR Storage Vent Header				
1700-80.1 (EQT199)	Refined ACR Storage Tank	3/1971	1700-8 (RLP017)	55,000 gal	☐ Yes ⊠ No
1700-80.2 (EQT200)	Chlorinated ACR Storage Tank	6/1968	1700-8 (RLP017)	22,164 gal	☐ Yes ⊠ No
1700-81 (RLP018)	ACR Refining Vent				
1700-81.1 (EQT205)	NMP/PTZ Tote	1/2008	1700-81 (RLP018)	400 gal	☐ Yes ⊠ No
1700-81.2 (EQT 206)	Aqueous Actrene Tote	1/2008	1700-81 (RLP018)	400 gai	☐ Yes ⊠ No
1700-81.3 (EQT207)	Recovery Column Heels Tote	1/2008	(1700-81 (RLP018)	400 gal	☐ Yes ⊠ No
1700-81.4 (EQT208)	TBC Tote	1/2008	1700-81 (RLP018)	400 gal	☐ Yes ⊠ No
1700-81.5 (EQT209)	ACR Refining Column	9/2007	1700-81 (RLP018)	3 MMlb/yr	☐ Yes ⊠ No
1700-81.6 (EQT210)	ACR RC Condenser	9/2007	1700-81 (RLP018)	3 MMlb/yr	☐ Yes ⊠ No
1700-81.7 (EQT211)	ACR RC Reboiler	9/2007	1700-81 (RLP018)	3 MMlb/yr	☐ Yes 🖾 No

23. Emissions Inventory Questionnaire (EIQ) Forms [LAC 33:III.517.D.3; 517.D.6]

Complete one (1) EIQ for:

- Each emission source. If two emission sources have a common stack, the applicant may submit one EIQ sheet for the common emissions point. Note any emissions sources that route to this common point in Table 4 of the application.
- Each emissions CAP that is proposed. In general, this applies to each source that is part of the CAP.
- Each alternate operating scenario that a source may operate under. Some common scenarios are:
 - 1. Sources that combust multiple fuels
 - 2. Sources that have Startup/Shutdown max lb/hr emission rates higher than the max lb/hr for normal operating conditions would need an EIQ for the Startup/Shutdown emission rates for those sources
- Fugitive emissions releases. One (1) EIQ should be completed for each of the following types of fugitive emissions sources or emissions points:
 - 1. Equipment leaks.
 - 2. Non-equipment leaks (i.e. road dust, settling ponds, etc).

For each EIQ:

- Fill in all requested information.
- Speciate all Toxic Air Pollutants and Hazardous Air Pollutants emitted by the source.
- Use appropriate significant figures.
- Consult instructions.

The EIQ is in Microsoft Word Excel. Visit the following website to get to the EIQ form. http://www.deq.louisiana.gov/portal/DIVISIONS/AirPermits/AirPermitApplications.aspx

							5	State of L	ouisia	na							-	Date of	submitt	al
			(8)			Emissions	Inventory (Question	naire (EIQ) for Ai	r Polluta	ints						Nov	20	013
E	mission F	Point ID N	lo.		Descriptive	Name of the I	Emissions Source	e (Alt. Nam	e)			App	proximate Location	on of Stack o	Vent (se	e instruc	ctions)			
	- 11 - T	nation)				22 - 2	2 50						00 114 11	hi- n	NI			Determ	NIATO	,
*1	170	00-1			Empleion S		(0, 13, and 14 Manhole and Ex	hauet Blow	or	Method UTM Zor		15	06,"Address Mate Horizontal	hing-Primary 739000	mE	Ver	rtical	Datum 332		mN
Tem	po Subie	ct Item I	D No.		Zantaision 3	totage rank i	raminie and E)	maust Diowi		Latitude	30 0		3			5 "	dear	332		fredths
					100					Longitude	-		31		, 1		1		hund	lredths
		Γ0134																		
	and Dis			neter (ft)		Height of St		Gas Exit		Gas Flow at	Stack Ga		Normal Opera		Date of			ercent		
	d Charac ige? (yes		Disc	charge Ar	rea (ft²)	Above Grade	e (ft) Vel	ocity		litions, not at	Temper		Time (hours per year		onstruction Modificat			ighput Emission		•
O.d.	P () co	J. 110)							Stand	lard (ft³/min)	(°F))	(nouts per yea		, LJUILLE			21110310	, ii x 0111	
	no								00000					Au;		1972	Jan-		Jul-Sep	
		-	7 9	1.25	ft	53.8 f	t 34.0	00 ft/sec	2,50	00 ft^3/min	77°	F	8,760	hr/yr		1	Mar 25%	Jun 25%	25%	Dec 25%
					ft ²						1						2370	2376	25%	2370
-	1	. OF					(O		aluda v	240)	1			
Fuel		1			and Heat I			(la se)					Operating Para	Paran		uts)	r	escript	ion	
ruel	a	-		e of Fuel NA		Heat I	NA	nr)	1	Normal Operatin	a Rate/Thro	mahnut		42,000 ll		+		rescript	1011	
	b	_		A 17 A	(1	14/1			Maximum Opera			nit	42,000 N						
	С				1					Design Capacity				N		+			-	
	-	-			Notes	-	=			Shell Height (ft)				N						Tab.
										Tank Diameter (ft)			N						
										Tanks:		Roof	Floating Roo	of 🗆	Ex	ernal			Int	ternal
								3		Date Engine Ord					Engine	Model '	Year			
=				- 10						Date Engine Wa										
										SI Engines:		Rich Bu		Lean Burn		2 Stre	oke	0	4 Stro	ke
	Emission Point ID No. (Designa			ation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	7	Proj	posed Emission	Rates		Permitted Emission Rate (Current)	Add, Change, Delete, or	Com	tinuous pliance		ncentra Exiting		
Pollutant							Aver (lb/l	-	Maximum (lbs/hr)	Ann (tons		Annual (tons/yr)	Unchange	d	uiou					
THE REAL PROPERTY.	Particulate matter (PM ₁₀) Sulfur dioxide																7			std ft ³
-	Sulfur dioxide										-									by vol
	Nitrogen oxides Carbon monoxide										-						-			by vol
	Carbon monoxide Total VOC (including those listed be			-1	000	000			7.	2.57			3.55		_		-			by vol
Total VOC (including those listed be Lead			elow)	000	0%		0.8	51	2.57	3.5	00	3.56	U	-		-			by vol	
Chloroprene Chloroprene				000	0%	00126-99-8	0.5	55	1.75	2.4	12	2.42	U			-			by vol	
Chloroprene Toluene					000	0%	00120-99-8	0.0		0.27	0.3	_	0.38	U			-		_	n by vol
					500	570	00.00-00-0	0.0		V.2.1	0.5		0,50		-		-			a by vol

	2/4					- X	St	ate of Louisian	a							Date of	submittal	
						Emissions	Inventory Q	uestionnaire (I	EIQ) for Ai	r Pollutants						Nov	201	13
								*							1.	35		
E		Point ID N	No.		Descriptive	Name of the l	Emissions Source	(Alt. Name)		A	pproximate Locati	on of Stack or V	ent (see	instruct	tions)			
		gnation) 00-2				Strinners (Condenser Vent		Method		06,"Address Mat	ching-Primary Na	ame"			Datum	NAD83	
						on ppera c	Jondenser vent		UTM Zon		5 Horizontal		mE	Ver				mN
Tem	po Subje	ect Item H	D No.						Latitude	30 *		-	15				hundre	
	RLI	P0014	7		*				Longitude	-90 °	31		15		0.2		hundre	dths
	and Dis	The state of the s	Dia	meter (ft)	or Stack	Height of St	ack Stack Ga	s Exit Stack (Gas Flow at	Stack Gas Exi	Normal Opera	The state of the s	Date of				f Annua	The state of the s
	il Chara ige? (yes	cteristics	Dis	charge A	rea (ft²)	Above Grade	e (ft) Veloc	170	tions, not at	Temperature	Time (hours per ye		struction dificatio				Through on Point	This
Cita	Bc. (100	Or mo)						Standa	rd (ft³/min)	(°F)	(nours per ye	ivit	difficació					
	no	181		0.00		40.11				0.45	0.040			2006	Jan-		Jul-Sep	
	-	- 1		0.33	_It	62.4 f	t 1.36	ft/sec 7.1	ft^3/min	0 °F	8,760	hr/yr			Mar 25%	Jun 25%	25%	Dec 25%
					ft ²			1			1				*			
		Ty	pe of F	uel Used	d and Heat I	nput (see ins	structions)				Operating Par	ameters (incl	ude uni	ts)				
Fuel				e of Fuel			nput (MMBTU/hr)				Paramet			D	escript	ion	
	a			NA			NA	N	ormal Operating	g Rate/Throughpu	it	12,600 lbs/hr/s	stripper					
	b									ting Rate/Through	73	NA						
	С									Volume/Cylinder	Displacement	· NA						
		1/00			Notes				hell Height (ft)			NA				-		
	VOC emission r			rate includ	ies 0.01 lbs/yr	of 1,2-dichlorot	enzene	-	ank Diameter (f	THE RESERVE OF THE PERSON NAMED IN	T = : =	NA .	Exte				Inter	rnal
	VOC emission r							-	anks:	Fixed Roof	Floating Ro	oof 🗆	Engine l		'aar		Inter	illai
					,			The state of the s	ate Engine Ord	Built by Manufa	cturer	T	Eligine i	viouei i	cai			
									I Engines:	□ Rich I		Lean Burn		2 Stro	ke	O	4 Stroke	e
Em	Emission Point ID No. (Designal			ation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number		osed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change,	Conti		1.0000000000000000000000000000000000000	THE PARTY OF THE P	ion in G	110000000000000000000000000000000000000
Pollutant							Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Delete, or Unchanged	Met			Exiting	at Stack	•	
Particu	Particulate matter (PM ₁₀)																gr/st	d ft ³
	Sulfur dioxide																ppm b	by vol
Name and Address of the Owner, where	Nitrogen oxides																	by vol
-	Carbon monoxide Total VOC (including those listed be																	by vol
-	Total VOC (including those listed be) Lead			elow)	047	>95		3.02	4.43	13.22	17.36	С						by vol
	Lead Chloroprene				047	>05	00126 00 8	3	4.4	12.14	17.20	C	-			_		by vol
Chloroprene Toluene				000	>95	00126-99-8 00108-88-3	0.018	0.03	0.077	0.03	C						by vol	
Ammo					000	0%	07664-41-7	1.2	1.8	5.26	10.51	C						by vol

							8	State of	Louisiar	na -								Date of	submitt	al
						Emissions	Inventory	Question	nnaire (I	EIQ) for Air	Pollutan	ts						Nov	20	013
				+:			3			-/	The second secon	energy (1404	20	/13
E	mission P	oint ID N	No. I		Descriptive	Name of the I	Imiesione Form	roo (Alt No.	ma)			Ann	oximate Location	n of Staal-	Vent (ess	Inctero	tions)			
,,,,,		nation)	10.	h.	Descriptive	rame of the f	missions 30th	(Ce (AIL Na)	me)			Appro	OMINATE LOCATIO	on of Stack of	vent (see	mstruc	uons)			
		00-3				Poly Kettles	Vent Condens	ser		Method		00	6,"Address Matc	hing-Primary	Name"			Datum	NAD8	3
						100				UTM Zon		15	Horizontal	739000	mE		tical	332	7400	mN
Tem	po Subje	ct Item II	D No.						45	Latitude	30 8		3		15					redths
	RLP	0015			×					Longitude	°		31		15	-			hund	redths
	and Disc		Diam	eter (ft)	or Stack	Height of St	ack Stack	Gas Exit		Gas Flow at	Stack Gas 1	Exit	Normal Opera	ting	Date of		P	ercent o	of Annu	al
	l Charac		Disc	harge A	rea (ft²)	Above Grade	(ft) Ve	elocity		tions, <u>not</u> at	Temperati	ure	Time		nstruction			0 .	Throug	The state of the s
Chan	ge? (yes	or no)							Standa	ard (ft ³ /min)	(°F)		(hours per year	ar) I	Aodification 1	n		Emissio	on Poin	t
				14												0000	Jan-	Apr-	Jul-Sep	Oct-
	no	.	_	0.33	ft	62.4 f	t 4	.20 ft/sec	22	ft^3/min	34 °F		8,760	hr/yr		2006	Mar	Jun		Dec
					0.2												25%	25%	25%	25%
	,		-		ft²															
		Ty			and Heat I	nput (see ins	tructions)					0	perating Para	ameters (in	clude uni	ts)				
Fuel				e of Fuel		Heat In	nput (MMBTU	J/hr)						Paran			D	escript	ion	
	a			NA			NA		-	Normal Operating			S-	7,060 cha						
	Ь								1 1	Maximum Operat		Time and		N/	-					
	VOC emission r									Design Capacity/	Volume/Cylin	der Disp	placement	N/		-				
	VOC emission				Notes	610 4: 11			-	hell Height (ft)				N/		-				
	VOC emission				des 10 lbs/yr of	1,2-dichlorobe	enzene		I -	ank Diameter (f		6 1	El-vi- P	N/						1
	VOC emission								1 -	Tanks:	Fixed Ro	toot	Floating Roo	of 🗆	Exte		,		Int	ernal
									1 -	Date Engine Orde	The same of the sa				Engine l	Model 1	ear			
										Date Engine Was		ch Burn		Lean Burn		2 Stro	lre		4 Stro	ke
Em	Emission Point ID No (Decise			tion)	Control	Control	HAP / TAP		1 3	A Engines.	- Kit	T Duri	Permitted	Lean Duri	T-	2 5110	N.C		7340	NC
Lin	Emission Point ID No. (Designa			Lion)	Equipment	Equipment	CAS Numbe						Emission Rate	Add,						
	1700-3				Code	Efficiency			Prop	osed Emission F	lates		(Current)	Change,	Contin		Con	centra	tion in (Gases
	-													Delete, or	Comp	-		Exiting	at Stac	ck
	Pollutant								erage o/hr)	Maximum (lbs/hr)	Annua (tons/yr		Annual (tons/yr)	Unchanged						
	Particulate matter (PM ₁₀)																		gr/	std ft ³
	Sulfur dioxide																			by vol
	Nitrogen oxides Carbon monoxide																		ppm	by vol
	Carbon monoxide Total VOC (including those listed be																			by vol
diameter and	Total VOC (including those listed be Lead				047	>95		7	.84	35.54	34.35		34.92	С						by vol
Chloroprene Chloroprene					0.47	-00	00107.00.0		170	25.2	22.55	_	24.20							by vol
Chloroprene Toluene					047	>95 >95	00126-99-8 00108-88-3).12	35.2 0.34	33.82 0.53	-	0.53	C						by vol
Toluene					047	793	00108-88-3	-	1.14	0.34	0.33	_	0.33	- 0	-		-			by vol

						St	ate of Lou	isiana		The state of the s					Date	ofs	ubmitta	
					Emissions	Inventory Q	uestionnai	ire (EIQ) for Air	Pollutants					Nov	-	201	3
					× 1													
E	mission l	Point ID N	lo.	Descriptive	Name of the l	Emissions Source	(Alt. Name)		T	App	proximate Locati	on of Stack or V	ent (see	instruction	s)			
		gnation)		•			and the second second										WALKET SHOP	
	17	00-5		Unsti	ripped Emulsi	on Storage Tanks	Vent		Method		06,"Address Mate					-	NAD83	NI
700	0.14	- 4 T4 TY	V 9.1						UTM Zon Latitude	e 15	Horizontal 3		mE 15	Vertical		33274	hundr	mN edthe
I em	po Subje	ect Item II	No.						Lautude		31		15		-		hundr	
	GRI	P0008							Longitude	-90				×	_	-	nondi	Julio
Stack	and Dis		Diamete	r (ft) or Stack	Height of St	ack Stack Ga	as Exit S	Stack Gas	Flow at	Stack Gas Exit	Normal Opera	iting	Date of		Perce	nt of	Annua	il
0.70		cteristics	Dischar	rge Area (ft²)	Above Grade		city	Conditions	s, not at	Temperature	Time	Con	struction	or Ti			hrough	
Char	ige? (yes	or no)					S	Standard (ft ³ /min)	(°F)	(hours per ye	ear) Me	odificatio	n ,	Em	ission	Point	
							- 1					1 10 10 1	1	Ja	- A	or- J	ul-Sep	Oct-
	no	- 1	(0.167 ft	55.3 f	74.72	ft/sec	10.1	ft^3/min	77 °F	8,760	hr/yr		M			шт оср	Dec
		-	-		3015	1112					3). 33			25	_	%	25%	25%
			W	ft ²			1								8			
	1	Ty	pe of Fuel	Used and Heat I	nput (see ins	structions)					Operating Par	ameters (incl	ude unit	ts)				
Fuel			Type of			nput (MMBTU/h	r)					Parame		7	Desc	riptic	n	
	а		NA			NA		Norm	al Operating	Rate/Throughput		35.0 MMg	al/yr					10000
	b			- A		3		Maxir	num Operat	ing Rate/Throughp	out	NA						-
	С							Desig	n Capacity/	Volume/Cylinder D	isplacement	NA						
				Notes				Shell	Height (ft)			NA	*/***					
*CAP	for EIQ n	ios. 1700-5	3, 5.4, 5.5, 5	.6, 5.7, and 5.8. VO	C emissions rat	te includes 10 lbs/y	ут of 1,2-	Tank	Diameter (f	t)		NA						
				dichlorobenzene			1	Tank	s: 🗆	Fixed Roof	Floating Ro	of 🗆	Exter		(Inte	rnal
						L.		Annual Control of the	Engine Orde				Engine I	Model Year				
										Built by Manufact								
								SI En	gines:	□ Rich Bu		Lean Burn		2 Stroke			4 Strok	e
Em	ission Po	1700-5	. (Designatio	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number		Proposed	Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contir	iance			on in G	
Polluta	int				ř.		Average (lb/hr)	100	(lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meti	100				
Particu	late matte	er (PM ₁₀)															gr/s	td ft ³
-	dioxide																	by vol
-	en oxides																	by vol
	monoxi						12:										_	by vol
-	OC (incl	luding thos	e listed below	000	0%		0.67		3/t	2.94	2.77	С						by vol
Lead													-				-	by vol
Chloroprene				000	0%	00126-99-8	0.67		*	2.91	2.73	C	-					by vol
Toluene				000	0%	00108-88-3	< 0.01	_		0.03	0.03	U	-			-		by vol
41																	DUIL	U.A. A.D.I.

																	Total Control			-
								Sta	te of Lou	uisian	a				7			Date of	submitt	al
						Emissions	Invente	ory Qu	estionna	ire (E	IQ) for Air	r Pollutants						Nov	20	13
		160																		asorti
Er	nission P	oint ID N	0.		Descriptive	Name of the I	Emissions	Source (A	Alt. Name)			Ap	proximate Locati	on of Stack or V	Vent (see	instruc	tions)			
		nation)											*							
	1700	0-5.3			Unst	ripped Emulsi	on Storag	ge Tank N	10.6		Method		06, Address Mate			17		Datum-		
Ton	no Cubi	et Italia	NA								UTM Zon Latitude	15 30 °	Horizontal 3	739000	mE 15		tical -	332		mN redths
i em	po subjec	ct Item ID	NO.								Longitude		31		15					redths
	EQT	0150									Longitude	-20	31				-		nunu	i odula
	and Disc		Diame	eter (ft) o	r Stack	Height of St	ack S	tack Gas			Gas Flow at	Stack Gas Exit	Normal Opera		Date of			ercent o		
	Charac		Disch	arge Are	ea (ft²)	Above Grade	e (ft)	Velocit			ions, not at	Temperature	Time		struction			ghput		
Chan	ge? (yes	or no)								Standar	rd (ft³/min)	(°F)	(hours per ye	ear) M	odificatio	n		Emissio	n Poin	
														T.		1968	Jan-	Apr-	Jul-Sep	Oct-
	по	. 1	N	Af	t.	NAf	t NA	f	t/sec	NA		77 °F	8,760	hr/yr Jul		1309	Mar	Jun		Dec
				04	.2							-					25%	25%	25%	25%
			_	f	t".					11]								
		Ту			and Heat I	nput (see ins	truction	is)					Operating Par	ameters (incl	ude uni	ts)				
Fuel				of Fuel		Heat In	nput (MM	(BTU/hr						Parame			D	escript	on	
	a		1	NA			NA			N	ormal Operatin	g Rate/Throughput	t	35 MMg	al/yr					
	ь											ting Rate/Through	70	35 MMg						
	С									_		Volume/Cylinder I	Displacement	11,622		_				
4.00					Notes			2 31			hell Height (ft)	200		16.83						
*Tan	k is vente	ed to a com	imon vent		istripped emul	sion tanks, EIQ	No. 1700)-5, Unstri	pped	_	ank Diameter (1		T = : =	11.5						
				emuis	ion ranks vei	III					anks:		Floating Ro	of 🗆	Exte		,		Int	ernal
									1		ate Engine Ord				Engine	Model	rear			
												Built by Manufac		I san P		2 Stro	lea		4 Stro	lro
-			an I			G . 1 T	Die i	min I		S	I Engines:	□ Rich B		Lean Burn		2 3110	ке	u	4 5tro	Ke
Emi	ssion Poi	int ID No.	(Designat		Control Equipment	Control Equipment	HAP /						Permitted Emission Rate	4.11						
	1700-5.3				Code	Efficiency	CAS NO	miller		Propo	sed Emission	Rates	(Current)	Add, Change,	Contin		Con	centrat	ion in (Tases
													13-5175110	Delete, or	Comp			Exiting		and the same of th
Polluta	Pollutant							t	Average	e	Maximum	Annual	Annual	Unchanged	Met	hod				
	Particulate matter (PM ₁₀)					24			(lb/hr)	1.3-	(lbs/hr)	(tons/yr)	(tons/yr)							
-		er (PM ₁₀)																		std ft ³
Sulfur o														-					-	by vol
-	n oxides											_								by vol
	monoxid				000	000					5.00	-	*		-					by vol
Total VOC (including those listed below) Lead					000	0%			*	-+	5.29	*	-	U	-		_			by vol
Chloroprene					000	0%	00126	00.9	**	-+	5.23	+	*	Ü	-					by vol
Toluene					000	0%	00126		*	\rightarrow	0.05		*	U	-					by vol
Toluene					000	0.70	00100	-00-3	1140	-	0.03	 	+	+	-					by vol

								State of	Louisia	na				-					Date of	submitta	il
						Emissions	Invento	ory Questio	onnaire (EIQ) for A	Air Poll	utants							Nov	20	13
E	mission l	Point ID N	No.		Descriptive	Name of the	Emissions	Source (Alt. N	ame)			Ap	pproxima	te Locatio	on of Stack o	r Vent (see	instruc	tions)			
	(Desig	gnation)																			
	170	00-5.4	- 1		Unst	tripped Emuls	ion Storag	e Tank No. 7		Method			06,"Add	iress Mate	hing-Primary	Name"				NAD83	
										UTM Z		15	Horiz	zontal	739000	mE		tical .	332		mN
Tem	po Subje	ect Item II	D No.							Latitud		30 °		3			5 " .			hundr	
	EOT	TO LET								Longitu	ide	90°		31		15			-	hundr	edths
Etaalı	and Dis	T0151	Diama	eter (ft) o	C4l-	TI-1-14 - 6 G4		4	T 61-1	CFI	1 64-1	C E-4	I N	-10	<i>ii</i> 1	D. t. C		D.	oroont.	of Annua	1
A CANADA STATE OF THE STATE OF		cteristics				Height of St	Manager III	tack Gas Exit	The second second	Gas Flow at	100000000000000000000000000000000000000	Gas Exit	Norm	al Opera		Date of onstruction				Through	
	ige? (yes		Disch	narge Are	ea (ft ⁻)	Above Grade	e (IL)	Velocity		litions, <u>not</u> at lard (ft ³ /min)	710-0100	perature	Chou	rs per ye		Modification				n Point	
7 7	0				- 1				Stand	iaru (it /min)		(°F)	(200	us per je		I TO CHE I CHE I	-				
	no														An		1972	Jan-	Apr-	Jul-Sep	Oct-
1	110		N	Af	t	NA f	t NA	ft/sec	NA			77 °F	8,7	760	hr/yr Au	8	19/2	Mar	Jun		Dec
					,												1	25%	25%	25%	25%
			-	f	t ²							*				-		4			
		Ty	pe of Fu	el Used	and Heat I	nput (see ins	tructions	s)					Operat	ing Para	ameters (in	clude uni	its)			100	
Fuel				of Fuel			put (MM		1 1						Parar	neter	1	D	escript	on	
	a			NA			NA			Normal Operat	ing Rate/I	hroughput			35 MM	Igal/yr		at lease of		200	
	b			77					7 1	Maximum Ope	rating Rat	e/Throughp	put		35 MM	Igal/yr				The state of the	-
	c							4 0		Design Capaci	ty/Volume	/Cylinder D	Displacem	ent	14,95	A STREET WATER THE PERSON NAMED IN			,		
					Notes					Shell Height (f					20.	-					
*Tan						sion tanks, EIC	No. 1700-	-5, Unstripped	7	Tank Diameter	(ft)				1	2					
	*Tank is vented to a common vent for the				ion Tanks Ve	nt			1	Tanks:	7 Fix	ed Roof	Flo	oating Roo	of \square	Exte	rnal			Inte	rnal
										Date Engine O	rdered					Engine	Model Y	ear.			
										Date Engine W		y Manufact	turer				T				- T- V
12										SI Engines:		Rich Bu			Lean Burn		2 Stro	ke		4 Strok	e
Emi	Emission Point ID No. (Designation) 1700-5.4				Control Equipment Code	Control Equipment Efficiency	HAP/7		Proj	oosed Emission	n Rates		Emissi	nitted on Rate rrent)	Add, Change,	Comp	nuous			ion in G	
Pollutant				_					erage b/hr)	Maximum (lbs/hr)		nnual ons/vr)	12.000	nual ns/yr)	Delete, or Unchange	Mel	thod		Exiting	at Stack	c
Particulate matter (PM ₁₀)				-				(1	WILLY)	(-30.111)	- (*	3.7	1,131	3-1						gr/e	td ft ³
Sulfur dioxide											_						- V				by vol
	Nitrogen oxides																				by vol
	monoxid	le									_	-	1								by vol
Total V	Total VOC (including those listed below)				000	0%			sh.	5.40		sle	1	sje -	U						by vol
Lead										BYZAW								-		- Color or -	by vol
Chloroprene					000	0%	00126-9	99-8	*	5.34		#		*	U						by vol
Toluene					000	0%	00108-8			0.05		10		*	U						by vol
Toluene																				ppm	by vol

							5	tate of l	Louisiar	ıa	d .			,			Date of	submitt	al
						Emissions	Inventory (Question	nnaire (I	EIQ) for Air	r Pollutants						Nov	20	013
Er	nission P	oint ID N	lo.		Descriptive	Name of the B	Emissions Source	e (Alt. Nar	me)	1	Ap	proximate Location	on of Stack or V	Vent (see	instruc	tions)			
		nation)																	_
	1700	0-5.5	1		Unst	ripped Emulsi	on Storage Tan	k No. 8		Method UTM Zon	e 15	06,"Address Mate	739000	mE	Ver	tical	Datum		mN
Tem	no Subie	ct Item II) No							Latitude	30 °	3		15		iicai .	332		redths
20111	po buoje		2110.							Longitude	The second secon	31	,	15					iredths
	EQT	0152					3												
	and Disc	-		eter (ft) or		Height of St		Gas Exit		Gas Flow at	Stack Gas Exit	Normal Opera		Date of			ercent o		and the same of
77.0	l Charac ge? (yes		Disc	harge Area	a (ft ²)	Above Grade	e (ft) Vel	ocity	- Constitution of the Cons	tions, not at	Temperature	Time		struction odification	1000000		ighput Emission		ALTERNATION OF THE PARTY OF THE
Chan	ge: (yes	or no)			-			5	Standa	ard (ft³/min)	(°F)	(hours per ye	rar) IVI	odificatio	"		Emissi	n Poin	
	no												Aug		1972	Jan-		Jul-Sep	
			V	IA ft		NA f	t NA	_ft/sec	NA		77 °F	8,760	hr/yr	1	12/2	Mar	Jun	0.50	Dec
			į.	ft ²	2								1		- 1	25%	25%	25%	25%
																			1
		T			ind Heat I	nput (see ins			1 -			Operating Par			ts)				
Fuel	-	-	The same of the sa	of Fuel		Heat II	nput (MMBTU/ NA	hr)	- I		Date/Throughout		Parame			L	escript	ion	
	h		1	NA	-		NA		1 1		g Rate/Throughput ting Rate/Throughp		35 MMgs 35 MMgs		-				-
	C					-					Volume/Cylinder L		14,950		_		- 1		
	-				Notes				-	Shell Height (ft)	volumer Cymnider L	rispiacement	20.75						
*Tan	k is vente	ed to a cor	nmon vent			Ision tanks, EIO	No. 1700-5. Ur	stripped	1 1	Tank Diameter (f	t)		12			-			-
53,8963	*Tank is vented to a common v				on Tanks Ve				I	Tanks:	Fixed Roof	Floating Ro		Exter	rnal		0	Int	ternal
					4				Ī	Date Engine Ord	ered		+	Engine l	Model Y	ear .			
											Built by Manufact	turer							
-								*	5	I Engines:	□ Rich Bı	urn 🗆	Lean Burn		2 Stro	ke		4 Stro	ke
	Emission Point ID No. (Design 1700-5.5				Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number		Prop	osed Emission l	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl Met	liance		ncentra Exiting		
Pollutant									erage o/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Med	1100				
_	Particulate matter (PM ₁₀)															-			std ft ³
-	Sulfur dioxide													-					by vol
-	Nitrogen oxides Carbon monoxide							-			-	-	-	-					by vol
	Carbon monoxide Total VOC (including those listed			law)	000	000		-	*	5.40	*	als .	1.	-					by vol
-	Total VOC (including those listed Lead			iow)	000	. 0%		-		5.40			U	-		_			by vol
Chloroprene					000	0%	00126-99-8	-	*	5.34	+	+	U	-		_			by vol
Toluene				_	000	0%	00128-98-3	+	*	0.05	*	*	U						by vol
Toluene								1			1	1	-	1					hy vol

NA ft NA ft/sec NA 77 °F 8,760 hr/yr Sept 2007 Mar Jun D						St	tate of Lo	ouisiana							Date of	submitta	al
					Emissions	Inventory Q	uestionn	aire (EIQ) for Air	Pollutants					Nov	20	13
	E		No.	Descriptiv	e Name of the l	Emissions Source	(Alt. Name)		App	proximate Locati	on of Stack or V	Vent (see insti	ructions)			
Latitude 3.0 3.1 1.5				Unst	ripped Emulsi	on Storage Tank	No. 10		The state of the state of		THE RESERVE OF THE PERSON NAMED IN	And the second lives to th				Section 2012 Contract	
Eq10133	Tem	ро Subject Item П	D No.						Latitude	30 °	3	1	15 "	Vertical	332	hundi	edths
Playded Characteristic Change? (yes or no) Playded Characteristic Change? (yes or no) NA	Lab.	EQT0153	*						Longitude	-90	31		15			nundi	edus
NA ft NA	Physica	al Characteristics		THE REAL PROPERTY AND ADDRESS OF THE PARTY AND			The state of the s	Conditions	, not at	Temperature	Time	Con	struction or		ughput	Through	This
Type of Fuel Used and Heat Input (see instructions) Heat Input (MMBTU/hr)		no	NA		NA f	n NA	ft/sec	NA			8,760	hr/yr Sept	200	Mar Mar	Jun		Oct- Dec 25%
Full																	
A	Fuel	Ty					,				Operating Par						-
Maximum Operating Rate/Throughput Design Capacity/Volume/Cylinder Displacement 16,000 gal Shell Height (ff) Design Capacity/Volume/Cylinder Displacement 16,000 gal Shell Height (ff) Shell Heig	ruei	a			Heat I	The second secon	r)	Norms	l Operating	Rate/Throughput				1	Jescript	ion	
**Tank is vented to a common vent for the unstripped emulsion Tanks Vented to a common vent for the unstripped emulsion tanks, EIQ No. 1700-5, Unstripped Emulsion Tanks Vented to a common vent for the unstripped emulsion tanks, EIQ No. 1700-5, Unstripped Emulsion Tanks Vented to a common vent for the unstripped emulsion tanks, EIQ No. 1700-5, Unstripped Emulsion Tanks Vente Emulsion Tanks Vente Emulsion Tanks Vente Emulsion Rule (This Proposed Engine Vans Built by Manufacture SI Engines: Rich Burn Lean Burn 2 Stroke 4 Stroke **Tank Diameter (F) Tanks Floating Roof Equipment Date Engine Vans Built by Manufacture Tanks		b	de 1 de					Maxin	num Operati	ng Rate/Throughpu		17.5 MM g	gal/yr				
*Tank is vented to a common vent for the unstripped emulsion tanks, EIQ No. 1700-5, Unstripped Emulsion Tanks Vent	-	<u></u>		Notes				The second secon	Name and Address of the Owner, where the Owner, which is	olume/Cynnder D	ispiacement		gai				
Final Fina	*Tan	ik is vented to a con	nmon vent fo		lsion tanks, EIQ	No. 1700-5, Unst	tripped		The state of the s)							
Emission Point ID No. (Designation) 1700-5.6 Pollutant Average (lb/hr) Suffry dioxide Suffy dioxide Suffry dioxide Suffry dioxide Suffry dioxide Suffry di											Floating Ro	of 🗆	External			Inte	ernal
Emission Point ID No. (Designation) 1700-5.6 Pollutant Average (lb/hr) Particulate matter (PM ₁₀) Sulfur dioxide Nitrogen oxides Carbon monoxide Total VOC (including those listed below) One of the proposed Emission Rate (SI Engines: Si Engines: Si Engines: Si Engines: Si Rich Burn							1	Date E	Engine Orde	red			Engine Mod	el Year			
Emission Point ID No. (Designation) 1700-5.6 Pollutant Average (lb/hr) Particulate matter (PM ₁₀) Sulfur dioxide Nitrogen oxides Carbon monoxide Total VOC (including those listed below) Control Equipment Code Proposed Emission Rates (Current) Annual (tons/yr) (tons/yr) Annual (tons/yr) Continuous Change, Delete, or Unchanged Continuous Compliance Method Particulate matter (PM ₁₀) Sulfur dioxide Nitrogen oxides Total VOC (including those listed below) Oncentration in Gase Exiting at Stack Total VOC (including those listed below) Proposed Emission Rates (Current) Annual (tons/yr) (tons/yr) Continuous Compliance Method Proposed Emission Rates Formitted Emission Rate (Current) Add, Change, Delete, or Unchanged Total VOC (including those listed below) Annual (tons/yr) Formitted Emission Rates (Current) Annual (tons/yr) Continuous Compliance Method Faxiting at Stack Formitted Emission Rates (Current) Continuous Continuous Compliance Method Formitted Emission Rates Formitted Emission Rates (Current) Continuous Compliance Method Faxiting at Stack Formitted Emission Rates (Current) Continuous Compliance Method Formitted Emission Rates (Current) Formitted Emission Rates (Current) Formitted Emission Rates Formitted Emission Rates (Current) Formitted Emission Rates Formitted Emission Rates (Current) Formitted Emission Rates Fo								The same of the last of the la	or with the last own sales and the last own sales are the last own sales and the last own sales are the last own s								
Equipment Code Equipment Code Efficiency CAS Number Proposed Emission Rates Emission Rate (Current) Change, Delete, or Unchanged Continuous Compliance Method Change, Delete, or Unchanged Continuous Compliance Method Continuous Continuous Compliance Method Continuous Continuous Continuo								SI En	gines:	□ Rich Bu		Lean Burn	□ 2S	troke	0	4 Strol	te
Average (lb/hr) Annual (tons/yr) Unchanged Particulate matter (PM ₁₀) Sulfur dioxide Nitrogen oxides Carbon monoxide Total VOC (including those listed below) 000 0% Annual (tons/yr) (tons/yr) (tons/yr) (tons/yr) (tons/yr) (tons/yr) (tons/yr) (tons/yr) Total VOC (including those listed below) 000 0% Annual (tons/yr) (tons/yr) (tons/yr) Total VOC (including those listed below) 000 0% Annual (tons/yr) (tons/yr) (tons/yr) Total VOC (including those listed below) 000 0%	Emi			Equipment	Equipment			Proposed 1	Emission R	ates	Emission Rate	Change,	Compliano	('0)			
Sulfur dioxide ppm by v Nitrogen oxides ppm by v Carbon monoxide ppm by v Total VOC (including those listed below) 000 0% * 5.40 * * U ppm by v	Polluta	int					9-				Unchanged	Method					
Sulfur dioxide ppm by v Nitrogen oxides ppm by v Carbon monoxide ppm by v Total VOC (including those listed below) 000 0% * 5.40 * * U ppm by v															gr/s	td ft ³	
Carbon monoxide ppm by variety of the control of th	-													-	ppm	by vol	
Total VOC (including those listed below) 000 0% * 5.40 * * U ppm by																	
Lead ppm by		OC (including thos	se listed belo	w) 000	0%		3ft		5.40	*	*	U		_		-	
														-			
The state of the s	Chloroprene																-
Toluene 000 0% 00108-88-3 * 0.05 * * U ppm by ppm b	Toluene			000	0%	00108-88-3	*		0.05	*	*	U		_			

						Sta	ate of Louisi	ana					U.		Date of	submitta	d
					Emissions	Inventory Qu	uestionnaire	(EIQ) for Ai	r Pollutants						Nov	20	13
Eı		oint ID N	lo.	Descriptive	Name of the I	Emissions Source	(Alt. Name)		Ap	proximate Locati	on of Stack or V	ent (see i	nstruc	tions)			
		0-5.7		Unstr	ripped Emulsio	on Storage Tank N	No. 13	Method		06,"Address Mate						NAD83	
Tem	po Subje	ct Item II	D No.					UTM Zor Latitude Longitude	30 °	Horizontal 3	i.	mE 15		tical .	332		mN edths redths
Ctasl	EQT	0154	Discorts	- (84) S41	W.1.14 664	- L C - L C	T-14 C4-	l C - Fl - 1	Start Car Fult	N1 O	tina I	D-46		P		£ A	ol.
Physica	l Charac ge? (yes	teristics		r (ft) or Stack rge Area (ft ²)	Height of St Above Grade		ity Cor	ck Gas Flow at nditions, <u>not</u> at ndard (ft³/min)	Stack Gas Exit Temperature (°F)	Normal Opera Time (hours per ye	Con	Date of struction odification	900117	Throu	ghput	f Annu Through n Point	This
	no		NA		NAf	nA	ft/sec N	IA	77 °F	8,760	hr/yr Sept		2007	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep	Oct- Dec 25%
	_			ft²					16								
		Ty		Used and Heat I						Operating Par			is)				
Fuel			Type of		Heat I	nput (MMBTU/hr)				Parame			D	escript	on	
	a		NA			. NA			g Rate/Throughput		17.5 MM g		-				
	0					- 3		17/	iting Rate/Throughp		17.5 MM g		_				
-	İc			Notes					/Volume/Cylinder D	Displacement	10,000 g	gai	-				
*Tor	k is vent	ed to a cor	mmon went for	Notes	laion tanka EIC	No. 1700 5 Heat	ripped	Shell Height (ft) Tank Diameter (11.5		-				
1 ai	K 15 VCIIII	ou to a cor		Emulsion Tanks Ve		2 140. 1700-5, Olist	ripped	Tanks:		Floating Ro		Exter	rna!			Inte	ernal
	*Tank is vented to a common vent for						1	Date Engine Ord		1 loading No	<u> </u>	Engine N		/ear		1111	
							1		s Built by Manufact	urer		Longino I	10001	CILI			
							-	SI Engines:	□ Rich Bu		Lean Burn		2 Stro	ke		4 Strol	ce
Emission Point ID No. (Designation 1700-5.7				Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Pr	oposed Emission		Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl Meti	iance			ion in C	
Pollutant							Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Med	nou .				
Particulate matter (PM ₁₀)					-												atd ft ³
Sulfur dioxide				× 1				-			-	-					by vol
-	Nitrogen oxides Carbon monoxide								-	-	-	-					by vol
-				200	0.00			0.00		*		-		_			by vol
Total VOC (including those listed below			se listed below	000	0%		*	2:33	*	-	U	-		_		_	by vol
Chloroprene				000	0%	00126-99-8	101	2.31	*	*	Ü	-			,		by vol
Chloroprene Toluene				000	0%	00126-99-8	*	0.02	*	*	U	-				-	by vol
Toluene				000	070	00100-00-3		0.02	1		-						by vol

						St	ate of L	ouisiana						-		Date of	submittal	
					Emissions	Inventory Q	uestion	naire (El	(Q) for Ai	r Pollutants					*	Nov .	201	3
E		Point ID N	lo.	Descriptive	Name of the	Emissions Source	(Alt. Nam	e)	1	Ap	proximate Locati	on of Stack or	Vent (see	instruct	tions)			
		0-5.8		Unst	ripped Emulsi	on Storage Tank	No. 14		Method		06,"Address Mat	ching-Primary	Name"			Datum	NAD83	
									UTM Zon			739000	mE_	Vert	ical	3327		nN
Tem	po Subje	ct Item II	No.						Latitude	30 °			15				hundre	2000
	EQT	T0155							Longitude	-90°	31		15	."	-		hundre	dths
	and Dise	The second second		r (ft) or Stack ge Area (ft ²)	Height of St Above Grade	the state of the s	The second second		ns Flow at	Stack Gas Exit Temperature	Normal Opera		Date of	or			f Annual Through	
The state of the s	nge? (yes	ACCOUNTS AND ADDRESS OF THE PARTY OF THE PAR	Dischar	ge Area (IL)	TADOTO GRAGO	(11)			d (ft³/min)	(°F)	(hours per y	1	Aodification 1				n Point	
	no	Ì										. Sept	1	2007	Jan-		Jul-Sep	Oct-
		- 1	NA	ft .	NA f	ft NA	ft/sec	NA		77 °F	8,760	hr/yr	1	1200	Mar 25%	Jun 25%	25%	Dec 25%
				ft²											23%	2370	2370	2370
	1	Ту	pe of Fuel	Used and Heat I	nput (see ins	structions)					Operating Par	ameters (inc	lude uni	ts)			a company of	
Fuel			Type of	Fuel	Heat I	nput (MMBTU/h	r)					Param	eter		D	escript	on	
	a		NA			NA		No	mal Operating	g Rate/Throughput		17.5 MM	gal/yr					-
	b		411.0				, y	Ma	ximum Opera	ting Rate/Throughp	out	17.5 MM	gal/yr	-	W FE	TO AMILIO		AND THE
pto.	c							-		Volume/Cylinder D	Displacement	10,000	gal					
				Notes				She	ell Height (ft)			17						
*Tar	ik is vente	ed to a con		the unstripped emu		Q No. 1700-5, Unst	tripped	Tar	nk Diameter (f			11.						
				Emulsion Tanks Ve	nt		- 1	_	nks:		Floating Ro	oof \square	Exte				Inter	nal
							- 1		te Engine Ord				Engine	Model Y	ear			
							- 1	The second second	The state of the s	Built by Manufact		1						
	Emission Point ID No. (Designation)							SI	Engines:	□ Rich Bu		Lean Burn		2 Strol	ke		4 Stroke	
Em	ission Po	1700-5.8		n) Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number		Propos	ed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Conti	liance			ion in Ga at Stack	ises
Polluta	Pollutant						Aver:	_	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	noa				
-	articulate matter (PM ₁₀)																gr/sto	i ft³
																	ppm b	
	en oxides			THE RESERVE OF THE PERSON OF T		The state of the s			A STATE OF THE STA								ppm b	
-	monoxid																ppm b	
-	OC (incl	uding thos	e listed below	000	0%		*		2.33	*	*	U					ppm b	
Lead													-				ppm b	
Chloroprene				000	0%	00126-99-8	*		2.31	*	*	U	-				ppm b	
Toluene				000	0%	00108-88-3	*	_	0.02	-	*	U	-				ppm b	
Totalic											1	1					phin o	1 101

_	-																			
								State of	Louisia	ana			11					Date of	submitt	al
						Emissions	Inventory	Question	naire	(EIQ) for	Air	Pollutants						Nov	20	013
							•												20	r a al
E	mission P	oint ID N	0.		Descriptive	Name of the	Emissions Sou	rce (Alt. Na	me)			Ap	proximate Locati	on of Stack or	Vent (see	instruc	tions)			
	(Design	nation)								1			•							
	1700	0-5A			No.	6 Emulsion S	torage Tank I	Ianhole		Metho	210		06,"Address Mate						NAD8	_
OT:											Zone	30 °		739000	mE		tical	.332	7400	mN
Lem	po Subje	ct Item II) No.							Latitu	-	-90 °	3		15	-	39			redths
	EQT	0167								Longi	itude_	-90	31	-	13	2			nunc	redths
Stack	and Disc		Diame	ter (ft)	or Stack	Height of St	ack Stac	k Gas Exit	Stac	k Gas Flow a	t	Stack Gas Exit	Normal Opera	ating	Date of		P	ercent	of Annu	al
Physica	d Charac	teristics	Disch	arge Ar	ea (ft²)	Above Grad		elocity	Con	ditions, not a	t	Temperature	Time	Co	nstruction	n or	Throu	ighput	Throug	h This
Char	ige? (yes	or no)							Stan	dard (ft³/min	1)	(°F)	(hours per ye	ear) N	lodification	on		Emissi	on Poin	t
ľ		1			1		1		1		-)	-]	1	1	1	Jan-	Apr-	Jul-Sep	Oct-
	no	1		1.33 1	ft	53.8 1	ft 81	3.30 ft/sec	7,4	00 ft^3/n	min	77 °F	8,760	hr/yr Jul	1	1968	Mar	Jun	Jul Oc,	Dec
		1	-											- 1	,	'	25%	25%	25%	25%
			_	1	ft ²															
	T	Ту	pe of Fu	el Used	and Heat I	nput (see in	structions)			*			Operating Par	ameters (inc	lude uni	its)				
Fuel			Туре	of Fuel		Heat I	nput (MMBT	U/hr)]					Param	eter		D	escript	ion	
	a		1	NA .			NA			Normal Oper	rating	Rate/Throughput		42,000 lb/d	charges					
	b									Maximum O	perati	ng Rate/Throughp	out	NA					-	
	С							-	1	The same of the sa		olume/Cylinder D	Displacement	NA						
					Notes				1	Shell Height	(ft)			NA		-				
*Blov	ver opeati	ng time. I	Emission ra	ites vary	the same of the sa	on manhole ope	ening, samplin	g, and other	1	Tank Diamet				NA				-		14
					activities.					Tanks:		Fixed Roof	Floating Ro	oof 🗆		ernal			In	ernal
1]	Date Engine					Engine	Model '	Year			
												Built by Manufact		<u> </u>					15:	
F-										SI Engines:		□ Rich Bu		Lean Burn		2 Stro	ke		4 Stro	ke
Em	ission Po	int ID No.	. (Designat	ion)	Control Equipment	Control Equipment	HAP / TA						Permitted Emission Rate	4.33			(a)			
	1700-5A				Code	Efficiency	CAS Numb	er	Pro	oposed Emissi	ion R	ates	(Current)	Add, Change,		nuous	Cor	centra	tion in	Cases
1700-5A														Delete, or		oliance	1000		at Sta	The second second
Polluta	Pollutant							Ave	erage	Maximu	m	Annual	Annual	Unchanged	Mei	thod				
								(lt	o/hr)	(lbs/hr))	(tons/yr)	(tons/yr)							
	Particulate matter (PM ₁₀)																			std ft ³
	Sulfur dioxide Nitrogen oxides												,						-	by vol
														-	-	-				by vol
_	monoxid		a Mate 4 to 3		000	000			. 50	0.75		210	2.10		-		-			by vol
Lead	OC (incl	uding thos	e listed bel	ow)	000	0%		- 0).50	0.76		2.19	2.19	U	-		-		-	by vol
	Chloroprene				000	0%	00126-99-	8).34	0.52	_	1.49	1.49	U	+		-			by vol
Toluene					000	0%	00128-99-		0.05	0.32		0.23	0.23	U	-		-	-		by vol
7070011					000	070	00100-00-	-		0.00		0.23	0.23	-	-		_		-	by vol

						St	ate of L	ouisiana								Date of	submitt	al
					Emissions	Inventory Q	uestion	naire (EIC) for Air	r Pollutants						Nov	20)13
E		Point ID N gnation)	lo.	Descriptive	Name of the	Emissions Source	(Alt. Name	e)		Ap	proximate Locati	on of Stack or V	ent (see	instruc	tions)		20	
		00-13	4.	Pol	Kettles Manho	oles/Strainers (1 ar	nd 2)		Method UTM Zon	e 15	06,"Address Mat Horizontal		mE	Ver			NAD83	mN
Tem	1 10	ect Item II	No.						Latitude Longitude	30 °	3		15 15	"	-		hund	redths redths
Physica	and Dis	cteristics		ft) or Stack Area (ft ²)	Height of St Above Grad			Stack Gas Condition Standard	s, not at	Stack Gas Exit Temperature	Normal Opera Time (hours per ye	Cons	Date of struction odification		Throu	ghput '	f Annu Throug n Point	h This
	no	-	1	33 ft	58.2	ft 82.40	ft/sec	6,900	_ft^3/min	77_°F	8,760	hr/yr		1970	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep	Oct- Dec 25%
	т	Т,	no of Evol II	ft² sed and Heat I	nout (see Inc	tmustions)	_				Operating Par	ameters (inch	ıde uni	te)				
Fuel	-	I Iy	Type of F			aput (MMBTU/hr)				Operating Far	Paramet		I	D	escript	on	
	а		NA		220412	NA		Norm	al Operating	Rate/Throughput		82,000 lb						
	b		A STATE OF THE STA					Maxi	mum Operat	ing Rate/Throughp	out	NA						
7	c							Desig	n Capacity/	Volume/Cylinder D	Displacement	NA						
				Notes				Shell	Height (ft)		V	NA						
*Blov	ver opea	ting time.	Emission rates v	The state of the s	on manhole ope	ening, sampling, and	d other	Tank	Diameter (f	t)		NA						
				activities.				Tank	s: 🗆	Fixed Roof	Floating Ro	of 🗆	Exte	-		. 0	Int	ernal
									Engine Orde				Engine	Model Y	ear			
							- 1			Built by Manufact								
								SI E	igines:	□ Rich Bu		Lean Burn		2 Stro	ke		4 Strol	ke.
Em	Emission Point ID No. (Designation) 1700-13			Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number		Proposed	Emission F	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Conti	liance	2777777		ion in (at Stac	Service Control
Polluta	Pollutant						Avera	-6-	laximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	nod				
Particu	articulate matter (PM ₁₀)																gr/s	std ft ³
Sulfur	ulfur dioxide																ppm	by vol
-	trogen oxides								- W. T.								ppm	by vol
	arbon monoxide otal VOC (including those listed below)																THE OWNER OF THE OWNER, WHEN	by vol
	otal VOC (including those listed below)			000	0%		. 1.80	6	2.18	8.15	8.15	U						by vol
Lead	ead Chloroprene						/											by vol
				000	0%	00126-99-8	1.3		1.56	5.82	5.82	U						by vol
Toluene				000	0%	00108-88-3	0.18	8	0.21	0.79	0.79	U					-	by vol
																	ppm	by vol

-																				
							St	ate of I	ouisian	ıa								Date of	submitt	al
						Emissions	Inventory Q	uestion	naire (I	EIO) for A	r Pollut	ants						Nov	20	013
																		Nov	20	713
77	test P	afast ID N			D 1.1	N. 6.1														
E	(Design	oint ID N	0.		Descriptive	Name of the	Emissions Source	(Alt. Nam	1e)			App	proximate Location	on of Stack or	Vent (see	instruc	tions)			
	1700				Pol K	ettles Manhol	es/Strainers (3, 4	and 5)		Method			06,"Address Mate	ching-Primary N	Vame"			Datum	NAD8	3
		0.7.7.17	- 1							UTM Zo	ne	15	Horizontal	739000	mE	Ver	tical		7400	mN
Tem	oo Subje	ct Item ID	No.							Latitude	30		3		15	-			hund	redths
	-						У.			Longitud	e	0	31	*	15				hund	redths
Ctarl		0136	D'	(64)	St. I	TT 1 1 . 6 C	1 6 16	7 1. 1	St. 1		I 6: 1 6	F 4	N 10						6.1	,
	and Disc l Charac				or Stack	Height of St Above Grade		AND DESCRIPTION OF THE PARTY OF	A CONTRACTOR OF THE CONTRACTOR	Gas Flow at	Stack G		Normal Opera Time		Date of nstruction			ercent (WWW.
255.6	ge? (yes		Discl	harge Ar	rea (ft*)	Above Grade	e (ft) Veloc	aty		tions, <u>not</u> at ard (ft ³ /min)	Temper		(hours per ye		lodificatio			igaput Emissic	-	Control of the Control
						¥.			Gianda	ard (it /min)	1	1	Par Ju		1					
	no					F 444 174		.								1970	Jan-	Apr-	Jul-Sep	1
			_	2	it	59 1	ft 45.10	ft/sec	8,500)ft^3/min	77	°F	8,760	hr/yr	1		Mar 25%	Jun 25%	25%	Dec 25%
					ft ²	iv.	1							1			2370	2370	2370	2370
		T					4 41 >						O (1 P		1 1 .	4.5				
Fuel	-	1 9			and Heat I	nput (see ins		×					Operating Par			ts)				
r uei	3			of Fuel		Heat I	nput (MMBTU/hi NA	()	N	Normal Operation	a Date/Thr	oughnut		82,000 l		-		escript	on	
	b			11/1			HA			Maximum Oper			nut .	NA		_				
	С				-					Design Capacity	The state of the s	-		. NA		1				
		-			Notes					hell Height (ft)		Januar D	портисотноги	NA			-			
*Blov	er opeati	ng time. E	Emission ra	ates vary		on manhole ope	ening, sampling, an	d other		ank Diameter				NA						
					activities.				-	Tanks:		Roof	Floating Ro	of 🗆	Exte	rnal			Int	ernal
								- 1	E	Date Engine Or	dered				Engine l	Model ?	(ear			
									I	Date Engine Wa	s Built by N	/lanufact	urer							
									S	I Engines:		Rich Bu	ırn 🗆	Lean Burn		2 Stro	ke		4 Stro	ke
Emi	ssion Poi	nt ID No.	(Designa	tion)	Control	Control	HAP/TAP						Permitted						×	
		1700-13 <i>A</i>			Equipment Code	Equipment Efficiency	CAS Number		Prop	osed Emission	Rates		Emission Rate	Add,	Conti	nuous		-		
		1700-157			Code	Efficiency							(Current)	Change, Delete, or	Comp	liance	10000000	central Exiting		
Polluta	nt				4		1	Aver	rage	Maximum	Ann	nual	Annual	Unchanged	Met	hod		E-Munic	at Diac	
								(lb/		(lbs/hr)	(tons	s/yr)	(tons/yr)							
	ate matte	r (PM ₁₀)	3																gr/	std ft ³
Sulfur	-																			by vol
-	n oxides										-				-					by vol
	monoxid		- Hate II	1	000	000			20	0.40	- 10	0.4	1664							by vol
Lead V	OC (incli	iding those	e usted bel	iow)	000	0%		2.2	29	2.68	10.	.04	10.04	U	-				-	by vol
Chlorop	rene				000	0%	00126-99-8	1.6	64	1.92	7.	17	7.17	Ú	-				THE RESERVE OF THE PERSON NAMED IN	by vol
Toluene					000	0%	00120-99-6	0.2		0.26	0.9		0.98	Ü						by vol
					550	0.70	00100-00-3	0.2	-	0.20	0.	, ,	0.50	-	-					by vol

		100				5	State of Lo	uisiana							1	Date of	submitte	al
					Emissions	Inventory (Questionn	aire (EIC	() for Ai	r Pollutants	S					Nov	20	13
E		Point ID N	0.	Descriptive	Name of the	Emissions Source	ce (Alt. Name))	Г		Approximate Loca	tion of Stack or	Vent (see	instruc	tions)			3
)-14B.3		Stabil	izer and Catal	yst Tanks Manh	nole Vent		Method			atching-Primary 1 739000	Name" mE	Ver		Datum 3327	NAD83	mN
Tem		ect Item II	No.						UTM Zon Latitude Longitude	30 °		3,	15 15	и	iicai -	3321	hundi hundi	edths
	and Dis	P0013 scharge scteristics		er (ft) or Stack arge Area (ft²)	Height of St Above Grad	The state of the s	Gas Exit	Stack Gas Condition		Stack Gas Ex	The state of the s		Date of	l or			f Annu	The second second
	ige? (yes	Charles and the Control of the Contr	Discha	arge Area (II)	Above Grau	e (it) Year	ocity	Standard (1	(°F)	(hours per		lodification				n Point	
	no	-	NA	ft ft²	NA I	ft NA	ft/sec	NA	_ft^3/min	NA°F	8,760	_hr/yr Oct		1975	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
	1	Tv	ne of Fuel	Used and Heat I	nnut (see in	etructions)					Operating Po	rameters (inc	lude uni	te)				
Fuel		1	Туре о			nput (MMBTU/	hr)				Operating 12	Parame		1	D	escripti	on	
	a		N/			NA		Norm	al Operating	Rate/Through	put	3,000 16/	batch			in the same	L.	
	b							Maxi	mum Opera	ing Rate/Throu	ghput	NA						7 - 1
2	С							Desig	n Capacity/	Volume/Cylinde	er Displacement	NA						
				Notes				Shell	Height (ft)			NA						
	9	*Common	n vent for El	Q Nos. 1700-14B.1,	1700-14B.3. *	* 89 hr/yr.		Tank	Diameter (f	t) .		NA						
								Tank		Fixed Roof	Floating F	oof 🗆	Exte	rnal			Inte	ernal
							1		Engine Ord				Engine l	Model Y	ear			
						2)	1	The state of the s	THE RESERVE OF THE PERSON NAMED IN	Built by Manuf								
								SI Er	igines:	Rich	Burn 🗆	Lean Burn		2 Stro	ke		4 Strol	te
Em	ission Po	1700-14B	(Designation)	Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number		Proposed	Emission I	lates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin	liance	1000000000		ion in G	
Polluta							Averag	, -	(aximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	nod				
THE REAL PROPERTY AND ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY ADDRESS OF THE PERTY		er (PM ₁₀)					1.5**		9.10	0.067**	0.10**	С					gr/s	td ft ³
Sulfur																	ppm	by vol
-	n oxides					14												by vol
	monoxid		14 10 10 10 10 10															by vol
	OC (inc	uding those	e listed belov	w) 000	0%		0.11		0.60	0.50	0.72	C						by vol
Lead				200		2010				-			-			×		by vol
Chloro				000	0%	00126-99-8	0.08		0.09	0.37	0.37	U						by vol
Toluen	-			000	0%	00108-88-3	0.03	-	0.49	0.12	0.12	С	-					by vol
												and the same of th					Philli	01 101

					(4)	Sta	ate of Lo	uisiana							I	Date of	submitt	al
					Emissions	Inventory Qu	uestionna	aire (EI(() for Air	Pollutants					I	Nov	20	13
Ei		oint ID N	lo.	Descriptiv	ve Name of the	Emissions Source	(Alt. Name)			Ap	proximate Locati	on of Stack or V	ent (see i	instructi	ons)			
)-14B	1	Solu	ition Make up I	Manhole Common	Vent		Method			ching-Primary Na					NAD83	
Tem	no Subie	ct Item II) No						UTM Zone Latitude	e 15	Horizontal 3		mE 15	Vertice	cal _	3327		mN redths
	poodoje		71.0.						Longitude		31	-	15		_			redths
Ct 1	-	20006	- Di	(6) 5: 1	I = 11. 25	1 7 7 7					1 30 10				-			
Physica	and Disc l Charac ge? (yes	teristics		er (ft) or Stack arge Area (ft ²)	Height of St Above Grade			Stack Gas Condition Standard	s, <u>not</u> at	Stack Gas Exit Temperature (°F)	Normal Oper Time (hours per ye	Cons	Date of struction odification		Throu	ghput '	f Annu Throug n Point	h This
	no		_	1.5 ft	57	ft 104.70	ft/sec	11,100	_ft^3/min	77 °F	8,760	_hr/yr		9	Jan- Mar	Jun	Jul-Sep	Dec
	:81		_	ft²				§							25%	25%	25%	25%
		Ty	_	l Used and Heat							Operating Par			ts)				
Fuel			Туре		Heat I	nput (MMBTU/hr	7)	-				Paramet			D	escript	on	
	a		N	Α	-	NA			17.1	Rate/Throughput		3,000 lb/ba	atch					
ĺ	0				-				-	ing Rate/Through		NA NA						
-	C			Notes				-	Height (ft)	Volume/Cylinder I	Displacement	NA NA						
				Tyotes	-11				Diameter (f			NA NA						
							1	Tank		Fixed Roof	Floating Ro		Exter	rnal	-		Int	ernal
									Engine Orde		1		Engine I		ar			
										Built by Manufac	turer							
									ngines:	□ Rich B		Lean Burn		2 Strok	e		4 Stro	ke
3		int ID No 1700-14	. (Designati B	on) Control Equipment Code	Control Equipment Efficiency	HAP/TAP CAS Number		Proposed	l Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl Met	liance			ion in (
Polluta							Averag (lb/hr	9"	laximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr-)	Unchanged	Met	100				
	ate matte	er (PM ₁₀)		000	0%		1.47		9.10	0.07	0.00	A						std ft ³
Sulfur																	THE OWNER OF TAXABLE PARTY.	by vol
	n oxides											-	-					by vol
-	monoxid		n listed hala) 000	0.0%		0.12	_	0.60	0.56	0.00	-	-	_				by vol
Lead	OC (Incli	uding thos	se listed belo	(w) 000	0%		0.13		0.60	0.56	0.09	С	-	_				by vol
Chloro	orene			000	0%		0.084		0.09	0.37	0	A	-	-				by vol
Toluen				000	0%		0.084		0.09	0.12	0	A	-	-	_	_		by vol
							0.05	_		1		1	1					by vol

					The second second second				CARPOTE S	ALCOHOLD WATER	THE RESIDENCE OF STREET	CALL OF STREET	State of the last							
*	7	4	and deve	i Lacked in Lake																
						St	ate of L	ouisiana			41 V 1		4 - 1 - 25-	California de la compansión de la compan				Date of	submitta	al
										~	21									
					Emissions	Inventory Q	uestionn	aire (EIC) for Ai	r Pollu	tants							Nov	20	13
Er		oint ID No).	Descripti	ve Name of the	Emissions Source	(Alt. Name	*)	T		Ap	proximate	Location	on of Stack or	Vent (see	instruc	tions)			
		nation) -14B.1							Mathed			06 " A -1 -1-	an Mate	shin - Drimann N	Iama"			Datum	NAD83	
	1700	-14B.1			Acetic Acid	l Make Up Tank			Method UTM Zon		15			ching-Primary N 739000	mE	Ver	tical		Married Woman or Williams	mN
Temi	oo Subie	ct Item ID	No.						Latitude	30		. 11011201	3		15		licai	332		redths
			2,583						Longitude		_	-	31	•	15					redths
	EQT	0137	1								- 3	_		•						
Stack	and Dis	charge	Diamet	ter (ft) or Stack	Height of S	tack Stack Ga	s Exit	Stack Gas	Flow.at	Stack (Gas Exit	Normal	Opera	ting	Date of		P	ercent	f Annu	al
		cteristics	Disch	arge Area (ft²)	Above Grad	e (ft) Veloc	ity	Condition	s, not at	Tempe	erature		Time	177.	struction	or	Throu	ighput	Through	n This
Chan	ge? (yes	or no)						Standard (ft ³ /min)	(°	F)	(hours	per ye	ar) M	odification	on		Emissi	n Point	£
															Ī.		¥	A	1.10.	T 0 **
	no		NA	. ft	NIA	ft NA	ft/sec	NIA	ft^3/min	NIA	°F	8,76	0	hu/ser		1 1	Jan- Mar	Apr- Jun	Jul-Sep	Oct- Dec
			111	10	NA	ft NA	lusec	NA	_1t.3/1mn	NA	- F	6,70	0	hr/yr	1		25%	25%	25%	25%
		1		ft ²													2570	2570	2570	25.10
			e 77																	
		Lyl		Used and Heat	_							Operation	ig Par	ameters (incl		its)		-		-
Fuel			Type		Heat I	nput (MMBTU/hi	-)							Parame	-	-	L	escript	ion	
	a		N	A	-	NA			al Operating		270 -			3,000 1b/b		-	-	-		100
	D	-							mum Operat					134,173	-	-				
	С								n Capacity/	Volume/C	Cylinder D	isplacemen	it	1,590 g		-				-
				Notes					Height (ft)					10.83		-				
	*Thi	s tank is ve	nted to a co	ommon vent, EQI No	. 1700-14B, Ac	etic Acid Tanks.		Tank	Diameter (f					NA						
	19.							Tank			d Roof	Float	ting Roo	of 🗆	Exte			Π.	Inte	ernal
							- 1		Engine Ord					10	Engine	Model)	Year			
								Date	Engine Was	Built by	Manufact	urer								
								SI E	igines:		Rich Bu	ırn		Lean Burn		2 Stro	ke		4 Strol	ke
Emi	ssion Po	int ID No.	(Designati		Control	HAP/TAP		II.				Permit								
		1700-14B.	1	Equipmen		CAS Number		Proposed	Emission I	Rates		Emission		Add,	Conti	nuous				
		1700-140.	1	Code	Efficiency			1 m 1 m 1 m 1 m 1 m 1 m 1 m 1 m 1 m 1 m				(Curre	ent)	Change,		liance	100000000000000000000000000000000000000		tion in G	
Polluta	nt					a de				1	1	A	1	Delete, or Unchanged		thod		Exiting	at Stack	ic
· Onula	ii.			1	1		Avera (lb/h	0	laximum (lbs/hr)		mual ns/yr)	Annu (tons/		Unchanged	1 '					
Particul	ate matte	r (PM ₁₀)					(10/11)	1)	(AND STARK)	(20)	J.	(collar	34)		-					std ft ³
Sulfur d		(* 1,10)								-			-	 	-					by vol
	noxides									-					-					by vol
	monoxid	e								-					1					by vol
		uding those	listed help	w) 000	0%		. 1		2.79	-	sje -	10		Ü	-					by vol
Lead	o (me)	- July mose) 000	070				2.17	-		-		0	+					by vol
Chlorop	rene			000	0%		*		0.09		*	-		A	-		_			by vol
Toluene				000	0%		*		0.50	+	sk	-		A	-		_	-		by vol
					370				0.00	+		+		/1	+		1			by vol
																			DUIL	

			9					State	of Louisi	ana								Date of	submitt	al
						Emissions	Invento	ry Quest	ionnaire	(EIQ) fo	r Air	Pollutants					1	Nov	20	013
To		afait TD N			D1-11	Ni	2-1-1	211						-654	4 /					
E		oint ID N nation)	0.		Descriptive	Name of the I	emissions S	ource (Alt.	Name)			App	proximate Location	on of Stack or V	ent (see i	nstruci	nons)			
		-14B.2		`		Acetic Acid	Hold Up T	ank		Met	thod		06,"Address Mato	hing-Primary Na	ıme"		1	Datum	NAD83	3
	-,,30										M Zone	15	and the same of th		mE	Vert			400	mN
Tem	po Subje	ct Item II	No.								itude	30 °	3		15					redths
			1							Lon	ngitude	-90 °	31	٠.	15	70		1	hund	redths
C.		0138			6 1	**	1 5	10 =		10		5. 1.5. = . 1				-				
	and Disc I Charac			eter (ft) o		Height of St	CHOSTING DAVING	ack Gas Exi	ent.	k Gas Flow	7.020	Stack Gas Exit	Normal Opera		Date of truction			ercent o		A STATE OF THE STA
	ge? (yes		Disc	harge Ar	ea (ft*)	Above Grade	(It)	Velocity		nditions, <u>not</u> ndard (ft³/m		Temperature (°F)	Time (hours per ye		dification			ghput Emission	-	
	9	/							Stan	ioaro (it /m	un)	(F)	(nours per je		- Inches			- IIII		
	no																Jan-		Jul-Sep	20000000
		.	V	IA	ft 1	NA f	t NA	ft/sec	N	A ft^3	3/min	NA°F	8,760	hr/yr	1		Mar	Jun	0.500	Dec
					ft²												25%	25%	25%	25%
		Ту			and Heat I	nput (see ins							Operating Par			s)				
Fuel				of Fuel		Heat I	nput (MMI	BTU/hr)						Paramet	-		D	escript	on	
	a			NA		1	NA		_			Rate/Throughput		3,000 lb/ba						
	D								_			ng Rate/Throughp	1771	481,601 g	-	-				
-	С		٠.		27.							olume/Cylinder D	isplacement	600 gal						
	stern *				Notes	1700 140 4	de Acido	-1	_	Shell Heigh				5.83						
11	" I hi	s tank is ve	ented to a	common	vent, EQI No.	1700-14B, Ace	euc Acid Ta	nks,		Tank Dian			El alas	4.25	For	1				
										Tanks:	2	Fixed Roof	Floating Roo	of 🗆	Exter		7		Int	ernal
7										Date Engir					Engine N	viodel Y	еаг			
							×			SI Engine		Built by Manufact Rich Bu		Lean Burn		2 Stro	ke		4 Stro	ke
Em	ecion Po	int ID No	. (Designa	tion) I	Control	Control	HAP/T	AP		131 Eligine	.3.	U KICII DU	Permitted	-Jean Duin		20110	ive.		1000	
Ein	andii k U	111 110	. (Designa	LIJU)	Equipment	Equipment	CAS Nur	25 1 1 1 1 2 1					Emission Rate	Add,						
		1700-14B	.2		Code	Efficiency			Pr	oposed Emi	ission R	ates	(Current)	Change,	Contin	100000000000000000000000000000000000000	Con	centrat	ion in (Gases
														Delete, or	Compl Meth			Exiting		
Polluta	nt					2.			Average	Maxim		Annual	Annual	Unchanged	Meti	ivu				
									(lb/hr)	(lbs/h	hr)	(tons/yr)	(tons/yr)							
-	ate matte	er (PM ₁₀)																		std ft ³
Sulfur										-										by vol
-	n oxides monoxid	la .								+										by vol
			e listed be	low)	000	0%		-	ajs	0.40	6	*	aje	U						by vol
Lead	oc (mer	doing tilos	e nated be	10 W)	000	070				0,40	U			0			-			by vol
Chloro	orene				000	0%		_	*	0.09	9	*		A		-				by vol
Toluen					000	0%		_	*	0.50		*		A						by vol
-								_		1	_									by vol

		7				Sta	ate of Louisia	na						Da	te of s	ubmitta	l l
					Emissions	Inventory Qu	uestionnaire	(EIQ) for Ai	r Pollutants					No	v	201	13
E		Point ID N gnation)	lo.	Descriptive	Name of the E	Emissions Source ((Alt. Name)		Ap	proximate Locati	on of Stack or V	Vent (see in	structio				
	170	00-20			CD Refinir	ng Column Jet		Method UTM Zon	e 15	06,"Address Mat Horizontal	ching-Primary N 739000	ame" mE	Vertic		3327	NAD83 400	mN
Tem		ect Item II	No.					Latitude Longitude	30 °		1	15 "		=	_	hundr	
Physica	and Dis	charge cteristics		er (ft) or Stack arge Area (ft²)	Height of Sta Above Grade	The second secon	ty Cond	k Gas Flow at ditions, <u>not</u> at dard (ft ³ /min)	Stack Gas Exit Temperature ("F)	Normal Opera Time (hours per ye	Con	Date of estruction of odification		Through	put T	f Annua hrough n Point	Company of the Company
	no	-	_	0.167 ft	63.5 ft	3.50	ft/sec 5	ft^3/min	65 °F	8,760	hr/yr		1970	Mar .	Apr- Jun 5%	Jul-Sep 25%	Oct- Dec 25%
		Ty	ne of Fuel	Used and Heat I	nnut (see ins	tructions)		<u> </u>		Operating Par	ameters (incl	ude units				-	
Fuel		1	Type of		_	put (MMBTU/hr)			Operating rai	Paramet		,	Des	cripti	on	
	a b		N/	Α		NA		Maximum Opera	g Rate/Throughput ting Rate/Throughp		17,000 lb NA	o/hr .					-1.00,00
	Ic			Notes				Design Capacity/ Shell Height (ft)	Volume/Cylinder D	Displacement	NA NA						
								Tank Diameter (f	fixed Roof	Floating Ro	NA iof	Extern	nal		П	Inte	rnal
								Date Engine Ord		1 loading Ro	101	Engine M	2000		Ц.	into	
_									Built by Manufact		Lean Burn		2 Stroke		П	4 Strok	e
Em	Emission Point ID No. (Designation) 1700-20			Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number		posed Emission I		Permitted Emission Rate (Current)	Add, Change, Delete, or	Continu Complia	ance		ntrati	on in G	
Polluta	nt	1		-			Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Metho	od				
		er (PM ₁₀)															td ft ³
Sulfur											-						by vol
-	n oxides monoxid	la		000	0%		0.75	0.83	3.30	3.30	U	-					by vol
-			e listed belov	w) 000	0%		2.83	3.11	12.40	12.40	Ü		-	_			by vol
Lead	oc (mei	using thos	o nated belot	000	070		2.03	5.11	12.40	12.40	0		-				by vol
Chloro	orene			045	95%	00126-99-8	2.83	3.11	12.4	12.4	U	1	_	7			by vol
Toluen				000	0%	00108-88-3	<0.01	<0.01	< 0.01	<0.01	U		-				by vol
Ammor	nia			000	0%	07664-41-7	< 0.01	< 0.01	< 0.01	< 0.01	U					ppm	by vol

							S	tate of Lou	uisiana									Date of	submitt	al
						Emissions	Inventory ()uestionna	ire (EI	Q) for Air	Pollutants	s						Nov	20	13
			16								Al .				110					
E		oint ID N	lo.		Descriptive	Name of the l	Emissions Source	e (Alt. Name)				Approximate	Locatio	on of Stack or V	Vent (see	instruc	tions)			
		nation) 0-20A				CD D-C-l C	Salaman Tot (Sala	>		Method		06 "Addre	es Mato	hing-Primary N	ame"			Datum	NADR	
	1700	J-20A				CD Relining C	Column Jet (Spa	re)		UTM Zone		15 Horizon		739000	mE	Ver	tical		7400	mN
Tem	po Subje	ct Item II	No.							Latitude	30 °		3		15	"				redths
										Longitude	-90 °		31	ŧ.	15	11			hund	redths
		0140																		
	and Disc			neter (ft)		Height of St				s Flow at	Stack Gas E	. 1	7		Date of			ercent		
	d Charac ige? (yes		Disc	charge A	rea (ft²)	Above Grade	e (ft) Velo	eity		ns, not at	Temperatur	2000	Time	- 42.00	struction odification	77.55.55.3		ighput Emissic		h This
Citat	ige: (yes	or no)			1				Standard	l (ft³/min)	(°F)	(nours	per ye	ar) M	odificatio	'n		Emissi	n rom	L
	no	- 1			_		7	- 1								1970	Jan-	Apr-	Jul-Sep	Oct-
	110			0.167	ft	63.4 f	t 3.5	0 ft/sec	5	ft^3/min	65 °F	Spare	е	hr/yr	l	1970	Mar	Jun		Dec
					ft ²												25%	25%	25%	25%
Lance of		Ту			l and Heat I				_			Operatin	g Par	ameters (incl		ts)				
Fuel			Тур	e of Fuel		Heat I	nput (MMBTU/	hr)						Parame			D	escript	ion	
	a			NA			NA				Rate/Through			17,000 1	o/hr	-		*		
	0								,		ing Rate/Throu			NA.		-		-		
	C	<u></u>			NY - 4						/olume/Cylinde	er Displacemen	t	NA NA		-				
					Notes					ell Height (ft)	N 160			NA NA		-				
								- 1	-	nks:	Fixed Root	f Float	ting Roo		Exte	rnal		0	Int	ernal
			,						100,000	e Engine Orde		1 104	ung No	<u>ы</u>	Engine 1		/ear		III	cinai
								- 1			Built by Manu	facturer			Longino	Toder,	Cai		-	
į.										Engines:		h Burn		Lean Burn	0	2 Stro	ke		4 Stro	ke
Em	ission Po	int ID No	. (Design	ation)	Control	Control	HAP/TAP			0		Permit	Ama		T				-	
1000000			1.75		Equipment	Equipment	CAS Number	1	Duanas	ed Emission I		Emission		Add,						
		1700-20	A		Code	Efficiency		1	Fropos	ed Emission I	ates	(Curre	ent)	Change,	Comp			ncentra		
D. II. de						1				76.7			-	Delete, or	Met			Exiting	at Sta	ek
Polluta	int							Averag (lb/hr)		Maximum (lbs/hr)	Annual (tons/yr)	Annu (tons/		Unchanged	1		(
Particu	late matte	er (PM _{1c})			-			(10/111)		(-waite)	(10110131)	(-Stade	3-7						pri	std ft ³
Sulfur		(IU)																		by vol
-	n oxides														1					by vol
Carbon	monoxid	le																		by vol
Total \	OC (incl	uding thos	se listed b	elow)															ррп	by vol
Lead																			ppn	by vol
Chloro																			ppn	by vol
Toluene Ammonia																				by vol
II Ammo	nia										1						1		nnn	hy vol

						Sta	ate of Louis	iana						Date	f submitt	al
					Emissions	Inventory Qu	uestionnaire	(EIQ) for Ai	r Pollutants					Nov	20	013
. 1	Zmieslo- 1	Point ID N		Down! if	Name of the	F 1 1 - C	AL N					· · · · · ·				
		nation)	0.	Descriptive	e Name of the	Emissions Source	(Alt. Name)		Ар	proximate Locati	on of Stack or	Vent (see in	istruction	15)		
		0-21A			2MM Pound	CD Storage Tank		Method		06,"Address Mat	ching-Primary N	lame"		Datum	NAD8	3
-		2						UTM Zon		Horizontal	739000	mE	Vertica	1 33		mN
Ten	npo Subje	ect Item III	No.					Latitude	30 °	3	-	15 "			man .	redths
-	FOR	50141						Longitude	-90°	31		15 "			hund	redths
C/	k and Dis	T0141	Di i	(60) 64 1			- 1 2		15 15 51					-		
	al Chara			(ft) or Stack	Height of St	COLUMN TO A STATE OF THE PARTY	AA TAGABIGATANA TAGABANANA	ck Gas Flow at	Stack Gas Exit	Normal Opera	111111111111111111111111111111111111111	Date of		Percen	of Annu	
	nge? (yes		Discharg	e Area (ft²)	Above Grade	e (ft) Veloci		nditions, <u>not</u> at ndard (ft³/min)	Temperature	Time (hours per ye		struction o			ion Poin	
	,						Sta	ndard (It /min)	(°F)	(nours per ye	111	ouncation		Zittise	OH A OH	
Ĺ.,	no	- 1		· Section 1		- 1				-	Jan		1972 Ja	n- Apr-	Jul-Sep	
		- 1	0	.25 ft	48.2 1	ft 0.38	ft/sec	1 ft^3/min	23 °F	8,760	hr/yr		IV.	lar Jun		Dec
				ft ²									25	5% 25%	25%	25%
	1	Tv	ne of Fuel I	sed and Heat I	nnut (see ins	structions)		T		Operating Par	ometers (incl	ude unite	.)			
Fuel		1	Type of F			nput (MMBTU/hr				Operating rai	Parame	-	')	Descrip	tion	
	a		NA		Acat I	NA NA	/	Normal Operating	g Rate/Throughput		93.6 MM	-		Descrip	LIGHT	
	b							170	ting Rate/Throughp		19,753,37					
eah ·	c							The second secon	Volume/Cylinder D		279,700					
				Notes				Shell Height (ft)	Torumor Cymraer 2	портисотноги	48	8				
				11000				Tank Diameter (f	1)		31.5					
							1	Tanks:	Fixed Roof	Floating Ro		Extern	nal		Int	ernal
							1	Date Engine Orde				Engine M	100.72			
									Built by Manufact	urer	T					
								SI Engines:	☐ Rich Bu		Lean Burn		2 Stroke		4 Stro	ke
En	ission Po	1700-21A	(Designation)	Control Equipment Code	Control Equipment Efficiency	HAP/TAP CAS Number	Pr	oposed Emission F	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Continu	ance	Concentr Exitin	ation in 6	
Pollut	ant						Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Metho	od			
Particu	late matte	er (PM ₁₀)													gr/	std ft ³
Sulfur	dioxide														- Carlo aye	by vol
Nitrog	en oxides														ppm	by vol
	n monoxid														ppm	by vol
-	VOC (incl	uding those	e listed below)	000	0%		1.32	1.69	5.77	5.77	U				ppm	by vol
Lead															ppm	by vol
Chloro	prene			000	0%	00126-99-8	1.32	1.69	5.77	5.77	Ü				ppm	by vol
																by vol
															ppm	by vol

						Sta	ate of Louis	iana	E.	41				Date of	submitt	al
					Emissions	Inventory Qu	estionnaire	(EIQ) for Air	Pollutants					Nov	20	013
	K												: e	1101	20	,,,
Er	nission P	oint ID No.		Descriptive	Name of the l	Emissions Source (Alt. Name)		Ap	proximate Locatio	on of Stack or V	ent (see ins	tructions)			Consult 1
	(Design	on the second second										v 10		_		21
	1700	-25A			Product	Drying CAP		Method	e 15	06,"Address Mato		mE	Vertical	Datum		mN
Tem	no Subjec	t Item ID No	_					UTM Zon Latitude	30 °	Horizontal 3	,	15 "	vertical	332		redths
X CIII	po Buojec	t Hem ID 140						Longitude		31		15 "			100	redths
	GRP	0007						Songrado								
	and Disc		Diameter (f	t) or Stack	Height of St	ack Stack Ga	s Exit Sta	ck Gas Flow at	Stack Gas Exit	Normal Opera	ting I	Date of	F	ercent o	of Annu	al
	Charac		Discharge .	Area (ft²)	Above Grade	e (ft) Veloci		nditions, <u>not</u> at	Temperature	Time		truction or	Thro	ughput		
Chan	ge? (yes	or no)				-	Sta	ndard (ft³/min)	(°F)	(hours per ye	ar) Mo	dification		Emissio	on Poin	t
							* 1			~		1	Jan-	Apr-	Jul-Sep	Oct-
	no		NA	ft	NA i	ft NA	ft/sec 1	NA ft^3/min	NA °F	8,760	hr/yr		Mar	Jun		Dec
ł	-						-						25%	25%	25%	25%
			-	_ft ²		i	1									
		Type	of Fuel Us	ed and Heat I	nput (see ins	structions)				Operating Para	ameters (inclu	ide units)				
Fuel			Type of Fu	el	Heat I	nput (MMBTU/hr)				Paramet	er	1	Descript	ion	
	а	~	NA			NA		Normal Operating	g Rate/Throughput		30,000 lb/	/hr				
	b							Maximum Operat	ting Rate/Throughp	out	NA					
	С								Volume/Cylinder D	Displacement	, NA					
				Notes				Shell Height (ft)			NA				Sin .	
								Tank Diameter (f		_	NA					
								Tanks:	Fixed Roof	Floating Ro		Externa			Int	ternal
							- 1	Date Engine Ord				Engine Mo	del Year			
							1 .		Built by Manufact		<u> </u>		G: 1		10	
								SI Engines:	□ Rich Bu	·	Lean Burn	□ 2	Stroke		4 Stro	ke
Em	ission Poi	nt ID No. (De	esignation)	Control Equipment	Control Equipment	HAP / TAP CAS Number			-	Permitted Emission Rate			1			
		1700-25A		Code	Efficiency	CAS Number	P	roposed Emission l	Rates	(Current)	Add, Change,	Continuo	ous	ncentra	tion in	Cases
				1						(Delete, or	Complia	nce	Exiting		COMPLETE.
Polluta	nt						Average	Maximum	Annual	Annual	Unchanged	Metho	d			
							(lb/hr)	(lbs/hr)	(tons/yr)	(tons/yr)						
	late matter	r (PM ₁₀)														std ft ³
Sulfur															The same of the sa	by vol
	n oxides															by vol
-	monoxide		. 11 1	000	0.00		15.6	-	60.00	60.17						by vol
-	OC (inch	iding those lis	ted below)	000	0%		15.6	*	68.20	69.17	C		_			by vol
Lead	orana			000	0%	00126 00 9	13.0	-	56.8	57.55			-			by vol
Toluen				000	0%	00126-99-8 00108-88-3	5.3	*	23.1	24.16	C	-	_	-	-	by vol
A Olucii				000	070	00100-00-3	J.5	-	23.1	24.10	<u> </u>	-				n by vol

								tate of	Louisi	ana							Date of	submitte	al
	:*: 					Emissions	Inventory	Question	maire	(EIQ) for Ai	r Pollutants					0 (-1	Nov	20	13
. E		Point ID N gnation)	lo.	-	Descriptive	Name of the I	Emissions Source	e (Alt. Na	me)		A	proximate Locati	on of Stack or	Vent (see	instruc	tions)		,	
	17	00-25				East Was	sh Belt Dryer			Method	191	06,"Address Mat						NAD83	
										UTM Zor			739000	_mE		tical -	332		mN
Tem	ipo Subj	ect Item II	No.							Latitude	30 °	3	-				-		
	EQ	T0142								Longitude	-90°	31		15	+			nundi	redths
	k and Di		Diam	eter (ft) or	Stack	Height of St	ack Stack	Gas Exit		ck Gas Flow at	Stack Gas Exit	Normal Opera		Date of				f Annu	
	al Charange? (ye	s or no)	Disc	harge Area	a (ft²)	Above Grade	e (ft) Vel	ocity		nditions, <u>not</u> at ndard (ft³/min)	Temperature (°F)	Time (hours per ye		struction odificatio				Through n Point	
														1		Jan-	Apr-	Jul-Sep	Oct-
	no			14.1 ft	1	31 f	t 18.2	0 ft/sec	15,4	400 ft^3/min	104 °F	8,760	hr/yr		1970	Mar	Jun		Dec
	-			ft ²	ı			_								25%	25%	25%	25%
	T	Ty	pe of Fu	el Used a	nd Heat I	nput (see ins	structions)			1		Operating Par	ameters (inc	lude unit	ts)				
Fuel		T		of Fuel			nput (MMBTU/	hr)					Parame			D	escript	on	
	a			NA			NA			Normal Operatin	g Rate/Throughput		30,000 1	b/hr					eng accident
1	b								1	170	ting Rate/Through		NA			752			4.5
	c										Volume/Cylinder I		NA				20		
					Notes					Shell Height (ft)			NA						
-		*Co	vered unde			Product Drying	CAP			Tank Diameter (ft)		NA						
				-		*				Tanks:	Fixed Roof	Floating Ro	of 🗆	Exter	rnal			Inte	ernal
							¥			Date Engine Ord	ered			Engine l	Model Y	ear			
											s Built by Manufac	turer							
										SI Engines:	□ Rich B		Lean Burn		2 Stro	ke		4 Strol	ke
Em	ission P	1700-25		2110 200100	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number		Pro	oposed Emission	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl Metl	liance	250.00		ion in (
Polluta	ant								rage /hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meti	nou				
		er (PM ₁₀)																gr/s	std ft ³
Sulfur	dioxide																	ppm	by vol
Nitroge	en oxide	S																ppm	by vol
Carbon	monoxi	de																ppm	by vol
Total V	OC (inc	luding thos	e listed be	low)	000	0%			ılı:	2.55	Mr.	aje .	C					ppm	by vol
Lead									1-1-									ppm	by vol
Chloroprene 000						0%	00126-99-8		*	2.12	101	*	C						by vol
Toluene 000						0%	00108-88-3		**	0.86	191	*	С						by vol
rodelle																		ppm	by vol

							St	ate of Louis	siana	18					. 1	Date of	submitt	al .
				ŭ		Emissions	Inventory Q	uestionnair	e (EIQ) for Air	r Pollutants					1	Nov	20	013
E		Point ID N	0.		Descriptive	Name of the I	Emissions Source	(Alt. Name)		Ap	proximate Location	on of Stack or V	ent (see i	instruct	tions)			
		0-26				West Wa	sh Belt Dryer		Method	di .	06,"Address Mate	hing-Primary Na	une"			Datum	NAD83	3
			R				*		UTM Zon				mE	Vert	tical	332		mN
Tem	po Subje	ct Item II	No.						Latitude	30 °	3		15		-			redths
	EQT	T0143							Longitude	-90 °	31	,	15		-	_	hund	redths
	and Dis		Dian	neter (ft)	or Stack	Height of St	ack Stack Ga		ack Gas Flow at	Stack Gas Exit	Normal Opera	ting 1	Date of		Pe	ercent o	f Annu	al
	al Charac ige? (yes		Disc	charge A	rea (ft²)	Above Grade	e (ft) Veloc		onditions, <u>not</u> at andard (ft³/min)	Temperature (°F)	Time (hours per ye	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	struction dificatio			ghput ' Emissio		
	no			14.1	ft	31 f	ft 18.20	ft/sec 1	5,400 ft^3/min	104 °F	8,760	hr/yr		1970	Jan- Mar	Apr- Jun	Jul-Sep	Oct- Dec
. 1			_		ft²										25%	25%	25%	25%
	1	Tv	pe of F	iel Used	and Heat I	nput (see ins	structions)		1.		Operating Par	ameters (incl	ide unit	ts)				
Fuel		1	-	e of Fuel			nput (MMBTU/h	r)				Paramet		<u> </u>	D	escript	on	
	a		-	NA			NA		Normal Operating	g Rate/Throughput	5	30,000 lb	/hr					
	b								No.	ting Rate/Throughp		NA			-			
	С				7				Design Capacity/	Volume/Cylinder I	Displacement	NA				Or .		
					Notes		11		Shell Height (ft)		8	NA					- N	
		*Co	vered und	er EIQ N	O. 1700-25A, F	roduct Drying	CAP		Tank Diameter (f	(t)		NA				W		
								1	Tanks:	Fixed Roof	Floating Ro	of 🛮	Exter				Int	ernal
V.									Date Engine Ord	the same of the sa			Engine N	Model Y	ear			
										Built by Manufact								
									SI Engines:	□ Rich Bı	3000	Lean Burn		2 Stro	ke		4 Stro	ke
	Emission Point ID No. (Designation)				Control Equipment Code	Control Equipment Efficiency	HAP/TAP CAS Number	1	roposed Emission l		Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl Meti	liance		centra Exiting		
Polluta	ant	1.00						Average (lb/hr)	Maximum (lbs/br)	Annual (tons/yr)	Annual (tons/yr)	Unchanged						
	late matte	er (PM ₁₀)								The state of the s								std ft ³
-	dioxide					1												by vol
	en oxides										-							by vol
	monoxid		- 15-7 11	1	000	000		-	0.55	-	-							by vol
The same of the sa	OC (incl	uding thos	e listed be	elow)	000	0%		*	2.55	*		С						by vol
Lead Chloro	prene				000	0%	00126 00 0	*	2.12	*	+							by vol
_					000	0%	00126-99-8 00108-88-3	*	0.86	*	*	C	-					by vol
Toluene					000	070	00100-00-3	-	0.00	-	-		-					by vol

						St	ate of Louisian	1						Ī	ate of	submitt	al
					Emissions	Inventory Q	uestionnaire (E	IQ) for Ai	r Pollutants					N	lov	20)13
E	mission Po (Design		0.	Descriptive	Name of the E	Emissions Source	(Alt. Name)	T	Áp	proximate Locati	on of Stack or V	ent (see i	nstructio	ons)			
	1700	and the second	- 1		East Hot I	Oryer Exhaust		Method		06,"Address Mat	ching-Primary N	ame"		D		NAD83	3
Ton	po Subjec	4 Idam III	Nie					UTM Zon Latitude	15 30 °	Horizontal 3		mE 15	Vertic	al _	3327		mN redths
1 em	po Subjec	t Hem II	No.					Lantude		31	M	15		_			redths
	EQT							Dongitude						_			
Physica	and Discl al Charact age? (yes o	teristics		(ft) or Stack e Area (ft ²)	Height of Sta Above Grade	The same of the sa	ity Conditi	as Flow at	Stack Gas Exit Temperature	Normal Opera Time (hours per ye	Con	Date of struction odification		Throug	hput	f Annu Throug n Point	h This
	no			7			Standar	d (ft³/min)	(°F)	(nouts per ye	Jac')					Jul-Sep	
				3 ft	65.5 ft	67.40	ft/sec 28,600	ft^3/min	250 °F	8,760	hr/yr	l l	1		Jun 25%	25%	25%
	1		er iv														
Fuel		1 y	Type of F	sed and Heat I		tructions) put (MMBTU/hr	<u> </u>			Operating Par	Paramet		s)	Do	scripti	on	
, uci	a		NA	der	Heat III	NA NA		rmal Operating	g Rate/Throughput		30,000 lb			De	scripu	UII	
	b								ting Rate/Throughp	out	NA						
	c		14:5						Volume/Cylinder D		NA						
				Notes				ell Height (ft)			NA						
	THE RESERVE TO SERVE	*Cov	ered under EIC	NO. 1700-25A, I	roduct Drying	CAP	Та	nk Diameter (f	t)		NA						
							Та	nks:	Fixed Roof	Floating Ro	of 🗆	Exter	nal			Inte	ernal
								te Engine Orde				Engine N	Iodel Yea	ar			
						DE V	Da	te Engine Was	Built by Manufact								
							SI	Engines:	☐ Rich Bu	irn 🗆	Lean Burn		2 Stroke			4 Strol	ke
Emi	ission Poir	1700-27	(Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Propos	ed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compli	iance			on in (
Polluta	nt						Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meth	boi				
Particul	late matter	(PM ₁₀)			The state of the s	1										gr/s	std ft ³
Sulfur o																	by vol
the same of the same of	n oxides																by vol
C	monoxide	and the second s														-	by vol
	OC (includ	ding those	listed below)	000	0%		*	13.03	*	sh.	С						by vol
Lead	arana.			2000	0.07	00126.00.0	-	10.01	-								by vol
Chlorop Toluene				000	0%	00126-99-8 00108-88-3	*	10.86	非	ate .	C	-					by vol
- Olderic				000	070	00100-00-3		4.41	-		-					THE OWNER WHEN PERSON NAMED IN	by vol
								-				I				Perki	-7 101

							S	tate of l	Louisia	na			11				Date of	submitt	al
						Emissions	Inventory (uestion	maire ((EIQ) for Air	Pollutants						Nov	20	013
										(Nov	20	113
E	mission l	Point ID N	No.		Descriptive	Name of the	Emissions Source	e (Alt. Nar	ne)		Ap	proximate Location	on of Stack or V	ent (see in	nstrue	tions)			
4		gnation)						. (on or beneat or ,	(000 1					
	170	00-28	1 3			West Hot	Dryer Exhaust			Method		06,"Address Mate					Datum	NAD8	3
										UTM Zon				mE		tical	332		mN
Ten	po Subje	ect Item I	D No.	06.						Latitude	30 °	3		15					lredths
	FO	T0145								Longitude	°	31		15 '				nund	lredths
Stack	k and Dis	The state of the s	Diam	eter (ft) o	or Stack	Height of S	tack Stack G	as Exit	Stack	k Gas Flow at	Stack Gas Exit	Normal Opera	ting	Date of		P	ercent o	f Annu	ıal
		cteristics	Discl	iarge Ar	ea (ft²)	Above Grad		city	Cone	ditions, not at	Temperature	Time		struction	or	Throu	ighput	Throug	h This
Cha	nge? (yes	or no)		0					Stan	dard (ft ³ /min)	(°F)	(hours per ye	ar) Mo	odification	1		Emissi	n Poin	t
			*											1 1		Jan-	Apr-	Jul-Sep	Oct-
	no			3 f	ft I	65.5	ft 67.4	0 ft/sec	28,6	600 ft^3/min	250 °F	8,760	hr/yr		1970	Mar	Jun	Jul-oct	Dec
		-	3 15 3 15					_							1	25%	25%	25%	25%
			_	f	ft ²														
	T	T	ype of Fu	el Used	and Heat I	nput (see in	structions)				· .	Operating Par	ameters (incl	ude units	5)				
Fuel			Type	of Fuel		Heat I	nput (MMBTU/I	nr)					Paramet	ter		D	escript	on	
	а		1	A			NA			Normal Operating	Rate/Throughput		30,000 16	/hr					
	b						-			The second secon	ing Rate/Throughp		NA						
	С										Volume/Cylinder I	Displacement	NA						
-					Notes					Shell Height (ft)			NA					10.	
		*Co	vered unde	r EIQ NO). 1700-25A, F	Product Drying	CAP			Tank Diameter (f			NA						
										Tanks:	Fixed Roof	Floating Ro	of 🗆	Exteri	_	,		Int	ernal
										Date Engine Orde				Engine M	lodel 1	ear			
										SI Engines:	Built by Manufact		Lean Burn		2 Stro	ko		4 Stro	ke
Em	ission Po	oint ID No	. (Designat	tion)	Control	Control	HAP/TAP			ox Engines.	L Kich Di	Permitted	I Darn		~ 5410	MC		· Duo	NC.
Lin	iission i c	mit ID 140	. (Designa)	uon)	Equipment	Equipment	CAS Number					Emission Rate	Add,						
		1700-21	8		Code	Efficiency		1	Pro	posed Emission I	Rates	(Current)	Change,	Continu		Cor	centra	ion in (Gases
			R U										Delete, or	Compli Meth	Charles and the		Exiting	at Stac	k
Pollut	ant			- 1			ž.		rage	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged						
Particu	late matte	er (PM ₁₀)						(ID	/hr)	(IDS/III)	(tons/yt)	(tons/yr)		-				/	std ft ³
	dioxide	ct (1 141(0)						+										THE RESERVE TO THE PERSON NAMED IN	by vol
	en oxides							1											by vol
Carbon	monoxi	de																	by vol
Total V	VOC (inc	luding tho	se listed bel	ow)	000	0%			*	13.03	*	*	C				-117,2711		by vol
Lead																		ppm	by vol
Chloro					000	0%	00126-99-8		*	10.86	ış:	*	С					_	by vol
Toluene 000 0% 00108-88-3									*	4.41	*	*	С	-					by vol
III																		20.25.200	Inne seed

								State of	Louisian	na :							Date of	submittal	
						Emissions	Invento	ory Questio	nnaire (EIQ) for Ai	r Pollutants						Nov	201	3
E		Point ID N	No.		Descriptive	Name of the	Emissions :	Source (Alt. Na	ıme)		A	Approximate Locat	ion of Stack or V	Vent (see	instruc	tions)			
		00-45	l		No.	1 East Dryer	Cooling Co	mpartment		Method		06,"Address Ma	tching-Primary N 739000	ame" mE	17	tical		NAD83	mN
Tem		ect Item II	D No.							UTM Zon Latitude Longitude	30 °		3 1	15	17	iicai .	332	hundre	edths
Physica	and Dis al Chara- nge? (yes	charge cteristics		neter (ft) o		Height of St Above Grade	The second second	tack Gas Exit Velocity	Condi	Gas Flow at at at ard (ft ³ /min)	Stack Gas Exi Temperature (°F)	TO THE PROPERTY OF THE PARTY OF	Con	Date of struction odification		Throu	ighput '	f Annua Through n Point	
	no		-	2.67 f	ft ft ²	49.6	ft	61.60 ft/sec	20,65	0 ft^3/min	122 °F	8,760	_hr/yr		1970	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
-	1	Ty	me of Eu	rel Used	and Heat I	nput (see ins	tructions	.)	-			Operating Par	rameters (incl	ude uni	te)				
Fuel			The second second	e of Fuel	and Heat I	-	nput (MM)		1 1			Operating rai	Paramet		13)	D	escripti	on	
100	а		The second second	NA		ALCIAL A	NA	O L CHIL)	1	Normal Operating	g Rate/Throughpu	ut	30,000 lb						
A TOTAL	b								N	Maximum Opera	ting Rate/Through	hput	NA NA	•	77.	-	1-15		
		-			Notes					Shell Height (ft)	+ Oldinor Cylinder	Displacement	NA						
		*Co	vered unde	er EIQ NO		Product Drying	CAP		-	Tank Diameter (f	t)	· F	NA						
									1	Tanks:	Fixed Roof	Floating Re	oof 🗆	Exte	rnal			Inter	rnal
									I	Date Engine Ord	ered			Engine l	Model Y	/ear			
									1	Date Engine Was	Built by Manufa	acturer							
					7				5	SI Engines:	□ Rich I	Burn 🗆	Lean Burn	ø.	2 Stro	ke		4 Stroke	е
		int ID No 1700-45	. (Designa		Control Equipment Code	Control Equipment Efficiency	HAP / T	The state of the s	Prop	osed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Comp	liance			ion in G	1,7000000000
Polluta	int								erage o/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	nou				
-	late matte	er (PM ₁₀)																gr/st	d ft ³
-	dioxide																	ppm b	y vol
THE RESERVE	en oxides																	ppm b	
-	monoxid																	ppm b	-
-	OC (incl	uding thos	se listed be	low)	000	0%			*	< 0.01	*	*	U					-	oy vol
Lead					000	0.5	00107	0.0		0.01				-				_	y vol
Chloro					000	0%	00126-9		*	<0.01	*	**	U	-					oy vol
Toluene 000 0% 00108-88-3										<0.01	· ·	*	U	-					by vol
																		ppm	by vol

						-												
		S C					Sta	ate of Louisi	ana							Date of	submitt	al
						Emissions	Inventory O	uestionnaire	(EIQ) for Air	Pollutants					1	Nov	20	013
											8				- 1	1404	20	713
T.		TD N			D 1 1			711 12 1										
L	The state of the s	oint ID N	10.		Descriptive	Name of the I	Emissions Source	(Alt. Name)		Ap	proximate Location	on of Stack or \	Vent (see	instruc	tions)			
	- 0	0-46			No. 1	West Dryer	Cooling Comparts	ment	Method		06,"Address Mate	hing-Primary N	ame"			Datum	NAD8	3
						. Troubly of	comparts		UTM Zon			739000	mE	Ver	tical		_	mN
Tem	po Subje	ct Item II	No.						Latitude	30 0	3		15				hund	redths
									Longitude	°	31	1	15	."	3		hund	lredths
C/ 1		0147	71		- I					T =					-			
	and Disc al Charac	The state of the s		eter (ft) or	Carried Sector	Height of St		Transport 1	ck Gas Flow at	Stack Gas Exit	Normal Opera		Date of	NAME OF TAXABLE PARTY.			of Annu	-3-500
	ige? (yes		Disc	harge Area	a (ft°)	Above Grade	e (ft) Veloc	10.00	nditions, <u>not</u> at ndard (ft³/min)	Temperature (°F)	Time (hours per ye	and the second second	struction odification			O .	Througon Poin	Million St. March 2000
	8 (3				1		J	Star	noaro (it /min)	(F)	(nours per je		Outreatio			ASKREGGE	OIL E OIL	
	no	- 1		2.25.2									1	1970	Jan-	Apr-	Jul-Sep	
		.	-	2.67 ft	-	49.6 f	ft 61.60	ft/sec 20,	650 ft^3/min	122 °F	8,760	hr/yr	1	13.0	Mar	Jun	0.50	Dec
		İ		ft ²	2					-					25%	25%	25%	25%
									,									
		Ту			ınd Heat Iı	nput (see ins					Operating Par	_		ts)				
Fuel	_			of Fuel		Heat I	nput (MMBTU/hr	7)		D 50		Parame				escript	ion	
	a			NA			NA			g Rate/Throughput	to the second se	30,000 11	o/hr	-				
	0									ting Rate/Throughp		NA.		-				
_	c				NI-4			-		Volume/Cylinder I	Displacement	NA		-		-		
		*Co	vared unde	-	Notes	Product Drying	CAR		Shell Height (ft)			NA NA		-				
		- 00	vereu unue	EIQ NO.	1700-23A, P	roduct Drying	CAP		Tank Diameter (f	Fixed Roof	Floating Do		Exte	1			In	ternal
									Tanks: □ Date Engine Ord		Floating Ro	of 🗆	1		V		ш	ernai
- 7								1		Built by Manufact	- L		Engine	Model	rear			
								- 1	SI Engines:	Rich Bu		Lean Burn	Ø	2 Stro	lce	П	4 Stro	ke
Em	ission Poi	int ID No	. (Designa	tion)	Control	Control	HAP / TAP	Г	Di Diigines.		Permitted	Total Dari	T	- Otto	1			ite.
			(10 0016111	2 6	Equipment	Equipment	CAS Number				Emission Rate	Add,						
		1700-46	i .		Code	Efficiency		Pr	oposed Emission I	Kates	(Current)	Change,	Conti		Cor	centra	tion in	Gases
D. 11					- 1							Delete, or	Met			Exiting	at Sta	ek
Polluta	int			1	- 1			Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged						
Particu	late matte	r (PM.a)						(10/111)	(Ios/III)	(tons/j1)	(tous/j1)		+		-	5		std ft ³
	dioxide	(* * * * 107									1		1					by vol
-	en oxides														1			by vol
-	monoxid	le		-					1		†	T						by vol
Total V	OC (inch	uding thos	se listed be	low)	000	0%		*	< 0.01	*		U						by vol
Lead													-					by vol
Chloro					000	0%	00126-99-8		<0.01		*	U					ppn	by vol
Toluen	е				000	0%	00108-88-3	*	< 0.01	*	*	U						by vol
																	nnn	har wol

		V				St	tate of I	Louisia	na								Date of	submitta	al
					Emissions	Inventory Q	uestion	naire (EIQ) for Air	Polluta	nts						Nov	20	13
E		Point ID N	0.	Descriptive	Name of the	Emissions Source	(Alt. Nan	ne)		111111111111111111111111111111111111111	App	proximate Locati	on of Stack or V	ent (see i	nstructi	ions)			
		0-47		No.	2 East Dryer	Cooling Compart	ment		Method			06,"Address Mat	ching-Primary N	ame"			Datum	NAD83	
					- Subt Sijek	compare	ittosie		UTM Zon		15	Horizontal		mE	Verti				mN
Tem	po Subje	ect Item ID	No.						Latitude	30 0		3	T	15				hundi	redths
				× .					Longitude	-90 °		31	1	15	10	-		hundi	redths
	-	TO148																-	
	and Dis			er (ft) or Stack	Height of St		_		Gas Flow at	Stack Gas		Normal Opera		Date of				f Annu	
- 40	al Chara nge? (yes		Dischar	rge Area (ft²)	Above Grade	e (ft) Veloc	city		itions, not at	Tempera	ture	Time (hours per ye	The state of the s	struction odification			-	Through n Point	
Caller	age. Ges	01 110)				W 1	l	Stand	lard (ft³/min)	(°F)	1	(nours per ye	car) Iva	diffication	1		DIMI5510	A VIIII	
	12.0	1				- 1				-	- 1				1970	Jan-	Apr-	Jul-Sep	Oct-
	no	.		2.67 ft	49.6	ft 61.60	ft/sec	20,65	50 ft^3/min	122 °F	7	8,760	hr/yr		1970	Mar	Jun		Dec
		- 1		-2						100	- 1		1			25%	25%	25%	25%
				ft²															
		Ty	pe of Fuel	Used and Heat I	nput (see ins	structions)						Operating Par	ameters (incl	ude unit	s)				
Fuel		La C	Type of	Fuel	Heat I	nput (MMBTU/h	r)						Paramet	er		D	escript	on	
	a		NA			NA			Normal Operating	Rate/Throu	ghput		30,000 16	/hr					
	b								Maximum Operat	ting Rate/Th	roughp	ut	NA						
	С								Design Capacity/	Volume/Cyli	nder D	isplacement	NA		1				
				Notes					Shell Height (ft)				NA						
		*Cov	ered under E	EIQ NO. 1700-25A,	Product Drying	CAP			Tank Diameter (f	t)			NA			15			
									Tanks:	Fixed R	oof	Floating Ro	oof 🗆	Exter	nal			Inte	ernal
									Date Engine Orde	ered				Engine N	Aodel Y	ear			
							1		Date Engine Was	Built by Ma	mufacti	urer							
									SI Engines:	□ R	ich Bu	rn 🗆	Lean Burn	7	2 Strok	ce		4 Strol	ce
Em	ission Po	1700-47	(Designatio	n) Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	-	Prop	posed Emission I	Rates		Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compli	iance			ion in C	
Polluta	ant					×.	Aver (lb/	rage hr)	Maximum (lbs/hr)	Annu (tons/y		Annual (tons/yr)	Unchanged	Wieti	lou		*		
Particu	late matte	er (PM ₁₀)																gr/s	std ft ³
	dioxide																	ppm	by vol
Nitroge	en oxides				FILE COLD		5 5		213									ppm	by vol
Carbon	monoxid	le																ppm	by vol
Total \	OC (incl	uding those	e listed below	v) 000	0%		-	k	< 0.01			*	U					ppm	by vol
Lead																		ppm	by vol
Chloro	prene			000	0%	00126-99-8	,	dt .	< 0.01	zje		shi	U						by vol
Toluene 000 0% 00108-88-3								tk .	<0.01	zje		*	U						by vol
																		ppm	by vol

																	. K			
								State of I	ouisia	ana								Date of	submitt	al
						Emissions	Inventory	Question	naire	(EIO) for	Air	Pollutants					- 1	.,	20	
						ZIZIZIGIA	zii (ciitoz y	Question	MILLIAN C	(212) 101	Z MAR	2 Onticums					1	Nov	20	013
		2				10								(9)						
E		oint ID N	lo.		Descriptive	Name of the I	Emissions Sou	rce (Alt. Nan	ne)			App	proximate Location	on of Stack or	Vent (see	instruc	tions)			
		nation)				X				1										
	170	0-48			No. 2	2 West Dryer	Cooling Comp	partment		Method	_		06,"Address Mato		mE	17		Datum		
Tom	an Cubia	ct Item II	D NI.							UTM :		30 0	Horizontal 3	739000	- me		tical -	332		mN redths
Tem	po Subje	ct item ii	D INO.							Longit	_	-90 °	31		15	-	-			redths
	EQT	0149								Longit	rude_	-50			- 15	_			попо	reduis
Stack	and Disc	charge	Diam	eter (ft)	or Stack	Height of St	ack Stack	Gas Exit	Stack	k Gas Flow at		Stack Gas Exit	Normal Opera	ting	Date of		P	ercent o	f Annu	al
	l Charac		Disc	harge Ar	ea (ft²)	Above Grade	e (ft) V	elocity	Con	ditions, <u>not</u> at		Temperature	Time	Cor	struction	or	/4	ghput	-	
Chan	ge? (yes	or no)	Δ.	777.					Stan	dard (ft ³ /min)		(°F)	(hours per ye	ar) M	odificatio	n		Emissio	n Poin	t
					- 1		- 1								1	i l	Jan-	Apr-	Jul-Sep	Oct-
	no			2.67	ft	49.6 f	61	.60 ft/sec	20,6	550 ft^3/m	nin	122 °F	8,760	hr/yr		1970	Mar	Jun	Jul Doj	Dec
193			_		. 1										3	.	25%	25%	25%	25%
			_		ft ²			-												
		T	vpe of Fu	iel Used	and Heat I	nput (see ins	structions)						Operating Par	ameters (inc	ude uni	ts)				
Fuel				of Fuel			nput (MMBT	U/hr)						Parame			D	escript	ion	
	a			NA	* * * * * * * * * * * * * * * * * * *		NA			Normal Opera	ating !	Rate/Throughput		30,000 1	b/hr					
	ь									Maximum Op	peratir	ng Rate/Throughp	ut	NA						
	С									Design Capac	city/V	olume/Cylinder D	isplacement	NA				- 4		
					Notes					Shell Height	(ft)	A		NA						
		*Co	vered unde	er EIQ NO	O. 1700-25A, F	Product Drying	CAP			Tank Diamete	er (ft)			NA						3
										Tanks:		Fixed Roof	Floating Ro	of .	Exte	rnal			Int	ernal
										Date Engine	_				Engine 1	Model)	'ear	K 8		
				1 9						Date Engine	Was I	Built by Manufacto	urer		,			-		
										SI Engines:		□ Rich Bu	ırn 🗆	Lean Burn	Ø	2 Stro	ke		4 Stro	ke
Em	ission Po	int ID No	. (Designa	tion)	Control	Control	HAP/TAI						Permitted							
		1700-48	0		Equipment	Equipment Efficiency	CAS Numb	er	Pro	posed Emissi	on Ra	ates	Emission Rate	Add,	Contin	nuous				
		1700-40			Code	Efficiency				•			(Current)	Change, Delete, or	Comp		-	centra Exiting		
Polluta	nt							Ave	rage	Maximur	n T	Annual	Annual	Unchanged	Met	hod		Lating	at Stat	.K
									/hr)	(lbs/hr)		(tons/yr)	(tons/yr)							
Particu	late matte	er (PM ₁₀)								1									gr/	std ft ³
Sulfur	dioxide																			by vol
Nitroge	n oxides																26		ppn	by vol
-	monoxid																		ррп	by vol
-	OC (incl	uding tho	se listed be	elow)	000	0%			*	< 0.01		*	*	U					THE RESERVE OF THE PERSON NAMED IN	by vol
Lead													,						-	by vol
Chloro					000	0%	00126-99-		*	< 0.01		*	*	U						by vol
Toluen	е		1		000	0%	00108-88-	3	*	< 0.01		*		U						by vol
4																			ppp	hy vol

		E 0)				^	St	ate of Louisia	nna						1	Date of	submitt	al
						Emissions	Inventory Q	uestionnaire	(EIQ) for Ai	r Pollutants						Nov	20	013
E		Point ID N gnation)	lo.		Descriptive	Name of the	Emissions Source	(Alt. Name)		Ap	proximate Locati	on of Stack or V	ent (see	instruct	ions)			
	17	00-50				Stabilize	r Tanks Vent		Method		06,"Address Mate	Name and Address of the Owner, where the Party of the Owner, where the Party of the Owner, where the Owner, which is		77			NAD8	
Tem	po Subi	ect Item II	No.						UTM Zon Latitude	e 15	Horizontal 3		mE 15	Verti	ical -	332	7400 hund	mN redths
	-								Longitude	-90 °	31	1	15			5.4	hund	redths
66.1		P0009		(80)	6. 1					1 = 1 = = 1			2		70			
Physic	al Chara	scharge acteristics s or no)		eter (ft) (harge Ar	1	Height of St Above Grade	The second secon	city Cond	k Gas Flow at ditions, <u>not</u> at dard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Opera Time (hours per ye	Cons	Date of struction odification		Throu	ghput	of Annu Throug on Poin	h This
	no	_	_	0.25	ft	. 54 1	ft 5.43	ft/sec 16	ft^3/min	77 °F	*	hr/yr			Jan- Mar	Jun	Jul-Sep	Dec
					ft²			-							25%	25%	25%	25%
	T	Ту	pe of Fu	el Used	and Heat I	nput (see ins	structions)				Operating Par	ameters (incl	ıde unit	ts)		1516		(n)
Fuel				of Fuel		Heat I	nput (MMBTU/h	r)				Paramet	er		D	escript	on	
	a	-]	NA			NA			Rate/Throughput							- bry	4-56
5.	0	-							Deliver of the Paris of the Par	ing Rate/Throughp		NA		-				
-	Ic				Notes				Shell Height (ft)	Volume/Cylinder D	Isplacement	NA NA						
	*61.12 h	r/yr venting	z: Commor	vent for		0-50.1, 50.2, 5	0.3, 50.4, 50.5, 50.	6.	Tank Diameter (f	t)		NA NA						
				0.0000000000000000000000000000000000000		, ,			Tanks:	Fixed Roof	Floating Ro		Exter	rnal			Int	ernal
			ī						Date Engine Orde				Engine N	Model Ye	ear			
									Date Engine Was	Built by Manufact	urer							
									SI Engines:	☐ Rich Bu	ırn 🗆	Lean Burn		2 Strok	e		4 Stro	ke
Em	ission Po	1700-50		tion)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Pro	posed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin	liance			ion in (THE CONTRACT OF
Polluta	nt							Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meth	noa				
		er (PM ₁₀)															gr/s	std ft ³
The second second	lioxide																	by vol
-	n oxides		SALES TO SERVE									1.8						by vol
-	monoxi						17											by vol
-	OC (inc	luding thos	e listed bel	low)	000	0%	*	19.3	afe	0.57	0.59	C			*			by vol
Lead					000	000	00108 55 5	10.5	1	0.55								by vol
Toluen					000	0%	00108-88-3	19.3	*	0.57	0.59	С						by vol
							-											by vol
-																	Phili	0) 101

					(4) (4)		Sta	ate of L	ouisia	ına					V		Date of	submitt	al
						Emissions	Inventory Q	uestionr	naire ((EIQ) for Air	Pollutants						Nov	20	013
E	mission P	oint ID No			Descriptive	Name of the I	Emissions Source	(Alt. Name	e)		Ap	proximate Location	on of Stack or V	ent (see i	instruct	tions)			
	(Design	nation)									•		1						
	1700	0-50.1				Stabilize	r Tank No. 1			Method		06,"Address Mato					Datum		
Tar	no Subi-	ct Item ID	Nie							UTM Zon Latitude	e 15	Horizontal 3		mE 15	Vert	ucal -	3327		mN redths
Lem	po subje	ct Item ID	140.							Longitude		31		15		-			redths
	EQT	0156												13				uiiu	
	and Disc			eter (ft) o		Height of St				Gas Flow at	Stack Gas Exit	Normal Opera		Date of			ercent o		
	al Charac		Disc	harge Ar	ea (ft²)	Above Grade	(ft) Veloc	ity		litions, not at	Temperature	Time		struction	227.00		ghput		Contract Con
Char	nge? (yes	or no)							Stand	dard (ft ³ /min)	(°F)	(hours per ye	ar) Mo	dificatio	n		Emissio	n Poin	t
	200												0-1		1975	Jan-	Apr-	Jul-Sep	Oct-
	no		1	NA .	ft	NA f	t NA	ft/sec	NA	ft^3/min	65 °F	*	hr/yr Oct		19/3	Mar	Jun		Dec
					6.2											25%	25%	25%	25%
		7	-		ft ²														
		Typ			and Heat I	nput (see ins						Operating Para	ameters (incl	ıde unit	ts)				
Fuel		-		of Fuel		Heat I	nput (MMBTU/hr	r)					Paramet			D	escripti	on	
	a			NA .			NA				g Rate/Throughput		12,200 lb/b	atch					
	b										ting Rate/Through		NA						
-	C				N						Volume/Cylinder I	Displacement	1,050 ga	al	-				
*Covi	red und	FIO N- 1	700 50 1	Ptobili	Notes	Manimu	sion rate occurs on	lu mik a a		Shell Height (ft)			5		-				-
Cove	ned under	EIQ NO. I	700-30,		ks are filling.	viaximum emis	sion rate occurs on	ny wnen		Tank Diameter (f	fixed Roof	Floating Par	4	Exter	mal			1	armal
					and finning.					Tanks: Date Engine Orde		Floating Ro	of 🗆	Engine N		laar		ını	ernal
											Built by Manufac	turer		Engine I	viouei i	ear			
										SI Engines:	Rich B		Lean Burn		2 Stro	ke	П	4 Stro	ke
Em	ission Po	int ID No.	(Designs	tion) I	Control	Control	HAP / TAP			Billion		Permitted			7.5.1.0		hed	Dix	
			(~ corgine		Equipment	Equipment	CAS Number					Emission Rate	Add,		140				
		1700-50.1			Code	Efficiency			Pro	posed Emission I	Kates	(Current)	Change,	Contin			centrat		
													Delete, or	Met	ALTON TO THE PARTY OF THE PARTY		Exiting	at Stac	ck
Polluta	ant							Aver	-	Maximum	Annual	Annual	Unchanged	1		10			
Particu	late matte	r (PM)						(lb/h	ir)	(lbs/hr)	(tons/yr)	(tons/yr)							63
Sulfur		/ (I 141]0)	-								1	 			-		- 6		std ft ³
	en oxides										 				-			-	by vol
-	monoxid														-				by vol
-		uding those	listed be	low)	088	0%		aje		595.89	*	*	U	7					by vol
Lead																			by vol
Toluen	e				088	0%	00108-88-3	z)t		595.89	*	*	U						by vol
																			by vol
II .																		nnn	hy vol

				S	tate of Loui	isiana						Date of	submitta	i
			Emissions	Inventory Q	uestionnai	re (EIQ) for A	ir Pollutants					Nov	201	13
Emission Point ID No	0.	Descriptive	Name of the I	Emissions Source	(Alt. Name)		Ap	proximate Locati	on of Stack or V	Vent (see instr	uctions)			
(Designation) 1700-50.2			Stabilize	r Tank No. 2		Method UTM Z	one 15	06,"Address Mate	ching-Primary N		Vertical	and the second of the second o	NAD83	mN .
Tempo Subject Item ID EQT0157	No.					Latitude	30 8	31	1	15 "			hundr	edths
Stack and Discharge Physical Characteristics Change? (yes or no)	Diameter (Height of St Above Grade		city C	tack Gas Flow at Conditions, <u>not</u> at tandard (ft³/min)	Stack Gas Exit Temperature (°F)	Normal Opera Time (hours per ye	Con	Date of estruction or odification		ughput	of Annua Through on Point	This
no	NA	ft ft²	NA f	i NA	ft/sec	NA ft^3/mir	65 °F		hr/yr Oct	197	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
Ту		ed and Heat I	nput (see ins	structions)		T		Operating Par	ameters (incl	ude units)				
Fuel	Type of Fu	el	Heat In	nput (MMBTU/h	r)				Parame	ter	I	escript	ion	
a b c	NA			NA		Maximum Oper	ng Rate/Throughput rating Rate/Throughpy/Volume/Cylinder I	put	12,200 lb/8 NA 1,050 g					1
- B		Notes				Shell Height (ft)	1	5					
*Covered under EIQ No. 1			Maximum emiss	sion rate occurs or	nly when	Tank Diameter			4					
		tanks are filling.			1	Tanks:	Fixed Roof	Floating Ro	of 🗆	External			Inte	rnal
						Date Engine Or				Engine Mode	el Year			
					1	The second of th	as Built by Manufact			2.5			10. 1	
						SI Engines:	□ Rich Bı	172-111	Lean Burn	□ 2 St	roke	0	4 Strok	(e
Emission Point ID No. 1700-50.2		Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	1	Proposed Emission	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Continuou Compliane	(n		ion in G at Stack	
Pollutant					Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Method				
Particulate matter (PM ₁₀)													gr/st	td ft ³
Sulfur dioxide					5-							9		by vol
Nitrogen oxides	UL PRES	2		-									ppm	by vol
Carbon monoxide													ppm	by vol
Total VOC (including those	e listed below)	088	0%		*	595.89		*	U				ppm	by vol
Lead													ppm	by vol
Toluene		088	0%	00108-88-3	非	595.89	*	. *	U				ppm	by vol
													ppm	by vol
													ppm	by vol

							St	ate of I	Louisian	ia						.	Date of	submitt	tal
					Emissions	Inve	ntory Q	uestion	maire (F	EIQ) for Air	Pollutants						Nov	20	013
E	nission P	oint ID N	0.	Descripti	ve Name of the	Emissio	ons Source	(Alt. Nan	ne)		Ap	proximate Location	on of Stack or V	Vent (see	instruct	tions)			
	(Design										-	E COMPANY OF THE PARTY OF THE P							
	1700	-50.3			Stabilize	er Tank	No. 3			Method	15	06,"Address Mate	The state of the s		37		Datum		
Tom	no Subje	ct Item II) No							UTM Zone	30 °	Horizontal 3		mE 15		tical -	332	7400	mN Iredths
A CIII	po subje	r Hem H	7110.							Longitude	Charles and	31		15					iredths
	EQT	0158													•				
	and Disc		Diame	ter (ft) or Stack	Height of St		Stack Ga			Gas Flow at	Stack Gas Exit	Normal Opera	-	Date of			ercent (
Barbara .	l Charac ige? (yes		Disch	arge Area (ft²)	Above Grad	e (ft)	Veloc	city		tions, not at	Temperature	Time	AND THE RESERVE	struction			ghput		and the second second
Chan	ige: (yes	or no)				- 1		- 1	Standa	ard (ft ³ /min)	(°F)	(hours per ye	ar) Mi	odificatio	n		Emissic	n Poin	it.
	no				1			- 1	1				Jul	1	1968	Jan-	Apr-	Jul-Se	p Oct-
		1	N	Aft	NA	ft	NA	ft/sec	NA	ft^3/min	65 °F		hr/yr	1	1900	Mar	Jun		Dec
		- 1		ft ²]	-						1	1			25%	25%	25%	25%
г .		Ту		Used and Heat								Operating Par			ts)	-			
Fuel				of Fuel	Heat I	nput (N	MMBTU/hi	r)		Inches in Contraction	Data (Theorem		12,200 lb/l		-	D	escript	ion	
	b		15	A	-	INA	A				Rate/Throughput ing Rate/Through		12,200 lb/t	batch	-				
	c				+	28					Volume/Cylinder I		1,050 g	al					
				Notes						Shell Height (ft)	voidiller Cymrider 1	Displacement	5 5	,ai	_				- 3
*Cove	red under	EIO No.	1700-50, St	abilizer Tanks Vent.	Maximum emis	sion rat	le occurs on	ly when	1	Tank Diameter (f	n)		4			-			
A SEPARA				tanks are filling						Tanks:	Fixed Roof	Floating Ro	of 🛛	Exte	rnal			In	ternal
									Ī	Date Engine Orde	ered			Engine l	Model Y	ear .			
					9				I	Date Engine Was	Built by Manufac	turer							
									S	I Engines:	□ Rich B	urn 🗆	Lean Burn		2 Stro	ke		4 Stro	oke
		int ID No 1700-50.	. (Designat	ion) Control Equipmen Code	Control t Equipment Efficiency	_2000120	P / TAP Number	÷	Prop	osed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Comp Met	liance		centra Exiting		
Polluta									rage /hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	nou				
D	late matte	r (PM ₁₀)																	/std ft ³
Sulfur						3								-					n by vol
-	n oxides				-									-					n by vol
	monoxid		e listed belo	ow) 088	0%			-	地	595.89	*	*	U	-				_	n by vol
Lead	oc (men	oung thos	e usted belo	Jw) 088	0%	-		-		393.89	-	-		-					n by vol
Toluen	e	_		088	0%	001	08-88-3	—	*	595.89	- *	+	Ü	+		_			n by vol
2010011					970	001	20 00 0			2,3.07				1					n by vol
								1											n by vol

						St	ate of Lou	islana						Date o	submitt	al
	W-				Emissions	Inventory Q	uestionnai	re (EIQ) for A	ir Pollutants					Nov	20	013
E		Point ID N	0.	Descriptive	Name of the I	Emissions Source	(Alt. Name)		Ap	proximate Locati	on of Stack or V	Vent (see i	nstruction	s)		
	170	0-50.4			Stabilize	r Tank No. 4		Method	- V 100	06,"Address Mat	ching-Primary N	ame"		Datum	NAD83	3
								UTM Zo				mE	Vertical	332		mN
Tem	pe Subj	ect Item II	No.					Latitude		31	-	15		-	7	redths
	-	T0159				A	Λ	Longitud		31	-				- nuno	redths
	and Dis		Diame	ter (ft) or Stack	Height of St	ACTUAL CONTRACTOR OF THE PARTY	The state of the s	tack Gas Flow at	Stack Gas Exit	Normal Opera		Date of	1	Percent		
The second	al Chara age? (yes	cteristics or no)	Disch	arge Area (ft²)	Above Grade	(ft) Veloc		Conditions, <u>not</u> at tandard (ft³/min)	Temperature (°F)	Time (hours per ye		struction odification	500	Emiss	Throug on Poin	
	no	. 1	N/	A ft	NA f	NA NA	ft/sec	NA ft^3/min	65 °F	*	hr/yr Jul		1968 Jan M		Jul-Sep	Oct- Dec
			_	ft²									25	% 25%	25%	25%
	1	Ty	pe of Fue	l Used and Heat I	nput (see ins	tructions)				Operating Par	ameters (incl	ude units	5)			
Fuel			-	of Fuel		iput (MMBTU/hi	r)				Parame		-	Descrip	tion	
	a			A		NA ·		Normal Operati	ng Rate/Throughput		12,200 lb/l	batch				
e e e	b	PER PROPERTY	-1					Maximum Oper	ating Rate/Through	put	NA					
The same of	c							Design Capacity	//Volume/Cylinder I	Displacement	2,330 g	al				
				Notes				Shell Height (ft)	,		9.5				N.	
*Cove	red unde	r EIQ No.	1700-50, St	abilizer Tanks Vent. 1	Maximum emiss	sion rate occurs on	ly when	Tank Diameter			4.5					
				tanks are filling.			- 1	Tanks:		Floating Ro	of 🗆	Exteri			Int	ernal
							- 1	Date Engine Or				Engine M	Iodel Year			
									as Built by Manufac						1.0	
177		TD N	(%)	T				SI Engines:	□ Rich B		Lean Burn		2 Stroke		4 Stro	ke
Em	ission Po	1700-50.	(Designati	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	- 1	Proposed Emission	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contine	ance	Concentra Exitin	tion in (
Polluta	nt						Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meth	ou			
Particul	ate matte	er (PM ₁₀)													gr/s	std ft ³
	dioxide					3			-						- 100	by vol
-	n oxides			entr			1									by vol
-	monoxi															by vol
	OC (inc	luding thos	e listed belo	ow) 088	0%		*	595.89	*	*	U					by vol
Lead					- 25											by vol
Toluen	е			088	0%	00108-88-3	*	595.89	*	3fe	U					by vol
							-		-		-	-				by vol
						M. Control of the Con		1							ppin	by vol

								State of	Louisi	ana								Date of	submitt	al
						Emissions	Invento	ry Questic	onnaire	(EIQ) for A	ir Pollu	itants						Nov	20	013
E		Point ID N	io.		Descriptive	Name of the I	Emissions S	ource (Alt. N	ame)			Ap	proximate Locati	on of Stack or	Vent (see	instruc	tions)			
		0-50.5				Stabilize	r Tank No.	5		Method			06,"Address Mat	ching-Primary	Name"			Datum	NAD8	3
700										UTM Z		15		739000	_mE		tical	332	7400	mN
Tem	po Subje	ect Item II) No.							Latitude	_	0°	31		15					redths
	EQ1	Г0160	_				21			Longitu	de -9	0	31	t.	13	-		14	nund	reduis
Annual Control	and Dis			eter (ft) or		Height of St	2000	ack Gas Exit	2000	ck Gas Flow at		Gas Exit	Normal Opera	The state of the s	Date of			ercent o		The state of the s
	d Chara ge? (yes	or no)	Disch	arge Area	a (ft²)	Above Grade	e (ft)	Velocity		nditions, <u>not</u> at ndard (ft ³ /min)		perature (°F)	Time (hours per ye		nstruction Iodificatio			ighput ' Emissic		
	no		N	A ft		NA f	t NA	ft/sec	N	A ft^3/mi	n 6	5 °F	*	hr/yr Jul		2007	Jan- Mar	Apr- Jun	Jul-Sep	Oct- Dec
				ft ²	2					_			14				25%	25%	25%	25%
		Ty	pe of Fu	el Used a	nd Heat I	nput (see ins	tructions)					Operating Par	ameters (inc	lude uni	ts)				
Fuel			Type	of Fuel		Heat I	nput (MMI	BTU/hr)						Param	eter		D	escript	ion	
	a		1	NA			NA			Normal Operat	ing Rate/T	hroughput	\	5,000 lb/	batch					
	b									Maximum Ope	rating Rate	e/Throughp	out	NA						
	С									Design Capaci	ty/Volume/	Cylinder D	Displacement	1,050	gal					
					Notes					Shell Height (f	t)			5						
*Cove	red unde	r EIQ No.	1700-50, S			Maximum emis	sion rate oc	curs only when	1	Tank Diameter				4						
				tanks	s are filling.				1			ed Roof	Floating Ro	oof 🗆	Exte				Int	ernal
										Date Engine O					Engine 1	Model	Year			
										Date Engine V				I P		2.54			1.04	1 -2
177	' D	' A TO N	(D :		G ()	6	TTATO / 7	- T		SI Engines:		Rich Bu		Lean Burn		2 Stro	ке		4 Stro	ке
Em	ission Po	1700-50	. (Designat		Control Equipment Code	Control Equipment Efficiency	HAP / T		Pr	oposed Emissio	n Rates		Permitted Emission Rate (Current)	Add, Change, Delete, or	Conti	liance		ncentra Exiting		
Polluta	nt							1000	verage lb/hr)	Maximum (lbs/hr)		nnual ons/yr)	Annual (tons/yr)	Unchanged	Met	noa				÷
_		er (PM ₁₀)					7.0												gr/	std ft ³
-	lioxide									×										by vol
-	n oxides																			by vol
	monoxio																		-	by vol
_	OC (incl	luding thos	se listed bel	ow)	088	0%			*	595.89		雅	ajt .	U						by vol
Lead					000	0.00	00100	0.2	*	505.00		-		77	-		_			by vol
Toluen	e		,		088	0%	00108-8	8-3	. *	595.89		*	-	U	-					by vol
-				_	+						_			+	-		_	-	Name and Address of the Owner, where	by vol

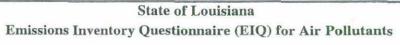
							Ä.	State o	of Louisi	ana									Date of	submitt	al
						Emissions	Invento	ry Questi	onnaire	(EIQ) for A	ir Pollu	tants							Nov	20	013
E		Point ID N	No.		Descriptive	Name of the	Emissions S	ource (Alt. I	Name)	1	*	Ap	proximate L	ocatio	on of Stack or	Vent (see	instruc	tions)			
		(nation) 0-50.6				Stabilizer	Tank - LD	750		Method				_	hing-Primary N					NAD8	
Tem		ect Item D	D No.							UTM Zo Latitude Longitud	30	-	Horizont	al 31		mE 15	"	tical	332	hund	mN redths
Stook	EQT	го161	Diam	-t (Ft)	Starl. I	TT 1-14-654	1 6	10 1	I G	LG FI	10.10	7 - F- 14	. N 16		T	D. C		D		FAnnu	al
Physica		cteristics		eter (ft) or harge Area		Height of St Above Grade		ack Gas Exit Velocity	Cor	ck Gas Flow at aditions, <u>not</u> at adard (ft ³ /min)	Tempe	Gas Exit erature (F)	Normal (Ti (hours p	me	Con	Date of estruction odification		Throu	ighput	of Annu Throug on Poin	h This
	по	-	N	NAft		NA 1	n NA	ft/sec	N	IA ft^3/min	65	<u>°</u> °F	*	-	hr/yr Jul		2007	Jan- Mar 25%	Apr- Jun . 25%	Jul-Sep 25%	Oct- Dec 25%
				ft²																	
W 1		Ty			nd Heat I	nput (see ins		-	_				Operating	Para	ameters (incl		ts)	-			
Fuel	9			of Fuel NA		Heat L	nput (MMF NA	TU/hr)	-	Normal Operation	Data (Th	- shout		_	Parame 1,800 lb/b		-		escript	ion	
	b			·			NA		\exists	Maximum Oper	ating Rate/	Throughp	out		NA						
	1			7	Notes				-	Design Capacity Shell Height (ft)		yunder L	Displacement	_	300 ga	41	_			-	
*Cove	red unde	r EIO No.	1700-50. S			Maximum emis	sion rate occ	curs only whe	en	Tank Diameter					3		1				
					are filling.					Tanks:		d Roof	Floatin	ig Roo		Exte	rnal			Int	ernal
							*	4		Date Engine Or		T		0		Engine	Model Y	r'ear			
										Date Engine Wa		Manufact	turer								
										SI Engines:		Rich Bu			Lean Burn		2 Stro	ke		4 Stro	ke
Emi	ssion Po	int ID No 1700-50.	. (Designa		Control Equipment Code	Control Equipment Efficiency	HAP / T CAS Nun		Pr	oposed Emission	Rates		Permitte Emission I (Curren	Rate	Add, Change, Delete, or		liance			tion in (
Polluta	Pollutant				4		100	verage (lb/hr)	Maximum (lbs/hr)		nual ns/yr)	Annua (tons/yr		Unchanged	Met	thod					
Particul	ate matte	er (PM ₁₀)																		gr/	std ft ³
Sulfur c	Contract of the Contract of th																				by vol
-	n oxides								es Whx	1		7								ррп	by vol
-	monoxid																				by vol
-	OC (incl	uding thos	se listed bel	low)	088	0%			+	595.89		*	*		U						by vol
Lead																					by vol
Toluene	2				088	0%	00108-8	8-3	*	595.89		#.5	*	1000	U						by vol
																					by vol
																				ppn	by vol

181	3	1911			Sta	te of Louisia	na						·	Date of	submitt	tal
				Emissions 1	Inventory Ou	estionnaire (EIO) for Air	Pollutants					,	Nov	20	013
					, ,	-							1	40V	20	013
		0.	Descriptive	Name of the E	missions Source (Alt. Name)		Ap	proximate Location	on of Stack or V	ent (see in	structio	ons)			
		7		Inhibitor	Mix Tank		Method		06,"Address Mate	hing-Primary Na	ame"		I	Datum	NAD8	3
					a make a make						mE	Vertic		,		mN
Subjec	t Item ID	No.					Latitude	30 °			15 "		_		hund	fredths
-						-	Longitude	-90 °	31		15 "		_		hund	iredths
		D!i	- (ft) au St- 1	Walaki CC:	-t- B: 1-C	E-te C:	G File	State Con Entr	No		D. /		n		E A	1
								E-								
		Dischar	rge Area (It-)	ADOVE Grade	veloci		The state of the s		10000						-	
						Gtant	Jane (16 /mm)	(2)								
no			0.167.6	FO. 5	100		5007	27.05		Jun]	UGX		-	Jul-Sep	
			J.10/ II	59 ft	1.06 f	Vsec 1	H^3/min	37 °F		nr/yr	1				250%	Dec 25%
	- 1		ft ²		1	Q.							2570	25.70	2570	2370
								3	O	4 (1)	j					1
	Ty								Operating Par)	D	a a a mile t	law	
				Heat In			Normal Operation	Pate/Throughout					D	escript	ion	
b		INA		-	14/4						atti					
c											s					
			Notes					oranio Cymraer D	Aspacoment.			-0-				
3			*1060 hrs/yr)		4						
			and the second of the				Tanks:		Floating Ro		Extern	al			Int	ternal
													ar			
	*	4.							turer							
							SI Engines:			Lean Burn	□ 2	Stroke	e		4 Stro	ke
sion Poi	nt ID No.	(Designation	Andreas Control of the Control of th	Control	HAP/TAP				Permitted							
	1700 51		Equipment	Equipment	CAS Number	Pro	posed Emission F	ates	Emission Rate	Add,	Continu	ous			-	
	1/00-51		Code	Efficiency	- 1			2000 (O.T.)	(Current)	Change,						
t					1	Average	Maximum	Annual	Annual				,	extring	at Stac	CIK
					* 1	(lb/hr)	(lbs/hr)	(tons/yr)	(tons/yr)	- mananged						
te matter	r (PM ₁₀)														gr/	std ft ³
oxide																by vol
oxides															ppm	by vol
																by vol
C (inclu	iding those	e listed below	000	0%		2.0	2.0	1.06	1.17	С						by vol
				- 22												by vol
ene			000	0%	00126-99-8	2.0	2.0	1.06	1.17	C						by vol
																by vol
	(Design 1700 Subject EQT and Disc Character (yes and Disc Character) (y	sision Point ID N (Designation) 1700-51 D Subject Item ID EQT0162 Ind Discharge Characteristics (Per (yes or no)) Ty Sion Point ID No. 1700-51 t te matter (PM ₁₀) oxide oxides nonoxide C (including those	sision Point ID No. (Designation) 1700-51 Discharge Characteristics e? (yes or no) Type of Fuel Type of NA Discharge Characteristics e? (yes or no) Type of Fuel Type of NA Discharge Characteristics e? (yes or no) Type of Fuel Type of NA Discharge Characteristics e? (yes or no) Type of Fuel Type of NA Discharge Characteristics e? (yes or no)	Sion Point ID No. (Designation) 1700-51 Discharge Characteristics e? (yes or no) Discharge Area (ft²) Type of Fuel Used and Heat In the standard of the s	Emissions Sission Point ID No. (Designation) 1700-51 Descriptive Name of the E Inhibitor Subject Item ID No. EQT0162 Ind Discharge Characteristics e? (yes or no) Discharge Area (ft²) Type of Fuel Used and Heat Input (see instance) Type of Fuel Used and Heat Input (see instance) Notes *1060 hrs/yr Sion Point ID No. (Designation) 1700-51 Control Equipment Code Reficiency t te matter (PM ₁₀) oxide oxides onoxide Oxides oxides onoxide Oxides oxides	Emissions Inventory Quession Point ID No. (Designation) 1700-51 Descriptive Name of the Emissions Source (Annihibitor Mix Tank Discharge Characteristics Properties	Emissions Inventory Questionnaire (Session Point ID No. (Designation) 1700-51	Emissions Inventory Questionnaire (EIQ) for Air ission Point ID No. (Designation) Inhibitor Mix Tank Method UTM Zone Latitude Longitude Long	Emissions Inventory Questionnaire (EIQ) for Air Pollutants Saison Point ID No. (Designation) Inhibitor Mix Tank	Emissions Inventory Questionnaire (EIQ) for Air Pollutants Sasion Point ID No. (Designation) 1700-51	Emissions Inventory Questionnaire (EIQ) for Air Pollutants Sasion Point ID No. (Designation) 1700-51 Inhibitor Mix Tank Method UTM Zone 15 Horizontal 739000 31 1 1 1 1 1 1 1 1	Emissions Inventory Questionnaire (EIQ) for Air Pollutants Sasion Point ID No. (Designation) (Designation) (T)0-51 (T)	Emissions Inventory Questionnaire (EIQ) for Air Pollutants Subject Item ID No. (Designation) (1700-51) (Inhibitor Mix Tank	Emissions Inventory Questionnaire (EIQ) for Air Pollutants	Emissions Inventory Questionnaire (EIQ) for Air Pollutants	Emissions Inventory Questionnaire (EIQ) for Air Pollutants

							St	tate of Lo	ouisiana									Date of	submitt	al
					Emission	s Inve	entory Q	uestionn	aire (EI	Q) for Air	r Pollutants							Nov	20	013
E		oint ID N	0.	Descrip	tive Name of the	Emissio	ons Source	(Alt. Name)		A	pproxima	te Locati	ion of Stack o	or Vent (se	e instruc	tions)		1	
		nation) 0-53	1		Stripped En	nulsion '	Tank No. 1	ĺ		Method				tching-Primary	y Name" mE	17	tical		NAD83	mN
Tem	po Subje	ct Item ID	No.							UTM Zon Latitude Longitude	30 0	5. Hori	zontal 31	739000		5 " 5 "	ucai .	332	hund	redths
	_	0163					191 R0			Longitude	-50									
Physica	and Disc al Charac age? (yes	teristics		ter (ft) or Stack arge Area (ft ²)	Height of S Above Grad	The state of the s	Stack Ga Veloc	all a second	Stack Ga Condition Standard	ns, <u>not</u> at	Stack Gas Exit Temperature (°F)		Time urs per y	0	Date of Construction Modificat	on or	Throu	ighput	of Annu Throug on Point	h This
	no	. "	-	0.167 ft ft ²	38	ft	NA	_ft/sec	NA	ft^3/min	77 °F	8,	760	_hr/yr Ju	n	1968	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
	T	Tw	no of Fue	l Used and He	t Input (acc in	otwood	one)					Onena	ting Par	rameters (in	nelude w	ite)				1
Fuel	-	l ly		of Fuel			MMBTU/h	r)	-			Opera	ung Fai	-	meter	T	D	escript	ion	
	a b			A		N/			Max	imum Operat	g Rate/Throughputing Rate/Through	hput	Ш	25,141,	bs/batch ,309 gal					
	С			Notes					_	gn Capacity/ l Height (ft)	Volume/Cylinder	Displacen	nent		22 gal .83	-				
			-	Trotes						k Diameter (f	t)				1.5	1				
								1.	Tan		Fixed Roof	F	loating Ro	oof 🗆	Ex	ternal			Int	ernal
									Date	Engine Orde	ered				Engin	Model	Year			
									Date	Engine Was	Built by Manufa									
								-	SI F	ingines:	☐ Rich I	Burn		Lean Burn		2 Stro	ke		4 Strol	ke
Emi	Emission Point ID No. (Designation) 1700-53		on) Contro Equipme Code	A STATE OF THE PARTY OF THE PAR		P/TAP Number		Propose	d Emission I	Rates	Emiss	mitted ion Rate urrent)	Add, Change, Delete, o	Com	tinuous pliance ethod	1000000		tion in (
Polluta	nt							Avera	-	Maximum (lbs/hr)	Annual (tons/yr)		nual ns/yr)	Unchange	ed	etnou				
Particul	late matte	r (PM ₁₀)																	gr/s	std ft ³
Sulfur					4														ppm	by vol
Nitroge	n oxides																		ppm	by vol
	monoxid	_																	ppm	by vol
THE R. P. LEWIS CO., Land Low, Low, Low, Low, Low, Low, Low, Low,	OC (incl	uding those	e listed belo	ow) 088	0%			<0.0		< 0.01	< 0.01	<	0.01	U						by vol
Lead																				by vol
Chlorop				088	0%		26-99-8	<0.0		< 0.01	< 0.01		0.01	U						by vol
Toluene	e			088	0%	001	08-88-3	<0.0		< 0.01	< 0.01	<	0.01	U						by vol
																			ppm	by vol

								State of	Louisia	na	-							Date of	submitt	al
						Emissions	Inventory	Question	nnaire (EIQ) for Air	Pollutants							Nov	20	013
E	mission P	oint ID N	No.	De	scriptive	Name of the l	Emissions Sour	ce (Alt. Na	me)		1	Approxim	ate Locatio	on of Stack or	Vent (see	instruc	tions)			
	16	nation)										A TOTAL CONTRACTOR							marches are	
	170	0-54				Stripped Em	ulsion Tank No	0.2		Method				ching-Primary 739000	Mame" mE	37.		Datum		mN
Tem	po Subje	ct Item II	D No.							UTM Zon Latitude	30 0	13 Hor	izontal 3		- me		tical	332	7400 hund	Iredths
A CIII	po sauje	ct item i	0 110.							Longitude			31		, 15	-				Iredths
		0164														_				123002
	and Disc			ter (ft) or Sta		Height of St	1	Gas Exit		Gas Flow at	Stack Gas Ex		mal Opera		Date of			ercent (
	al Charac age? (yes		Disch	arge Area (fi	t ²)	Above Grade	e (ft) Ve	elocity		itions, <u>not</u> at	Temperature	The state of the s	Time		nstruction Iodification		1 Transaction	ighput Emissic		The second second
Cital	iger (yes	or no)							Stand	ard (ft ³ /min)	(°F)	(no	urs per ye	ar)	Toomcan)II	- 4	Emissi	n Poin	
	no	16			- 1		- 1							. Jun		1968	Jan-		Jul-Sep	
				0.167 ft	-	38 f	t NA	ft/sec	NA	ft^3/min	77 °F	8	,760	hr/yr	1	1200	Mar	Jun	0.50	Dec
				ft^2			- 1							- 1			25%	25%	25%	25%
											<u> </u>									
		T	-		Heat L	nput (see ins			1 1			Opera	ting Par	ameters (in		its)				
Fuel	-		Туре	A A		Heat I	nput (MMBTU	J/hr)	1 1	N 10 "	D . CL			60,000 lb		-	L	escript	ion	
	h		IN.	A	_		NA		- 1	Normal Operating	The state of the s			25,141,3		-				
	C								-1 1	Maximum Operat			ment			-				
	1			No	tec		-311170			Design Capacity/ Shell Height (ft)	v oldine/Cynnde	Displace	nem	11,622		+				
				110	tes				- 1	Tank Diameter (f	1)			11.		1				
									1 1	Tanks:	Fixed Roof	F	loating Ro		Exte	ernal			Int	ernal
										Date Engine Ord			T		Engine	Model 1	Year			
										Date Engine Was		facturer								
										SI Engines:		Burn		Lean Burn		2 Stro	oke		4 Stro	ke
Em	ission Po	1700-5	. (Designati 4	Equ	ontrol cipment Code	Control Equipment Efficiency	HAP / TAP CAS Numbe		Prop	posed Emission I	Rates	Emis	rmitted sion Rate urrent)	Add, Change, Delete, or	Comp	nuous oliance thod		ncentra Exiting		
Polluta	int				3			92,00	erage o/hr)	Maximum (lbs/hr)	Annual (tons/yr)		nnual ons/yr)	Unchanged	· Me	moa				
_	late matte	r (PM ₁₀)				1	90 9	-												std ft3
-	dioxide																			by vol
	en oxides								1		-				-		-			by vol
	monoxid		F . 11 1		000	000			0.01	0.01	0.01		0.01				-		-	by vol
	OC (incli	uding tho	se listed belo	ow)	088	0%		<	0.01	<0.01	<0.01	-	<0.01	U	-		-		-	by vol
Lead Chloro	prene				000	0.0%	00126-99-8		0.01		-0.01	-	-0.01	Ü	-		-			by vol
Toluen					088	0% 0%	00126-99-8		0.01	<0.01	<0.01	_	<0.01	U	-	_	-		-	by vol
Torden					000	0.70	00100-00-3		0.01	VU.U1	20.01		.0.01	— <u> </u>			-			by vol

	(I					Sta	ate of Louisia	na							Date of	submittal
					Emissions	Inventory Qu	uestionnaire (EIQ) for Air	Pollutants						Nov	2013
E		oint ID I	No.	Descriptive	Name of the I	missions Source ((Alt. Name)		Ap	proximate Locati	on of Stack or V	ent (see	instruc	tions)		
	-	0-55			Stripped Em	ulsion Tank No. 3		Method		06,"Address Mat						NAD83
Torri	no Cubic	of Item T	D.N.					UTM Zon Latitude	e 15	Horizontal 3		mE 15		tical -	3327	400 mN hundredths
1 em	po Subje	ct Item I	D No.					Lantude		31		15				hundredths
N I I	EQT	0165						Songrado			-					
Physica	and Disc d Charac ge? (yes	cteristics		er (ft) or Stack orge Area (ft ²)	Height of St Above Grade	The second secon	ity Cond	Gas Flow at itions, not at ard (ft³/min)	Stack Gas Exit Temperature (°F)	Normal Opera Time (hours per ye	Con	Date of struction odificatio		Throu	ghput	f Annual Through This n Point
	по			0.167 ft	38 f	NA NA	ft/sec NA	ft^3/min	77 °F	8,760	hr/yr Jun		1968	Jan- Mar	Apr- Jun	Jul-Sep Oct- Dec
3				ft²						40				25%	25%	25% 25%
		T	pe of Fuel	Used and Heat I	nput (see ins	tructions)				Operating Par	ameters (incl	ude unit	ts)			
Fuel			Type of			put (MMBTU/hr)				Paramet			D	escript	on
	a		N/	4		NA			Rate/Throughput		60,000 lbs/					
PIN K	0								ing Rate/Throughp		25,141,309					
	le ,	L-		Notes				Design Capacity/ Shell Height (ft)	Volume/Cylinder I	Displacement	11,622 g 16.83		-			
				Tioles				Tank Diameter (f	1)		11.5		_	-		
							1 -	Tanks:	Fixed Roof	Floating Ro		Exter	rnal			Internal
								Date Engine Orde	ered			Engine N	Model Y	(ear		
								Date Engine Was	Built by Manufact	turer						
								SI Engines:	☐ Rich Bt	urn 🗆	Lean Burn		2 Stro	ke		4 Stroke
Em	ssion Poi	1700-5	o. (Designation	Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Prop	oosed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin	liance			ion in Gases at Stack
Polluta	nt						Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	noa			
	ate matte	r (PM ₁₀)		п												gr/std ft ³
Sulfur																ppm by vol
-	n oxides															ppm by vol
-	monoxid		se listed belov	w) 088	0%		40.01	e0.01	-0.01	-0.01	7.7	-				ppm by vol
Lead	oc (men	Julia Gio	se fisted belov	(7) 088	0%		<0.01	<0.01	<0.01	<0.01	U					ppm by vol
Chloro	orene			088	0%	00126-99-8	<0.01	< 0.01	<0.01	< 0.01	U	-				ppm by vol
Toluen				088	0%	00108-88-3	<0.01	<0.01	<0.01	<0.01	U					ppm by vol
																ppm by vol



Date	of	submittal

Nov

2013

																-			
E		Point ID N	No.	Desc	riptiv	e Name of the I	Emissions Source ((Alt. Name))			Approximate Locati	on of Stack or V	Vent (see	instruc	tions)			
	2	gnation)										22 27 22							
	170	00-56					10, 13, and 14			Method		06,"Address Mat			***		Datum		T
Ton	C	ect Item II	D.N.		Unsti	ripped Storage	Tanks Depressure	e Vent		UTM Zone Latitude	90 °	15 Horizontal 3	739000	mE 15		tical	3327	400 ml	
1 en	ipo Subje	ect Item Li	U No.								And the second second	31	0		-		_		
	RL	P0016	1							Longitude	-90	31		15	-			hundred	ins
Stack	and Dis	charge	Diame	eter (ft) or Stac	k	Height of St	ack Stack Gas	s Exit	Stack (Gas Flow at	Stack Gas Ex	xit Normal Opera	ating	Date of		P	ercent o	f Annual	
Physic	al Chara	cteristics	Disch	arge Area (ft²		Above Grade		ity	Condit	tions, not at	Temperatur	re Time	Con	struction	or	Thro	ighput '	Through T	his
Cha	nge? (yes	or no)		9.6					Standa	rd (ft ³ /min)	(°F)	(hours per ye	ear) M	odificatio	on		Emissio	n Point	1
														1		Ť	Δ=-	Jul-Sep (2-4
	no			0.167 ft		55 f	719.00	ft/sec	945	ft^3/min	77 °F	2.92*	hr/yr Aug		1972	Jan- Mar	Apr- Jun		Oct- Dec
		-	-	0.107 10		331	715.00	10300	743		11.	2.72	, im/yi	1	,	25%	25%		25%
				ft ²									1			2370	23 10	23 /0 2	570
	T	T	vpe of Fu	el Used and l	Teat	Input (see ins	structions)					Operating Par	ameters (incl	ude uni	its)				
Fuel		1		of Fuel			nput (MMBTU/hr)				o per uning r un	Parame		1	Г	escripti	on	
	a			NA			NA		N	ormal Operating	Rate/Through	put	42,000 lb/c				- Continu	011	
	b										ing Rate/Throu		NA						
	c											er Displacement	NA		_				
	-			Note	S					hell Height (ft)			NA						
			**2.	92 hr/yr combin		ting time				ank Diameter (f	t)		NA						
									T	anks:	Fixed Roof	f Floating Ro	of 🗆	Exte	rnal			Intern	al
									, D	ate Engine Orde	ered			Engine		Year			
								1	The same	THE RESERVE THE PERSON NAMED IN COLUMN 2 IS NOT THE PERSON NAMED I	Built by Manu	facturer							
										I Engines:		Burn	Lean Burn		2 Stro	ke		4 Stroke	
En	ission Po	oint ID No	. (Designat	tion) Con	trol	Control	HAP/TAP					Permitted	T						
				Equip	ment	Equipment	CAS Number		Duone	osed Emission I	Pates	Emission Rate	Add,						
		1700-56	6	Co	de	Efficiency			Frope	sed Emission F	kates	(Current)	Change,	- Control and	nuous	Con	centrat	ion in Gas	es
- II						1 1							Delete, or		thod		Exiting	at Stack	
Pollut	ant					1 1		Avera	_	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/vr)	Unchanged						
Partice	late matt	er (PM ₁₀)				-		(lb/hr	r)	(IDS/III)	(tolls/yt)	(tolis/yt)	-	-		_		- (-1)	0.3
-	dioxide	C1 (x 1+110)				 							-	-				gr/std :	
-	en oxides					1			$\overline{}$	*	 		-	-				ppm by	
-	monoxi								-		_							ppm by	_
Total '	VOC (inc	luding tho	se listed bel	ow) 0	00	0%		2178	8	2178	3.18	4.41	C	1				ppm by	
Lead																		ppm by	_
Chloro	prene			. 0	00	0%	00126-99-8	1484.	.7	1484.7	2.17	3.00	C	1		-		ppm by	
Toluer		-		0	00	0%	00108-88-3	232.2	2	232.2	0.34	0.47	С					ppm by	
												T						ppm by	vol

						Sta	ate of Louisia	na							Date of	submittal	
			*	×	Emissions	Inventory Qu	uestionnaire (EIQ) for Air	r Pollutants						Nov	2013	
E		oint ID Nonation)	0.	Descriptive	Name of the I	Emissions Source	(Alt. Name)		Ap	proximate Locat	on of Stack or V	Vent (see	instruc	tions)	-		
	170	0-57		ID.	lisobutylene (I	DIB) Storage Tank	bk	Method		06,"Address Mai	Management of the Contract of					NAD83	
Tom	no Suble	ct Item ID	No					UTM Zon Latitude	e 15		739000	mE 15		tical	332	hundred	
A CINI	po subje	ct item in	140.					Longitude		31	-	15	-		+	hundred	
	-	0166															
Physica	and Dis l Charac ge? (yes	eteristics	Diameter (f Discharge		Height of St Above Grade	The same of the sa	ity Cond	Gas Flow at itions, <u>not</u> at ard (ft³/min)	Stack Gas Exit Temperature (°F)	Normal Oper Time (hours per y	Con	Date of struction odification		Throu	ghput	of Annual- Through 7 on Point	his
	no		0.16	57 ft	10 f	t 0.09	ft/sec 0	ft^3/min	82 °F	8,760	hr/yr Jun		1972	Jan- Mar	Apr- Jun		Oct- Dec
				ft²				4						25%	25%	25%	25%
		Ty	pe of Fuel Us	ed and Heat I	nput (see ins	structions)				Operating Par	rameters (incl	ude uni	ts)	1		a rein n	
Fuel		LLO.	Type of Fu	el	Heat Ir	nput (MMBTU/hr)				Parame	ter		D	escript	on	
	a		NA			NA		Normal Operating	g Rate/Throughput		144,1801						
	b								ing Rate/Throughp		25,000 8						
-	С							The second name of the second na	Volume/Cylinder D	Displacement	2,700 g	al	-				-
				Notes				Shell Height (ft)			12		-		_		
							1 1	Γank Diameter (f	Fixed Roof	Floating Ro	8 pof	Exte	rnal			Intern	al
								Date Engine Ord		I John M.	01	Engine 1		/ear		Aitoin	-
									Built by Manufact	urer	1	Lingino	T T	Cu			
								SI Engines:	□ Rich Bu		Lean Burn		2 Stro	ke		4 Stroke	
Emi	Emission Point ID No. (Designation) 1700-57			Control Equipment Code	Control Equipment Efficiency	HAP/TAP CAS Number	Prop	osed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl Met	liance			ion in Gas at Stack	ses
Polluta	ollutant					Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	nou					
	ate matte	r (PM ₁₀)												5		gr/std	ft ³
Sulfur c												-				ppm by	_
-	n oxides		7				100					-				ppm by	
	monoxid		No. 21 1 1	000	0.00		0.00	0.00		0.11						ppm by	_
Lead	OC (inch	iding those	e listed below)	000	0%		0.02	0.02	0.11	0.11	Ü	-				ppm by	_
Lead				-					-			-				ppm by	-
				_								-				ppm by	-
									1		-	-				ppm by	_
																ppin 0)	+ 0.

															_			_	
							St	ate of Lo	uisiana	1						1	Date of	submitte	al
						Emissions	Inventory Q	uestionna	aire (E	IQ) for Air	Pollutants						Nov	. 20	13
E	nission P	oint ID N	0.	1	Descriptive	Name of the E	Emissions Source	(Alt. Name)			Ap	proximate Location	on of Stack or V	ent (see i	instruct	tions)			
		nation)		0.7															0-
	170	0-60			Diisobutyl	ene Nitrosate	(DIBN) Storage	Tank No. 3		Method		06,"Address Mato			-		Datum		
700	6.11									UTM Zone	30 0	Horizontal 3	739000	mE 15	Vert	tical	3327		mN
Tem	po Subje	ct Item II	No.							Latitude	-90 °	31		15		-			redths redths
	EQT	0168								Longitude	-90	31						nund	reduis
	and Disc		Diame	ter (ft) or	Stack	Height of Sta	ack Stack G	as Exit	Stack G	as Flow at	Stack Gas Exit	Normal Opera		Date of		P	ercent o	f Annu	al
	l Charac		Disch	arge Area	(ft ²)	Above Grade	(ft) Veloc	city		ons, not at	Temperature	Time		struction			ghput		
Chan	ige? (yes	or no)							Standar	d (ft³/min)	(°F)	(hours per ye	ar) M	odificatio	n	1	Emissic	n Point	
															1077	Jan-	Apr-	Jul-Sep	Oct-
	no		_	0.083 ft		6 f	t0.34	ft/sec	0	ft^3/min	82 °F	8,760	hr/yr Sept		1977	Mar	Jun		Dec
	4			- 2												25%	25%	25%	25%
1				ft²								(4)						-	
		Ту	pe of Fue	el Used a	nd Heat I	nput (see ins	tructions)					Operating Par	ameters (incl	ude unit	ts)			11	T.
Fuel			Type	of Fuel		Heat In	put (MMBTU/h	r)					Parame	ter		D	escript	on	
	a		N	NA.			NA			170	Rate/Throughput		4,600 lb/b						
	b								,		ing Rate/Throughp		32,900						
	С								_	THE RESERVE OF THE PERSON NAMED IN	Volume/Cylinder D	Displacement	700 ga	ıl					
				I	Notes					ell Height (ft)		1	6						
									_	nk Diameter (ft			4.5						
									-	inks:	Fixed Roof	Floating Ro	of 🗆	Exter				Int	ernal
									_	ate Engine Orde				Engine N	Model Y	ear			
											Built by Manufact		I n		2.64			164	
		TD N	(D. 1		a I	0 1 1	Win /min		SI	Engines:	□ Rich Bu		Lean Burn		2 Stro	ке		4 Stro	ке
Em	ission Poi	1700-60	. (Designat		Control Equipment Code	Control Equipment Efficiency	HAP/TAP CAS Number	1	Propos	sed Emission F	lates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin	liance		centrat Exiting		
Polluta								Averag	_	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	noa				
	late matte	r (PM ₁₀)																	std ft ³
Sulfur														-					by vol
100	en oxides													-				-	by vol
	monoxid									0.01				-					by vol
-	OC (incl	uding thos	e listed bel	ow)	000	0%		0.01		0.01	0.06	0.06	U	-		_			by vol
Lead				-					_					-					by vol
-				-		1		-	_	*	-	-		+					by vol
				-				-			-	-		-				-	by vol

						Sta	ate of Louis	iana						Da	ate of	ubmitta	l
*					Emissions 1	Inventory Qu	uestionnaire	(EIQ) for Ai	r Pollutants					N	ov	20	13
E		oint ID Nonation)	0.	Descriptive	Name of the E	missions Source	(Alt. Name)		Ap	proximate Locati	on of Stack or V	Vent (see in	nstructio	ns)			
	170	0-61		Diisobuty	lene Nitrosate (DIBN) Storage T	Tank No. 4	Method		06,"Address Mat			** **			NAD83	
Tem	po Subje	ct Item ID	No.					Latitude Longitude	30 8	Horizontal 31	-	mE 15 "		_	3327	hundr	
6: 1		0169															
Physics	and Disc d Charac ge? (yes	cteristics		ft) or Stack e Area (ft²)	Height of Sta Above Grade	The same of the sa	ity Con	ck Gas Flow at nditions, <u>not</u> at ndard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Oper Time (hours per ye	Con	Date of struction of odification		hrough	hput T	f Annua Through n Point	Thi
	no		0.0	183 ft	6 ft	0.34	ft/sec	0 ft^3/min	82 °F	8,760	hr/yr Sept		1977 N	1ar	Apr- Jun 25%	Jul-Sep 25%	Oct De 259
				ft ²											25 70	2570	
		Ty		sed and Heat I	nput (see inst	ructions)				Operating Par	ameters (incl	ude units	s)				
Fuel			Type of Fu	iel	Heat Inp	put (MMBTU/hr)	0.00			Parame			Des	cripti	on	
	b		NA		ſ	NA		Maximum Opera	Rate/Throughput ting Rate/Throughp	out	4,600 lb/b 32,900 g	gal		_	- Service		,
				Notes				Shell Height (ft)	Volume/Cylinder D	Displacement	700 ga	-					
				110105				Tank Diameter (f	(t)		4.5						
								Tanks:	Fixed Roof	Floating Ro	oof 🗆	Exterr	nal			Inte	rnal
								Date Engine Ord	ered			Engine M	Iodel Yea	r			
								Date Engine Was	Built by Manufact	turer							
				-				SI Engines:	☐ Rich Bu	arn 🗆	Lean Burn		2 Stroke			4 Strok	e
Emi	ssion Poi	int ID No. 1700-61	(Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Pr	oposed Emission l	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Continu	ance			ion in G	
Polluta	nt						Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meth	oa ,				
-	ate matte	r (PM ₁₀)														gr/s	td ft ³
Sulfur																ppm	
	n oxides					- say - Construction		W								ppm	
	monoxid							-								ppm	-
	OC (incli	iding those	listed below)	000	0%		0.01	0.01	0.06	0.06	U					ppm	
Lead								-		-						ppm	-
											-	-	_			ppm	_
									-	-						ppm	
																ppm	by v

					×		S	tate of I	Louisiana	i									Date of	submitt	al
						Emissions	Inventory (Question	maire (E	IQ) for Air	Pollut	ants							Nov	20	013
E		oint ID N	Vo.		Descriptive	Name of the	Emissions Sourc	e (Alt. Nan	ne)			App	proximate Lo	cation	of Stack or V	ent (see	instruc	tions)			
	100	0-62	- 1		Diisobuty	lene Nitrosate	(DIBN) Storage	Tank No.	5	Method					ing-Primary Na				Datum	NAD8	3
Tana	- C.Li	- 14 - T	N.N.							UTM Zon	30	15	Horizontal	1 Caban	739000	mE 15		tical	332	7400	mN Fradalas
1 em	po Subje	ct Item II	No.							Latitude Longitude			-	31		15	-				lredths lredths
	EQT	0170								Longitude				- J.Z.		- 10	-				ircutis
	and Disc			neter (ft)		Height of St		as Exit		as Flow at	Stack G	as Exit	Normal Op	perati	(ATT)	Date of		P	ercent	of Annu	ıal
	l Charac ge? (yes		Dis	charge A	rea (ft²)	Above Grad	e (ft) Velo	city		ons, not at	Tempe		Tim		2.00	struction	C 103C		-	-	h This
Chai	ge: (yes	or no)				7		1	Standar	d (ft³/min)	(")	F)	(hours pe	r yea	r) Mid	dificatio	n		Emissi	on Poin	t
	no														Sept		1977	Jan-	Apr-	Jul-Sep	Oct-
		.		0.083	ft	6	ft 0.3	4 ft/sec	0	ft^3/min	82	°F	8,760	h	иг/уг		19//	Mar	Jun	0.50	Dec
					ft ²		1	- 1									- 1	25%	25%	25%	25%
	1	70	6.17											-		1 1					
Fuel		13				nput (see in			-				Operating I	Para	meters (inch		ts)	-		• 27.27	
Fuel	2	-	Тур	ne of Fuel		Heat 1	nput (MMBTU/I	nr)	Ne	rmal Operating	Data/The	oughput		+	Paramet 4,600 lb/ba		_		escript	ion	
	b			14/3			IVA			ximum Operating			111t	-	32,900 g		-				
	c									sign Capacity/				ŀ	700 ga		-				
					Notes				_	ell Height (ft)	· Oldinor C	Junuer D	rispiacement	$\overline{}$	6		_	-			-
					2,000				1000	nk Diameter (f)			-	4.5						
										nks: 🗵		Roof	Floating	Root	f D	Exte	rnal			Int	ernal
									Da	te Engine Orde	ered					Engine 1		/ear			
				·A					Da	te Engine Was	Built by I	Manufact	urer								
			Y						SI	Engines:		Rich Bu	irn [ם כ	Lean Burn		2 Stro	ke		4 Stro	ke
Em	ission Po	int ID No 1700-62		ation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	A R	Propos	ed Emission I	lates		Permitted Emission Ra (Current)	ate	Add, Change, Delete, or	Compl	liance			tion in (
Polluta	nt					42		Aver (lb/	rage /hr)	Maximum (lbs/hr)	200000	nual s/yr)	Annual (tons/yr)		Unchanged	Met	noa				
D	ate matte	er (PM ₁₀)																		gr/	std ft ³
Sulfur																					by vol
-	n oxides			300																	by vol
	monoxid		a list- i i	alawi)	000	000			01	0.01	-	ne.	0.00	_	11						by vol
Lead	OC (inch	uding thos	se usted b	elow)	000	0%		0.1	וט	0.01	0.	.06	0.06	-	U	-		_			by vol
Cedu								-						-							by vol
						7		-			-		-	-							by vol
															V			-			by vol

					110	St	ate of Louisian	ia				-			Date of	submitta	I
					Emissions	Inventory Q	uestionnaire (F	EIQ) for Ai	r Pollutants						Nov	201	13
E	(Desig	Point ID N	lo.	Descriptive		Emissions Source	(Alt. Name)		Ap	proximate Locati			instruct		Detum	NAD92	
	170	00-63			Vent He	eader System		Method UTM Zon	e 15	06,"Address Mat Horizontal	739000	mE	Vert			NAD83	mN
Tem		ect Item II	O No.					Latitude Longitude	30 °	31	1	15 15	*			hundre	edths
Physica	and Dis	charge cteristics		(ft) or Stack ge Area (ft ²)	Height of St Above Grade		city Condit	Gas Flow at tions, not at ard (ft³/min)	Stack Gas Exit Temperature (°F)	Normal Opera Time (hours per ye	Con	Date of struction odification		Throu	ghput '	f Annua Through In Point	
	no		0.	125 ft	33.1 1	ft 6.52	ft/sec 5	ft^3/min	41 °F	1,004*	hr/yr Sept		2001	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
				ft²	V												
×		Ty		Jsed and Heat I						Operating Par	ameters (incl	ude unit	is)		,0		
Fuel	-	-	Type of l	Fuel	Heat I	nput (MMBTU/hi					Parame	ter		D	escripti	on	
	b .	Aprile 1 ₄	NA			NA	M	laximum Opera	g Rate/Throughput ting Rate/Throughp	out	NA NA NA	7 5					- 11-
	1			Notes		2		hell Height (ft)	Volume/Cylinder D	Displacement	NA NA						
		-		110165				ank Diameter (f	t)		NA		-				
							-	anks:	Fixed Roof	Floating Ro		Exter	nal			Inter	rnal
							D	ate Engine Ord	ered			Engine N	Model Y	ear			
							D	ate Engine Was	Built by Manufact	turer							
			-				S	I Engines:	□ Rich Bu	arn 🗆	Lean Burn		2 Strol	ke		4 Strok	e
Em	ission Po	1700-63	. (Designation	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Propo	osed Emission l	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl Meth	iance			ion in G at Stack	
Polluta							Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	lygett	iou				
	late matte	er (PM ₁₀)					100									gr/st	d ft ³
-	lioxide																oy vol
-	n oxides			11-24-1-1													y vol
	monoxid																oy vol
	OC (incl	uding thos	e listed below)	000	0%		5.41	*	2.72	2.18	C	-					by vol
Lead	nem e			2000	000	00104 00 0		*		212	1						by vol
Chloro				000	0%	00126-99-8	5.4	*	2.7	2.17	С	-					by vol
Toluen	е			7000	0%	00108-88-3	0.01	4.	0.01	0.01	U	-					by vol
																ppm	by vol

			-				St	tate of Lo	uisiar	na							Date of	submitt	al
						Emissions	Inventory Q	uestionna	ire (1	EIQ) for Air	Pollutants						Nov	20	13
							9 9												
E	mission P	oint ID No	0.	D	Descriptive	Name of the l	Emissions Source	e (Alt. Name)			Ap	proximate Location	on of Stack or V	ent (see	instruc	tions)			
	(Design	nation)																	
	1700	-63.1				No. 1 CD	Solution Tank			Method		06,"Address Mate			-		Datum		
70	0.11	· II TO	NT.							UTM Zon Latitude	e 15	Horizontal 3		mE 15		tical .	332	7400	mN redths
Ten	ipo Suoje	ct Item ID	1NO.							Longitude	The second second	31		15	•				redths
	EQT	0171								Longitude								Hullo	redins
	and Disc		Diame	ter (ft) or S	Stack	Height of St	ack Stack G	as Exit	Stack	Gas Flow at	Stack Gas Exit	Normal Opera	ting	Date of		P	ercent	f Annu	al
	al Charac		Disch	arge Area	(ft ²)	Above Grade	e (ft) Velo	city	Condi	itions, <u>not</u> at	Temperature	Time	1	struction	0.0000000		ighput		
Chai	nge? (yes	or no)						1	Stand	ard (ft³/min)	(°F)	(hours per ye	ar) Mo	odificatio	n		Emissi	n Poin	t
	no	1					1						Aug		1968	Jan-	Apr-	Jul-Sep	Oct-
	no	. 1	N	A ft	1	NAI	t NA	ft/sec	NA	ft^3/min	32 °F	*	hr/yr Aug	1	1900	Mar	Jun		Dec
				ft^2												25%	25%	25%	25%
					2.														
		Ty			ıd Heat L	nput (see in		,	L			Operating Par			ts)				
Fuel			Type			Heat I	nput (MMBTU/h	nr)	-				Parame		_	D	escript	ion	
ı	a		, N	IA			NA				g Rate/Throughput		20,750 lb/c	harge	-				
	D										ting Rate/Through	30.	NA		-				
	С				7.1				P-4		Volume/Cylinder I	Displacement	3,690 g	al	-				
-		*Cone	alidated		lotes	Vent Header S			- 1	Shell Height (ft)			13		-				
		Cons	ondated ur	ider EIQ INC	0. 1700-03,	vent Header S	system		-	Tank Diameter (f	Fixed Roof	Floating Ro	7.5	Exte	rnel.			Int	ernal
										Tanks: Date Engine Ord		Floating Ro	of 🗆	Engine I	2000	Vear		ш	Ciliai
						•			9-		Built by Manufac	turer		Lingine	Viouei	i cai			
									4-	SI Engines:	Rich B		Lean Burn	0	2 Stro	ke		4 Stro	ke
En	ission Poi	int ID No.	(Designati	ion) (Control	Control	HAP / TAP	T				Permitted		T					
				E	quipment	Equipment	CAS Number		Prop	oosed Emission I	Dates	Emission Rate	Add,	Conti					
		1700-63.1	1	1	Code	Efficiency			riop	Josed Ellission I	Kates	(Current)	Change,	Comp		2000	icentra		1
Pollut									_	Maximum	Annual	Annual	Delete, or Unchanged	Met			Exiting	at Stac	ek
ronut	ant							Averag		(lbs/hr)	(tons/yr)	(tons/yr)	Officialiged						
Particu	late matte	r (PM ₁₀)						(IO/III)		(IDDIAL)	(20.00.)	(001207)						gr/	std ft ³
-	dioxide	10/																	by vol
Nitrog	en oxides																		by vol
Carbon	n monoxid	е																ppm	by vol
Total '	VO€ (inch	uding those	e listed belo	ow)	088	0%		*		98.30	ile	*	С					ppm	by vol
Lead						1													by vol
Chlore					088	0%	00126-99-8	*		98.47	*	*	С	-					by vol
Toluer	ie				088	0%	00108-88-3	*		0.19	*	*	U	-		-			by vol
													1					DDII	I DV VOI

								St	ate of Lo	uisiana											Date of	submitta	d
			 			Emissions	Inve	entory Q	uestionna	aire (EI	Q) for Air	Pollu	tants			* *					Nov	20	13
E		oint ID N	lo.		Descriptive	Name of the	Emissi	ons Source	(Alt. Name)		1		Ap	proxima	te Locati	on of Stac	k or V	ent (see	instruct	tions)			
		nation) 0-63,2				No. 2 CD	Solutio	on Tank			Method			06,"Ad	dress Mat	ching-Prim	ary Na	ame"			Datum	NAD83	
									2		UTM Zon	_	15		zontal	73900		mE	Vert	tical	3327		mN
Tem	po Subje	ct Item II	No.								Latitude Longitude	-90	-		31	-		15 15		-		hundi	
		0175									Longitude				- 31	<u>.</u>						numo.	odulo
Physics	and Disc l Charac ge? (yes	eteristics		eter (ft) (harge Ar		Height of St Above Grad	100120000	Stack Ga Veloc	September 1	Stack Gas Condition Standard	ns, <u>not</u> at	Tempe	Gas Exit erature (F)	1-400	nal Opera Time urs per ye		Cons	Date of struction edification		Throu	ghput	f Annu Through n Point	This
	no		N	IA	ft	NA I	ft ,	NA	ft/sec	NA	ft^3/min	32	°F		*	hr/yr	Jul		1972	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep	Oct- Dec 25%
			_		ft ²		1					Ì								2370	23 70	2370	2570
		Ty	pe of Fu	el Used	and Heat I	nput (see ins	structi	ions)						Opera	ting Par	ameters	(incl	ude uni	ts)				
Fuel			Туре	of Fuel			nput (N	MMBTU/hr	r)								ramet			D	escripti	on	
	a b		1	NA			NA	A			nal Operating					20,75		narge					
	c										imum Operat gn Capacity/	-	- T		oent	3	NA 690 ga	al .	-				
			-		Notes						l Height (ft)	VolumerC	yunder D	rspracen	ilent	٥,	13	1,1					
		*Con	solidated u	nder EIQ		Vent Header S	ystem				Diameter (f	t)					7.5						
										Tan	ks: 🗹	Fixed	d Roof	F	loating Ro	of		Exte				Inte	rnal
											Engine Orde							Engine l	Model Y	ear			
	**										Engine Was		Manufacti Rich Bu			Lean Bui			2 Strol	le o		4 Strok	
Emi		1700-63.	(Designat	tion)	Control Equipment Code	Control Equipment Efficiency		P / TAP Number			ngines:	lates	RICH BU	Per Emiss	mitted sion Rate arrent)	Add Chang Delete	, ge,	Contin Compl	iuous iance	Con	centrat	ion in G	ases
Polluta	nt								Averag (lb/hr)		Maximum (lbs/hr)	251,210,000	nual as/yr)		nual ns/yr)	Unchar	iged	Met	nod				
	ate matter	r (PM ₁₀)																				gr/s	td ft ³
Sulfur							TV.																by vol
-	n oxides monoxide		-	-			_					-				-							by vol
-			e listed bel	ow)	088	0%			1/4		98.30	-	zje	-	sje .	C							by vol
Lead	- Cilicio	one aros	o motor bel	0.17)	000	070				_	20.30	-										_	by vol
Chlorop	rene				088	0%	001	26-99-8	*	_	98.47	1	*		*	C						-	by vol
Toluene					088	0%		08-88-3	*		0.19		*		*	U							by vol
																						ppm	by vol

The same of the sa						and the same of th														
								Sta	ate of Lou	uisiana	a							Date of	submitt	al
						Emissions	Inve	entory O	uestionna	ire (E	IQ) for Air	Pollutants						Nov	20	013
																		1407	20	,13
E.	niccion D	oint ID N			Denoulation	Name of the l	Contact	one Cour	(Ala Noma)				V		Vant (a	1	tions)			
IC.I		nation)	0.		Descriptive	rame of the l	EIIIISSI	ous source	(AIL Name)			A	Approximate Locati	on of Stack or	vent (see	instruc	uons)			
)-63.3			R	ecovered CD	Storag	ge Tank No.	. 1		Method		06,"Address Mate	ching-Primary N	lame"			Datum	NAD83	3
											UTM Zone		15 Horizontal	739000	mE		tical	332		mN
Tem	po Subje	ct Item II	No.								Latitude	30 °	3	•	15	met.			100000000000000000000000000000000000000	redths
	FOT	70176									Longitude	°	31		15	"			hund	redths
Stack	and Disc	0176	Diev	eter (ft)	or Stack I	Height of St	ack l	Stack Ga	e Evit	Stack C	as Flow at	Stack Gas Exi	it Normal Opera	ating	Date of		D	ercent	of Annu	al
	l Charac			harge Ar	Care Maraganasa	Above Grade		Veloc	NAME OF TAXABLE PARTY.		ions, not at	Temperature	- 77		nstruction	or		ighput		
	ige? (yes		Disc	nai ge Ai	ica (II)		(22)	, 0100			rd (ft ³ /min)	(°F)	(hours per ye	201	odification	ESCAL.		Emissi	_	Company of the last of the las
										1					1	1				1-0-
	no		,	NA.	ft	NA f	ft	NA	ft/sec	NA	ft^3/min	65 °F	*	hr/yr Jun		1968	Jan- Mar	Apr- Jun	Jul-Sep	Oct- Dec
,		.	-1	171		11/2		11/1	. TU SCC	14/7	11 3/11111	03 1		_111/91	1	1	25%	25%	25%	25%
			-		ft ²	10.4								*,						
	1	Tv	pe of Fr	iel Used	and Heat I	nput (see ins	struct	tions)					Operating Par	ameters (inc	lude uni	its)				
Fuel				e of Fuel	1			MMBTU/hr	r)				Francisco V and	Parame		T	D	escript	ion	
	a			NA				Α		No	ormal Operating	Rate/Throughp	ut	40,000 lt						
	ь											ing Rate/Throug		NA						
	С					1				De	esign Capacity/	Volume/Cylinder	r Displacement	8,156	gal					
	F				Notes						nell Height (ft)			15						
		*Cons	solidated	under EIC	No. 1700-63,	Vent Header S	ystem			Ta	ank Diameter (fi			10						
									*		anks: 🗵	Fixed Roof	Floating Ro	of 🗆	Exte				Int	ernal
		*									ate Engine Orde				Engine	Model '	Year			
										-		Built by Manufa		<u> </u>				- 1,20	15	
-										SI	Engines:	□ Rich		Lean Burn		2 Stro	ke		4 Stro	ke
Em	ission Po	int ID No.	(Designa	tion)	Control	Control Equipment		AP / TAP S Number					Permitted Emission Rate							
		1700-63.	3		Equipment Code	Efficiency	CAS	rumber		Propos	sed Emission F	tates	(Current)	Add, Change,		nuous	Cor	centra	tion in (Cases
														Delete, or		liance		Exiting		1000000
Polluta	nt					4 7 -			Averag	e	Maximum	Annual	Annual	Unchanged	Met	thod				
D		(2)							(lb/hr))	(lbs/hr)	(tons/yr)	(tons/yr)		-					
-	late matte	r (PM ₁₀)								e				-	+					std ft ³
Sulfur	n oxides								-					-	-		-			by vol
-	monoxid	le.					7			-				-	-		_			by vol
-		uding thos	e listed be	low)	088	0%			sk	_	98.30	*	nir	C	+		_			by vol
Lead	_ (-	20.00			1	1				-	by vol
Chloro	prene				088	0%	00	126-99-8	*		98.47	*	*	С					_	by vol
Toluen	е				088	0%		108-88-3	*		0.19	*	+	U						by vol
														1						hy vol

								State	of Louisian	na (Ti	Date of	submitt	al
				155		T2	*				D. H		34						
						Emissions	Invent	ory Questi	ionnaire (EIQ) for Ai	r Pollutants					1	Nov	20	13
E	mission P	oint ID N	lo.		Descriptive	Name of the	Emissions	Source (Alt. 1	Name)		Ap	proximate Locati	on of Stack or V	ent (see	instruc	tions)		-	
	(Desig	nation)														*			
	1700)-63.4	- 1		I	Recovered CD	Storage T	ank No. 2		Method		06,"Address Mat						NAD83	
										UTM Zon			10000	mE.	Veri	ical	3327	1.00	mN
Ten	po Subje	ct Item II	D No.							Latitude	30 8		-	15		-			redths
	FOT	20177								Longitude	-90 °	31	- '	15		-		hund	redths
Stool	and Disc	0177	Diam	otom (F6)	or Stack	Height of St		Stack Gas Exit	Ct. I	Gas Flow at	Strain G. P. It	I N		D 4 6		D.		f Annu	-1
	al Charac			arge Ar		Above Grade		Velocity		itions, not at	Stack Gas Exit Temperature	Normal Opera	1,000	Date of struction	or	4		Chroug	
1.00	ige? (yes		Disci	narge Ar	rea (III)	Above Grade	e (11)	velocity		ard (ft ³ /min)	(°F)	(hours per ye		dificatio				n Point	
									Stand	ard (ir /iiiii)	(F)	(month per)							
	no	- 1			4		-		1				Jun Jun		1968	Jan-	Apr-	Jul-Sep	12.55
			N	A	ft	NA 1	ft NA	ft/sec	NA	ft^3/min	65 °F	als.	hr/yr		1200	Mar	Jun		Dec
		1			ft ²		- 1					100	1		- 1	25%	25%	25%	25%
		Ty	pe of Fu	el Used	and Heat I	nput (see ins						Operating Par	ameters (incl	ude uni	ts)				
Fuel	1			of Fuel		Heat I	nput (MIV	IBTU/hr)					Paramet	er		D	escripti	on	
	a		1	AV			NA		1	Normal Operating	Rate/Throughput		40,000 lb/	day		- 2			
	b									Maximum Opera	ing Rate/Throughp	out	NA						
	С) i						I	Design Capacity/	Volume/Cylinder D	Displacement	8,156 g	al .					38
					Notes				S	Shell Height (ft)			15						
		*Con	solidated ur	nder EIQ	No. 1700-63,	Vent Header S	ystem		1	Fank Diameter (f	t)		10						
										Γanks: ☑	Fixed Roof	Floating Ro	of 🗆	Exte	rnal			Inte	ernal
									. 1	Date Engine Ord	ered			Engine I	Model Y	ear			
									I	Date Engine Was	Built by Manufact	turer							
										SI Engines:	□ Rich Bu	urn 🗆	Lean Burn		2 Strol	ke		4 Strol	ke
Em	ission Poi	int ID No.	. (Designat	tion)	Control	Control	HAP/	100000		*		Permitted							
		1700-63.	AT.		Equipment	Equipment	CAS No	mber	Prop	osed Emission I	Rates	Emission Rate	Add,	Contin	mous				
		1700-03.	*		Code	Efficiency		1				(Current)	Change,	Compl	Daniel Co.			ion in (
Polluta	nt							-		Manimum	T Annual	Annual	Delete, or	Meth		,	Exiting	at Stac	k
A GARAGE									(lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	(tons/yr)	Unchanged						
Particu	ate matte	r (PM ₁₀)							(AUTHA)	(((-0.00.7.)						arle	td ft ³
	lioxide	10/									 		1					-	by vol
	n oxides	*********																	by vol
Carbon	monoxide	e ,																	by vol
Total V	OC (inch	ding thos	e listed bek	ow)	088	0%			*	98.30	*	zje	C						by vol
Lead																			by vol
Chloro	orene				088	0%	00126	99-8	*	98.47	*	*	C						by vol
Toluen	2				088	0%	00108	88-3	*	0.19	*	28	U					ppm	by vol
1																		ppm	by vol

							Sta	ate of Louisia	na						T I	Date of	submitte	al
						Emissions	Inventory Qu	uestionnaire (EIQ) for Air	Pollutants					1	Nov	20	13
Er	nission P	oint ID N	lo.		Descriptive	Name of the I	Emissions Source ((Alt. Name)		App	proximate Location	on of Stack or V	ent (see in	nstruct	tions)			
		nation)									Name to the section of the section of the							
	1700	-63.5				CD H	eels Tank		Method	e 15	06,"Address Matc		mE	Mari		Datum 3327		mN
Tem	no Subjec	ct Item II	No						UTM Zone	30 0	Horizontal 3		15	Ver	ucai -	332		redths
	po ouoje.	Ct Atem 14	7110.						Longitude		31		- 15		-			redths
	EQT	0178		and the state of t														C.E.A.D.
	and Disc		Diam	eter (ft)	or Stack	Height of St	ack Stack Ga		Gas Flow at	Stack Gas Exit	Normal Opera		Date of		Pe	ercent o	f Annu	al
-	d Charac		Disc	harge Ar	rea (ft²)	Above Grade	e (ft) Veloci		litions, <u>not</u> at	Temperature	Time		struction			ghput		
Chan	ge? (yes	or no)						Stand	lard (ft³/min)	(°F)	(hours per yes	ar) Mo	dification	n		Emissio	n Point	ı
		- 1			1			92						1990	Jan-	Apr-	Jul-Sep	Oct-
	no		1	NA	ft	NA f	ft NA	ft/sec NA	ft^3/min	75 °F	ale	hr/yr Sept		1990	Mar	Jun		Dec
		- 1			-2									- 1	25%	25%	25%	25%
			· -		ft ²													100
		Ту	pe of Fu	iel Used	and Heat I	nput (see ins	structions)				Operating Para	ameters (inch	ude unit	s)				
Fuel				of Fuel		Heat I	nput (MMBTU/hr					Paramet			D	escript	on	
	а			NA			NA			g Rate/Throughput		650 lb/l	ır					
	b				f					ting Rate/Throughp	and the same of th	NA			-			
	С	L		`						Volume/Cylinder D	Displacement	8,315 g	al					
		40	21.1 1	1 FIG	Notes				Shell Height (ft)	20	W 10	14						
		*Con	solidated t	inder EIQ	2 No. 1700-63,	Vent Header S	System		Tank Diameter (f		F .: D	10	F	1			T	1
							3 N	1	Tanks:	Fixed Roof	Floating Ro	of 🗆	Exter		,		Int	ernal
									Date Engine Orde				Engine N	Model)	ear			
									SI Engines:	Built by Manufact		Lean Burn		2 Stro	lra	П	4 Stro	ke
Emi	lecion Poi	int ID No	. (Designa	tion)	Control	Control	HAP/TAP		SI Engines.	□ Alch Do	Permitted	Dean Burn		~ 5410	i e		1000	N.C
EIII	1551011 X 0	111 110 140	. (Designa	ition)	Equipment	Equipment	CAS Number				Emission Rate	Add,						
		1700-63.	.5		Code	Efficiency		Pro	posed Emission I	Rates	(Current)	Change,	Contin		Con	central	ion in (Gases
												Delete, or	Compli			Exiting	at Stac	:k
Polluta	int						i	Average	Maximum	Annual	Annual	Unchanged	1/2011		l			
Dard'an	lata matta	- (D) ()						(lb/hr)	(lbs/hr)	(tons/yr)	(tons/yr)				-			3
	late matte	(PM ₁₀)											-		-			std ft ³
	en oxides												1		-			by vol
	monoxid	le .								-	 							by vol
			se listed be	low)	088	0%		*	98.30	*	*	C			_			by vol
Lead		- 0																by vol
Chloro	prene				088	0%	00126-99-8		98.47	*		C .					-	by vol
Toluen	е				088	0%	00108-88-3	*	0.19	*	*	U					ррп	by vol
																		The State of the S

							St	ate of Louis	iana							Date of	submitt	al
						Emissions	Inventory Q	uestionnair	e (EIQ) for Ai	r Pollutants	*					Nov	20)13
E		Point ID I	No.		Descriptive	Name of the	Emissions Source	(Alt. Name)		Ap	proximate Locati	on of Stack or V	ent (see i	nstruc	tions)			
		0-63.8				Crude CD St	orage Tank No. 3	1	Method	ne 15	06,"Address Mate		me"	Vert		Datum 3327	THE RESIDENCE IN COLUMN 2 IN COLUMN 2	mN
Ten		ect Item I	D No.						UTM Zor Latitude Longitude	30 °	3 31	T	15	11	ucar .	332	hund	redths redths
Physic	and Di	cteristics		neter (ft) charge An	or Stack rea (ft²)	Height of St Above Grade		city Co	ack Gas Flow at anditions, <u>not</u> at andard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Opera Time (hours per ye	Cons	Date of truction dification		Throu	ercent o ghput ' Emissio	Throug	h This
	no	-	1		ft ft²	NA f	n NA	ft/sec	NAft^3/min	59 °F		hr/yr Mar	×	1971	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
	T	T	vne of Fr	iel Used	and Heat I	nput (see ins	tructions)		T		Operating Par	ameters (incl	ıde unit	s)				-
Fuel	-	T		e of Fuel	and Meat I		nput (MMBTU/h	r)			Operating ran	Paramet			D	escripti	on	
	a			NA			NA		Normal Operatin	g Rate/Throughput		36 MM lb	/yr				and the same	a les de centre
	b								The state of the s	ting Rate/Throughp		NA			16 17 70			
	c								AND DESCRIPTION OF THE PERSON NAMED IN COLUMN 2 IS NOT THE OWNER, THE PE	Volume/Cylinder I	Displacement	25,750 g	al					
		*C	1: 1-1-1		Notes	¥7 . 1 1			Shell Height (ft)			27		_				
		"Cor	isolidated t	under Ex	2 No. 1700-63,	Vent Header S	ystem		Tank Diameter (Floating Ro	13	Exter	nál			Int	ernal
									Tanks: Date Engine Ord		Floating Ro		Engine N	-	/ear		And	Ciriai
										s Built by Manufac	turer		Dilgino i	TOUCH I	· Cui			
		-						1	SI Engines:	Rich Bu		Lean Burn		2 Stro	ke		4 Stro	ke
Em	ission P	1700-63	. (Designa	ation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	P	roposed Emission		Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin	iance		centrat Exiting		
Polluta	int							Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meth	100				
Particu	late mat	er (PM ₁₀)														C SHOWING		std ft ³
-	dioxide																ppm	by vol
THE REAL PROPERTY.	en oxide																	by vol
	monoxi																	by vol
Street, Square,	OC (inc	luding tho	se listed be	elow)	088	0%		*	98.30	*	+	C						by vol
Lead					0.7.0	0.5												by vol
Chloro					088	0%	00126-99-8	*	98.47	*	*	C						by vol
Toluen	е				088	0%	00108-88-3	*	0.19	排	als.	U						by vol
												1		2			ppm	Uy VUI

								State of	Louisia	ana	1						Date of	submitt	tal
						Emissions	Inventory	Question	maire	(EIQ) for A	r Pollutants						Nov	20	013
E	mission P	oint ID N	0.		Descriptive	Name of the I	Emissions Sou	rce (Alt. Nar	ne)		A	pproximate Location	on of Stack or V	ent (see	instruc	tions)			
		nation)	- 1															****	
	1700	-63.9				Refined CI	Storage Tank	k		Method UTM Zo	ne 1:	06,"Address Mate 5 Horizontal	739000	mE	Ver	tical		NAD8.	mN
Tem	po Subjec	ct Item II	No.							Latitude	30 0	3		15		iicai -	332	1100000	redths
										Longitud	e -90 °	31		15	"			hund	iredths
		0182												v					
	and Disc			eter (ft) o		Height of St		Gas Exit		k Gas Flow at	Stack Gas Exit			Date of		1001		of Annu	100
	ige? (yes		Discl	iarge Ar	ea (ft*)	Above Grade	e (It)	elocity		ditions, <u>not</u> at dard (ft ³ /min)	Temperature (°F)	Time (hours per ye		struction	100000000000000000000000000000000000000			Throug	
7.20.00	0 0	0.50000						χ	Stan	dard (it /min)	(E)	(mount per)							
	no	1	N	A 4		NTA (NYA.	61	.,	602/-1	NA °F	*	Mar		1971	Jan-	Apr-	Jul-Sep	
		.	1	A f		NAf	t NA	ft/sec	N	A ft^3/min	NA °F		hr/yr	1	1	Mar 25%	Jun 25%	25%	Dec 25%
		1		f	ft ²		1				1		- H - 14			20.0	25,0	2370	20,10
	T	Ty	ne of Fu	el Used	and Heat I	nput (see ins	tructions)					Operating Par	ameters (incl	ude uni	its)				
Fuel				of Fuel	and Heat I		nput (MMBT	U/hr)	1			Operating I at	Parame		1	D	escript	ion	
	a			NA			NA		i	Normal Operation	g Rate/Throughpu	it ç.	77 MM I				-		
	b								1	Maximum Oper	ating Rate/Through		NA						
	С									Design Capacity	/Volume/Cylinder	Displacement	50,000	gal					
					Notes	-			4	Shell Height (ft)			24						
	*	*Con	solidated u	nder EIQ	No. 1700-63,	Vent Header S	System			Tank Diameter (16	¥ .					
										Tanks:		Floating Ro	of 🗆	Exte	-			Int	ternal
										Date Engine Or				Engine l	Model '	Year			
										SI Engines:	s Built by Manufac		Lean Burn		2 Stro	ka		4 Stro	le e
Fm	ission Poi	int ID No	. (Designa	tion)	Control	Control	HAP / TAP	, T		SI Engines:	□ Rich B	Permitted	Lean Burn	T	4 5110	I .		43110	ке
Zin	1381011 2 01	1700-63.		non)	Equipment Code	Equipment Efficiency	CAS Number	4	Pro	oposed Emission	Rates	Emission Rate (Current)	Add, Change, Delete, or	Comp	nuous liance	1000000		tion in	
Polluta									erage /hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	inou				
-	late matte	er (PM ₁₀)												-				-	std ft ³
-	dioxide									-				-				-	by vol
-	en oxides									-	-	-		-					by vol
-	monoxid		se listed bel	OW)	088	0%		_	*	09.30	+	*	C	-					by vol
Lead	oc (men	duling thos	e nsien nei	UW)	088	070				98.30	1		-	-				-	by vol
Chloro	prene				088	0%	00126-99-8		*	98.47	sie .	*	C	1					by vol
Toluen					088	0%	00128 99 8		*	0.19	No.	*	U	1				-	by vol
					Val.					2157			1	-				PF	hu wal

				8		St	ate of Louisi	ana						Date	of su	bmittal
					Emissions	Inventory Q	uestionnaire	(EIQ) for Air	r Pollutants					Nov	1	2013
E		Point ID N gnation)	lo.	Descripti	ve Name of the	Emissions Source	(Alt. Name)		Ap	proximate Locati	on of Stack or V	ent (see in	struction	ns)		
		0-63.10	- 4		Inhibitor Fir	nal Make-up Tank		Method		06,"Address Mat	THE RESERVE THE PERSON NAMED IN COLUMN 2 IS NOT THE OWNER.			_	-	AD83
Tom	no Subl	ect Item II) No					UTM Zon Latitude	e 15	Horizontal 3	739000	mE 15 "	Vertica	13	3274	00 mN hundredth
A CARA	po Subje	ect Item II	7140.				*	Longitude		31	a .	15 "		-		hundredth
	EQ.	Г0172		Λ		-					**					2
Physica	and Dis al Chara ige? (yes	cteristics		ter (ft) or Stack arge Area (ft ²)	Height of S Above Grad	CONTRACTOR OF THE PROPERTY OF	city Con	ck Gas Flow at aditions, <u>not</u> at adard (ft³/min)	Stack Gas Exit Temperature (°F)	Normal Opers Time (hours per ye	Con	Date of struction of odification		hroughp	ut Ti	Annual crough Th Point
	no	_	NA	Aft	NA	ft NA	ft/sec N	A ft^3/min	34 °F	+	hr/yr Jun		1968 N	in- Ap	n	ol-Sep Oc De
				ft²									2:	5% 25	%	25% 25
		Ту	pe of Fue	l Used and Heat	Input (see in	structions)				Operating Par	ameters (incl	ude units	5)			
Fuel			The second secon	of Fuel	Heat I	nput (MMBTU/hi	r)				Parame			Descr	iptio	n
	a		N	IA .		NA			g Rate/Throughput		12,000 lb/l	batch			-	10150
	Ь	-							ting Rate/Throughp		NA				_	
	lc .			Notes	1			Shell Height (ft)	Volume/Cylinder D	Displacement	22,164 g	gai				
		*Con	solidated un	ider EIQ No. 1700-6	3. Vent Header	System		Tank Diameter (f	1)		12					
						0,000	1.	Tanks:	Fixed Roof	Floating Ro		Extern	nal			Internal
				+75				Date Engine Orde	ered			Engine M	lodel Yea	r		
							1		Built by Manufact	turer						
								SI Engines:	□ Rich Bu	ırn 🗆	Lean Burn		2 Stroke		3 4	Stroke
Emi	ission Po	1700-63:1	. (Designati	on) Control Equipmen Code	Control t Equipment Efficiency	HAP / TAP CAS Number	Pro	oposed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Continu	ance			n in Gases t Stack
Polluta	int		М				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meth	od			*
_		er (PM ₁₀)														gr/std ft
-	lioxide															ppm by v
-	n oxides										-		_			ppm by v
-	monoxio		e listed belo	ow) 088	0%		sh	98.30	4	11	C	-			_	ppm by v
Lead	oc (mei	doing mos	e nated belo	(W) U88	0%			98.30	-		-		_		-	ppm by v
Chloro	prene			088	0%	00126-99-8		98.47		*	C	-			_	ppm by v
Toluen				088	0%	00108-88-3	*	0.19	*	*	U	1				ppm by v
																ppm by v

						p to		Sta	te of Louis	siana											Date of	submitt	al
						Emissions	Inven	tory Qu	estionnair	e (EIC) for Air	Polluta	ants							-	Nov	20	13
E		oint ID N	lo.		Descriptive	Name of the I	Emission	s Source (Alt. Name)				App	proxima	te Location	on of Stac	ck or V	ent (see i	instruc	tions)			
	1700-	-63.11	201			Inhibitor	Hold-up	Tank			Method					ching-Prin						NAD83	
Tem		ct Item II	D No.	SI							UTM Zon Latitude Longitude	307		Hori	zontal 3		00	mE 15		tical -	332	hund	mN redths redths
Physica	and Disc al Charac age? (yes	charge cteristics		neter (ft) charge A	or Stack rea (ft²)	Height of St Above Grade		Stack Gas Velocit	ty C	ack Gas ondition andard		Stack G	rature		Time urs per ye		Cons	Date of truction dification		Throu	ighput	of Annu Throug on Point	h This
	no		<u>.1</u>	NA	ft ft ²	NAf	t N	Af	t/sec	NA	_ft^3/min	34	°F		*	hr/yr	Jun		1968	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
		T.	ma of E	rel Hend	l and Heat I	nput (see ins	trustic		-	_				Onere	ting Por	ameters	Gnol	ido unit					
Fuel	-		-	e of Fuel				MBTU/hr)					_	Opera	ing rai	-	ramet		ls)	D	escript	on	
	a			NA		IACAT II	NA	TID I CITIL		Norm	nal Operating	Rate/Thro	oughput				000 lb/b				Cockipi	011	
	b				-					-	mum Operat			ut			NA		s.		_		
	С						-				gn Capacity/		-		nent	2	2,164 g	al					
					Notes						Height (ft)						27						
		*Con	solidated	under EI	Q No. 1700-63,	Vent Header S	ystem			Tank	Diameter (f	t)					12						
1.7									1	Tanl	s: 🗹	Fixed	Roof	F	oating Ro	of		Exter	rnal			Int	ernal
1										Date	Engine Ord	ered						Engine N	Model Y	l'ear			
					6.				-	Date	Engine Was		_										
										SI E	ngines:		Rich Bu			Lean Bu	ırn		2 Stro	ke		4 Strol	ke
Emi		int ID No 1700-63.	. (Designa	ation)	Control Equipment Code	Control Equipment Efficiency	HAP A	TAP umber	1	Proposed	Emission I	Rates		Emiss	mitted ion Rate irrent)	Ad Char Delet	nge,	Contin Compl Metl	iance	. 120.22.00		ion in (
Polluta									Average (lb/hr)	100	Aaximum (lbs/hr)	Ann (tons	California I	1000	nnual ns/yr)	Uncha	nged	Meti	iou				į.
	late matte	er (PM ₁₀)																					std ft ³
Sulfur										_						-							by vol
-	n oxides									_						_							by vol
	monoxid		na liat- d i	law's	000	00"			*	-	00.20	-			*	-							by vol
Lead	OC (Inch	uoing tho	se listed be	elow)	088	0%		-	-	_	98.30	 '		_	-	C						-	by vol
Chloro	prene				088	0%	00124	5-99-8	*	_	98.47	 	+		10.	-					-	-	by vol
Toluen					088	0%		8-88-3	*	_	0.19		k	_	*	U				,			by vol
							-010			-		1				1					-		by vol

				A		St	ate of Lo	uisiana								Date of	submitt	al
					Emissions	Inventory Q	uestionna	ire (EIQ) for Ai	r Pollutants						Nov	20	13
E		Point ID N	0.	Descriptive	e Name of the	Emissions Source	(Alt. Name)			Ap	proximate Locati	on of Stack or V	ent (see	instruct	ions)			
		00-64			Water Solut	ion Exhaust Fan			Method UTM Zon	e 15	06,"Address Mate	Name and Address of the Owner, where the Person of the Owner, where the Person of the Owner, where the Person of the Owner, where the Owner, which the Owner, where the Owner, which the Owner, w	ame"	Vert			NAD83	mN
Tem	-	ct Item II	No.		5		40		Latitude Longitude	30 °	3		15 15	н	_	332	hund	redths
Physics	and Disc al Charac age? (yes	cteristics		er (ft) or Stack rge Area (ft²)	Height of St Above Grade	780977	ity	Stack Gas Conditions Standard (, not at	Stack Gas Exit Temperature (°F)	Normal Opera Time (hours per ye	Con	Date of struction odification		Throu	ghput	of Annu Throug on Point	h This
	no		_	1.33 ft	53.6 _. 1	ft 29.80	ft/sec	2,500	ft^3/min	77 °F	8760*	hr/yr	×	1972	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
		Tv	ne of Fuel	Used and Heat I	nnut (see ins	structions)				L	Operating Par	ameters (inch	ude uni	ts)				
Fuel		~3	Type of			nput (MMBTU/hr)				opening in	Paramet			D	escripti	on	
	a b		NA			NA				Rate/Throughput ing Rate/Throughp	out	2,500 cf NA	m			1	uer-ol	AUV/LUD
	С							Desig	n Capacity/	Volume/Cylinder D	Displacement	NA				¥		
				Notes			0.		Height (ft)			NA						
				*Blower operating ti	me.				Diameter (f			. NA	-	<u></u>				- ,
								Tank		Fixed Roof	Floating Ro		Exter Engine I		200		Inte	ernal
									Engine Orde	Built by Manufact	urer	1	Engine i	viouei i	car			
									gines:	Rich Bu		Lean Burn		2 Strol	ke		4 Strol	ce
Em	ission Po	1700-64	(Designatio	n) Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number			Emission F		Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl Met	nuous liance	Con	centrat	ion in (Jases
Polluta	int						Average (lb/hr)	~	aximum lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	lylet	iiou				
Particu	late matte	r (PM ₁₀)					0.01		1.56	0.05	0.04	С					gr/s	std ft ³
Sulfur	dioxide																	by vol
-	en oxides	-	EE KUDT S														ppm	by vol
_	monoxid																ppm	by vol
Total V	OC (inch	uding those	e listed belov	v) 000	. 0%		0.025		0.13	0.11	0.11	U					ppm	by vol
Lead																		by vol
Chloro				000	0%	00126-99-8	0.02		0.02	0.08	0.08	U						by vol
Toluen	e			000	0%	00108-88-3	< 0.01		0.11	0.03	0.03	U				-		by vol
																	ppm	by vol

	A COLUMN TWO IS NOT THE OWNER.																	
							Sta	ate of Loui	siana		7			14	I	Date of	submitt	tal
					9	Emissions	Inventory Ou	uestionnair	e (EIQ) for A	ir Pollutants				2	,	Vov	20	013
															1	,0,	20	013
E	nission P	oint ID N	0.		Descriptive	Name of the I	Emissions Source	(Alt. Name)		Ap	proximate Location	on of Stack or V	ent (see i	nstruct	tions)		-	
	(Design	nation)				¥			1	•	•							
	170	0-66				Poly Build	ing Wall Fans		Method		06,"Address Mate					Datum		
TT.	0.11								UTM Z	THE PARTY OF THE P	Horizontal 3		mE 15	Vert	tical _	3327		mN
Lem	po Subje	ct Item II	No.						Latitude		31		15 15		-	-		dredths dredths
	EOT	0185							Longitu	de°	31		13		-		Hunc	aredins
	and Disc	charge	Diame	ter (ft) o	r Stack	Height of St	ack Stack Ga	s Exit S	tack Gas Flow at	Stack Gas Exit	Normal Opera	ting I	Date of		Pe	ercent o	f Annu	ual
hard to the state of the late of	d Charac	A CONTRACTOR OF THE PARTY OF TH	Disch	arge Are	ea (ft²)	Above Grade	(ft) Veloc		Conditions, <u>not</u> at	Temperature	Time		struction	0.00000				gh This
Char	ige? (yes	or no)			1			St	tandard (ft³/min)	(°F)	(hours per ye	ear) Mo	odificatio	n]	Emissio	n Poin	ıt
														1000	Jan-	Apr-	Jul-Se	p Oct-
	no	. (N/	A_fi	t I	NA f	NA NA	ft/sec 4	76,365 ft^3/mi	n 77 °F	8,760	hr/yr		1968	Mar	Jun		Dec
					, [25%	25%	25%	25%
			-	f	t*				8									
		Ту	pe of Fue	l Used	and Heat I	nput (see ins	THE RESERVE OF THE PERSON NAMED IN COLUMN 1				Operating Par	ameters (incl	ude unit	ts)	1.			
Fuel			Туре			Heat I	put (MMBTU/hr					Paramet			D	escript	ion	
	а		N	Α			NA			ing Rate/Throughput		476,365 C	FM					
	b				, a					rating Rate/Through		NA	-					
	c									ty/Volume/Cylinder I	Displacement	NA						
		4			Notes				Shell Height (f			NA						
					7.				Tank Diameter			NA						
								- 1		☐ Fixed Roof	Floating Ro	of 🛮	Exter				In	ternal
									Date Engine C	ORDER TO SELECT OR SERVICE AND ADDRESS OF THE PERSON NAMED IN COLUMN TWO IS NOT THE PERSON NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS NAMED IN COLUMN TWO IS			Engine N	Model Y	Year			
		185								as Built by Manufac		1 7		A 01			10.	
									SI Engines:	□ Rich B		Lean Burn		2 Stro	ke		4 Stro	oke
Em	ission Po	int ID No. 1700-66	. (Designati		Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	1	Proposed Emissio	n Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl	iance	0.000	centra Exiting		
Polluta	A Park						V	Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meti	hod				
-	late matte	er (PM ₁₀)															gr	/std ft ³
-	dioxide																	n by vol
_	en oxides																	n by vol
-	monoxid												-				_	n by vol
	OC (incl	uding thos	e listed belo	ow)	000	0%		6.38	53.74	27.94	27.94	U	-					n by vol
Lead							0010100	1	121		15.00							n by vol
Chloro				_	000	0%	00126-99-8	3.61	4.34	15.83	15.83	U	-		-		Terrane and the same of	n by vol
Toluen	е			-	000	0%	00108-88-3	1.19	21.19	5.19	5.19	U	-		-		100	n by vol

				E A		S	tate of L	ouisiana									Date of	submittal	
					Emissions	Inventory (Pollutan	ts					7	Nov	201	3
E	nission I	Point ID N	No.	Descripti	ve Name of the	Emissions Source	e (Alt. Nam	e)	T		Approx	cimate Locati	on of Stack or V	ent (see	instruc	tions)			
		gnation) 00-67	-		Stripped Em	ulsion Tank No.	4		Method				ching-Primary N					NAD83	
Tem	po Subje	ect Item I	D No.						UTM Zon- Latitude Longitude	30 8	15	Horizontal 3		mE 15	**	tical -	332	hundre hundre	
	EQ	ГО186							Longitude						-			numar.	
Physica	and Dis I Chara ge? (yes	cteristics		ter (ft) or Stack arge Area (ft ²)	Height of S Above Grad	The state of the s	the state of the s	Conditio	ns, <u>not</u> at l (ft³/min)	Stack Gas I Temperatu (°F)	ure	Normal Opera Time (hours per ye	Con	Date of struction odification		Throu	ghput	of Annua Through on Point	
	no		-	0.167 ft	38	ft NA	_ft/sec	NA	ft^3/min	77 °F		8,760	hr/yr Jun		1968	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
			<u> </u>	ft²															
		Ty		el Used and Heat							Op	erating Par	ameters (incl	ude uni	ts)	- 1	Jul		
Fuel				of Fuel	Heat I	nput (MMBTU/l	nr)	-					Parame	-	-	D	escript	ion	_
	b			IA (NA		Ma	mal Operating kimum Operat	ing Rate/Thro	oughput		60,000 lbs/ 25,141,30	9 gal					
	С								ign Capacity/	Volume/Cylin	der Displ	acement	11,622 8		-				
				Notes					ll Height (ft)				16.83						
									k Diameter (f	Fixed Ro	of	Floating Ro	11.5 of	Exte	rnal	-		Inter	mal
				9					e Engine Orde		101	1 loating Ro	01 🔟	Engine 1		rear .		Airto	Title .
			**				- 1		e Engine Was		ufacturer			Tangino .	T	-			
1	Sec.				92				Engines:		ch Burn		Lean Burn		2 Stro	ke		4 Stroke	е
Em	ssion Po	1700-67	. (Designat	Control Equipmen Code	Control Equipment Efficiency	HAP/TAP CAS Number		Propose	ed Emission F	lates	Е	Permitted mission Rate (Current)	Add, Change, Delete, or	Contin	liance			tion in G	
Polluta	nt						Avera (lb/h	0	Maximum (lbs/hr)	Annual (tons/yr		Annual (tons/yr)	Unchanged	Met	nod				
-		er (PM ₁₀)																gr/st	
Sulfur																		ppm b	-
-	n oxides						-							-				ppm l	
	monoxio				- 65		-		2.6			0.51		-				ppm l	
-	OC (incl	uding tho	se listed bele	ow) 088	0%	-	<0.0)1	<0.01	< 0.01		<0.01	U	-					y vol
Lead	orana			OPP	0.07	00126 00 0	-0.0	11	-0.01	.0.01		-0.01	7.7	-				ppm l	-
Chloro				088	0%	00126-99-8 00108-88-3	<0.0		<0.01	<0.01		<0.01	U	-					y vol
Toruell				088	0%	00108-88-3	<0.0	11	<0.01	<0.01		< 0.01	U	-				-	oy vol
																		ppin	Jy YUI

	State of Louisiana														1	Date of submittal				
											5					1	Late of Boothitten			
	Emissions Inventory Questionnaire (EIQ) for Air Pollutants																Nov	20	013	
TC:	nission P	oint ID N	lo T		Descriptive	Name of the l	Emissions Source	(Alt Name)		Approximate Location of Stack or Vent (see instructions)										
(Designation)					Descriptive	rame of the	Emissions Source	(All. Name)	Approximate Location of Stack or Vent (see Instructions)											
1700-68						ulsion Tank No. 5			Method 06,"Address Matching-Primary Name"							Datum NAD83				
									UTM Zone		739000	rtical 3327400 mN								
Tempo Subject Item ID No.										Latitude 30 ° 3				15 " hundredths					lredths	
								Longitude°			31 '			5 " hundredths						
EQT0187																				
Stack and Discharge Diameter				0.00		Height of Stack Stack C					Stack Gas Exit	Normal Opera		Date of Construction or			Percent of Annual			
Physical Characteristics Change? (yes or no) Disc			charge A	rea (ft*)	Above Grade (ft) Velocity		ity	Condition		Temperature	Time (hours per ye	SWIMS I		odification		Throughput Through This Emission Point				
				_			Standard ((It /min)	(°F)	(nours per ye	171	navancation			Emission Form				
no										ft^3/min	77_°F		Jul		1968	Jan-	Apr-	Jul-Sep	Oct-	
			_	0.167	ft	38 f	t NA	ft/sec	NA			8,760	hr/yr	1900		Mar	Jun		Dec	
					-7											25%	25%	25%	25%	
				ft ²		v														
Fuel	Type of Fuel Used and Heat Input (see instructions)								Operating Parameters (include units)											
	Type of Fuel			el Heat Input (MMBTU/hr)			•)					Parameter			Description					
	a NA			NA				Norn	nal Operating	l Operating Rate/Throughput			60,000 lbs/batch							
	ь								Maximum Operating Rate/Throughput				25,141,30	25,141,309 gal			4			
	С									Design Capacity/Volume/Cylinder Displacement 11,622 gal										
Notes									Shell Height (ft) 16.83											
,								Tank Diameter			t)	11.5		45						
K									Tanl	Tanks: Fixed Roof Floating Roof			of 🗆	External Internal					ternal	
									Date Engine Ordered					Engine Model Year				(4)		
									Date Engine Was Built by Manufacturer											
									SI Engines: Rich Burn			ırn 🗆	Lean Burn	n Burn 🗆 2 Str			oke 4 Stroke			
Emission Point ID No. (Designation) 1700-68				ation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number		Proposed	l Emission Rates		Permitted Emission Rate (Current)	Add, Change, Delete, or	Continuous Compliance		Concentration in Gases Exiting at Stack				
Pollutant					141			Averag (lb/hr)		laximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged Method							
Particulate matter (PM ₁₀)							-										gr/	std ft ³		
Sulfur dioxide																ppm by vol				
Nitrogen oxides											1 × V				ppm by vol		by vol			
Carbon	monoxid	le								4.0							ppm by vol		by vol	
Total VOC (including those listed below			elow)	088	0%		< 0.01		<0.01	< 0.01	<0.01	U			ppm by vol					
Lead						NO									ppm by vol					
Chloroprene					088	0%	00126-99-8	< 0.01		< 0.01	< 0.01	< 0.01	U			ppm by vol			by vol	
Toluene					088	0%	00108-88-3	<0.01		< 0.01	< 0.01	< 0.01	U			ppm by vol				
											1	1				1		nnn	hu vol	

							S	tate of I	onisia	na					_	- I	Date of	submitt	al
						Emissions				EIQ) for Air	Pollutants						Nov	20	13
																1			
E	nission I	Point ID N	lo.		Descriptive	Name of the	Emissions Source	(Alt. Nan	ne)		Ap	proximate Locati	on of Stack or V	ent (see	instruc	tions)		-	
		(nation)																	
	170	00-69	- 1			Stripped Em	ulsion Tank No. 9	9		Method		06,"Address Mat						NAD83	
Town	- Cult	ct Item II	D.NI-							UTM Zon Latitude	e 15	Horizontal 3	739000	mE 15		tical _	332	AND THE STATE OF	mN redths
rem	po Subje	ct item ii	D 140.							Longitude		31	-	15					redths
Arr -	EQ7	го188								Longitude			-	- 10		-		mono	roduis
Stack	and Dis	charge	Dian	neter (ft)	or Stack	Height of St	tack Stack G	as Exit	Stack	Gas Flow at	Stack Gas Exit	Normal Opera	ating	Date of		Pe	ercent o	f Annu	al
		cteristics	Disc	charge A	rea (ft²)	Above Grad	e (ft) Velo	city		itions, <u>not</u> at	Temperature	Time	7.11	struction			-	Throug	
Chan	ge? (yes	or no)						1	Stand	lard (ft³/min)	(°F)	(hours per ye	ear) Mo	odificatio	n]	Emissic	n Point	t
7.					-		1	1								Jan-	Apr-	Jul-Sep	Oct-
7	no	.		0.167	ft	38	ft NA	ft/sec	NA	ft^3/min	77 °F	8,760	hr/yr Jul	-	2007	Mar	Jun		Dec
															. [25%	25%	25%	25%
		- 1	_		ft ²			- 1											
		Ту	pe of F	iel Used	and Heat I	nput (see ins	structions)					Operating Par	ameters (incl	ude uni	ts)				
Fuel				e of Fuel			nput (MMBTU/h	r)					Paramet	ter		D	escript	on	
	а	п_		NA			NA			Normal Operating	Rate/Throughput		60,000 lbs/	batch					
	b		*							Maximum Operat	ing Rate/Through	put	25,141,309	9 gal			,		
199	С									Design Capacity/	Volume/Cylinder I	Displacement	16,000 g	gal					
			3		Notes					Shell Height (ft)			20.75						
										Tank Diameter (fi			12						
								1		Tanks:	Fixed Roof	Floating Ro	of 🗆	Exte				Inte	ernal
										Date Engine Orde				Engine 1	Model Y	ear			
										The same of the sa	Built by Manufac				2.0			10: 1	
			(F) 1							SI Engines:	□ Rich B		Lean Burn		2 Stro	ke		4 Strol	ke
Emi	ssion Po	1700-69		ation)	Control Equipment Code	Control Equipment Efficiency	HAP/TAP CAS Number		Prop	oosed Emission R	lates	Permitted Emission Rate (Current)	Add, Change,	Contin	S. Accomply and the			ion in C	
Polluta	nt							Avei (lb/		Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Delete, or Unchanged	Met	hod	ľ	Extring	at Stac	K
Particul	ate matte	r (PM ₁₀)						, , , , ,										gr/s	std ft ³
Sulfur c																		-	by vol
Nitroge	n oxides		V					1 1		e in ordinal restaura								ppm	by vol
	monoxid																	ppm	by vol
	OC (incl	uding thos	e listed be	elow)	088	0%		<0.	.01	< 0.01	<0.01	<0.01	U					ppm	by vol
Lead																			by vol
Chlorop					088	0%	00126-99-8	<0.		<0.01	<0.01	<0.01	U						by vol
Toluene					088	0%	00108-88-3	<0.	.01	<0.01	<0.01	<0.01	U	_				THE OWNER WHEN PERSON NAMED IN	by vol
												1						ppm	by vol

								State of	Louisia	ına								Date of	submitt	al
					4,	Emissions	Inventory	Question	nnaire ((EIQ) for Ai	r Pollu	tants						Nov	20)13
E	nission P (Design	oint ID N	lo.		Descriptive	Name of the l	Emissions Sou	irce (Alt. Na	me)	- 1		Ap	proximate Location	on of Stack or	Vent (see	instruc	tions)			
		0-70				Stripped Emu	lsion Tank N	0. 11		Method			06,"Address Mato	hing-Primary N	ame"			Datum	NAD83	3
										UTM Zor		15	Horizontal	739000	mE		tical		7400	mN
Tem	po Subje	ct Item II	D No.							Latitude	30	-	3		15					redths
	EQT	0189								Longitude	-90	-	31		15				hund	redths
	and Disc		Diam	eter (ft) o	r Stack	Height of St		k Gas Exit		Gas Flow at		Gas Exit	Normal Opera	(6)	Date of			ercent o		
100	d Charac	and the state of	Disc	harge Are	ea (ft²)	Above Grad	e (ft)	elocity		litions, <u>not</u> at		erature	Time		struction	0.350		ighput '		State of the state
Chai	ige? (yes	or no)			- 1				Stand	dard (ft³/min)	(,	F)	(hours per ye	ar) M	odificatio	n		Emissio	n Poin	
	200	- 1									1			Jul		2007	Jan-	Apr-	Jul-Sep	Oct-
	no	. 1	_	0.167 f	t .	38	t NA	ft/sec	N/	ft^3/min	77	°F	8,760	hr/yr		2007	Mar	Jun		Dec
					t ²						1			1			25%	25%	25%	25%
			_															4		
		Ty			and Heat I	nput (see in							Operating Par			ts)				
Fuel			THE RESERVE OF THE PERSON NAMED IN	of Fuel		Heat I	nput (MMBT	U/hr)						Parame			D	escript)	ion	
	a			NA			NA		-	Normal Operation				60,000 lbs		-				
	D .								-	Maximum Opera				25,141,30		-				
	Ic .				Ninter				-	Design Capacity	Volume/C	yunder L	Displacement	16,000 20.75		-				
					Notes				-	Shell Height (ft) Tank Diameter (6)			12	,	-				
					-				1	Tanks:	-	d Roof	Floating Ro		Exte	rnal			Int	ernal
										Date Engine Ord		1	1 Journa Act		Engine 1	-	Year		A.I.	orrita.
										Date Engine Wa		Manufact	turer	T	IB					
										SI Engines:		Rich Bu		Lean Burn		2 Stro	ke		4 Stro	ke
Em	ission Poi	int ID No	. (Designa	tion)	Control	Control	HAP/TA	P					Permitted							
					Equipment	Equipment	CAS Numb	er	Pro	posed Emission	Rates		Emission Rate	Add,	Contin					
		1700-70)	- 1	Code	Efficiency			110	poseu Emission	ra tes		(Current)	Change,	Comp			ncentra		
Polluta		101							40.00000	Maximum	T Av	nual	Annual	Delete, or Unchanged	Met			Exiting	at Stac	:k
r onuts				- 1				The state of the s	erage o/hr)	(lbs/hr)	1500000	ns/yr)	(tons/yr)	Officialiged						
Particulate matter (PM ₁₀)										, , , , ,	1								gr/	std ft ³
	dioxide	107											1							by vol
Nitroge	en oxides																			by vol
Carbon	monoxid	е							D 0										ррп	by vol
Total V	OC (inch	uding tho	se listed be	low)	088	0%		<	0.01	<0.01	<	0.01	<0.01	U					ppm	by vol
Lead						н Т														by vol
Chloro					088	0%	00126-99-		0.01	<0.01		0.01	<0.01	U	-				_	by vol
Toluen	е				088	0%	00108-88-	3 <	0.01	<0.01	-	0.01	<0.01	U	-		-			by vol

-	-	-																	
					*:		St	ate of Lo	ouisiar	na		10				I	Date of	submitta	al
					Emissions	Invent	ory Q	uestionn	aire (l	EIQ) for Air	r Pollutants					1	Nov	20	13
E	mission F	Point ID N	No.	Descriptive	Name of the I	Emissions	Source	(Alt. Name))		Ap	proximate Locati	on of Stack or	Vent (see	instruct	ions)			
		(nation)																	
	170	00-71	- 1		Stripped Emu	dsion Tan	k No. 12	2		Method		06,"Address Mate						NAD83	
Tom	no Cubia	ct Item I	D NI-							UTM Zon Latitude	e 15	Horizontal 3	739000	_mE 15	Vert	ical _	332	400 hundi	mN
1 em	ipo Suoje	ct Item I	D No.							Longitude	The state of the s	31	*	15		-		hundi	
	EQT	го190								Longitude	-90			. 13		-		Hullul	eduis
	and Dis		Diameter	r (ft) or Stack	Height of St	ack S	tack Ga	as Exit	Stack	Gas Flow at	Stack Gas Exit	Normal Opera	ting	Date of		Pe	ercent c	f Annu	al
The second second	al Charac	The state of the s	Dischar	ge Area (ft²)	Above Grade	e (ft)	Veloc	ity	Condi	itions, <u>not</u> at	Temperature	Time		struction			- A	Through	
Char	ige? (yes	or no)							Standa	ard (ft ³ /min)	(°F)	(hours per ye	ar) M	odificatio	n	. 1	Emissio	n Point	
		- 1		1		1		. 1						1	F	Jan-	Apr-	Jul-Sep	Oct-
	no	22	().167 ft	38 f	t NA		ft/sec	NA	ft^3/min	77 °F	8,760	hr/yr Jul		2007	Mar	Jun	оп оср	Dec
1														,		25%	25%	25%	25%
				ft²		1													
7		Ty	pe of Fuel	Used and Heat I	nput (see ins	truction	s)					Operating Par	ameters (incl	ude uni	ts)				
Fuel			Type of	Fuel	Heat Ir	aput (MM	BTU/hr	r)					Parame	ter		D	escript	on ,	
	а		NA			NA			N	Normal Operating	Rate/Throughput		60,000 lbs/	/batch					
	b	OC 1							N	Maximum Opera	ing Rate/Through	put	17,287,06	9 gal					
	С		\$7						I	Design Capacity/	Volume/Cylinder I	Displacement	16,000	gal					
				Notes					S	Shell Height (ft)			20.75	5	1				
									Т	Tank Diameter (f	t)		12						
									7	Tanks:	Fixed Roof	Floating Ro	of 🗆	Exte	rnal			Inte	ernal
									Ī	Date Engine Orde	ered			Engine !	Model Y	ear			
								l	I	Date Engine Was	Built by Manufact	turer							
				2.54					5	SI Engines:	□ Rich B	urn 🗆	Lean Burn		2 Strol	ke		4 Strol	ce
Em	ission Po	1700-71	. (Designation	Control Equipment Code	Control Equipment Efficiency	HAP / CAS Nu			Prop	osed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin	liance			ion in C	
Polluta	int					* 7		Averag	_	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	noa				
Particu	late matte	er (PM ₁₀)																gr/s	td ft ³
Sulfur	dioxide																		by vol
	en oxides																	ppm	by vol
-	monoxid																	ppm	by vol
_	OC (incl	uding thos	se listed below	088	0%			< 0.01	1	< 0.01	< 0.01	< 0.01	U					ppm	by vol
Lead																		ppm	by vol
Chloro				088	0%	00126-		< 0.01		< 0.01	<0.01	< 0.01	U					ppm	by vol
Toluen	e	-		088	0%	00108-	88-3	< 0.01	1	<0.01	<0.01	< 0.01	U						by vol
																		ppm	by vol

						Sta	ate of Louis	iana							Date of	submitt	al
					Emissions	Inventory Qu	uestionnaire	e (EIQ) for A	ir Pollutants						Nov	20	13
E	nission P	oint ID N	lo.	Descriptive	Name of the E	Emissions Source	(Alt. Name)		Ap	pproximate Locati	on of Stack or V	ent (see i	instruct	tions)			
	(Design	The state of the s						at the second									
	170	0-72			Stripped Emu	lsion Tank No. 15	5	Method	ne 15	06,"Address Mat		mE	37		Datum		
Tem	no Subject	ct Item II) No.					UTM Zo Latitude	30 °	5 Horizontal 3		15	Vert	ncai -	3327		mN redths
x em	po Subjec	ct Item A	No.					Longitud		31		15		-			redths
	EQT	0191												-			
	and Disc		Diameter (ft) or Stack	Height of Sta	ack Stack Ga	s Exit Sta	ack Gas Flow at	Stack Gas Exit	Normal Opera	ating]	Date of		P	ercent o	f Annu	al
	d Charac		Discharge	Area (ft²)	Above Grade	(ft) Veloc		onditions, not at	Temperature	Time		struction	1 40000		ghput		SUN TO A PERSON NAMED OF
Chan	ge? (yes	or no)					Sta	andard (ft³/min)	("F)	(hours per ye	ear) Mo	dificatio	n		Emissio	n Point	L.
		- 1				100	1				1.1	- 1	2007	Jan-	Apr-	Jul-Sep	Oct-
	no	.]	0.1	67 ft	38 f	t NA	ft/sec	NA ft^3/min	77 °F	8,760	hr/yr Jul		2007	Mar	Jun		Dec
				ft ²			1.			1			1	25%	25%	25%	25%
		Ty		sed and Heat I		The second secon		У.		Operating Par			ts)				
Fuel			Type of Fu	ıel	Heat In	iput (MMBTU/hr	7)				Paramet			D	escripti	on	
	a		NA			NA			ng Rate/Throughput		60,000 lbs/l		-				
	D	*						2	ating Rate/Through		17,287,069		-				
	С	3		27					/Volume/Cylinder I	Displacement	10,000 g	al	-				
				Notes				Shell Height (ft)			20.75						
							[Tank Diameter		Floating Ro	12	Exter				T-4	ernal
								Tanks:		Floating Ro	of 🗆	Engine N		laar		ш	emai
								Date Engine Or	as Built by Manufac	oturar		Eligine I	VIOUEI I	Cai			
								SI Engines:	Rich B		Lean Burn		2 Stro	ke		4 Stro	ke
Em	ission Poi	int ID No	(Designation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	P	roposed Emission		Permitted Emission Rate (Current)	Add, Change,	Contin		Соп	centrat	ion in (Gases
Polluta	nt			_			Average	Maximum	Annual	Annual	Delete, or Unchanged	Compl Metl			Exiting	at Stac	k
							(lb/hr)	(lbs/hr)	(tons/yr)	(tons/yr)	Chamber						
***	late matte	r (PM ₁₀)															std ft ³
Sulfur																	by vol
-	n oxides		PC PC			-4		1							,		by vol
	monoxid																by vol
-	OC (inch	uding thos	se listed below)	088	0%		<0.01	<0.01	<0.01	<0.01	U	-					by vol
Lead				000	000	00126 00 9		-0.00	<0.01	(0.01	- 11	-					by vol
Chloro				088	0%	00126-99-8 00108-88-3	<0.01	<0.01	<0.01	<0.01	U	-		-			by vol
Toruell				000	070	00100-00-3	<0.01	<0.01	<0.01	70.01	0	-					by vol

		15				Sta	ate of Louis	iana							Date of	submittal	
					Emissions	Inventory Qu	uestionnaire	(EIQ) for A	ir Pollutants						Nov	2013	
E		Point ID N	0.	Descriptive	Name of the	Emissions Source	(Alt. Name)		Ap	proximate Locati	on of Stack or V	ent (see	instruc	tions)			
		00-73		91	Stripped Emu	dsion Tank No. 16	i	Method		06,"Address Mat	The second live and the se			-		NAD83	
Tem		ect Item II	No.					UTM Zo Latitude Longitud	30 °	Horizontal 3		mE 15		tical	332	hundred hundred	ths
Physica	and Dis	cteristics		ter (ft) or Stack arge Area (ft ²)	Height of St Above Grad		ity Con	ck Gas Flow at nditions, <u>not</u> at ndard (ft³/min)	Stack Gas Exit Temperature (°F)	Normal Opera Time (hours per ye	Con	Date of struction odification		Throu	ghput	of Annual Through T on Point	his
	no	-	*:	0.167 ft	38 1	n NA	ft/sec N	IA ft^3/min	77 °F	. 8,760	hr/yr Jul		2007	Jan- Mar 25%	Apr- Jun 25%		Dec 25%
	T	Ty	pe of Fue	l Used and Heat l	nput (see in	structions)		T		Operating Par	ameters (incl	ude uni	ts)	7777		<u></u>	
Fuel			Type			nput (MMBTU/hr	•)				Paramet	-		D	escript	ion	
	а		N	A		NA		Normal Operation	g Rate/Throughput		60,000 lbs/	batch			- 1		
100	b				× 2				ating Rate/Throughp		17,287,069	The second second					
	С								/Volume/Cylinder I	Displacement	10,000 g	gal					
				Notes				Shell Height (ft)			20.75						
				*		8	-	Tank Diameter (12	-					-
								Tanks:		Floating Ro	of 🗆	Exte				Intern	al
				1				Date Engine Or				Engine l	Model)	(ear			-
							1		s Built by Manufac		Lean Burn		2 Stro	les		4 Stroke	
Em	ission Po	1700-73	(Designati	on) Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Pr	SI Engines:		Permitted Emission Rate (Current)	Add, Change,	Contin	nuous	Con	centra	tion in Gas	ses
Polluta	int	50				_	Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Delete, or Unchanged	Met	hod		Exiting	at Stack	
Particu	late matte	er (PM ₁₀)														gr/std	ft ³
Sulfur	dioxide															ppm by	
Nitroge	en oxides															ppm by	vol
-	monoxi															ppm by	
NAME AND ADDRESS OF TAXABLE PARTY.	OC (inc	luding thos	e listed belo	w) 088	0%		<0.01	<0.01	< 0.01	<0.01	U					ppm by	
Lead																ppm by	_
Chloro				088	0%	00126-99-8	<0.01	<0.01	<0.01	<0.01	U	-				ppm by	
Toluen	e			088	0%	00108-88-3	<0.01	< 0.01	<0.01	<0.01	U	-				ppm by	
																ppm by	vol

Latitude 30 % 3									State of	Louisia	ına							Date of	submitt	al
Part Part							Emissions	Inventor	y Questio	nnaire	(EIQ) for Air	Pollutants						Nov	20)13
Trop Trop	E			0.	-	Descriptive	Name of the	Emissions S	ource (Alt. Na	ame)	-	Ap	proximate Location	on of Stack or V	ent (see	instruc	tions)			
Latitude						Fini	shing Stabiliz	er Make-up	Bag Filter	ř	The second secon					37				
Stack and Discharge Physical Characteristics Discharge Aren (ft) Above Grade (ft) Velocity Conditions, not at Standard (ft /min) Temperature (Ft) control (Ft) Percent of Annual (Ft) Physical Characteristics Physical	Tem	po Subje	ct Item II	No.								30 °					tical	332	A CONTRACTOR OF THE PARTY OF TH	mN redths
Stack and Discharge Discharge (ft) or Stack Discharge Area (ft) Above Grade (ft) Above Grade (ft) Above Grade (ft) Velocity Conditions, not at 1 Temperature (ft) Te		FOT	0193								Longitude	°	31		15				hund	redths
Standard (it/min) Final Final Standard (it/min) Final Fina		and Disc	charge				CANADA AND AND AND AND AND AND AND AND AN	100 (0.0) The contract of the				State of the state	the same of the sa			or				AL CONTRACTOR
Notes			The state of the s	Disci	iarge Ar	rea (ft")	Above Grad	e (II)	velocity											
Type of Fuel Used and Heat Input (see instructions)		no	.	_	0.67	ft	25	ft	30.00 ft/sec	1,20	00 ft^3/min	77_°F	aje	hr/yr Jul		2007	Mar	Jun		Oct- Dec 25%
Full				_													2570	2370	2570	2376
Normal Operating Rate/Throughput Normal Operation of Normal Operation Nor			Ту			and Heat I							Operating Par			ts)				
Maximum Operating Rate/Throughput Design Capacity/Volume/Cylinder Displacement NA	Fuel						Heat I	nput (MMB	TU/hr)								D	escript	on	
Design Capacity/Volume/Cylinder Displacement		a		1	NA.		FI	NA			Normal Operating	g Rate/Throughput		3,000 cfi	n			- 65	-	
Shell Height (ft)		b			(1						Maximum Operat	ting Rate/Throughp	out	NA						
Tank Diameter (ft)		С									Design Capacity/	Volume/Cylinder I	Displacement	NA						
Tanks: Fixed Roof Floating Roof External Internal Inte						Notes					Shell Height (ft)									
Date Engine Ordered Date Engine Was Built by Manufacturer SI Engine Was Built by Manufacturer SI Engine Was Built by Manufacturer SI Engine Was Built by Manufacturer SI Engine Was Built by Manufacturer SI Engine Was Built by Manufacturer SI Engines: Rich Burn Lean Burn 2 Stroke 4 Stroke 4 Stroke Remitted Remitte						*214 hr/yr		Maria de la companya			Tank Diameter (f	t)		NA			,			
Date Engine Was Built by Manufacturer											Tanks:	Fixed Roof	Floating Ro	of 🗆	Exte	rnal			Int	ernal
Emission Point ID No. (Designation) 1700-74 Code Control Equipment Code Efficiency Proposed Emission Rates Code Average (lb/hr) (lbs/hr) (lbs/hr) Carbon monoxide Carbon monoxide Carbon monoxide Carbon monoxide Control Equipment Code Efficiency Proposed Emission Rates Proposed Emission Rates Proposed Emission Rates Current) Add, Change, Delete, or Unchanged Continuous Compliance Method Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Control Compliance Method Continuous Compliance Method Control Compliance Method Continuous Compliance Method Control Compliance Method Continuous Compliance Method Control Compliance Method Continuous Compliance Method Control Compliance Method Control Compliance Method Control Compliance Method Continuous Compliance Method Control Compliance Metho											Date Engine Orde	ered			Engine l	Model Y	(ear			
Emission Point ID No. (Designation) 1700-74 Code Code Control Equipment Code Efficiency Code Average (Ib/hr) (Ibs/hr)										Date Engine Was	Built by Manufact	turer								
Equipment Code Cas Number Proposed Emission Rates Emission Rate (Current) Change, Delete, or Unchanged Concentration in Ga Exiting at Stack Continuous Compliance Method Change, Delete, or Unchanged Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Continuous Compliance Method Concentration in Ga Exiting at Stack Continuous Compliance Method Continuous Compliance Method Continuous Compliance Method Continuous Compliance Method Continuous Compliance Method Continuous Compliance Method Continuous Compliance Method Continuous Compliance Method Continuous Compliance Method Continuous Compliance Method Continuous Compliance Method Continuous Compliance Method Continuous Compliance Method Continuous Continuous Compliance Method Continuous Contin											SI Engines:	Rich Bu	urn 🗆	Lean Burn		2 Stro	ke		4 Stro	ke
Average (lb/hr) (lbs/hr) (tons/yr) (tons/yr) Particulate matter (PM ₁₀) 018 99% 0.023 0.023 0.001 0.01 C gr/std Sulfur dioxide Nitrogen oxides Carbon monoxide Total VOC (including those listed below) Lead Chloroprene	Em	ission Po			tion)	Equipment	Equipment	7		Pro	posed Emission I	Rates	Emission Rate	Change,	Comp	liance				
Sulfur dioxide ppm b Nitrogen oxides ppm b Carbon monoxide ppm b Total VOC (including those listed below) ppm b Lead ppm b Chloroprene ppm b	Polluta	int							1.75					Unchanged	Met	noa				
Sulfur dioxide ppm by Nitrogen oxides ppm by Carbon monoxide ppm by Total VOC (including those listed below) ppm by Lead ppm by Chloroprene ppm by	Particu	late matte	er (PM ₁₀)			018	99%		0	0.023	0.023	0.001	0.01	C					gr/	std ft ³
Carbon monoxide ppm b Total VOC (including those listed below) Lead ppm b Chloroprene ppm b	Sulfur	dioxide																		
Total VOC (including those listed below) Lead Chloroprene ppm by ppm by ppm by ppm by ppm by ppm by	Nitroge	en oxides																	ppm	by vol
Lead ppm by Chloroprene ppm by the control ppm by t	Carbon	monoxid	le ·			a.													ppm	by vol
Chloroprene ppm b	Total V	OC (inch	uding thos	e listed bel	ow)		2			_									ppm	by vol
																			ppm	by vol
	Chloro	prene				2									-				ppm	by vol
	Toluen	е																	ppm	by vol

								Sta	ate of L	ouisiar	ıa	-								Ī	Date of	submitte	al
			34			Emissions	Inve	ntory Qu	uestion	naire (l	EIQ) for A	ir P	ollutants							1	Vov	20	13
E		oint ID N	lo.		Descriptive	Name of the l	Emissio	ons Source ((Alt. Nam	ie)	7		Ap	proximat	e Locati	on of Stack	or Ven	t (see in	structi	ons)			
		0-75				Resin	90 Rail	lear			Method UTM Z	опе	15			ching-Frima			Vertic	_		NAD83	mN
Tem	po Subje	ct Item II	No.								Latitude	-	30 °	-	31			15 " 15 "		- -	3321	hundi	redths
		0194		1																			
Physica	and Disc d Charac ge? (yes	cteristics		neter (ft) charge A	Transfer (GC) (Transfer (LP))	Height of St Above Grade		Stack Ga Veloci	W. II. CO. CO.	Condi	Gas Flow at tions, <u>not</u> at ard (ft ³ /min)		tack Gas Exit Cemperature (°F)		al Opera Time rs per ye		Constr	te of uction o fication		Throu	ghput '	of Annu Through n Point	h This
	no		= 5=	0.25		4 f	t l	NA	ft/sec	NA	ft^3/mi	1	356 °F	8,7	60	hr/yr J	al	2	2007	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
					ft²			14						2									
		Ty				nput (see ins		The second leaves to the second						Operati	ng Par	ameters (i	nclud	e units)				
Fuel				e of Fuel		Heat I		AMBTU/hr)								meter	-		De	escript		
	a			NA			NA	Α			Committee of the second		ate/Throughput				00 gal/y	/r					
	D	-										MILLEY	Rate/Throughp				AV	_		_	- 11		
	C				NI 4					-			ume/Cylinder D	Displaceme	ent		00 gal	_			Railca		
		-			Notes						hell Height (f						NA NA						
					1					-	ank Diameter	-	Fixed Roof	Flo	ating Ro			Extern	al			Inte	ernal
									- 1	1	anks:			FIO	ating Ro	of E	-	ngine Mo		or T	Ц	Ditt	oi ii di
									- 1		NAME OF TAXABLE PARTY.	Name and Address of the Owner, where the Owner, which is the Owner, whic	ilt by Manufact	urer			101	ignic Wi	odel 1e	au		_	
										Person	I Engines:		Rich Bu			Lean Burn			Strok	e		4 Strol	ke
Emi	ssion Po	1700-75		ation)	Control Equipment Code	Control Equipment Efficiency		P/TAP Number			osed Emission			Perm Emissio (Cur	nitted on Rate	Add, Change Delete,	, ,	Continu Complia	ious ance	Cone	central	ion in C	Gases
Polluta	nt								Aver (lb/l		Maximum (lbs/hr)		Annual (tons/yr)	Anr (tons		Unchang	100	Metho	od				
Particul	'articulate matter (PM ₁₀)																					gr/s	std ft ³
Sulfur	lioxide																						by vol
-	n oxides					0 1										4							by vol
-	monoxid														W								by vol
	OC (incl	uding thos	e listed be	elow)	000	0%			<0.0	01	0.23		< 0.01	<0	.01	U							by vol
Lead																							by vol
			- 1				H.J.					_		-									by vol
									-		_		-		-	-		-				by vol	
-														1								ppm	by vol

								Sta	ate of I	ouisian	a							Λ		1	Date of	submitt	al
						Emissions	Inver	tory Q	uestion	naire (I	EIQ) for Ai	r Pollut	tants							. 1	Nov	20	013
Eı	mission F	Point ID N	io.		Descriptive	Name of the I	Emission	ns Source	(Alt. Nam	ne)			Apr	proxima	te Locatio	on of Stac	k or V	ent (see i	instruct	ions)			
	(Desig	nation)	1							ATTO TO				•		*				4			
	170	0-76				Rosin	S Raile	ar			Method		15		dress Mato				**		Datum		
Torr	no Suble	ct Item II) No								UTM Zor Latitude	ie 30	15	Hori	zontal	73900	00	mE 15	Vert	ical _	332	400	mN redths
rem	po subje	ct item ii	7140.								Longitude	-			31			15		-			redths
	EQT	Г0195									Songitude									-			. Juille
	and Dis	-	Dian	neter (ft)	or Stack	Height of St	the Salarian	Stack Ga			Gas Flow at	Stack G		Norr	nal Opera	ting		Date of			ercent o		
		cteristics	Dis	charge A	rea (ft²)	Above Grade	e (ft)	Veloc	ity		tions, <u>not</u> at	100	erature		Time			struction			ghput		
Chan	ige? (yes	or no)							- [Standa	ard (ft³/min)	(0)	F)	(ho	urs per ye	ar)	Mo	dificatio	n	1	Emissio	n Poin	3
	44.47																Tool		2007	Jan-	Apr-	Jul-Sep	Oct-
	no	. 1		0.25	ft	4 f	t N	JA.	ft/sec	NA	ft^3/min	356	°F	8,	,760	hr/yr	Jul		2007	Mar	Jun		Dec
					6.2															25%	25%	25%	25%
			0 4-		.ft²																		
		Ty	-		l and Heat I	-								Opera	ting Par	ameters	(inclu	ude unit	ts)				
Fuel			Тур	e of Fuel		Heat I	_	MBTU/h	r)								ramet			D	escript	on	
	a			NA			NA				Iormal Operatin				y .	260,	,000 ga	al/yr					
	р							-			Aaximum Opera		1700				NA				_		
	Ic				NY 4						esign Capacity	Volume/C	ylinder D	Displacen	nent	20),000 g	al			Railca	r	
	Notes										hell Height (ft)	0.					NA		-				
											ank Diameter (-	l Roof	-	lostine D-	of.	NA	Exter	mal		r	Test	ernal
										-	anks:		1001	P	loating Ro	01		Engine N		aar		ını	emai
									1	-	Date Engine Ord Date Engine Wa		Manufact	urer	1			Engine P	viouei i	cai			
						(6)				- Delan	I Engines:	S Built by I	Rich Bu			Lean Bu	rn	0	2 Strol	ke		4 Stro	ke
Em	ission Po	int ID No	. (Design	ation)	Control	Control	HAP	/TAP			Birrior				mitted	1							
		1700-76			Equipment Code	Equipment Efficiency		Number	5	Prop	osed Emission	Rates		Emiss	sion Rate urrent)	Add Chan Delete	ige,	Contin	iance		centrat Exiting		
Polluta									Aver (lb/	rage hr)	Maximum (lbs/hr)	/5-1	nual is/yr)	7000	nnual ns/yr)	Uncha	nged	Meti	noa				
-		er (PM ₁₀)																					std ft ³
-	dioxide																						by vol
-	en oxides					,						-								. Z.			by vol
	monoxid		- 11-1-21	-1	000	000	1		-	01	0.22	-	0.01	-	-0.01			-		- 1"			by vol
_	OC (incl	uding tho	se listed b	elow)	000	0%			<0.	.01	0.23	<(0.01	-	:0.01	U							by vol
Lead					-				-	-		-		-		-		-					by vol
									-	-		1-		-					-				by vol
								-		+		_		-							by vol		

							State of	Louisia	na				*			Date of	submittal	
				*	Emissions	Inventory	Questio	nnaire (EIQ) for Air	Pollutants						Nov	201	3
E	mission Point ID (Designation)	No.		Descriptive	Name of the I	Emissions Sou	rce (Alt. Na	me)		A	Approximate Loca	tion of Stack	or Vent (see	instruc	tions)	1.		
	1700-77				Octopol S	Storage Tank			Method		06,"Address M	atching-Primar					NAD83	
Tom	po Subject Item	ID No.							UTM Zon Latitude	30 0	5 Horizontal	739000	mE	Ver	tical	3327	400 n	nN
1 CH	EQT0196								Longitude	-		31		5 "			hundre	
Stack	and Discharge	Dian	neter (ft)	or Stack	Height of St	ack Stack	Gas Exit	Stack	Gas Flow at	Stack Gas Exi	t Normal Ope	rating	Date of		P	ercent o	f Annual	
	al Characteristics age? (yes or no)	Disc	charge A	rea (ft²)	Above Grade		elocity		itions, <u>not</u> at ard (ft³/min)	Temperature	Time (hours per		Constructio Modificati			O .	Through n Point	This
	no	-	0.25	ft	4 f	t NA	ft/sec	NA	ft^3/min	77 °F	8,760	hr/yr Ju	1	2007	Jan- Mar	Apr- Jun	Jul-Sep	Oct- Dec
		_		ft ²											25%	25%	25%	25%
	r	ype of Fu	iel Used	l and Heat I	nput (see ins	tructions)					Operating Pa	rameters (ii	iclude un	its)				
Fuel		THE RESERVE OF THE PARTY OF THE	e of Fuel		Heat In	iput (MMBT)	J/hr)] [7,722			Para			D	escript	on	
	a		NA		4)	NA		4 1	Normal Operating				gal/yr				-	
	0							4 1	Maximum Operat	The state of the s			A	-			3000	
	C			Notes				4 -	Design Capacity/	Volume/Cylinder	Displacement		00 gal	-				
-				Notes				1 1	Shell Height (ft)	× = =			7	+				
								1 h	Tank Diameter (f	Fixed Roof	Floating F			ernal			Inter	nal
	1	*							Date Engine Orde		Though I			Model)	/ear		Bitor	iiai
		*							Date Engine Was	the same of the sa	cturer	1	Lingino	Model	001			
							#11		SI Engines:	□ Rich		Lean Burn		2 Stro	ke		4 Stroke	
Emi	ission Point ID N		tion)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Numbe		Prop	oosed Emission F	lates	Permitted Emission Rate (Current)	Add, Change, Delete, o	Com	inuous oliance			ion in Ga at Stack	ises
Polluta								erage o/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchange	ed	thod				
-	ate matter (PM ₁₀)																gr/stc	l ft ³
Sulfur c	A CONTRACTOR OF THE PROPERTY O							4									ppm b	
	n oxides																ppm b	
-	monoxide	and the said	I and	000	0.00				0.01			-					ppm b	
Lead	OC (including the	ose listed be	iow)	000	0%		<(0.01	0.01	<0.01	<0.01	U					ppm b	
LACRU							-					-			-		ppm b	-
							-				+				-		ppm b	_
							+			 	+		-				ppm b	
																	ppin	3 .01

form_7203_r01 10/22/10

Emission Point ID No. (Designation) 1700-79 Tempo Subject Item ID No. EQTIO198 Stack and Discharge Physical Characteristics Change? (yes or no) NA ft Above Grade (ft) Above	The same of the sa																						
Emission Point ID No. Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Rate of the Name of the Emission Rate of the Name of the Emission Rate of the Name of the Emission Rate of the Name of the Emission Rate of the Name of the Emission Rate of the Name of the Emission Rate of the Name of the Name of the Emission Rate of the Name of the									St	ate of L	ouisiai	na				10000					Date of	submitt	al
Emission Point ID No. Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emissions Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Source (Alt, Name) Descriptive Name of the Emission Rate of the Name of the Emission Rate of the Name of the Emission Rate of the Name of the Emission Rate of the Name of the Emission Rate of the Name of the Emission Rate of the Name of the Emission Rate of the Name of the Name of the Emission Rate of the Name of the				9			Emissions	Inve	ntory O	uestion	naire (EIO) for	Air	Pollutants							Nau	20	013
Chesignation 1700-79									J &												Nov	20	/13
Chesignation 1700-79									1														
Trop Trop	Em			No.		Descriptive	Name of the l	Emissio	ons Source	(Alt. Nam	ie)			Ap	proximate Locat	ion of Stac	k or V	ent (see	instruc	tions)			
Tempo Subject Rem ID No. EQUID 98 Stack and Discharge Physical Characteristics Discharge Area (nt) Above Grade (n) Velocity Velocity Velocity Stack and Discharge area (nt) NA nt nt nt nt nt nt nt n			NATURAL PROPERTY.						D .			Math	ad		O6 "Address Mo	tabina Prim	ary No	irna"			Datum	NADR	2
Latitude 3.0 * 3 * 1.5		1700	0-19			,	Emergency Sta	abilizer	Drummin	ıg			-	15		The second secon	The Party of the P		Ver			7400	mN
Stack and Discharge Physical Characteristic Change? (yes or no)	Temp	o Subiec	ct Item II	D No.																ucai	332		redths
Stack and Discharge Diameter (ft) or Stack Height of Stack Above Grade (ft) Velocity Velocity Velocity Conditions, not at Stack Gas Exit Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions, not at Stack Gas Exit Conditions Control												Long	gitude		3				•			hund	redths
Physical Characteristics Change? (yes or no) NA		EQT	0198										-						E				
Standard (R ² /min) (*F) (hours per year) Modification Image: Control Image: Co				Diam	eter (ft)	or Stack	Height of St	ack	Stack Ga	as Exit			21/2	Stack Gas Exit	Normal Oper	ating	1	Date of		P	ercent (f Annu	ıal
NA R 4 ft NA ft/sec NA ft/3/min 77 °F * hr/yr Jul 2007 Jan-Mar 25%			and the second s	Disc	harge Ar	rea (ft²)	Above Grade	e (ft)	Veloc	city				•							ighput	-	
NA ft 4 ft NA ft/sec NA ft/3/min 77 °F * hr/yr Jul 2007 Mar 25%	Chang	er (yes	or no)			- 1					Stand	lard (ft³/mir	n)	(°F)	(hours per y	ear)	Mo	dificatio	n		Emissi	n Poin	t
NA 11			- 1			- 1				-										Jan-	Apr-	Jul-Sep	Oct-
Type of Fuel Used and Heat Input (see instructions)	1	no	- 1	7	NA 1	ft	4 f	t I	NA	ft/sec	NA	ft^3/	min	, 77 °F	*	hr/yr	Jul		2007	Mar	Jun		Dec
Type of Fuel Used and Heat Input (see instructions) Type of Fuel Heat Input (MMBTU/hr)				_		2							- 2					(4)		25%	25%	25%	25%
Fuel				_		ft ²																	4
Normal Operating Rate/Throughput Normal Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operating Rate/Throughput Normal Operation Normal Operation Normal Operation Normal Operation N			Ty	ype of Fu	el Used	and Heat I	nput (see ins	structi	ions)						Operating Pa	rameters	(inch	ude uni	ts)				
Maximum Operating Rate/Throughput Design Capacity/Volume/Cylinder Displacement NA	uel			Туре	of Fuel		Heat I	nput (N	AMBTU/h	r)						Pa	ramet	er		E	escript	on	
Design Capacity/Volume/Cylinder Displacement NA NA NA NA NA NA NA NA NA NA		a			NA			N/	A	× .	Ī	Normal Ope	erating	Rate/Throughput		1,0	00 gal	/уг					
Notes Shell Height (R) NA Tank Diameter (R) NA Tank Diameter (R) NA Tank Diameter (R) NA Tank Diameter (R)		b									1	Maximum C) perati	ng Rate/Throughp	put		NA						
*20 DRUMS (1,000 gallons) per year Tank Diameter (ft)		С									1	Design Capa	acity/V	olume/Cylinder D	Displacement		NA						
Tanks: Fixed Roof Floating Roof External						The second secon					3	Shell Height	t (ft)									1	
Date Engine Ordered Date Engine Was Built by Manufacturer Date Engine Was Built by Manufacturer SI Engine Was Built by Manufacturer SI Engine Was Built by Manufacturer Date Engine Was Built by Manufacturer SI Engines: Rich Burn Lean Burn 2 Stroke				* 20	DRUMS	(1,000 gallons	s) per year					Tank Diame	eter (ft))			NA						
Date Engine Was Built by Manufacturer SI Engines: Rich Burn Lean Burn 2 Stroke										1		Tanks:		Fixed Roof	Floating R	oof		Exte	rnal			Int	ernal
Emission Point ID No. (Designation) 1700-79 Code Code Code Control Equipment Code Code Code Code Code Code Code Code										- 1								Engine l	Model \	Year			
Emission Point ID No. (Designation) 1700-79 Code Control Equipment Code Code Code Code Code Continuous Compliance (Current) Compliance (Ib/hr) Code Compliance (Ib/hr) Code Compliance (Ib/hr) Code Compliance (Ib/hr) Code Compliance (Ib/hr) Code Continuous Compliance (Current) Code Continuous Compliance (Current) Code Code Code Code Code Continuous Compliance (Ib/hr) Code C											1	Date Engine	e Was										
Equipment Code Equipment Code Efficiency CAS Number Proposed Emission Rates Emission Rate (Current) Change, Delete, or Unchanged Continuous Compliance Method Particulate matter (PM ₁₀) Sulfur dioxide Nitrogen oxides Carbon monoxide Total VOC (including those listed below) 000 0% 0.35 0.35 0.35 0.01 0.01 U Continuous Compliance (Current) Continuous Continuous (Current) Continuous (Current) Continuous (Current) Continuous (Current) Continuous (Current) Continuous (Current) Continuous (Current) Continuous (Current) Continuous (Current) Continuous (Current) Continuous (Current) Continuous (Current) Continuous (Current) Continuous (Current) C		-										SI Engines:	:	□ Rich Bu	urn 🗆	Lean Bu	rn		2 Stro	ke		4 Stro	ke
Proposed Emission Rates Current Change, Delete, or Unchanged Continuous Compliance Method Particulate matter (PM ₁₀)	Emis	sion Poi	int ID No	. (Designa	tion)	. contra manual terra.	TO MAKE THE PARTY OF THE PARTY																
Pollutant Average (lb/hr) (lbs/hr) (tons/yr) Delete, or Unchanged (lb/hr) Particulate matter (PM ₁₀) Sulfur dioxide Nitrogen oxides Carbon monoxide Total VOC (including those listed below) 000 0% 0.35 0.35 <0.01 <0.01 U Lead			1700-79	9	- 1			CAS	Number		Prop	posed Emiss	sion R	ates	The second secon	100		Contin	nuous	C			C
Average					- 1	Code	- Dimension								(Current)						Exiting		
Carbon monoxide Carbon function for the listed below Construction for the listed below Carbon function for the listed below Carbon function function for the listed below Carbon function fun	Pollutan	t								Aver	rage	Maximu	um	Annual	Annual			Met	hod		2,000		
Sulfur dioxide Nitrogen oxides Carbon monoxide 0.35 Total VOC (including those listed below) 000 0.35 0.35 0.35 0.01 0.01 U 0.01 U				1								(lbs/hr	r)	(tons/yr)	(tons/yr)								
Nitrogen oxides											- 1											gr/	std ft ³
Carbon monoxide 0.35 0.35 0.01 U Lead 0.35 0.35 0.01 0.01 0.01	a constant and a cons																					ppm	by vol
Total VOC (including those listed below) 000 0% 0.35 0.35 <0.01 <0.01 U Lead																							by vol
Lead																				-		_	by vol
		C (inclu	iding thos	se listed be	low)	000	0%		2	0.3	35	0.35		<0.01	<0.01	U		-					by vol
Toluene 000 0% 00108-88-3 0.35 0.35 <0.01 <0.01 U						200	000	0.01	00.00.0	-				- : 0.01	- 0.01								by vol
	oluene					000	0%	001	08-88-3	0.3	35	0.35		<0.01	<0.01	U		-		-			by vol
														-	-	-		-		-		-	by vol

						Sta	ate of Louisi	ana						T I	Date of	submitt	al
				ε	Emissions	Inventory Qu	uestionnaire	(EIQ) for Air	r Pollutants					1	Nov	20	113
E		oint ID N	lo.	Descriptive	Name of the I	Emissions Source	(Alt. Name)		Ap	proximate Location	on of Stack or V	ent (see in	nstruct	ions)			
		nation) 0-80			ACR Storag	ge Vent Header		Method		06,"Address Mate	ching-Primary Na	ume"			Datum	NAD83	3
Tam	on Culti	ct Item II	D.N.			4		UTM Zon Latitude	e 15	Horizontal 3	102.000	mE 15 '	Vert	ical	332		mN redths
1 em			No.					Longitude		31	·	15		-			redths
Stack	RLP	charge	Diame	ter (ft) or Stack	Height of St	ack Stack Ga	Evit Sto	ck Gas Flow at	Stack Gas Exit	Normal Opera	ting I	Date of		Pe	rcent	f Annu	al
Physica		cteristics		arge Area (ft ²)	Above Grade	Protection of the protection o	ity Cor	nditions, <u>not</u> at ndard (ft ³ /min)	Temperature (°F)	Time (hours per ye	Cons	truction of		Throu	ghput '	Through Point	h This
	no		_	0.17 ft	50 f	t NA	ft/sec N	IA ft^3/min	23 °F	8,760	hr/yr Jul		2007	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep	Oct- Dec 25%
				ft²							1			2370	25 70	2370	2370
		Ty	The second second	el Used and Heat I						Operating Par			s)				
Fuel	-			of Fuel	Heat Ir	aput (MMBTU/hr	-)				Paramet	er		D	escript	on	
	b		- N	IA		NA		The state of the s	g Rate/Throughput ting Rate/Throughp		NA NA	_			_		
	c								Volume/Cylinder D		NA						
	1			Notes				Shell Height (ft)	volumer Cymrider E	Displacement	NA						
		VOC	emission rat	te inleudes 2.4 lbs/yr o	f 1,2 dichlorobe	enzene		Tank Diameter (f	t)		NA						
							1	Tanks:	Fixed Roof	Floating Ro	of 🗆	Exteri	nal			Int	ernal
								Date Engine Ord	ered			Engine M	Iodel Y	ear			
							1	Date Engine Was	Built by Manufact	turer							
								SI Engines:	☐ Rich Bu	arn 🗆	Lean Burn		2 Strol	ke		4 Strol	ke
Em	ssion Po	1700-80	. (Designati	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Pr	oposed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contine Compli Meth	ance			ion in C	
Polluta					7 3		Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meth	ou _				
The second second second	ate matte	er (PM ₁₀)														THE RESERVE AND ADDRESS OF THE PERSON.	std ft ³
Sulfur																THE RESERVE OF THE PERSON NAMED IN	by vol
-	n oxides				2 1/2 2											_	by vol
	monoxid		e listed belo	ow) 000	007		0.02	0.00	0.00	0.07	6	-				_	by vol
Lead	OC (Incl	uoing thos	e usted belo	JW) 000	0%		0.02	0.09	0.09	0.07	C				-		by vol
LAU								-									by vol
-								+								_	by vol
																	by vol

_																		
						St	ate of Lo	uisian	ia							Date of	submitt	al
					Emissions	Inventory Q	uestionna	aire (E	EIO) for Air	Pollutants						Nov	20	013
30						Consider a secondariant of the			~~~~~ ∞~~ ±0°°							1404	20	113
E		oint ID No.		Descriptive	Name of the	Emissions Source	(Alt. Name)			App	proximate Location	on of Stack or V	ent (see	instruc	tions)			
		nation)																
	1700)-80.1	1		Refined AC	R Storage Tank			Method		06,"Address Mate Horizontal	hing-Primary N 739000	ame" mE	V	tical	Datum		mN
Tem	no Subje	ct Item ID No.	-						UTM Zone Latitude	30 *	Horizontai 3		me 15		ucai .	332		redths
2 0.11	po odoje	ALLIN AD 110.							Longitude	-90 °	31		15					redths
		0199	100											-				
	and Disc		Diameter (ft)	or Stack	Height of St	CANADA TOTAL TOTAL	AND DESCRIPTION OF THE PARTY OF		Gas Flow at	Stack Gas Exit	Normal Opera		Date of		1126.0	ercent o		\$35500 mm
A CONTRACTOR OF THE PARTY OF TH	d Charac		Discharge A	rea (ft²)	Above Grad	e (ft) Veloc	city		tions, <u>not</u> at	Temperature	Time		struction			ighput	-	
Char	ige? (yes	or no)						Standa	ard (ft ³ /min)	(°F)	(hours per ye	ar) M	odificatio	n		Emissio	n Poin	t .
	110											Mar		1971	Jan-	Apr-	Jul-Sep	Oct-
4	no		NA	ft	NS	ft NA	ft/sec	NA	ft^3/min	23 °F	*	hr/yr		17/1	Mar	Jun .		Dec
	100			6,2											25%	25%	25%	25%
				_ft²	1 18					-								
				d and Heat I							Operating Par			ts)				
Fuel]	Type of Fuel	l	Heat I	nput (MMBTU/hi	r)					Parame			D	escript	on	
	a		NA			NA			-	Rate/Throughput		3 MM lb	/уг					
	D								A STATE OF THE PARTY OF THE PAR	ing Rate/Throughp		NA						
	c			NT 4						/olume/Cylinder D	isplacement	50,000 g	gal					
		Emissions for	m this source	Notes te are routed to	amission noi-t	1700 80			hell Height (ft)	×		34		-				
		Eliussions If	mi uns sourc	e are routed to	emission point	1700-00		-	ank Diameter (ft	Fixed Roof	Floating Roo	16 of \square	Exter	rnal			Int	ernal
									Date Engine Orde		I loading Roo	л Ц	Engine N		Year	Ш	ши	Ciliai
								_		Built by Manufacti	urer		Luginer	10del	cai			
								_	I Engines:	☐ Rich Bu		Lean Burn		2 Stro	ke		4 Stro	ke
Em	ission Poi	int ID No. (Des	ignation)	Control	Control	HAP/TAP					Permitted		T					
		,	- /	Equipment	Equipment	CAS Number		Dron	osed Emission R	ates	Emission Rate	Add,	C					
		1700-80.1		Code	Efficiency			rrope	oseu Emission R		(Current)	Change,	Contin		1000	centrat		
Dallert				-					Maniana	I Ammel	Annual	Delete, or	Meti		1	Exiting	at Stac	k
Polluta	int.					(a) 3	Averag		Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged						
Particu	late matte	er (PM ₁₀)					(III/III		((10.00.3-7	(or/e	std ft ³
Sulfur	******	V											1					by vol
-	n oxides																	by vol
Carbon	monoxid	e															ppm	by vol
Total V	OC (incl	uding those liste	ed below)	000	0%		*		0.03	*	#:	С					ppm	by vol
Lead																		by vol
				-									-					by vol .
				-			-	-					-		_			by vol
																	2323 224	DV VOI

						St	ate of Louisi	ana							Date of	submitt	al
					Emissions 1	Inventory Q	uestionnaire	(EIQ) for Air	r Pollutants						Nov	20	013
E		Point ID N	ło.	Descriptive	Name of the E	missions Source	(Alt. Name)		Ap	proximate Locati	on of Stack or V	ent (see i	nstruc	tions)			
		0-80.2			Chlorinated A	CR Storage Tank	6	Method UTM Zon	e 15	06,"Address Mat	the same of the sa	mE	Ver			NAD8:	mN
Tem		ect Item II Γ0200	D No.					Latitude Longitude	30 °	3		15 15	11		332	hund	redths redths
Physica	and Dis	charge cteristics		er (ft) or Stack rge Area (ft ²)	Height of Sta Above Grade	Carlo Carlo	ity Con	ck Gas Flow at additions, <u>not</u> at adard (ft ³ /min)	Stack Gas Exit Temperature (°F)	Normal Opera Time (hours per ye	Cons	Date of struction edification	THE PARTY NAMED IN	Throu	ighput Emissi	of Annu Throug on Poin	h This t
	110	- ·	NA	ft	NS ft	NA	ft/sec N	A ft^3/min	23 °F	de	hr/yr Jun		1968	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
	T	Ty	pe of Fuel	Used and Heat I	nput (see inst	ructions)				Operating Par	ameters (inclu	ide unit	s)				
Fuel			Type of	THE RESERVE AND ADDRESS OF THE PERSON NAMED IN		put (MMBTU/hr)			1	Paramet			D	escript	ion	
	a b		N/	<u> </u>		NA		Maximum Operat	Rate/Throughput ing Rate/Throughp		3 MM lb/ NA						100
	10			Notes				Shell Height (ft)	Volume/Cylinder D	risplacement	22,164 g 27	at					
		Emissio	ons from this	source are routed to	emission point 17	700-80		Tank Diameter (ft	1)		12				-		
							1	Tanks:	Fixed Roof	Floating Ro		Exter	nal			Int	ernal
								Date Engine Orde				Engine N	Model Y	ear			
									Built by Manufact	urer							
								SI Engines:	☐ Rich Bu		Lean Burn		2 Stro	ke		4 Stro	ke
Em	ission Po	int ID No. 1700-80.	. (Designation	n) Control Equipment Code	Control Equipment Efficiency	HAP/TAP CAS Number	Pro	oposed Emission P	tates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin	iance	VER. 201		ion in (The Columbia of the
Polluta	ant						Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meth	10 d				
Particu	late matte	er (PM ₁₀)														gr/s	std ft ³
	dioxide															ppm	by vol
-	en oxides			. +									1			ppm	by vol
	monoxio																by vol
-	OC (incl	uding thos	e listed belov	v) 000	0%		At .	0.04	*	*	С						by vol
Lead																	by vol
																	by vol
									 	 							by vol
-																ppm	Uy YUL

									the state of the s								
						St	ate of Louis	iana							Date of	submitt	al .
					Emissions	Inventory Q	uestionnaire	(EIQ) for Ai	r Pollutants						Nov	20	013
E	mission P	oint ID N	lo.	Descriptiv	e Name of the l	Emissions Source	(Alt. Name)		Ap	proximate Locati	on of Stack or V	ent (see	instruc	tions)			-
		nation)	-					1972 N 1975	7								
	170	0-81	1		ACR R	efining Vent		Method	ne 15		ching-Primary N		17		Datum		
Tem	no Subie	ct Item II) No					UTM Zor Latitude	30 *	Horizontal 3		mE 15		tical	332		mN redths
A CIII	po subje	ct item it	110.					Longitude		31		15					redths
	RLP	20018						and the same			•						
	and Disc			ter (ft) or Stack	Height of St			ck Gas Flow at	Stack Gas Exit	Normal Opera		Date of			ercent (
	al Charac age? (yes		Disch	arge Area (ft²)	Above Grade	e (ft) Veloc		nditions, <u>not</u> at	Temperature	Time		struction	110000		ighput		
Char	iger (yes	or no)			1	1	Sta	ndard (ft³/min)	(°F)	(hours per ye	ear) Mo	odificatio	n	2	Emissi	n Poin	t
	по	- 1									Jul	1	2007	Jan-	Apr-	Jul-Sep	
		.	_	0.33 ft	70.2	ft 0.13	ft/sec	1 ft^3/min	82 °F	8,760	hr/yr		2007	Mar	Jun		Dec
		1		ft ²							. 1			25%	25%	25%	25%
					<u></u>				L	<u></u>							
		Ту	_	l Used and Heat						Operating Par			ts)				
Fuel	-			of Fuel	Heat I	nput (MMBTU/hr	()		D		Paramet			D	escript	ion	
	a		N	A	-	NA			g Rate/Throughput		1,123 lb/	hr					
	0								ting Rate/Through		NA NA						
	10			Notes				Shell Height (ft)	/Volume/Cylinder I	Displacement	NA NA	-	-				
				Notes				Tank Diameter (Fr)		NA NA		-				
								Tanks:		Floating Ro		Exter	rnal			Int	ernal
								Date Engine Ord		Trouting re	<u> </u>	Engine N	-	Year		****	
								The second secon	s Built by Manufac	turer		- Barre					
								SI Engines:	□ Rich B		Lean Burn		2 Stro	ke		4 Stro	ke
Em	ission Po	int ID No 1700-81	. (Designati	on) Control Equipment	Control Equipment Efficiency	HAP / TAP CAS Number	Pı	roposed Emission	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl	liance	2010000	centra Exiting		
Polluta	int						Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meth	hod				
Particu	late matte	er (PM ₁₀)								fi.						gr/	std ft ³
	dioxide															ppm	by vol
-	en oxides															ppm	by vol
	monoxid																by vol
-	OC (incl	uding thos	se listed belo	ow) 000	0%		1.00	10.00	2.20	2.20	U						by vol
Lead																	by vol
Hydrod	chloric aci	id		000	0%	-	0.3	4.5	0.7	0.7	U	-		-			by vol
					-				-	-	-	-					by vol
II .										1						DOIL	DV VOI

			7					State o	f Louisi	ana					7.						Date of	submitt	al
					En	missions	Inventor	y Questi	onnaire	(EIQ) for	r Air	Pollutar	ıts								Nov	20	13
E		Point ID N	lo.	Descr	ptive Na	me of the E	missions So	urce (Alt. N	lame)				App	oroxima	te Locati	on of Stack	or Ve	nt (see i	instruct	ions)	7		
		00-82			1	ACR Solver	nt Blend Ta	nk		Meth	hod M Zone		15		iress Mate	ching-Prima		ne" nE	Vert			NAD83	mN
Tem	.,	ct Item II	D No.							Latit		30 °	- 13	11011	31	7	_	15	11	-	332	hund	redths
Physica	and Dis	charge cteristics		ter (ft) or Stack arge Area (ft²)	126.00	leight of Sta bove Grade	The second	ck Gas Exit Velocity	Con	ck Gas Flow ditions, <u>not</u> ndard (ft ³ /mi	at	Stack Gas Temperat	Second Contract Contr	4	nal Opera Time irs per ye		Const	ate of ruction lification		Throu	ghput '	f Annu Throug on Point	h This
ì	no	-	_	0.167 ft	-	30 ft	NA	ft/sec	N	Aft^3/	/min	25 °F		ta .	ηs	hr/yr So	ept		2007	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
-	T	Ty	ne of Fue	l Used and H	eat Innu	nt (see inst	tructions)		-	Γ				Operat	ing Par	ameters (inclu	de unit	ts)				
Fuel		1	Туре		The state of the s		put (MMB)	(U/hr)	-					Opera	ing i ui		amete			D	escripti	on	
	a b		N	A			NA			Normal Ope Maximum (Operati	ng Rate/Thr	oughpu				NA	/уг			01		
	Ic .		*Hours	Notes of venting vary	per solven	nt used				Design Cap Shell Heigh Tank Diame	nt (ft)		nder Di	isplacem	ent	96	0 gals 9						
										Tanks:	v	Fixed Ro	oof	Fl	oating Ro	of [Exter	100			Inte	ernal
										Date Engine		the second second second	nufactu	irer		1	11	angine n	Model Y	ear			
										SI Engines			ch Bur			Lean Buri	1		2 Strol	ce	П	4 Strol	ke
Emi	ission Po	1700-82	. (Designati	on) Cont Equipa Cod	ent Eq	Control juipment fficiency	HAP/TA		Pro	oposed Emis				Peri Emissi	mitted ion Rate rrent)	Add, Chang Delete,	е,	Contin	lance		centrat	ion in (Sases
Polluta	nt								verage (lb/hr)	Maximu (lbs/h	- Carlotte	Annua (tons/y	7	Character	nual ns/yr)	Unchang		Meth	hod				
		er (PM ₁₀)																				gr/s	itd ft ³
Sulfur																						-	by vol
-	n oxides			1.0																			by vol
	monoxid								2.12							-							by vol
	OC (incl	uding thos	e listed belo	w) 000		0%			0.13	0.14		0.01		0.	.037	C	_						by vol
Lead	lossett				_	000	00107.10		0.40	0.11		0.71			.01		_						by vol
	loroethy			000		0%	00127-18		0.40	0.56		0.01		-	0.01	C	-						by vol
-	(mixed i			000		0%	01330-20		0.10	0.14		0.001			100.	C	-						by vol
DICHIOL	umethan	е		000		0%	00075-09	-2	7.05	9.90		0.02		0	0.02	C						ppm	by vol

						Sta	ate of Louis	iana	0)					I	Date of	submitt	al
					Emissions	Inventory Q	uestionnair	e (EIQ) for Ai	r Pollutants					1	Nov	20	013
E	mission P	oint ID No.		Descriptive	Name of the	Emissions Source	(Alt Name)		An	proximate Location	on of Stack or V	ent (see in	struction	one)	-		
_	(Design			Descriptive	THAIR OF THE	Dinissions Bource	(Para Hame)	1	· · · · ·	promine Boend	on or stack of v	cir (see in	ou acu	UKAS)			
	3-	95	7		Diver	sion Tank		Method		06,"Address Mate	hing-Primary Na	ame"			Datum	NAD8	3
				#			*.	UTM Zor				mE	Vertic	cal _	3327		mN
Tem	po Subjec	ct Item ID N	vo.					Latitude	30 °	3		15 "					redths
	EQT	0202	X					Longitude	-90 °	31		15 "		-		hund	redths
Stack	and Disc	charge	Diameter (ft) or Stack	Height of St	tack Stack Ga	s Exit Sta	ack Gas Flow at	Stack Gas Exit	Normal Opera	ting 1	Date of		Pe	rcent o	f Annu	al
	al Charac		Discharge	Area (ft²)	Above Grad	e (ft) Veloc		onditions, <u>not</u> at	Temperature	Time		struction o	r	Throu	~ .	_	
Chai	ige? (yes	or no)				1	Sta	andard (ft³/min)	(°F)	(hours per ye	ar) Mo	dification		J	Emissio	n Poin	t
	20			- 1							Sant		995	Jan-	Apr-	Jul-Sep	Oct-
	по		NA	ft	NA	ft NA	ft/sec	NA ft^3/min	77 °F	8,760	hr/yr Sept	'		Mar	Jun		Dec
				ft ²										25%	25%	25%	25%
		Туре		sed and Heat I						Operating Par)				
Fuel			Type of Fu	ıel	Heat I	nput (MMBTU/hr	-)				Paramet			De	escripti	on	
	a		NA			NA		1	g Rate/Throughput	*	27,000 gal	l/hr					
	b								ting Rate/Throughp		NA		-				
	С			DY 4					Volume/Cylinder I	Displacement	660,222 g	gal	Op	en tanl	k WWI	treatm	ent
				Notes				Shell Height (ft)	6.V		NA NA						
								Tank Diameter (Floating De	NA NA	Extern	ol.			Int	ernal
							1	Tanks: □ Date Engine Ord		Floating Ro	of 🗆	Engine Mo		ar T		ш	emai
								The same of the sa	s Built by Manufac	turer		Engine Mi	oder re	aı			
								SI Engines:	Rich B	the state of the s	Lean Burn		Stroke	e		4 Stro	ke
Em	ission Poi	int ID No. (I	Designation)	Control	Control	HAP/TAP		DX 2016		Permitted							
		3-95		Equipment Code	Equipment Efficiency	CAS Number	P	roposed Emission	Rates	Emission Rate (Current)	Add, Change, Delete, or	Continu Complia	nce			ion in (
Polluta							Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Metho	od				
	late matte	r (PM ₁₀)															std ft ³
-	dioxide																by vol
-	en oxides									-							by vol
17000000	monoxid				0.00		0.01		0.01				_			-	by vol
	OC (inch	uding those l	usted below)	000	0%		<0.01	<0.01	<0.01	0.21	С		_			-	by vol
Lead				000	007	00126 00 5	-0.01	+0.07	-0.01	0.10	6		-				by vol
Chloro				000	0%	00126-99-8 00108-88-3	<0.01 <0.01	<0.01	<0.01	0.19	C		-				by vol
roluen				- 000	070	00100-00-3	<0.01	<0.01	20.01	0.01		-	-				by vol

					1	St	ate of Louisia	ana		8					Date of	submitt	al
			*	58) K	Emissions	Inventory Q	uestionnaire	(EIQ) for Ai	r Pollutants						Nov	20)13
E		n Point ID	No.	Descriptiv	e Name of the l	Emissions Source	(Alt. Name)	- I - ×	Ap	proximate Locati	on of Stack or V	ent (see	instruc	tions)			
	596	4-95			Sur	ge Tank		Method UTM Zon	e 15	06,"Address Mat Horizontal		mE	Ver		Datum 332	-	mN
Tem		ject Item I	D No.		*	4		Latitude Longitude	30 °	31		15 15	"	-	552	hund	redths redths
	and I	QT0203 Discharge		eter (ft) or Stack	Height of St	ack Stack Ga		k Gas Flow at	Stack Gas Exit	Normal Opera	nting]	Date of		Pe	ercent o	f Annu	ıal
-		racteristics es or no)	Disch	narge Area (ft²)	Above Grade	e (ft) Veloc		ditions, <u>not</u> at dard (ft³/min)	Temperature (°F)	Time (hours per ye	The second secon	struction dificatio	111111111111111111111111111111111111111		ghput ' Emissio		A CONTRACTOR OF THE PARTY OF TH
	no	_	N	Aft	NA f	n NA	ft/sec N/	Aft^3/min	77 °F	8,760	hr/yr Sept		1995	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
		T	- vna of Eu	el Used and Heat		<u> </u>				O Po	(:)			-			
Fuel	-	1		of Fuel	The second secon					Operating Par	Paramet		(S)	D			
a uei	a			NA	Heat	nput (MMBTU/hr NA		Normal Operation	g Rate/Throughput		27,000 ga			D	escript	on	
	b	-	A			INA			ting Rate/Throughp		NA NA	1/111	_		-	lla. La	
	c	1						the same of the same	Volume/Cylinder D		660,000	ra1	-	pen tan	k wwī	treatm	ent
	_			Notes				Shell Height (ft)	volume/Cylinder L	rispiacement	NA NA	541	_	pen tan	45 11 11 2	douth	one -
				11000				Tank Diameter (f	1)		NA						
								Tanks: □	Fixed Roof	Floating Ro		Exter	nal			Inte	ernal
							1	Date Engine Ord				Engine N	Model Y	ear			
									Built by Manufact	turer							
								SI Engines:	□ Rich Bu		Lean Burn		2 Stro	ke		4 Strol	ke
Em	ission	4-95	o. (Designat	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Pro	posed Emission I	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl	iance		centrat Exiting		
Polluta	nt					×	Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	nod				
		tter (PM ₁₀)														gr/s	std ft ³
Sulfur																ppm	by vol
Nitroge																ppm	by vol
Carbon		A CONTRACTOR OF THE PARTY OF TH														ppm	by vol
	OC (ir	cluding tho	se listed bel	ow) 000	0%		0.52	2.36	2.29	2.11	U						by vol
Lead			72.														by vol
Chloro				000	0%	00126-99-8	0.5	2.14	2.17	1.99	U						by vol
Toluen	е			000	0%	00108-88-3	0.01	0.1	0.06	0.06	U						by vol
																ppm	by vol

							Sta	ate of L	ouisian	a		7				Date of	submit	tal
						Emissions	Inventory Qu	uestioni	naire (E	(IQ) for Air	Pollutants					Nov	2	013
																1101	1 2	013
Er	nission P	oint ID No.			Descriptive	Name of the I	Emissions Source	(Alt Nam	e)		An	proximate Location	on of Stack or V	ent (see inst	ructions			
	(Design				Descriptive	Traine or the l	Dimiggions Source	(7816- 1 10111	-)		749	prominate Locali	or Diack of V	cire (occ mo	z de exoras,			
	5-9	95				Aera	tion Tank			Method	3 3	06,"Address Mato	hing-Primary Na	ıme"	(4)	Datum	NAD8	13
										UTM Zone					Vertical	332		mN
Tem	po Subjec	ct Item ID	No.							Latitude	30 °	3		15 "			- volume a	dredths
	EQT	0204		c						Longitude	-90 °	31		15 "		-	hund	dredths
Stack	and Disc	harge	Diame	ter (ft) or	r Stack	Height of St	ack Stack Ga	s Exit	Stack (Gas Flow at	Stack Gas Exit	Normal Opera	ting I	Date of		Percent	of Ann	ual
	l Charac		Disch	arge Are	ea (ft²)	Above Grade	e (ft) Veloc	ity	Condit	tions, <u>not</u> at	Temperature	Time	Cons	truction or	Thi	oughput		•
Chan	ge? (yes	or no)							Standa	rd (ft ³ /min)	(°F)	(hours per ye	ar) Mo	dification		Emissi	on Poir	at
					1		1	- 1							Jan-	Apr-	Jul-Se	D Oct-
	no		N	A ft		NA f	t NA	ft/sec	NA	ft^3/min	77 °F	8,760	hr/yr Sept	19	95 Mai			Dec
			_		İ										25%	25%	25%	25%
			-	ft	2										_		+	
		Тур	e of Fu	el Used :	and Heat I	nput (see ins	structions)					Operating Par	ameters (inclu	ide units)	-			
Fuel			Туре	of Fuel		Heat I	nput (MMBTU/hr	7)			N		Paramet	er		Descrip	tion	
	а		1	NA.			NA		N	ormal Operating	Rate/Throughput		27,000 ga	/hr			*	
	b								, M	Iaximum Operat	ing Rate/Throughp	put	NA					
	С								-		Volume/Cylinder D	Displacement	660,000 g	gal	Open	ank WW	T treatn	nent
					Notes				S	hell Height (ft)			NA					
										ank Diameter (fi			NA	•				
								1	_	anks:	Fixed Roof	Floating Ro	of 🗆	External			In	iternal
								- 1	_	ate Engine Orde				Engine Mod	lel Year			
									_		Built by Manufact		ļ				1.0	· ·
*7					G				S	I Engines:	□ Rich Bu		Lean Burn	□ 2.5	Stroke		4 Str	oke
Emi	ission Poi	nt ID No. (Designat	ALCOHOLD .	Control Equipment	Control Equipment	HAP / TAP CAS Number					Permitted Emission Rate	4.11					
		5-95		1	Code	Efficiency	CAS Humber		Propo	osed Emission F	lates	(Current)	Add, Change,	Continuo		oncentra	tion in	Gases
												,	Delete, or	Complian	ce		at Sta	
Polluta	nt							Aver	age	Maximum	Annual	Annual	Unchanged	Method				
								(lb/l	ar)	(lbs/hr)	(tons/yr)	(tons/yr)						
-	late matte	r (PM ₁₀)																/std ft ³
Sulfur					9											04	_	n by vol
	n oxides																	n by vol
-	monoxid		listad b. I		000	O.Ca.		-0.1	01	0.03	0.00	0.00	U					m by vol
Lead V	OC (incli	iding those	nsted bel	OW)	000	0%		<0.0	U1	0.03	0.02	0.02	0		_			m by vol
Chloro	nrene			-	000	0%	00126-99-8	<0.0	01	0.02	0.02	0.02	Ü		-			m by vol
Toluen				-	000	0%	00126-99-8	<0.0		<0.02	<0.02	<0.02	U		-			m by vol
2 Oldell				-	000	070	30100-00-3	70.0	01	VV.01	VU.U1	VO.01	<u> </u>		_			m by vol

-							State of 1	Louisia	na						T,	Date of	submitt	al
					Emissions	Inventor	y Question	maire (EIQ) for Ai	r Pollutants						Nov	20	13
	<u>*</u>																	
E	mission Point ID N	No.	-	Descriptive	Name of the I	Emissions So	urce (Alt. Nar	ne)		A	pproximate Locati	on of Stack or V	ent (see i	instruc	tions)			
	(Designation)									80							NIA DOS	
	1700-83				ACR Dru	unming Vent	t		Method UTM Zon	e 15	06,"Address Mat Horizontal		mE	Vert			NAD83 400	mN
Tem	po Subject Item II	D No.							Latitude	30 0	Horizontai 3		15		ucai _	3321		redths
527027770	r								Longitude		31	•	15					redths
	RLP0019										×		5					
	and Discharge		neter (ft)	WH DAVIDS STATE	Height of St		k Gas Exit		Gas Flow at	Stack Gas Exit	Normal Opera		Date of				f Annu	
	d Characteristics age? (yes or no)	Disc	charge Ar	rea (ft²)	Above Grade	e (ft)	elocity		litions, not at	Temperature	Time		struction odificatio				Through n Point	
Canada	ge. Ges or no)							Stand	lard (ft³/min)	(°F)	(hours per ye	ear) IVIC	Juncano	11		CHHSSIC	n roini	
	no		141									Sept		2007	Jan-		Jul-Sep	
		1	NA	ft	NA f	t NA	ft/sec	NA	ft^3/min	NA °F	8,760	hr/yr		2007	Mar	Jun	250	Dec
				ft ²		-	-					1		1	25%	25%	25%	25%
171	Ty			and Heat I	nput (see ins						Operating Par			ts)	-			-
Fuel	9		e of Fuel NA		Heat Ir	NA NA	U/hr)	1	Named Occupie	Data/Thannahaus		Paramet			D	escript	on	
	b		IVA			INA			The second secon	g Rate/Throughput ting Rate/Through		2,000 drun	ns/yr	_		_	_	
	c								STATE OF THE STATE	Volume/Cylinder	M. Carrier	NA NA				_		
				Notes					Shell Height (ft)	voidiner Cymrider 1	Displacement	NA NA						
These e	emissions are from	an open sh	ned which		ith a ventilation	fan to minim	nize employee		Tank Diameter (f	t)		NA						
				exposure.					Tanks:	Fixed Roof	Floating Ro		Exter	rnal		П	Inte	ernal
	v 8								Date Engine Ord	ered			Engine N	Model Y	ear			
		,			5 .					Built by Manufac	cturer							
									SI Engines:	□ Rich B		Lean Burn		2 Stro	ke		4 Strol	ke
Emi	ission Point ID No	. (Designa	ation)	Control	Control	HAP/TA					Permitted							
	1700-83			Equipment Code	Equipment Efficiency	CAS Numb	er	Proj	posed Emission I	Rates	Emission Rate (Current)	Add,	Contin	uous	C		ion in (
				Coue	Zinciency						(Current)	Change, Delete, or	Compl	DICTOR STATE OF THE PARTY OF TH			at Stac	
Polluta	nt							rage	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Meth	hod				
Particul	late matter (PM ₁₀)						(ID)	/hr)	(IOS/III)	(tolls/y1)	(LOHS/y1)		-		-		arle	std ft ³
Sulfur o										1		-						by vol
Nitroge	n oxides																	by vol
	monoxide																ppm	by vol
Total V	OC (including thos	se listed be	elow)	000	0%		0.	20	0.35	0.020	0.340	C					100 00	by vol
Lead																		by vol
	loroethylene			000	0%	00127-18-		04	0.08	0.01	0.01	U						by vol
-	(mixed isomers)			000	0%	01330-20-		003	0.02	0.001	0.001	U	-					by vol
DICHIOI	omethane			000	0%	00075-09-	2 0.	10	1.44	0.02	0.02	U					ppm	by vol

			8					Sta	ate of L	ouisian	a									Date	of sul	bmíttal	
						Emissions	Inven	tory Qu	uestionn	naire (E	EIQ) for Air	r Pollut	ants					19.		Nov		201	3
E	nission P	oint ID N	10.	Des	criptive	Name of the I	Emission	s Source ((Alt. Name	e)		-	App	proxima	te Locatio	on of Stack	or Vent	(see inst	ructions)			
	1700			A	dvance	Fibres System			Shipping		Method					hing-Prima	ry Name				-	AD83	
Tem	no Subjec	ct Item II) No			(Emulsion	Blend 7	Tank)			UTM Zon Latitude	e 30	15	Hori	zontal 3	739000	mE	15 "	Vertical	3	32740	hundre	mN edths
I CIII	po Subjet	ct Atem II	No.								Longitude				31		3	15 "				hundre	
		0212																					
Physica	and Disc d Charac ge? (yes	teristics		eter (ft) or Sta narge Area (ft		Height of St Above Grade	The second second	Stack Gas Veloci		Condit	Gas Flow at tions, <u>not</u> at ard (ft ³ /min)		Gas Exit erature F)		Time urs per ye		Date Constru Modifi	ction or	Th	Percei roughp Emi	ıt Th		II II
	no		N	A ft ft²		NA f	t N	Α	ft/sec	NA	ft^3/min	NA	°F	8,	760	hr/yr		20	008 Jar Ma 25°	r Ju	1	l-Sep	Oct- Dec 25%
	T	Ty	ne of Fu	el Used and	Heat I	nput (see ins	structio	ns)		T				Operat	ting Par	ameters (include	units)			_		
Fuel				of Fuel	Alcut			MBTU/hr)	1				Ореги	- B Z 411		ameter			Descr	ption	1	
	a			NA			NA			N	ormal Operatin	g Rate/Thi	roughput										
	b				1 4					N	laximum Opera	ting Rate/	Throughp	out			NA						
	С				7.					D	esign Capacity/	Volume/C	Cylinder D	Displacen	nent		NA				H		
				Not	es					S	hell Height (ft)						NA						
									14	T	ank Diameter (f						NA						
										-	anks:		Roof	Fl	oating Ro	of		External				Inte	rnal
									- 1	_	Date Engine Ord						En	gine Moo	del Year				
									1	-	Date Engine Was					I D		= 1	C4 1		- 4	C41-	
										S	I Engines:		Rich Bu	-		Lean Bur	n	□ 2;	Stroke	Į.] 4	Strok	e
Em	ission Poi	1700-84.	. (Designa A	Equi	ntrol ipment iode	Control Equipment Efficiency		/ TAP lumber		Propo	osed Emission]	Rates		Emiss	mitted ion Rate irrent)	Add, Chang Delete,	e, C	Continuo Complian Method	ice	Concent Exit		n in G	and the same of
Polluta									Avera (lb/h		Maximum (lbs/hr)	1500000	nual ns/yr)	10000	nual ns/yr)	Unchan	ged	Method					
	late matte	r (PM ₁₀)																				gr/st	d ft ³
Sulfur							1				W												y vol
-	n oxides																					ppm l	
-	monoxid								V.					-									oy vol
-	OC (inch	uding thos	se listed be	low)	000	0%			<0.0	01	<0.01	<(0.01	<	0.01	U						-	oy vol
Lead												-		-					_			-	by vol
Chloro					000	0%		6-99-8	<0.0		<0.01		0.01		0.01	U			_				oy vol
Toluen	e				000	0%	0010	8-88-3	<0.0	01	<0.01	<	0.01		0.01	U	_		-				by vol
II .												4										DAIII	JY VUI

						1	S	tate of Louis	siana								Date of	submitta	il
					*	Emissions	Inventory Q	uestionnair	e (EIQ) for	Air Poll	utants						Nov	20	13
Er	(Desig	oint ID N	lo.				Emissions Source				Ap	proximate Locat			instruc		Datum	NA DOS	
	1700)-84B			Advance	a name of the second se	(AFS) Emulsion Loading)	n Shipping	Metho	_	15	The second secon	tching-Primary N 739000	mE	Ver	tical		NAD83 400	mN
Tem		ct Item II	No.			,	,		Latitue Longi	de 3	80° 90°	The state of the s		15 15		,		hundr	
Physica	and Disc	charge cteristics		neter (ft) charge Ai		Height of St Above Grade		city C	ack Gas Flow at onditions, <u>not</u> at andard (ft ³ /min)	Tem	Gas Exit perature (°F)	Normal Oper Time (hours per y	Con	Date of struction odification		Throu	ighput '	f Annua Through on Point	This
	по				ft	NA f	t NA	_ft/sec	NAft^3/π	in NA	_°F	8,760	_hr/yr		2008	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
	I	Ty	pe of Fu	uel Used	and Heat I	nput (see ins	tructions)		T			Operating Par	rameters (incl	ude uni	ts)		-		
Fuel	-		~	e of Fuel			put (MMBTU/b	r)					Parame			D	escript	on	
	a b			NA			NA		Normal Opera Maximum Op	erating Rat	e/Throughp	put	NA				717	7.6	34.
	C				Notes				Design Capac Shell Height		/Cylinder L	Displacement	NA NA		-				
					Tiotes				Tank Diamete				NA		_				
									Tanks:		ed Roof	Floating Re	oof 🗆	Exte	rnal			Inte	rnal
-									Date Engine	Ordered		-		Engine l	Model Y	ear ear			
									Date Engine	Was Built b	y Manufact	turer							
									SI Engines:		Rich Bu	urn 🗆	Lean Burn		2 Stro	ke		4 Strol	re
Emi	ssion Poi	int ID No 1700-84		ation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	P	roposed Emissi	on Rates	*	Permitted Emission Rate (Current)	Add, Change, Delete, or	Contin Compl Met	liance	5.000		ion in G at Stack	garden and an an an an an an an an an an an an an
Polluta	nt						×	Average (lb/hr)	Maximur (lbs/hr)	100	ons/yr)	Annual (tons/yr)	Unchanged	Met	iiou				
-	ate matte	r (PM ₁₀)	11.77	1															td ft ³
Sulfur d														-		-			by vol
Total Street, Square, or other Designation of the last	n oxides													-					by vol
-	monoxid		. 11		000	06			0.01		-0.01	0.01		-		-			by vol
-	OC (inch	uding thos	e listed be	elow)	000	0%		<0.01	< 0.01		<0.01	< 0.01	U	-		-			by vol
Lead Chlorop	rene				000	0%	00126-99-8	< 0.01	<0.01	_	<0.01	<0.01	Ü	-		-			by vol
Toluene					000	0%	00126-99-8	<0.01	<0.01		<0.01	<0.01	U	-					by vol
					000	0.70	00100-00-3	20.01	40.01		-0.01	-0.01							by vol

						Sta	ate of Loui	siana											Date of	submitt	al
					Emissions	Inventory Q	uestionnair	re (EIQ)) for Air	Pollut	ants								Nov	20	13
En		oint ID N	0.	Descriptive	Name of the E	missions Source	(Alt. Name)				App	proximate	Locatio	on of Stack	or V	ent (see i	nstruc	tions)			
	(Design		- 1		Liquid Disp	ersion Loading			Method			06,"Addr	ess Mato	hing-Prima	ary Na	me"			Datum	NAD83	
						Railcar Loading)			UTM Zone		15		ntal	73900		mE	Ver	tical	3327		mN
Temp	oo Subje	ct Item II	No.						Latitude	-90		-	31		-	15 15					redths redths
	EQT	0214							Longitude	-90		-	31		-	13				nulid	reduis
	and Disc		Diamete	er (ft) or Stack	Height of St			tack Gas I		Stack G	ALTERNATION OF THE PARTY OF THE	Norma	l Opera	ting		Date of			ercent o		
	l Charac ge? (yes		Discha	rge Area (ft²)	Above Grade	(ft) Veloc		onditions,		Tempe	PENANCE.	(hour	Time s per ye	02)		truction dificatio	5.75		ighput [_	The state of the s
Chan	ge. Gea	or no)				1	5	tandard (f	t'/min)	(°)	r)	(Hour	s per ye	ai)	MO	unicatio	"		Linisit		
	no	1	NIA.		NA f		ft/sec	NA	607/:-	NA	°F	8,70	50	he/s			2008	Jan- Mar	Apr- Jun	Jul-Sep	Oct- Dec
		.	NA	ft	NAf	t NA	Tusec	INA	ft^3/min	INA	Г	0,7	30	hr/yr	1			25%	25%	25%	25%
		1		ft²		1	-					}		-		-					
		Ту	pe of Fuel	Used and Heat I	nput (see ins	tructions)						Operati	ng Par	ameters	(inclu	ide unit	s)				
Fuel			Type of	f Fuel	Heat In	put (MMBTU/hr	:)							Pai	ramete	er		D	escripti	on	
	а		N/	Α		NA			al Operating						NA						
	b								num Operat						NA						
	С							_	Capacity/	Volume/C	ylinder D	Displaceme	nt		NA						
				Notes					Height (ft)						NA NA		-				
								Tank	Diameter (f	THE RESERVE OF THE PERSON NAMED IN	Roof	Flo	ating Ro	Brown	D D	Exter	mal			Int	ernal
							- 1		Engine Orde		Rooi	110	ating No	OI.		Engine I		/ear		HIT	Ciliai
									Engine Was		Manufact	urer		T		Lingine	vioder i	cai			
							1	SI En			Rich Bu			Lean Bur	n		2 Stro	ke		4 Stro	ke
Emi	ssion Po	int ID No 1700-85	. (Designatio	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number		Proposed	Emission F	Rates	181	Perm Emissio (Curr	n Rate	Add Chan Delete	ge,	Contin Compl Met	iance	130,000	ncentrat Exiting		
Polluta	nt						Average (lb/hr)		aximum lbs/hr)	1	nual s/yr)	Ann (tons		Unchar	ged	Iviet	lou				
	ate matte	r (PM ₁₀)								5										gr/s	std ft ³
Sulfur d			D .																	ppm	by vol
_	n oxides			•		7		-			-										by vol
	monoxid		11 . 11 .		000		0.000		0.002	-	01	0.0	21			-					by vol
	OC (incl	uding thos	se listed belov	w) 000	0%		0.003	_	0.003	0.	.01	0.0	JI	U							by vol
Lead Chlorop	rene			000	0%	00126-99-8	0.003		0.003	0	.01	0.0	71	U		-		_		The second second	by vol
Toluene				000	0%	00126-99-8	<0.003		<0.003		.001	<0.		U				_		_	by vol
CONTON					070	00100-00-3	30.001		~0.001	1				1							by vol
																				PP	

							Sta	ate of Louisi	iana					-	I	Date of	submitte	al
						Emissions	Inventory Q	uestionnaire	(EIQ) for Ai	r Pollutants					1	Nov	20)13
E		Point ID N	No.		Descriptive	Name of the I	Emissions Source	(Alt. Name)		Ap	pproximate Locati	on of Stack or V	ent (see	instruct	ions)			-
		mation) -93	- 1		F	ugitive Emissic	ons - Neoprene Ur	nit	Method		06,"Address Mate	ching-Primary Na	ame"		I	Datum	NAD83	3
						•			UTM Zor				mE	Verti	ical _	3327		mN
Tem	po Subje	ect Item II	D No.						Latitude Longitude	30 ° e -90 °	31		15		-			redths redths
	FUC	30004							Longitud	-90			13		-		nung	reduis
	and Dis	0	Dian	netèr (ft)	or Stack	Height of St	The same of the sa		ck Gas Flow at	Stack Gas Exit	Normal Opera		Date of				f Annu	
11 TO A STATE OF THE PARTY OF T	al Chara ige? (yes	or no)	Disc	charge A	rea (ft²)	Above Grade	e (ft) Veloci		nditions, <u>not</u> at ndard (ft³/min)	Temperature	Time (hours per ye		struction dification			-	Through n Point	
							1	Star	idara (it /min)	(°F)	(modes per ye	,		,				
	no	-	,	NA	ft	NA f	t NA	ft/sec N	IA ft^3/min	NA °F	8,760	hr/yr		1	Jan- Mar	Apr-	Jul-Sep	Oct-
		.	-			1121	· Aux	tu scc	Tr. Jimin	100	0,700			' F	25%	25%	25%	25%
			_		ft²						X.							
		Ту			l and Heat I	nput (see ins	tructions)				Operating Par	ameters (incl	ıde uni	ts)				
Fuel	-			e of Fuel		Heat In	iput (MMBTÚ/hr)				Paramet	er		D	escripti	on	
	a			NA			NA			g Rate/Throughput		NA				_	-	
	0								The second secon	ting Rate/Through		NA						
	Ic				Distant					/Volume/Cylinder I	Displacement	NA NA		-				
					Notes				Shell Height (ft) Tank Diameter (6)		NA NA		-				
									Tanks:	Fixed Roof	Floating Ro		Exte	rnal		П	Inte	ernal
									Date Engine Ord	ACTIVITIES OF THE PARTY OF THE	1 Journal Act		Engine l		ear			
								1	The second liverage and the se	s Built by Manufac	turer				,			
									SI Engines:	□ Rich B		Lean Burn		2 Strol	ce		4 Strol	ke
Em	ission Po	1-93	. (Designa	ation)	Control Equipment Code	Control Equipment Efficiency	HAP / TAP CAS Number	Pr	oposed Emission	Rates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Conti	liance			ion in C	
Polluta	int						П	Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met	nod				
-	late matte	er (PM ₁₀)															gr/s	std ft ³
_	dioxide																-	by vol
-	n oxides																	by vol
	monoxio								-		-						_	by vol
	OC (incl	uding thos	e listed be	low)	000	0%		0.57	0.57	2.23	2.23	U	-					by vol
Chloro	prenc		-		000	0.54	00126 00 8	0.27	0.37	1.60	1.00		-					by vol
Chloro					000	0%	00126-99-8 00108-88-3	0.37	0.37	0.22	1.60	U						by vol
	(mixed i	somers)			000	0%	01330-20-7	<0.01	<0.01	0.02	0.02	U						by vol
-																	Press	-,

Emission Point ID No. (Designation) 1-93	Control Equipment Code	Control Equipment Efficiency	HAP/TAP CAS Number	Pro	posed Emission R	ates	Permitted Emission Rate (Current)	Add, Change, Delete, or	Continuous Compliance	Concentration in Gases Exiting at Stack
Pollutant				Average (lb/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Method	
Dichloromethane			00075-09-2	< 0.01	< 0.01	0.02	0.02	U ·		ppm by vol
Tetrachloroethylene			00127-18-4	< 0.01	< 0.01	0.02	0.02	U		ppm by vol

						The second second	AND THE RESERVE AND THE PARTY									_		
							State of	Louisia	ana						,	Date of	submit	tal
					Emission	s Inventor	ry Questio	nnaire	(EIQ) for Ai	r Pollutants						Nov	20	013
E		Point ID N	lo.	Descr	iptive Name of th	e Emissions S	ource (Alt. Na	ime)	T	A	pproximate Locati	on of Stack or V	ent (see	instruc	tions)	~		
		-95				Clarifier			Method		06,"Address Mat	ching-Primary N	ame"			Datum	NAD8	3
									UTM Zon			739000	mE		tical	332	7400	mN
Tem	po Subje	ct Item II	No.						Latitude	30 8		3	15	_			•	iredths
	-		1						Longitude	-90 °	31	_'	15	_ "			hund	iredths
G. 1		QT	771	. (6:) C. I	1 77 11 6	G. 1 I G.		1 0. 1	0 7	10. 10. 54	I N 10		Y2 / 0		n		£ A	-1
	and Disc al Charac			eter (ft) or Stack	A STATE MADE AND A STATE OF	STATE OF THE PARTY	ck Gas Exit		k Gas Flow at ditions, <u>not</u> at	Stack Gas Exit	Normal Opera	CONTRACTOR OF THE PARTY OF THE	Date of struction				of Annu Throug	ALL MANAGEMENT
	nge? (yes		Disch	arge Area (ft²)	Above Gra	de (IL)	Velocity		dard (ft ³ /min)	Temperature (°F)	(hours per ye		odification				on Poin	
	8- 4				1	1		Stand	uaru (it /min)	(E)	(and and plant y							
	no							l				Sept		1995	Jan-	Apr-	Jul-Sep	0.00
		.	N	A ft	NA '	ft NA	ft/sec	NA.	ft^3/min	77 °F	8,760	hr/yr	1	1	Mar 25%	Jun 25%	2501	Dec
		^		ft ²	1	l		1				1			25%	25%	25%	25%
		Ту	-		eat Input (see i						Operating Par	The state of the s		ts)				
Fuel				of Fuel	Heat	Input (MMB'	TU/hr)	-				Parame	-		D	escript	ion	
	a			IA		NA		- 1	ALL DESCRIPTION OF THE PROPERTY OF THE PROPERT	g Rate/Throughput		27,000 ga	l/hr				3.0	
	b							4 1		ing Rate/Through		NA						
	С							4 1	and the same of th	Volume/Cylinder l	Displacement	125,000	gal	(Open tan	k WW	treatm	ent
				Notes				- 1	Shell Height (ft)			NA		_				
								1	Tank Diameter (f		T 5 . 5	NA	F /	<u></u>			Total	
									Tanks:	Fixed Roof	Floating Ro	of	Exte				Int	ernal
									Date Engine Ord				Engine l	Model Y	ear			
										Built by Manufac		T D		2 Stro	1		4 Stro	les
¥7	D.	- A VEN BY	/D 1		1 0 1	TIAD /TIA	n		SI Engines:	□ Rich B	urn □ Permitted	Lean Burn	U	2 5110	ке	U	43110	Re
Emi	ISSION POI	6-95	(Designat	ion) Contr Equipm Cod	nent Equipment	HAP / TA	DATE:	Proj	posed Emission I	Rates	Emission Rate (Current)	Add, Change, Delete, or	Contir Compl Metl	liance			ion in (Contract of the Contract of th
Polluta	nt							erage o/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Ivieti	nou				
_	late matte	r (PM ₁₀)															gr/s	std ft ³
	dioxide								-									by vol
	n oxides																ppm	by vol
	monoxid																	by vol
	OC (inclu	uding those	e listed belo	ow) 000	0%		<(0.01	< 0.01	<0.01		A						by vol
Lead																	and the same of the same of	by vol
Chlorop				000		00126-99		0.01	< 0.01	<0.01		A						by vol
Toluene	е			000	0%	00108-88	-3 <	0.01	< 0.01	<0.01		A	-				-	by vol
				Control of the Control					And the second s								ppm	by vol

			-			Sta	ate of Lou	iisiana										Date of	submitte	al
					Emissions	Inventory Qu	uestionna	ire (EIQ) for Ai	Pollut	ants							Nov	20	013
E		Point ID N	lo.	Descript	ve Name of the	Emissions Source	(Alt. Name)				App	proximat	e Locatio	on of Stack or	Vent (see	instruc	tions)			
	170	00-87		N	o. 10 Emulsion 8	Storage Tank Man	iway		Method UTM Zon	е	15			hing-Primary 1 739000	Name" mE	Ver	tical	Datum 3327		mN
Tem	po Subje	ect Item II	O No.						Latitude Longitude	30			31		15				hund	redths redths
		QTO																		
Physica	and Dis al Charac age? (yes	cteristics		ter (ft) or Stack arge Area (ft ²)	Height of St Above Grad		ity	Stack Gas Conditions Standard (s, not at	Stack G Temper	rature		al Opera Time rs per ye	Co	Date of instruction lodification		Throu	ercent o ghput ' Emissio	Throug	h This
	no	-	_	0.167 ft	55	ft 60.00	ft/sec	750	_ft^3/min	77	°F	8	1	hr/yr	0	2013	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
			7	ft²									8.70	1						
-		T	pe of Fue	l Used and Hea	Input (see in	structions)						Operati	ing Par	ameters (inc	lude uni	ts)				
Fuel			Type	of Fuel	Heat I	nput (MMBTU/hr	7)							Param	eter		D	escript	on	
	а		N	Α		NA		Norm	al Operatin	g Rate/Thre	oughput			42,000 16/	charge					
	b				/				mum Opera	-				NA						
	С							-	n Capacity/	Volume/C	ylinder D	Displaceme	ent	NA						
				Notes				Shell	Height (ft)					NA						
								-	Diameter (f					NA						
								Tank		Fixed	Roof	Flo	ating Ro	of 🗆	Exte				Int	ernal
								and the second name of	Engine Ord						Engine	Model Y	ear			
							- 1		Engine Was					ļ		1			10.	
								SIE	ngines:		Rich Bu	_		Lean Burn		2 Stro	ke		4 Stro	ke
Em	ission Po	1700-8	. (Designat	ion) Control Equipmen Code	Control Equipment Efficiency	HAP / TAP CAS Number		Proposed	Emission]	Rates	3	Emissi	nitted on Rate rrent)	Add, Change, Delete, or	Conti Comp Met			centrat Exiting		
Polluta							Average (lb/hr)	-	laximum (lbs/hr)		nual s/yr)		nual s/yr)	Unchanged	Met	nou				
		er (PM ₁₀)																		std ft ³
	dioxide																			by vol
	en oxides																			by vol
	monoxio											_								by vol
-	OC (incl	luding tho	se listed bel	ow) 000	0%		30.25		4097	1.	23			A	-					by vol
Lead					-	2010122			2527	-	0.2	-			-					by vol
Chloro				000	0%	00126-99-8	20.57	_	2527	-	83	-		A	-		_			by vol
Toluen	e			000	0%	00108-88-3	3.22		785	0.	13	-	_	A	+		_			by vol
T .					1							-				4.0			ווועע	UY YUI

							04	ate of Loui	ciono							. 1	Date of	submitt	al.
						T2 1 1			and the second second		D II						_ 000 01	- Jones	
						Emissions	Inventory Q	uestionnair	e (EIQ) for Air	Pollutants						Nov	20	13
																			- 1
E	nission F	Point ID N	0.		Descriptive	Name of the	Emissions Source	(Alt. Name)			Ap	proximate Location	on of Stack or V	ent (see	instruct	tions)			
		nation)							7										
	170	88-00			No.	13 Emulsion S	storage Tank Mai	iway		Method		06,"Address Mate			**		Datum	11110000	
Tom	na Euk!-	ct Item II	No							UTM Zon	e 15	Horizontal 3	The second second	mE 15	Vert	ical	3327	THE STATE OF	mN redths
) em	ho suple	ct item II) INO.							Longitude		31		15					redths
	EC	QTO						\$		Longitude	-50		V .	1.5				nunu	Journa
Stack	and Dis		Diam	eter (ft)	or Stack	Height of St	ack Stack Ga	s Exit St	ack Gas l	Flow at	Stack Gas Exit	Normal Opera	ting	Date of		P	ercent o	f Annu	al
The state of the s	l Charac	AND DESCRIPTION OF THE PERSON	Disc	harge Ar	rea (ft²)	Above Grade	e (ft) Veloc		onditions		Temperature	Time		struction			ghput	-	
Chan	ge? (yes	or no)					ix.	St	andard (I	[t³/min)	(°F)	(hours per ye	ar) Mo	dificatio	n		Emissio	n Point	
		1					1	1								Jan-	Apr-	Jul-Sep	Oct-
	no	. 1		0.167	ft	55 f	ft 60.00	ft/sec	750	ft^3/min	77 °F	26	hr/yr		2013	Mar	Jun		Dec
			_													25%	25%	25%	25%
			_		ft ²							(4)							
		Ту	pe of Fu	el Used	and Heat I	nput (see ins	structions)					Operating Par	ameters (inch	ude unit	ts)				
Fuel				of Fuel			nput (MMBTU/hi	r)				. 7	Paramet			D	escripti	on	
	a			NA '	10		NA		Norma	al Operating	Rate/Throughput		42,000 lb/cl	narge					
1011	b	2.75		(Maxin	num Operat	ing Rate/Throughp	out	NA					1	0.5
	С								Design	n Capacity/	Volume/Cylinder D	Displacement	NA						
					Notes				Shell I	Height (ft)			NA				3.		
										Diameter (f			NA						
									Tanks		Fixed Roof	Floating Ro	of 🗆	Exter				Int	ernal
										Engine Orde				Engine I	Model Y	ear			
								1			Built by Manufact			-	200			1.0.	
-			-						SI En	gines:	□ Rich Bu		Lean Burn	0 .	2 Stro	ke		4 Stro	ke
Em	ssion Po	int ID No	(Designa	tion)	Control Equipment	Control Equipment	HAP / TAP CAS Number					Permitted Emission Rate	Add,						
		1700-88			Code	Efficiency	,	F	roposed	Emission F	lates	(Current)	Change,	Contin		Con	centrat	ion in (Jases
													Delete, or	Compl	A CONTRACTOR OF THE PARTY OF TH		Exiting	at Stac	k
Polluta	nt	Tr.						Average (lb/hr)	1000000	aximum lbs/hr)	Annual (tons/yr)	Annual (tons/yr)	Unchanged	Met					
	ate matte	er (PM ₁₀)					*												std ft ³
Sulfur			10.0																by vol
-	n oxides		0.00																by vol
_	monoxid																		by vol
	OC (incl	uding thos	e listed be	low)	000	0%		46.41		4097	0.60		A					-	by vol
Lead					000	000	00107.00.0	- 12		0.507	0.50								by vol
Chloro					000	0%	00126-99-8	40		2527	0.52		A	-					by vol
Toluen					000	0%	00108-88-3	2.14	-	785	0.028	1	A	-					by vol
																		ppn	by vol

								State of	Louisiar	na .							-	Date of	submitt	al
						Emissions	Invento	ry Questio	nnaire (I	EIQ) for Air	Pollutants	i	*					Nov	20	13
Er	(Design		0.	I				ource (Alt. Na	me)	Mathad		•		n of Stack or Vo		instruc		Datum	NA DOS	
	170	0-89			No.	14 Emulsion S	torage I an	k Manway		Method UTM Zon	e	15 Horizont		ing-Primary Na 739000	nE	Ver		Datum 3327		mN
Tem		ct Item III	No.							Latitude Longitude	30 °	-	31	_	15 15					redths redths
Physica	and Disc I Charac ge? (yes	charge teristics		eter (ft) or S harge Area		Height of St.		ack Gas Exit Velocity	Condi	Gas Flow at tions, <u>not</u> at ard (ft ³ /min)	Stack Gas Ex Temperatur (°F)		ime	Cons	Pate of truction dificatio	1000000	Throu	ercent o ighput ' Emissio	Throug	h This
	no		-	0.167 ft		55 f	t	60.00 ft/sec	750	ft^3/min	77 °F	26	h	nr/yr		2013	Jan- Mar 25%	Apr- Jun 25%	Jul-Sep 25%	Oct- Dec 25%
				ft²								٠	-			=				
Fuel	_	Ту			nd Heat I	nput (see ins			1 +			Operating	g Para	meters (inclu		ts)				
ruei	a			of Fuel NA		Heat II	nput (MMI NA	(IU/nr)	1	Normal Operating	Rate/Throught	put	$\overline{}$	Paramete 42,000 lb/ch		-	D	escript	on	
	b						134.5		- 1	Aaximum Opera				NA	- 8-					
	С							4	-	Design Capacity/	Volume/Cylinde	er Displacement		NA						
				N	Votes				- 1	Shell Height (ft)			-	NA		-				
									I -	Tank Diameter (f	fixed Roof	Floati	ng Roo	NA .	Exte				Int	ernal
									I -	Tanks: Date Engine Orde		Floati	ng Roo		Engine l		Par		THE	emai
										Date Engine Was		facturer			Lingine	I I	cai			
										SI Engines:		Burn		Lean Burn		2 Stro	ke		4 Stro	ke
Emi	ssion Po	1700-89	. (Designa	and the same of th	Control quipment Code	Control Equipment Efficiency	HAP/T CAS Nur	2000	Prop	osed Emission l	Rates	Permitt Emission (Currer	Rate	Add, Change, Delete, or	Contin	liance	0.00000	centra Exiting		
Polluta	nt	E							erage b/hr)	Maximum (lbs/hr)	Annual (tons/yr)	Annua (tons/y		Unchanged	Met	hod				
	ate matte	r (PM ₁₀)																		std ft ³
Sulfur																			_	by vol
-	n oxides										1									by vol
	monoxid				000	0.00				1000			_						-	by vol
-	OC (incl	uding thos	e listed be	low)	000	0%		4	6.41	4097	0.60			A					_	by vol
Lead	25000				000	0.0%	00107.0	0.8	10	2527	0.52								and the same of the same of	by vol
Chloro Toluen					000	0%	00126-9		2.14	2527 785	0.52	-		A						by vol
Total					000	070	00100-0	0-3	6.14	703	0.020			Α						by vol
-	-														_				-	-

24. NSR Applicability Summary [LAC 33:III.504 and LAC 33:III.509] 🛛 N/A

This section consists of five tables. A-E, and is applicable only to new and existing major stationary sources (as defined in LAC 33:III.504 or in LAC 33:III.509) proposing to permit a physical change or change in the method of operation. It would also apply to existing minor stationary sources proposing a physical change or change in the method of operation where the change would be a major source in and of itself. Add rows to each table as necessary. Provide a written explanation of the information summarized in these tables. Consult instructions.

24.A. Project Summary

		A	В	С	D	E	F
Emission Point ID	Description	New, Modified, Affected, or Unaffected*	Pre-Project Allowables (TPY)	Baseline Actual Emissions (over 24-month period)	Projected Actual Emissions (TPY)	Post-Project Potential to Emit (TPY)	Changė
PM _{2.5}	24-Month Period: MM/I	DD/YYYY – MM/DD/YY	YYY				
						PM _{2.5} Change:	
PM ₁₀	24-Month Period: MM/I	DD/YYYY – MM/DD/YY	YY				
					<u> </u>	PM ₁₀ Change:	
SO ₂	24-Month Period: MM/I	DD/YYYY – MM/DD/YY	YYY				
				<u> </u>			
					<u> </u>	SO ₂ Change:	
NO _x	24-Month Period: MM/I	DD/YYYY – MM/DD/YY	YYY				
				<u></u>]	NO _X Change:	
co	24-Month Period: MM/I	DD/YYYY – MM/DD/YY					
	7						
						<u> </u>	

			<u></u>		СО	Change:	
voc	24-Month Period: MM/DD/	YYYY – MM/DD/YYY	Y				
	<u> </u>				voc	Change:	
CO ₂ e	24-Month Period: MM/DD/	YYYY - MM/DD/YYY	v				
					60.	Channel	
	emissions units are not required		Do about a sea	- 1:		Change:	
	reditable Contemporaneous						
	reditable Contemporaneou		В	c	D	E	F
ntempora Emission	_ 	/ – MM/DD/YYYY	B Pre-Project Allowables (TPY)	C Baseline Actual Emissions (over 24-month period)	D 24-Month Period	E Post-Project Potential to Emit (TPY)	F Chang
ontempora	nneous Period: MM/DD/YYYY	A Date of	Pre-Project Allowables	Baseline Actual Emissions (over		Post-Project Potential to Emit	
entempora Emission Point ID	nneous Period: MM/DD/YYYY	A Date of	Pre-Project Allowables	Baseline Actual Emissions (over		Post-Project Potential to Emit	
entempora Emission Point ID	nneous Period: MM/DD/YYYY	A Date of	Pre-Project Allowables	Baseline Actual Emissions (over		Post-Project Potential to Emit	
entempora Emission Point ID	nneous Period: MM/DD/YYYY	A Date of	Pre-Project Allowables	Baseline Actual Emissions (over		Post-Project Potential to Emit (TPY)	
Emission Point ID PM2.5	Description	A Date of	Pre-Project Allowables	Baseline Actual Emissions (over		Post-Project Potential to Emit (TPY)	
Emission Point ID PM2.5	Description	A Date of	Pre-Project Allowables	Baseline Actual Emissions (over	24-Month Period	Post-Project Potential to Emit (TPY)	

- -

		·		SO ₂ Change:
iO _x				
				NO _x Change:
со				
				CO Character
TIOG .				CO Change:
VOC				
		<u> </u>		
				VOC Change:
			<u> </u>	
CO₂e	· · · · · · · · · · · · · · · · · · ·			
	J	j		

24.C. BACT/LAER Summary

Emission Point ID	Pollutant	BACT/LAER	Limitation	Averaging Period	Description of Control Technology/Work Practice Standard(s)

24.D. PSD Air Quality Analyses Summary

		<u>A</u>	B	C	D	<u>E</u>	<u>F</u>	G	Н	I
Pollutant	Averaging Period	Preliminary Screening Concentration	Level of Significant Impact	Significant Monitoring Concentration	Background	Maximum Modeled Concentration	Modeled + Background Concentration	NAAQS	Modeled PSD Increment Consumption	Allowable Class II PSD Increment
		(μg/m³)	(μg/m³)	(μg/m³)	(μg/m³)	(μg/m³)	(μ <i>g/</i> m³)	$(\mu g/m^3)$	(μg/m³)	(μg/m³)
PM _{2.5}	24-hour		1.2	4				35		-
	Annual		0.3					15		<u> </u>
PM ₁₀	24-hour		5	10				150		30
	Annual		1	-				50		17
SO ₂	1-hour		7.8					195		<u>-</u>
	3-hour		25	-				1300		512
	24-hour		5	13				365		91
	Annual		1	-				80		20
NO _X	1-hour		7.5	-				188		•
	Annual		1	14				100		25
СО	1-hour		2000	-				40,000	-	-
	8-hour		500	575				10,000	-	-
Lead	3-month		-	0.1				1.5	-	-

	eview Offsets [LAC 33:III.517.D.16, LAC 33:III.504.D.4 & 5] N/A I project triggers Nonattainment New Source Review (NNSR).
NO _x :	
Is the applicant proposing to use internal of	offsets? Tyes No
If not, identify the source of the offsets.	Company:
•	Facility/Unit:
	Permit No.:
Is an ERC Bank Application included wit ☐ Yes ☐ No	h this application, or has an application already been submitted to LDEQ?
If the ERC application has already been so	ubmitted, give the date:
Identify the emissions units from which th	ne offsets will be obtained (reference specific Emission Point ID numbers).
VOC:	
Is the applicant proposing to use internal of	offcate? T Vec T Na
If not, identify the source of the offsets.	Company:
if not, identify the source of the offsets.	Facility/Unit:
	Permit No.:
Is an ERC Bank Application included with	h this application, or has an application already been submitted to LDEQ?
If the ERC application has already been su	ubmitted, give the date:
	ne offsets will be obtained (reference specific Emission Point ID numbers).
document should clearly differentiate between	sure the ERC Bank Application is completed properly. In the case of NO _X , the ween ozone season and non-ozone season actual emissions during the baseline e to indicate if a portion of the reductions are no longer surplus (e.g., due to new or a netting analysis, etc.).
24.F. Economic Impact	
Answer the following questions.	·
How many temporary jobs will be added	
How many permanent jobs will be added	as a result of this project?

24.G Notification of Federal Land Manager [LAC 33:III.504.E.1, LAC 33:III.509.P.1] Complete this section only if the proposed project triggers NNSR or PSD.

a. Is the proposed facility or modification located within 100 kilo	meters of a Cl	ass I Area? Tyes No
If Yes, determination of Q/d is not required; skip to the next questi	on. If No, cor	mplete the Q/d equation below:
$Q/d = \frac{PM_{10 \text{ (NEI)}} + SO_{2 \text{ (NEI)}} + NO_{X \text{ (NEI)}} + H_2SO_{4 \text{ (NEI)}}}{Class \text{ I km}} \text{ where:}$	PM _{10 (NEI)} SO _{2 (NEI)} NO _{X (NEI)} H ₂ SO _{4 (NEI)} Class I km	= net emissions increase of PM ₁₀ ^{1,2} = net emissions increase of SO ₂ ^{1,2} = net emissions increase of NO _X ^{1,2} = net emissions increase of H ₂ SO ₄ ^{1,2} = distance to nearest Class I Area ³
Q/d = + + + +	= = -	
If Q/d < 10, proceed to Section 25. If Q/d ≥ 10, complete the remains	under of this S	Section.
b. Has the applicant provided a copy of the application to the Fed	eral Land Ma	nager? 🗌 Yes 🔲 No
c. Does the application contain modeling that demonstrates no ad (AQRVs) in the Class I Area? Yes No	verse impact o	on Air Quality Related Values
d. If Yes, indicate the model used: VISCREEN PLUVU	ЕП 🗆 САІ	LPUFF Chher:4
e. Has the Federal Land Manager concurred that the proposed pro Yes No If Yes, please attach correspondence.	oject will not a	dversely impact any AQRVs?
If the net emissions increase of any pollutant is negative, enter " If the project did not trigger a netting analysis, use the project incorpollutant's significance level. In kilometers.	crease. In this	case, the value will be less than the
⁴ Model must be approved by LDEQ and the Federal Land Manage	<u>. </u>	

25. Environmental Assessment Statement (EAS or "IT" Question Responses) [La. R.S. 30:2018] ☐ Yes ☒ No

** This section is required when applying for new Part 70 operating permits and/or major modifications. Any applications for these permit types that do not include answers to these questions will not be considered to be administratively complete. **

For new Part 70 operating permits and/or major modifications, answers to these questions must be provided by the applicant to the local governmental authority and the designated public library at no additional costs to these entities. Consult instructions to determine what is considered to be a "local governmental authority" and a "designated public library". Indicate the name and address of the local governmental authority and the designated public library to which the answers to these questions were sent:

Name of	Local Governing	Authority	Name of	Designated Public	Library		
	Street or P.O. Box	<u>. </u>	Street or P.O. Box				
City	State	ZIP	City	State	ZIP		

Answer the following five questions on separate pages using full and complete answers. Include as many pages as necessary in order to provide full and complete answers. This information is required per Louisiana Revised Statutes 30:2018 (La. R.S. 30:2018).

Question 1: Have the potential and real adverse environmental effects of the proposed facility been avoided to the maximum extent possible? (This question requires the permittee to identify adverse environmental effects, both potential and real.)

Question 2: Does a cost benefit analysis of the environmental impact costs balanced against the social and economic benefits of the proposed facility demonstrate that the latter outweighs the former? (This question requires the permittee to perform a cost-benefit analysis, or at least a quantitative indication of the economic benefits and a qualitative description of the negative impacts expected from the permittee's operation. The latter should come from the answer to Question 1.)

Question 3: Are there alternative projects which would offer more protection to the environment than the proposed facility without unduly curtailing non-environmental benefits? (This question requires the permittee to demonstrate having considered alternate technologies.)

Question 4: Are there alternative sites which would offer more protection to the environment than the proposed facility site without unduly curtailing non-environmental benefits? (This is the question that deals directly with siting criteria.)

Question 5: Are there mitigating measures which would offer more protection to the environment than the facility as proposed without unduly curtailing non-environmental benefits? (This question requires the permittee to demonstrate having considered the most stringent techniques for reducing or more efficiently handling waste.)

PART 70 OPERATING PERMIT APPLICATION COMPLETENESS CHECKLIST

Instructions: Complete this checklist and submit with the completed air permit application.

LAC 33:Щ.	Completeness Questions Relative to the Part 70 Permit Application	Yes	No	NA	Location Within the Permit Application
517.A Timely Submittal	Was a Copy of the Application Also Submitted to EPA?	Х			Under Separate Cover
517.B.1,2 Certification	Does the Application include a Certification by a Responsible Official?	Х			Item 10 Section 3
517.B.3 Certification	Does the Application Include Certification by a Professional Engineer or their Designee:	х			Item 10 Section 3
517.D.1 Identifying Information	Does the Application Include:				
	Company Name, Physical and Mailing Address of Facility?	х			Items 1 & 2 Section 3
	2. Map showing Location of the Facility?	X			Figure 1
	3. Owner and Operator Names and Agent?	х			Item 1 Section 3
	4. Name and Telephone Number of Plant Manager or Contact?	х			Item 11 Section 3
517.D.2 SIC Codes, Source Categories	Does the Application Include a Description of the Source's Processes and Products?	х			Item 2 Section 3
	Does the Application Include the Source's SIC Code?	х			Item 5 Section 3
	Does the Application Include EPA Source Category of HAPs if applicable?	х			Section 3
517.D.3,6 EIQ Sheets	Has an EIQ Sheet been Completed for each Emission Point whether an Area or Point Source?	х			Item 23 Section 3
517.D.4 Monitoring Devices	Does the Application Include Identification and Description of Compliance Monitoring Devices or Activities?	х			Item 22 Section 3
517.D.5 Revisions and Modifications Only	For Revisions or Modifications, Does the Application include a Description of the Proposed Change and any Resulting Change in Emissions?	Х			Section 1 & Item 1, Section 3
517.D.7 General Information	Does the Application Include Information Regarding Fuels, Fuel Use, Raw Materials, Production Rates, and Operating Schedules as necessary to substantiate emission rates?	Х			Item 23 Section 3
517 D.8 Operating Limitations	Has Information Regarding any Limitations on Source Operation or any Applicable Work Practice Standards been Identified?	х			Item 22 Section 3
517.D.9 Calculations	Are Emission Calculations Provided?	Х			Appendix A

LAC 33:III.	Completeness Questions Relative to the Part 70 Permit Application	Yes	No	NA	Location Within the Permit Application
517.D.10 Regulatory Review	Does the Application Include a Citation and Description of Applicable Louisiana and Federal Air Quality Requirements and Standards?	Х			Item 22 Section 3
517.D.11 Test Methods	Has a Description of or a Reference to Applicable Test Methods Used to Determine Compliance with Standards been Provided?	X			Item 22 Section 3
517.D.12 Major Sources of TAPs	Does the Application include Information Regarding the Compliance History of Sources Owned or Operated by the Applicant (per LAC 33.III.5111)?	X			Item 14a Section 3
517.D.13 Major Sources of TAPs	Does the Application include a Demonstration to show that the Source Meets all Applicable MACT and Ambient Air Standard Requirements?	х			Section 2
517.D.14 PSD Sources Only	If Required by DEQ, Does the Application Include Information Regarding the Ambient Air Impact for Criteria Pollutants as Required for the Source Impact Analysis per LAC 33:III.509.K, L, and M?			х	
517 D.15 PSD Sources Only	If Required by DEQ, Does the Application Include a Detailed Ambient Air Analysis?			Х	
517.D.16, 18	Has any Additional Information been Provided?		X		
517.D.17 Fees	Has the Fee Code been Identified?	Х			Item 5 Section 2
	Is the Applicable Fee Included with the Application?		ļ 	X	
517.E.1 Additional Part 70 Requirements	Does the Certification Statement Include a Description of the Compliance Status of Each Emission Point in the Source with All Applicable Requirements?	х	i I		Item 10 Section 3
517E.2 Additional Part 70 Requirements	Does the Certification Statement Include a Statement that the Source will continue to Comply with All Applicable Requirements with which the Source is in Compliance?	х			Item 10 Section 3
517.E.3 Additional Part 70 Requirements	Does the Certification Statement Include a Statement that the Source will, on a timely basis, meet All Applicable Requirements that will Become Effective During the Permit Term?	х			Item 10 Section 3
517.E.4 Additional Part 70 Requirements	Are there Applicable Requirements for which the Source is not in Compliance at the Time of Submittal?		Х		
	Does the Application include a Compliance Plan Schedule?			х	
	Does the Schedule Include Milestone Dates for which Significant Actions will occur?			Х	
	Does the Schedule Include Submittal Dates for Certified Progress Reports?			Х	

LAC 33:III.	Completeness Questions Relative to the Part 70 Permit Application	Yes	No	NA	Location Within the Permit Application
517.E.5 Additional Part 70 Requirements Acid Rain	Is this Source Covered by the Federal Acid Rain Program?		х		
	Are the Requirements of LAC 33.III.517.E 1-4 included in the Acid Rain Portion of the Compliance Plan?			х	
517.E.6 Additional Part 70 Requirements	Have any Exemptions from any Applicable Requirements been Requested?		Х		
(Is the List and explanations Provided?			Х	
517.E.7 Additional Part 70 Requirements	Does the Application Include a Request for a Permit Shield?		Х		
	Does the Request List those Federally Applicable Requirements for which the Shield is Requested along with the Corresponding Draft Permit Terms and conditions which are Proposed to Maintain Compliance?			Х	
517.E.8 Additional Part 70 Requirements	Does the Application Identify and Reasonably Anticipated Alternative Operating Scenarios?		X		
	Does the Application include Sufficient Information to Develop permit Terms and Conditions for Each Scenario, Including Source Process and Emissions Data?			x	
517.F Confidentiality	Does the Application Include a Request for Non-Disclosure (Confidentiality)?		Х		
525.B. Minor Permit Modifications	Does the Application Include a Listing of New Requirements Resulting for the Change?		Х		
	Does the Application Include Certification by the Responsible Official that the Proposed Action Fits the Definition of a Minor Modification as per LAC 33:III.525.A.		Х		
	Does the Certification also Request that Minor Modification Procedures be Used?		Х		
	Does the Application, for Part 70 Sources, Include the Owner's Suggested Draft Permit and Completed Forms for the Permitting Authority to Use to Notify Affected States?		Х		-
La. R.S. 30:2018 – PSD/NNSR only	Has a copy of the answers to the questions posed in the Environmental Assessment Statement (Section 25) been sent to the local governing authority at no cost to the local governing authority?			х	
	Has a copy of the answers to the questions posed in the Environmental Assessment Statement (Section 25) been sent to the designated public library at no cost to the designated public library?			X	

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FIGURES

FIGURE 1 SITE LOCATION MAP

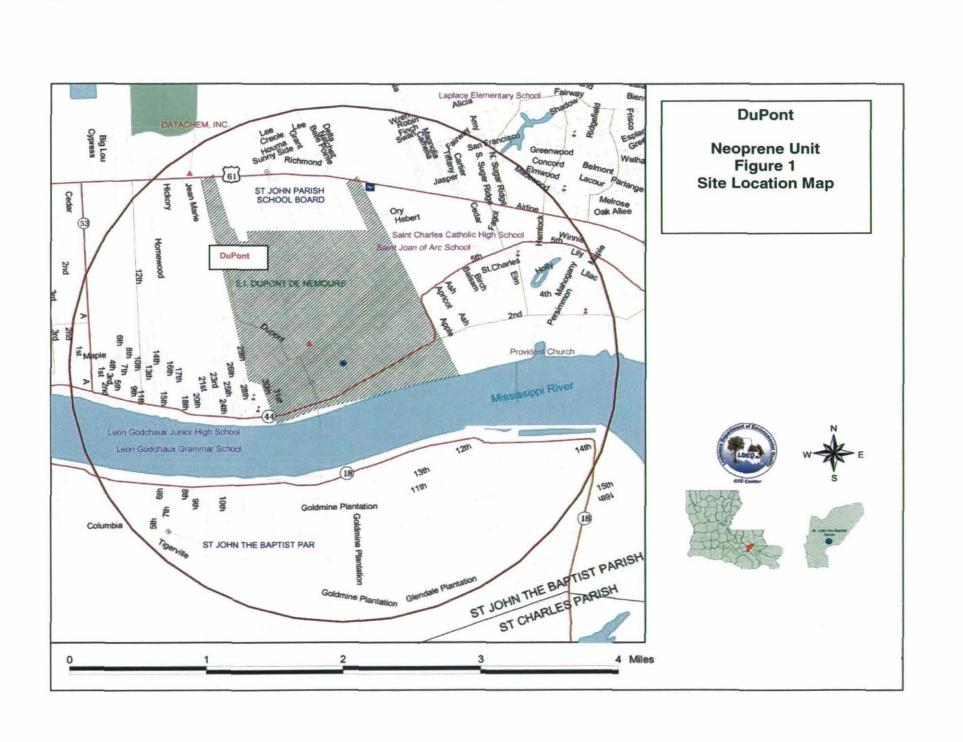
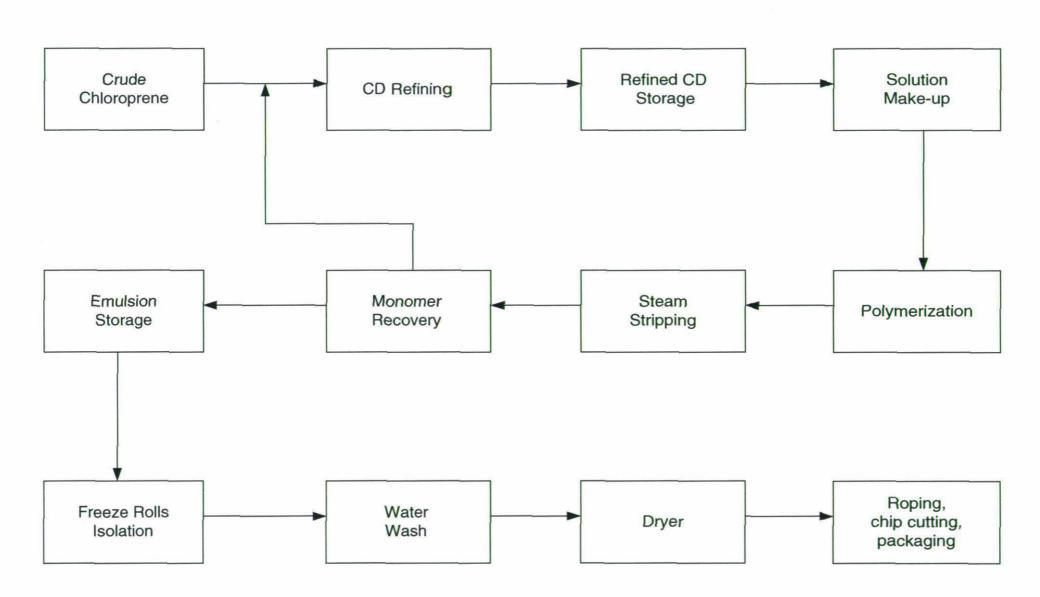
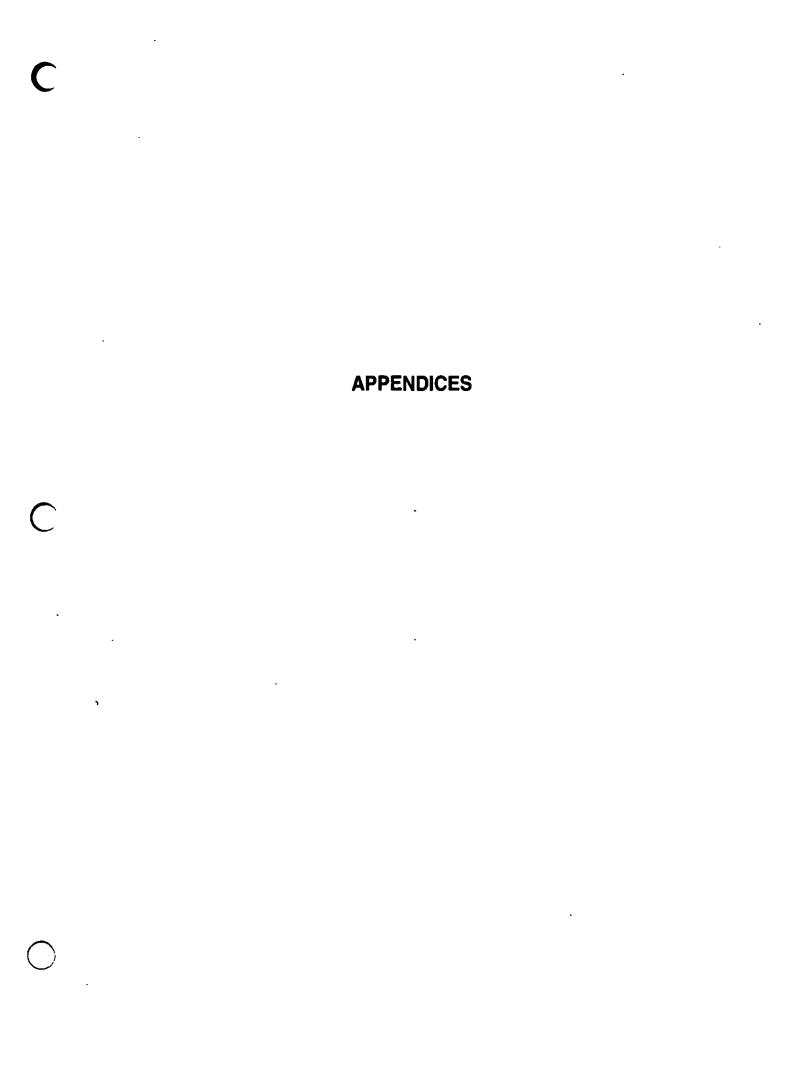


FIGURE 2 NEOPRENE UNIT PROCESS FLOW DIAGRAM

FIGURE 2
NEOPRENE UNIT PROCESS FLOW DIAGRAM





APPENDIX A AIR EMISSION CALCULATIONS



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT- PONTCHARTRAIN SITE

Source Description: No. 7 & 8 ESTs' Manway and EST 13 & 14 Strainer Exhaust Blower

TEMPO ID: EQT0134

Point Source ID No.: 1700-1

Page

1.

of

4

Basis:

The unstripped emulsion tank is vented down to atmospheric pressure and the nitrogen blanket which enters the top of the tank is turned off before opening the manway.

Emissions from the open manway and the agitator shaft seals are captured by the shaft seal ventilation system.

Emissions are based on spot sampling data conducted in September-October 2002 which showed an average chloroprene (CD) concentration of 16.3 ppm with a maximum concentration of 47 ppm.

The maximum concentration is estimated to be 10% greater than the maximum measured concentration.

Toluene and other VOC emissions are estimated using the fraction of saturation of CD. Conservatively assume ACR is still present in the material.

Based on field observation and engineering judgement, emissions from EST 13 & 14 drop strainer are insignificant.

Calculation basis provided by Mr. P. Offut, DuPont

Rated Capacity of Blower =

2500 cfm

Amount of Time Discharging =

8760 hours/yr

Average CD in Air Exhausted =

16.3 ppm CD by volume

Maximum CD in Air Exhausted =

51.7 ppm CD by volume

Molecular Weight of CD =

88.54 lb/lb-mole

Molecular Weight of Toluene =

92.14 lb/lb-mole

Molecular Weight of ACR =

122.99 lb/lb-mole

Temperature =

25 °C

Pressure =

14.696 psia

Average Emission Rates

Chloroprene

Using given information,

Average CD Emissions =

0.0408 cfm CD



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT-PONTCHARTRAIN SITE

Source Description: No. 7 & 8 ESTs' Manway and EST 13 & 14 Strainer Exhaust Blower

TEMPO ID: EQT0134

Point Source ID No.: 1700-1

Page

2

of

Using the Ideal Gas Law,

Average CD Emissions = Average CD Emissions =

0.000104 moles CD/minute 0.009221 lbs CD/minute

Average CD Emissions =

0.553 lbs CD/hour

Average CD Emissions = Average CD Emissions = 4847 lbs/yr 2.42 tons/yr

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation =

189.00 mm Hg

Total Vapor =

0.002550 moles/ft3

Mole Fraction CD = 0.001633333 %

CD Vapor =

0.00000004 moles/ft3

CD Partial Pressure =

0.012 mm Hg

Ratio =

0.000066

V.P. of Toluene at Saturation =

28.40 mm Hg

Toluene Partial Pressure =

0.0019 mm Hg

Toiuene Vapor = 0.000000006 moles/ft3

Toluene Vapor =

0.00002 moles/min

Toluene Vapor =

0.001 lb/min

Toluene Vapor =

0.09 lb/hr

Toluene Vapor =

0.38 tpy

ACR

Ratio =

0.000066

V.P. of ACR at Saturation =

42.28 mm Hq

ACR Partial Pressure =

0.0028 mm Hg

ACR Vapor =

0.00000001 moles/ft3

ACR Vapor =

0.00002 moles/min

ACR Vapor =

0.0029 lb/min

ACR Vapor =

0.17 lb/hr

ACR Vapor =

0.75 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT-PONTCHARTRAIN SITE

Source Description: No. 7 & 8 ESTs' Manway and EST 13 & 14 Strainer Exhaust Blower

TEMPO ID: EQT0134

Point Source ID No.: 1700-1

Page

3

of

4

Maximum Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions =

0.1293 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = Maximum CD Emissions =

0.000330 moles CD/minute 0.029187 lbs CD/minute

Maximum CD Emissions = Maximum CD Emissions =

1.751 lbs CD/hour

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation =

189.00 mm Hg

Total Vapor =

0.002550 moles/ft3

Mole Fraction CD =

0.00517 %

CD Vapor =

0.0000013 moles/ft3

CD Partial Pressure =

0.039 mm Hg

Ratio =

0.000208

V.P. of Toluene at Saturation =

28.40 mm Hg

Toluene Partial Pressure =

0.0059 mm Hg

Toluene Vapor =

0.00000002 moles/ft3

Toluene Vapor =

0.00005 moles/min

Toluene Vapor =

0.0046 lb/min

Toluene Vapor =

0.27 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT-PONTCHARTRAIN SITE

Source Description: No. 7 & 8 ESTs' Manway and EST 13 & 14 Strainer Exhaust Blower

TEMPO ID: EQT0134

Point Source ID No.: 1700-1

Page

4

of

4

ACR

Ratio =

0.000208

V.P. of ACR at Saturation =

42.28 mm Hg

ACR Partial Pressure =

0.0088 mm Hg

ACR Vapor = ACR Vapor =

0.0000003 moles/ft3 0.00007 moles/min

ACR Vapor =

0.0091 lb/min

ACR Vapor =

0.54 lb/hr

Summary

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
		Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	7110	0.812	2.569	3,555
Chloroprene	4847	0.553	1.751	2.423
Toluene	758	0.087	0.274	0.379
Total HAPs	5605	0.640	2.025	2.802
Total TAPs	5605	0.640	2.025	2.802



RTP Environmental Associates. Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Strippers Condenser Vent

TEMPO ID: RLP0014

Point Source ID No.: 1700-2 Page of

Basis:

Vapors from all three strippers pass through a vacuum pump to a single vent condenser cooled with -20 deg C brine.

Nitrogen flow is based on sampling data conducted by METCO on March 13, 2002 and March

Toluene emissions are estimated using the partial pressure of toluene produced in the unstripped emulsion.

Ammonia is added to the inlet of the condenser as an antifreeze and is emitted.

Calculation basis provided by Mr. P. Offut, DuPont

1,2-Dichlorobenzene emissions are based on a mass balance.

2 C Condenser Feed Temperature =

Condenser Exit Temperature = -14 C

Vapor Pressure of CD = 27.094 mm Hg @ -14 C

Vapor Pressure of Toluene = 2.566 mm Hg @ -14 C

Vapor Pressure of Toluene = 42.427 mm Hg @ 30 C

Vapor Pressure of ACR = 5.203 mm Hg @ -14 C

Vapor Pressure of ACR = 60.824 mm Hg @ 30 C

Molecular Weight of Toluene = 92.14 lb/lb-mole

Max. Mole Fraction Toluene = 0.00398

Molecular Weight of ACR = 122.99 lb/lb-mole

Max. Mole Fraction ACR = 0.000970 Operating Hours = 8760 hr

N2 flow =0.41250 lb/min N2 @ 760 mm Hg and 20 C

Average Emission Rates

Chloroprene

0.002934 moles/ft3 Total vapor =

CD vapor = 0.000105 moles/ft3 3.57 mole % CD

CD vapor = 0.009261 lbs CD/ft3 total vapor

Density of N2 = 0.08270 lb/ft3 760 mmHg & -14 deg C

N2 flow = 4.99 ft3/min for 3 strippers Total flow =

5.20 ft3/min for 3 strippers

CD Vapor flow = 0.19 ft3/min



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Strippers Condenser Vent

TEMPO ID: RLP0014

Point Source ID No.: 1700-2 Page 2 of 4

CD Vapor flow = 0.0482 lbs/min
CD Vapor flow = 2.89 lbs/hr
CD Vapor flow = 25309 lbs/yr

Toluene

Determine toluene content of feed to stripper condenser

Total vapor = 0.002764 moles/ft3

Liquid Mole Fraction Toluene = 0.003977 0.40 mole % toluene

Partial Pressure Toluene = 0.169 mm Hg

Toluene Vapor = 0.00000061 moles/ft3 0.0222 mole % toluene

Toluene Vapor flow = 0.0012 ft3/min

Total flow = 5.20 ft3/min

Toluene Vapor = 0.000003 moles/min

Toluene Vapor = 0.000294 lb/min

Determine toluene saturation at condenser exit conditions

Toluene Vapor = 0.000010 moles/ft3
Toluene Vapor = 0.000052 moles/min
Toluene Vapor = 0.004746 lb/min

Toluene enters the stripper below saturation conditions at the exit of the stripper. Assume that no toluene is removed.

Toluene Vapor = 0.000294 lb/min
Toluene Vapor = 0.02 lb/hr
Toluene Vapor = 154 lb/yr
Toluene Vapor = 0.08 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

3

of

Page

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Strippers Condenser Vent

TEMPO ID: RLP0014

Point Source ID No.: 1700-2

ACR

Determine ACR content of feed to stripper condenser

Total vapor = 0.002764 moles/ft3

Liquid Mole Fraction ACR = 0.000970 0.10 mole % ACR

Partial Pressure ACR = 0.0590 mm Hg

ACR Vapor = 0.00000021 moles/ft3 0.0078 mole % ACR

ACR Vapor flow = 0.00040 ft3/min

Total flow = 5.20 ft3/min

ACR Vapor = 0.000001 moles/min

ACR Vapor = 0.000137 lb/min

Determine ACR saturation at condenser exit conditions

ACR Vapor = 0.000020 moles/ft3
ACR Vapor = 0.000104 moles/min
ACR Vapor = 0.012845 lb/min

ACR enters the stripper below saturation conditions at the exit of the stripper. Assume that no ACR is removed.

ACR Vapor ≈ 0.000137 lb/min
ACR Vapor ≈ 0.01 lb/hr
ACR Vapor ≈ 72 lb/yr
ACR Vapor ≈ 0.04 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Strippers Condenser Vent

TEMPO ID: RLP0014

Point Source ID No.: 1700-2 Page 4 of

Ammonia

Based on Standard Operating Conditions,

Min NH3 addition per Stripper = 0 lb/hr
Max NH3 addition per Stripper = 1.5 lb/hr
Typically ammonia runs at 0.2 lb/hr

Ammonia has single addition point on vacuum pump discharge

NH₃ Addition to vacuum pump = 5256 lb/yr

Max NH_3 Addition = 39420 lb/yr at top of SOC

Mean NH₃ emissions assumed 2 x of typical addition 10512 lb/yr

 NH_3 Emissions = 10512 lbs/yr NH_3 Emissions = 1.20 lbs/hr NH_3 Emissions = 5.256 tpy

Maximum Emission Rates

Maximum emission rates are conservatively assumed to be 1.5 times the average emission rates.

Summary

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
	Į	Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	25535	2.915	4.372	12.768
Chloroprene	25309	2.889	4.334	12.654
1,2-Dichlrobenzer	0.01	0.000001	0.000002	0.000005
Toluene	154	0.018	0.026	0.077
Ammonia	10512	1.200	1.800	5.256
Total HAPs	25463	2.907	4.360	12.732
Total TAPs	35975	4.107	6.160	17.988



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3 Page 1 of 11

Basis:

Vapors from all 5 PK pass to a single vent condenser cooled by 2 deg C brine.

Assume all of the nitrogen flowing through the vent condenser will saturate with CD.

Assume vapors inlet and exit vent condenser are saturated with water

CD condensation in the condenser starts at about 6% CD in the inlet stream

Toluene emissions are based on sampling data on March 14, 2002 and March 18, 2002 by METCO Environmental.

On March 14, 2002 type AD was being produced, which includes toluene.

On March 18, 2002 type WHV was being produced which does not inloude toluene.

The average toluene emission rate measured was 0.2033 lb/hr for a product using a toluene-based stabilizer.

The highest toluene emission rate measured was 0.34 lb/hr for a product using a toluene-based stabilizer.

The average toluene emission rate measured was 0.0033 lb/hr for a product not using a toluene-based stabilizer.

The highest toluene emission rate measured was 0.0054 lb/hr for a product not using a toluene-based stabilizer.

Stabilizer, defoamer, Octopol and Dresinsate are added with the vent closed - insignificant emissions 1,2-Dichlorobenzene emissions are based on a mass balance.

Emulsification Temperature = 35 C Condenser Exit Temperature = 6 C

Worst case charge size = 41708 lb/charge

Worst Case Product Total Charges = 6743 charges/yr

ACR Type Charges = 6743 charges/yr Toluene Stabilizer Charges = 6557 charges/yr

Maximum Other Type Charges = 6381 charges/yr

Spec. Grav. Unstripped Emulsion = 1.060

Venting Time for Emulsification = 31.6 min/charge

Average Toluene Emissions = 0.2033 lb/hr with toluene-based stabilizer

Maximum Toluene Emissions = 0.3400 lb/hr with toluene-based stabilizer

Average Toluene Emissions = 0.0033 lb/hr without toluene-based stabilizer

Maximum Toluene Emissions = 0.0054 lb/hr without toluene-based stabilizer



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3 Page 2 of 11

Emission Rates

Emulsification

Determine the VOC's inlet the vent condenser to be piped to the new condensing system CD exit LPK =

1.5 % at start of emulsification

4.8 % 10 min after start of emulsification

6.8 % 15 min after start of emulsification

15.4 % 20 min after start of emulsification

26 % 31.6 min after start of emulsification

Charge Volume = 631 ft3/charge
Nitrogen Purge Rate = 158 ft3/charge
Avg. Displacement Charging Rate = 19.95 ft3/min

CD Displacement Rate = 0.30 ft3/min @ start of emulsification

CD Displacement Rate = 0.96 ft3/min @ 8.54 min after start of emulsification
CD Displacement Rate = 1.36 ft3/min @ 12.82 min after start of emulsification
CD Displacement Rate = 3.07 ft3/min @ 17.09 min after start of emulsification
CD Displacement Rate = 5.19 ft3/min @ 27 min after start of emulsification

nitrogen purge is off during emulsification

Average Displacement Rate = 19.95 ft3/min

% CD = 1.50 % @ start of emulsification

% CD = 4.80 % @ start of emulsification + 8.54 min % CD = 6.80 % @ start of emulsification + 12.82 min % CD = 15.40 % @ start of emulsification + 17.09 min % CD = 26.00 % @ start of emulsification + 27 min

Worst case of nitrogen saturated with CD and H2O at 35 C inlet condenser

Vapor Pressure of CD = 334.34 mm Hg Vapor Pressure of H2Q = 43.57 mm Hg

Total Vapor = 0.002468 moles/ft3

CD Vapor = 0.001086 moles/ft3 43.99 mole % CD

CD Vapor = 0.096122 lbs CD/ft3 total vapor

H2O Vapor = 0.000141 moles/ft3 5.73 mole % H2O

H2O Vapor = 0.002547 lbs H2O/ft3 total vapor

N2 Vapor = 0.001241 moles/ft3 50.28 mole % N2

N2 Vapor = 0.034739 fbs N2/ft3 total vapor



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

Page

3

of

11

At saturation exit condenser

Temperature =

6 C

Total Vapor =

0.002724 moles/ft3

CD Vapor Pressure =

104.34 mm Hg

CD Vapor =

0.00037399 moles/ft3

. 13.73 mole % CD

CD Vapor =

0.03311293 lbs CD/ft3 total vapor

H2O Vapor Pressure =

7.36 mm Hg

H2O Vapor =

0.00002637 moles/ft3

0.97 mole % H2O

H2O Vapor = (

0.00047470 lbs H2O/ft3 total vapor

N2 Vapor = 0.00047470 lbs 1320/11 N2 Vapor = 0.00232362 moles/ft3

85.30 mole % N2

N2 Vapor = 0.0

r = 0.06506138 lbs N2/ft3 total vapor

N2 Flow =

16.77 ft3/min @ start of emulsification

N2 Flow =

16.17 ft3/min @ 8.54 min after start of emulsification

N2 Flow =

15.81 ft3/min @ 12.82 min after start of emulsification 14.26 ft3/min @ 17.09 min after start of emulsification

N2 Flow = N2 Flow =

12.34 ft3/min @ 27 min after start of emulsification

Total Flow =

18.08 ft3/min @ start of emulsification

Total Flow =

17.16 ft3/min @ 8.54 min after start of emulsification

Total Flow =

18.08 ft3/min @ 12.82 min after start of emulsification

Total Flow =

18.08 ft3/min @ 12.82 min after start of emulsification 17.70 ft3/min @ 17.09 min after start of emulsification

Total Flow =

15.32 ft3/min @ 27 min after start of emulsification

CD Flow =

0.0654 lb/min @ start of emulsification

CD Flow =

0.1987 lb/min @ 8.54 min after start of emulsification

CD Flow =

0.2965 lb/min @ 12.82 min after start of emulsification

CD Flow =

0.5862 lb/min @ 17.09 min after start of emulsification

CD Flow =

0.5074 lb/min @ 27 min after start of emulsification

Straight line fit points and obtain area under curve

For first 8.54 min CD =

1.1283 lbs

For 8.54 to 12.82 min CD = For 12.82 to 17.09 min CD =

1.0577 lbs

For 17.09 to 27 min CD =

1.8855 lbs 5.4195 lbs

Total CD per Charge =

9.4910 lbs

Total CD per Year =

64002 lbs/vr

Total CD per Year =

32.00 tons/yr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3 Page 4 of 11

During emulsification, toluene emissions are quite low, per sampling much less than saturation at 2 C.

Conservatively assume toluene emissions are the same as measured by METCO even with the the larger, more efficient 2 C condenser.

Assume that toluene-based stabilizer types emit the same toluene as A-types (even though A-type stabilizer toluene is 2 times G-types).

A and G-type Maximum Toluene = 0.3400 lbs/hr Other Type Maximum Toluene = 0.0054 lbs/hr Average A and G-type Toluene = 0.2033 lbs/hr Average Other Type Toluene = 0.0033 lbs/hr Average A and G-type Toluene = 600 lbs/yr Average Other Type Toluene = 9 lbs/yr Total Toluene = 609 lbs/yr Total Average Toluene = 0.2065 lbs/hr

A similar DuPont facility in Louisville reported 0.054 lb/charge of ACR emissions for the types Pontchartrain will be making.

Conservatively assume ACR emissions are the same as the Louisville facility even with a larger, more efficient 2 C condenser.

ACR per Charge = 0.054 lbs/charge

Maximum ACR Emissions = 0.120 lbs/hr

Annual ACR Emissions = 364 lbs/yr

Average ACR Emissions = 0.120 lbs/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3 Page 5 of 11

Decompress Sampling

After stabilization, W types are cooled to 25 C, G-Types cooled to 33 C (GW to 30 C) and A-types are about 20 C.

After stabilization, the PK is vented for sampling through the sample port.

Once in a while, floating coag will be seen at this time and the manhole must be opened for skimming after stabilization.

Venting down occurs when the vast majority of the CD is converted to polymer and entrapped in the polymer, and after cool down of W types, so CD concentration in the vapor will be much less than during charging.

Although it is almost completely reacted in the process, assume ACR is still present.

Assume worst case of nitrogen saturated with CD, toluene, ACR and H2O and the Slocum vapor pressure for CD used in EST calculations.

Temperature =	25 C	
Vapor Pressure of CD =	189 mm Hg	
Vapor Pressure of Toluene =	28.40 mm Hg	
Vapor Pressure of ACR =	42.28 mm Hg	,
Vapor Pressure of H2O =	23.6 mm Hg	·
Total Vapor =	0.002550 moles/ft3	
CD Vapor =	0.000634 moles/ft3	24.87 mole % CD
CD Vapor =	0.056158 lbs CD/ft3 total	I vapor at saturation
Toluene Vapor =	0.000095 moles/ft3	3.74 mole % toluene
Toluene Vapor =	0.008782 lbs toluene/ft3	total vapor at saturation
ACR Vapor =	0.000142 moles/ft3	5.56 mole % ACR
ACR Vapor =	0.017450 lbs ACR/ft3 tot	al vapor at saturation
H2O Vapor =	0.000079 moles/ft3	3.11 mole % H2O
H2O Vapor =	0.001426 lbs H2O/ft3 tot	al vapor at saturation
Nitrogen Vapor =	0.001600 moles/ft3	62.73 mole % H2O
Nitrogen Vapor =	0.053274 lbs N2/ft3 total	vapor at saturation

Assume after the vent down occurs, 5 cfm nitrogen purge channels to vent and carries very little CD with it.



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3 Page 6 of 11

Total Volume of LPK = 825 ft3 Vapor Volume of LPK = 194 ft3 when fully charged Amount of Vapor Decompression = 13.23 ft3 exit the vent CD in Vapor Decompressed = 3.29 ft3 exit the vent CD in Vapor Decompressed = 0.18 lbs/charge exit the vent CD in Vapor Decompressed = 1246 lbs/yr exit the vent Toluene in Vapor Decompressed = 0.49 ft3 exit the vent Toluene in Vapor Decompressed = 0.0043 lbs/charge exit the vent Toluene in Vapor Decompressed = 29.28 lbs/yr exit the vent exit the vent ACR in Vapor Decompressed = 0.74 ft3 ACR in Vapor Decompressed = 0.01 lbs/charge exit the vent ACR in Vapor Decompressed = 86.60 lbs/yr exit the vent N2 in Vapor Decompressed = 8.30 ft3 exit the vent H2O in Vapor Decompressed = 0.41 ft3 exit the vent 0.5 N2 Purge = 0.00 ft3/min exit the vent Ventina Time = 1 min Total N2 Flow = 8.30 ft3/min exit the vent Total Venting Rate = 13.23 ft3/min exit the vent % CD of Total Venting Rate = 24.87 % CD exit the vent % Toluene of Total Venting Rate = 3.74 % toluene exit the vent % ACR of Total Venting Rate = 5.56 % ACR exit the vent Venting Temperature = 25 C exit the vent



RTP Environmental Associates. Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3 7 Page of 11

The PK emissions are directed to the vent condenser.

Using the same assumptions as for final emulsification venting calculations for initial vent down after stabilization,

> 6 C Temperature =

Total Vapor = 0.002724 moles/ft3 CD Vapor Pressure = 104.34 mm Ha

> CD Vapor = 0.00037399 moles/ft3 13.73 mole % CD

CD Vapor = 0.03311293 lbs CD/ft3 total vapor

Toluene Vapor Pressure = 9.77 mm Ha

> Toluene Vapor = 0.000035 moles/ft3 1.29 mole % toluene

Toluene Vapor = 0.003226 lbs toluene/ft3 total vapor

ACR Vapor Pressure = 16.39 mm Hg

> ACR Vapor = 0.000059 moles/ft3 2.16 mole % ACR

ACR Vapor = 0.007226 lbs ACR/ft3 total vapor

H2O Vapor Pressure = 7.36 mm Hg

> H2O Vapor = 0.00002637 moles/ft3 0.97 mole % H2O

0.00233502 lbs H2O/ft3 total vapor H2O Vapor =

N2 Flow = 8.30 ft3/min

% N2 of Total Flow = 85.30 %

Total Venting Rate = 9.73 ft3/min

CD Venting Rate = 1.3357 ft3/min CD Venting Rate = 0.3222 lb/min

CD Venting Rate = 0.3222 lbs/charge

CD Venting Rate = 2172 lbs/yr

Toluene Venting Rate = 0.1251 ft3/min

Toluene Venting Rate = 0.0314 lb/min

Toluene Venting Rate = 0.0314 lbs/charge

Toluene Venting Rate = 212 lbs/vr

ACR Venting Rate = 0.2098 ft3/min

ACR Venting Rate = 0.0703 lb/min

ACR Venting Rate = 0.0703 lbs/charge

ACR Venting Rate = 474 lbs/vr

H2O Flow = 0.0942 ft3/min

H2O Flow = 0.1992 lb/min

H2O Flow = 0.1992 lbs/charge

H2O Flow = 1343 lbs/yr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3 Page 8 of 1

Vent Open Sampling

In sample mode, the vent valve is opened, and the nitrogen purge closed off This period is for 1 minute; there will be some low concentration CD flows to the vent condenser for 1 minute.

This essentially repeats the emission for Decompress Sampling

Decompress for Wash

N2 in Vapor Decompressed =

After dropping the charge and displacing with 0.5 psig N2, the PK is vented down for water washing through the manway.

Normally, the manway with sight glass does not need to be opened to inspect the LPK is empty after dropping. However, once in a while the manhole must be opened to clean out popcom or coaq.

For these cases use data from decompress sampling for initial CD concentration early in the charging sequence (2% by volume) and assume that the venting occurs quickly It is assumed that toluene and ACR concentrations are proportional to the CD concentration. Assume after the vent down occurs, nitrogen purge channels to vent and carries very little CD with it.

Venting Temperature =	25 C	
Total Volume of LPK =	825 ft3	•
Amount of Vapor Decompression =	28 ft3	exit the vent
Total Vapor =	0.002550 moles/ft3	
CD Vapor =	0.000051 moles/ft3	2.00 mole % CD
CD Vapor =	0.004516 lbs CD/ft3	total vapor
Toluene Vapor =	0.000008 moles/ft3	0.30 mole % toluene
Toluene Vapor =	0.000706 lbs toluene	e/ft3 total vapor
ACR Vapor =	0.000011 moles/ft3	0.45 mole % ACR
ACR Vapor =	0.001403 lbs ACR/ft	3 total vapor
CD in Vapor Decompressed =	0.561 ft3	exit the vent
CD in Vapor Decompressed =	0.127 lbs/charge	exit the vent
CD in Vapor Decompressed =	855 lbs/yr	exit the vent
Toluene in Vapor Decompressed =	0.084 ft3	exit the vent
Toluene in Vapor Decompressed =	0.020 lbs/charge	exit the vent
Toluene in Vapor Decompressed =	134 lbs/yr	exit the vent
ACR in Vapor Decompressed =	0.126 ft3	exit the vent
ACR in Vapor Decompressed =	0.039 lbs/charge	
ACR in Vapor Decompressed =	266 lbs/yr	exit the vent

27.51 ft3

exit the vent



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3 Page 9 of 11

0.5 psig N2 Purge = 5.00 ft3/min exit the vent Venting Time = 1 min Total N2 Flow = 32.51 ft3/min exit the vent Total Venting Rate = 33.07 ft3/min exit the vent % CD of Total Venting Rate = 1.70 % CD exit the vent % Toluene of Total Venting Rate = 0.26 % toluene exit the vent % ACR of Total Venting Rate = 0.38 % ACR exit the vent 25 C Venting Temperature = exit the vent

The PK emissions are directed to the vent condenser.

Make the same assumptions as for final emulsification venting calculations.

Since nitrogen is much less than saturation at exit condenser conditions, condenser inlet and exit CD, toluene and ACR concentrations are essentially the same.

Total Venting Rate = 33.07 ft3/min CD Venting Rate = 0.561377 ft3/min CD Venting Rate = 0.135394 lbs/min CD Venting Rate = 0.14 lbs/charge CD Venting Rate = 913 lbs/yr Toluene Venting Rate = 0.084360 ft3/min Toluene Venting Rate = 0.021173 lbs/min Toluene Venting Rate = 0.02 lbs/charge Toluene Venting Rate = 143 lbs/vr ACR Venting Rate = 0.125573 ft3/min ACR Venting Rate = 0.042070 lbs/min ACR Venting Rate = 0.04 lbs/charge ACR Venting Rate = 284 lbs/yr

Vent Open for Wash

For PK wash, PK is empty and filled with nitrogen; vent valve is open, but nitrogen purge is off. There is a very low flow of vaporwith some low CD concentration to condenser for 10 minutes. chimney effect will draw air in through manway and out the vent, located nearby. There is no depressurization, so flow is deminimus and can be neglected.



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3 Page 10 of 11

Decompress to Emulsify

Before allowing emulsification to begin (vent valve to open), 0.3 psig must be detected in the LPK. A vent down from 0.3 to 0 psig occurs at the start of emulsification.

For this case use data from decompress sampling for initial CD concentration early in the charging sequence inlet the vent condenser (2% by volume) since the venting occurs quickly. It is assumed that toluene and ACR concentrations are proportional to the CD concentration.

1			
Venting Temperature =	25	С	
Total Volume of LPK =	825	ft3	
Amount of Vapor Decompression =	16.84	ft3	exit the vent
Total vapor =	0.002550	moles/ft3	•
CD Vapor =	0.000051	moles/ft3	2.00 mole % CD
CD Vapor =	0.004516	lbs CD/ft3 tota	al vapor
Toluene Vapor =	800000.0	moles/ft3	0.30 mole % toluene
Toluene Vapor =	0.000706	lbs toluene/ft3	total vapor
ACR Vapor =		moles/ft3	0.45 mole % ACR
ACR Vapor =	0.001403	lbs ACR/ft3 to	tal vapor
CD in Vapor Decompressed =	0.337	ft3	exit the vent
CD in Vapor Decompressed =	0.076	lbs/charge	exit the vent
CD in Vapor Decompressed =	513	lbs/yr	exit the vent
Toluene in Vapor Decompressed =	0.050616	ft3	exit the vent
Toluene in Vapor Decompressed =	0.011895	lbs/charge	exit the vent
Toluene in Vapor Decompressed =	80	lbs/yr	exit the vent
ACR in Vapor Decompressed =	0.075344	ft3	exit the vent
ACR in Vapor Decompressed =	0.023634	lbs/charge	exit the vent
ACR in Vapor Decompressed =	159	lbs/yr	exit the vent
N2 in Vapor Decompressed =	16.50	ft3	exit the vent
0.5 N2 Purge =	5.00	ft3/min	exit the vent
Venting Time =	1	min	
Total N2 Flow =		ft3/min	exit the vent
Total Venting Rate =		ft3/min	exit the vent
% CD of Total Venting Rate =		% CD	exit the vent
% Toluene of Total Venting Rate =		% toluene	exit the vent
% ACR of Total Venting Rate =		% ACR	exit the vent
Venting Temperature =	25	C .	exit the vent



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles Vent Condenser

TEMPO ID: RLP0015

Point Source ID No.: 1700-3

Page

11

11

The PK emissions are directed to the vent condenser.

Make the same assumptions as for final emulsification venting calculations.

Since nitrogen is much less than saturation at exit condenser conditions, condenser inlet and

exit CD concentration are essentially the same.

For vent down prior to emulsification

Since nitrogen is much less than saturation at exit condenser conditions -

21.84 ft3/min Total Venting Rate = CD Venting rate = 0.336826 ft3/min CD Venting rate = 0.081236 lbs/min CD Venting rate = 0.08 lbs/charge CD Venting rate = 548 lbs/yr Toluene Venting Rate = 0.050616 ft3/min Toluene Venting Rate = 0.012704 lbs/min Toluene Venting Rate = 0.01 lbs/charge Toluene Venting Rate = 86 lbs/yr ACR Venting Rate = 0.075344 ft3/min ACR Venting Rate = 0.025242 lbs/min ACR Venting Rate = 0.03 lbs/charge ACR Venting Rate = 170 lbs/yr

Summary

ACR is potentially emitted at a level of 0.54 tpy, although it is not present in the worst case product. Therefore, ACR totals are not part of the annual VOC emission totals and are calculated only for reference.

Compound	Total	Average	Maximum	Annual
}	Loss	Emission	Emission	Emissions
	j	Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	68685	7.841	35.631	34.342
Chloroprene	67635	7.721	35.171	33.818
1,2-Dichlorobenze	10	0.001	0.001	0.005
Toluene	1050	0.120	0.340	0.525
Total HAPs	68695	7.842	35.513	34.347
Total TAPs	68695	7.842	35.513	34.347



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Unstripped Emulsion Storage Tanks Common Vent & Cap

TEMPO ID: GRP0008

Point Source ID No.: 1700-5

Page

of

Basis:

Common vent for Unstripped Emulsion Storage Tank No. 6 (1700-5.3/EQT0150), Unstripped Emulsion Storage Tank No. 7 (1700-5.4/EQT0151), Unstripped Emulsion Storage Tank No. 8 (1700-5.5/EQT0152), Unstripped Emulsion Storage Tank No. 10 (1700-5.6/EQT0153), Unstripped Emulsion Storage Tank No. 11 (1700-5.7/EQT0154), and Unstripped Emulsion Storage Tank No. 14 (1700-5.8/EQT0155).

Emissions:

				•
Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
		Rate	Rate	ſ
	lb/yr	lb/hr	ib/hr	tpy
Total VOC	5898	0.673	-	2.949
Chloroprene	5826	0.665	-	2.913
1,2-Dichlorobenze	0.004	0.000	-	0.000
Toluene	51	0.006	-	0.025
Total HAPs	5877	0.671	-	2.938
Total TAPs	5877	0.671	-	2.938



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 6 Emulsion Storage Tank Manway & Stripper Feed Strainers

TEMPO ID: EQT0167

Point Source ID No.: 1700-5A Page 1 of 4

Basis:

No. 6 EST is used solely for storage of unstripped WBG-2 emulsion or stripped emulsion of other types. WBG-2 is fully converted, so CD emissions are deminimus even from unstripped WBG-2 emulsion.

The unstripped emulsion (USE) tank is vented down to atmospheric pressure and the nitrogen blanket which enters the top of the tank is turned off before opening the manway.

Ventilation around the two stripper feed strainers and ventilation on the popcorn drum and emulsion drum are connected to this blower. This is the source of CD to this emisssion point. Based on operator estimates, volume calculations and field observations, 5 to 6 gallons of emulsion drains from the strainer each cleaning.

When the emulsion drum is full, it is pumped back into the USE tank. When the popcorn drum is full it is moved to the drum pad and steamed before landfill disposal.

A strainer is to be cleaned each shift (12 hrs) minimum.

Strainer cleaning frequency does not correlate with stripper feed rate or strippers on line but does correlate with type and type changes (A's to W's in particular)

Per actual practice, while on A-types the frequency is about once/8 hr and once/12 hr while on W-types.

Emissions are based on spot sampling data conducted in September-October 2002 which showed an average chloroprene (CD) concentration of 3.4 ppm with a maximum concentration of 4.7 ppm.

The maximum concentration is estimated to be 10% greater than the maximum measured concentration.

Toluene and other VOC emissions are estimated using the fraction of saturation of CD. Conservatively assume ACR is still present in the material.

Calculation basis provided by Mr. P. Offut, DuPont

Rated Capacity of Blower =

Amount of Time Discharging =

Average CD in Air Exhausted =

Maximum CD in Air Exhausted =

Molecular Weight of CD =

Molecular Weight of Toluene =

Molecular Weight of ACR =

Temperature =

Pressure = ·

7400 cfm

8760 hours/yr

3.4 ppm CD by volume

5,17 ppm CD by volume

88.54 lb/lb-mole

92.14 lb/lb-mole

122.99 lb/lb-mole

25 °C

14.696 psia



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 6 Emulsion Storage Tank Manway & Stripper Feed Strainers

TEMPO ID: EQT0167

Point Source ID No.: 1700-5A Page 2

Average Emission Rates

Chloroprene

Using given information,

Average CD Emissions =

0.0252 cfm CD

Using the Ideal Gas Law,

Average CD Emissions = 0.000064 moles CD/minute

Average CD Emissions = 0.005682 lbs CD/minute

Average CD Emissions = 0.341 lbs CD/hour

Average CD Emissions = 2986 lbs/yr

Average CD Emissions =

1.49 tons/yr

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation = 189.00 mm Hg

Total Vapor = 0.002550 moles/ft3

Mole Fraction CD = 0.00034 %

CD Vapor = 0.00000001 moles/ft3

CD Partial Pressure = 0.003 mm Hg

Ratio = 0.000014

V.P. of Toluene at Saturation ≈ 28.40 mm Hg
Toluene Partial Pressure ≈ 0.0004 mm Hg

Toluene Vapor = 0.000000001 moles/ft3
Toluene Vapor = 0.00001 moles/min

Toluene Vapor = 0.001 lb/min
Toluene Vapor = 0.05 lb/hr
Toluene Vapor = 0.23 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 6 Emulsion Storage Tank Manway & Stripper Feed Strainers

TEMPO ID: EQT0167

Point Source ID No.: 1700-5A

Page

ACR

Ratio = 0.000014

V.P. of ACR at Saturation = 42.28 mm Hg ACR Partial Pressure = 0.0006 mm Hg

ACR Vapor = 0.000000002 moles/ft3 ACR Vapor = 0.00001 moles/min ACR Vapor = 0.0018 lb/min ACR Vapor = 0.11 lb/hr

ACR Vapor = 0.46 tpy

Maximum Emission Rates

Using given information,

Maximum CD Emissions = 0.0383 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = 0.000098 moles CD/minute Maximum CD Emissions = 0.008639 lbs CD/minute Maximum CD Emissions = 0.518 lbs CD/hour



RTP Environmental Associates, Inc. Kenner, Louisiana

of

4

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 6 Emulsion Storage Tank Manway & Stripper Feed Strainers

TEMPO ID: EQT0167

Point Source ID No.: 1700-5A Page 4

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation = 189.00,mm Hg

Total Vapor = 0.002550 moles/ft3

Mole Fraction CD = 0.000517 %

CD Vapor = 0.00000001 moles/ft3

CD Partial Pressure = 0.004 mm Hg

Ratio = 0.000021.

V.P. of Toluene at Saturation = 28.40 mm Hg

Toluene Partial Pressure = 0.0006 mm Hg

Toluene Vapor = 0.000000002 moles/ft3
Toluene Vapor = 0.00001 moles/min

Toluene Vapor = 0.0014 lb/min Toluene Vapor = 0.08 lb/hr

ACR

Ratio = 0.000021

V.P. of ACR at Saturation = 42.28 mm Hg

ACR Partial Pressure = 0.0009 mm Hg

ACR Vapor = 0.000000003 moles/ft3 ACR Vapor = 0.00002 moles/min ACR Vapor = 0.0027 lb/min

ACR Vapor = 0.16 lb/hr

Summary

Compound	Tota!	Average	Maximum	Annual
}	Loss	Emission	Emission	Emissions
	1	Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	4381	0.500	0.761	2.191
Chloroprene	2986	0.341	0.518	1.493
Toluene	467	0.053	0.081	0.234
Total HAPs	3453	0.394	0.599	1.727
Total TAPs	3453	0.394	0.599	1.727



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettle No. 1 & 2 Manway / Drop Strainers

TEMPO ID: EQT0135

Point Source ID No.: 1700-13 Page 1 of

Basis:

The manways and drop strainers on each PK are equipped with ventilation systems.

The strainer cleanings solids drums and emulsion drums are equipped with lids and protective ventilation.

Since the manway is seldom opened when the PK is charged, emissions should be small.

The manway on each PK is opened once per day for inhibitor spraying of the dome. Since this is done after the charge is completed and cooled, CD concentrations are low and emissions should be low.

Opening and cleaning the strainer after dropping the charge and water flushing results in emissions. Emissions are based on spot sampling data for the exhaust blower for PK 3, 4 & 5 conducted in September-October 2002 which showed an average chloroprene (CD) concentration of 14.45 ppm with a maximum concentration of 15.37 ppm.

The maximum concentration is estimated to be 10% greater than the maximum measured concentration.

Toluene and other VOC emissions are estimated using the fraction of saturation of CD. Conservatively assume ACR is still present in the material.

Calculation basis provided by Mr. P. Offut, DuPont

Rated Capacity of Blower = 6900 cfm
Amount of Time Discharging = 8760 hours/yr

Average CD in Air Exhausted = 14.45 ppm CD by volume

Maximum CD in Air Exhausted = 16.91 ppm CD by volume

Molecular Weight of CD = 88.54 lb/lb-mole
Molecular Weight of Toluene = 92.14 lb/lb-mole
Molecular Weight of ACR = 122.99 lb/lb-mole

Temperature = 30 °C Pressure = 14.696 psia

Average Emission Rates

Chloroprene

Using given information,

Average CD Emissions = 0.0997 cfm CD



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettle No. 1 & 2 Manway / Drop Strainers

TEMPO ID: EQT0135

Point Source ID No.: 1700-13

Page

2

of

4

Using the Ideal Gas Law,

Average CD Emissions = 0.000250 moles CD/minute
Average CD Emissions = 0.022144 lbs CD/minute
Average CD Emissions = 1.329 lbs CD/hour

11639 lbs/rr

Average CD Emissions = 11639 lbs/yr Average CD Emissions = 5.82 tons/yr

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation = 280.10 mm Hg

Total Vapor = 0.002508 moles/ft3

Mole Fraction CD = 0.001445 %

CD Vapor = 0.00000004 moles/ft3

CD Partial Pressure = 0.011 mm Hg

Ratio = 0.000039

V.P. of Toluene at Saturation = 36.61 mm Hg

Toluene Partial Pressure = 0.0014 mm Hg

Toluene Vapor = 0.000000005 moles/ft3
Toluene Vapor = 0.00003 moles/min
Toluene Vapor = 0.003 lb/min
Toluene Vapor = 0.18 lb/hr

Toluene Vapor =

0.79 tpy

ACR

Ratio = 0.000039

V.P. of ACR at Saturation = 53.19 mm Hg

ACR Partial Pressure = 0.0021 mm Hg

ACR Vapor = 0.00000001 moles/ft3
ACR Vapor = 0.00005 moles/min

ACR Vapor = 0.0058 lb/min. ACR Vapor = 0.35 lb/hr ACR Vapor = 1.54 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettle No. 1 & 2 Manway / Drop Strainers

TEMPO ID: EQT0135

Point Source ID No.: 1700-13

Page

3

of

Maximum Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions =

0.1167 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = Maximum CD Emissions = 0.000293 moles CD/minute 0.025910 lbs CD/minute

Maximum CD Emissions =

1.555 lbs CD/hour

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation =

280.10 mm Hq

Total Vapor =

0.002508 moles/ft3

Mole Fraction CD =

0.0016907 %

CD Vapor =

0.00000004 moles/ft3

CD Partial Pressure =

0.013 mm Hg

Ratio =

0.000046

V.P. of Toluene at Saturation =

36.61 mm Hg

Toluene Partial Pressure =

0.0017 mm Hg

Toluene Vapor =

0.00000001 moles/ft3 0.00004 moles/min

Toluene Vapor = Toluene Vapor =

0.0035 lb/min

Toluene Vapor =

0.21 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettle No. 1 & 2 Manway / Drop Strainers

TEMPO ID: EQT0135

Point Source ID No.: 1700-13

Page

ļ

of

4

ACR

Ratio = 0.000046

V.P. of ACR at Saturation = 53.19 mm Hg
ACR Partial Pressure = 0.0024 mm Hg

ACR Vapor = 0.00000001 moles/ft3
ACR Vapor = 0.00006 moles/min
ACR Vapor = 0.0068 lb/min
ACR Vapor = 0.41 lb/hr

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
	1	Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	16292	1.860	2.176	8.146
Chloroprene	11639	1.329	1.555	5.820
Toluene	1583	0.181	0.211	0.792
Total HAPs	13222	1.509	1.766	6.611
Total TAPs	13222	1.509	1.766	6.611



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles No. 3, 5 & 5 Manway / Drop Strainers

TEMPO ID: EQT0136

Point Source ID No.: 1700-13A

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Basis:

The manways, sample ports and drop strainers on each PK are equipped with ventilation systems. The strainer cleanings solids drums and emulsion drums are equipped with lids and protective ventilation.

With the changes in PK nitrogen blanketing and CD concentrations being low at the end of the charge, the emissions from the sample port should be very small

Since the manhole is seldom opened when the PK is charged, emissions should be small. The manway on each PK is to be opened once per day for inhibitor spraying of the dome. Since this is done after the charge is completed and cooled, CD concentrations are low and emissions should be low.

Opening and cleaning the strainer after dropping the charge and water flushing results in emissions. Emissions are based on spot sampling data conducted in September-October 2002 which showed an average chloroprene (CD) concentration of 14.45 ppm with a maximum concentration of 15.37 ppm.

The maximum concentration is estimated to be 10% greater than the maximum measured concentration.

Toluene and other VOC emissions are estimated using the fraction of saturation of CD. Conservatively assume ACR is still present in the material.

Calculation basis provided by Mr. P. Offut, DuPont

Rated Capacity of Blower = 8500 cfm

Amount of Time Discharging = 8760 hours/vr

Average CD in Air Exhausted = 14.45 ppm CD by volume

Maximum CD in Air Exhausted = 16.91 ppm CD by volume

Molecular Weight of CD = 88.54 lb/lb-mole

Molecular Weight of Toluene = 92.14 lb/lb-mole

Molecular Weight of ACR = 122.99 lb/lb-mole

Temperature = 30 °C Pressure = 14.696 psia

Average Emission Rates

Chloroprene

Using given information,

Average CD Emissions =

0.1228 cfm CD



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles No. 3, 5 & 5 Manway / Drop Strainers

TEMPO ID: EQT0136

Point Source ID No.: 1700-13A

Page

4

Using the Ideal Gas Law,

Average CD Emissions = 0.000308 moles CD/minute
Average CD Emissions = 0.027279 lbs CD/minute
Average CD Emissions = 1.637 lbs CD/hour
Average CD Emissions = 14338 lbs/yr
Average CD Emissions = 7.17 tons/yr

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation = 280.10 mm Hg

Total Vapor = 0.002508 moles/ft3

Mole Fraction CD = 0.001445 %

CD Vapor = 0.00000004 moles/ft3

CD Partial Pressure = 0.011 mm Hg

Ratio = 0.000039

V.P. of Toluene at Saturation = 36.61 mm Hg

Toluene Partial Pressure = 0.0014 mm Hg

Toluene Vapor = 0.000000005 moles/ft3
Toluene Vapor = 0.000004 moles/min
Toluene Vapor = 0.004 lb/min
Toluene Vapor = 0.22 lb/hr
Toluene Vapor = 0.98 tpy

ACR

Ratio = 0.000039

V.P. of ACR at Saturation = 53.19 mm Hg ACR Partial Pressure = 0.0021 mm Hg

ACR Vapor = 0.00000001 moles/ft3

ACR Vapor = 0.00006 moles/min

ACR Vapor = 0.0072 lb/min ACR Vapor = 0.43 lb/hr ACR Vapor = 1.89 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles No. 3, 5 & 5 Manway / Drop Strainers

TEMPO ID: EQT0136

Point Source ID No.: 1700-13A

Page

3

of

Maximum Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions =

0.1437 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = 0.000360 moles CD/minute Maximum CD Emissions = 0.031918 lbs CD/minute Maximum CD Emissions = 1.915 lbs CD/hour

Toluene

Using the Ideal Gas Law,

V.P. of CD at Saturation = 280.10 mm Hg

> Total Vapor = 0.002508 moles/ft3

Mole Fraction CD = 0.0016907 %

> CD Vapor = 0.00000004 moles/ft3

CD Partial Pressure = 0.013 mm Hg

> 0.000046 Ratio =

V.P. of Toluene at Saturation = 36.61 mm Hg

Toluene Partial Pressure = 0.0017 mm Hg

> Toluene Vapor = 0.00000001 moles/ft3

0.00005 moles/min Toluene Vapor =

Toluene Vapor = 0.0043 lb/min

Toluene Vapor = 0.26 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Kettles No. 3, 5 & 5 Manway / Drop Strainers

TEMPO ID: EQT0136

Point Source ID No.: 1700-13A

Page

4

of:

1

ACR

Ratio = 0.000046

V.P. of ACR at Saturation = 53.19 mm Hg

ACR Partial Pressure = 0.0024 mm Hg

ACR Vapor = 0.00000001 moles/ft3
ACR Vapor = 0.00007 moles/min
ACR Vapor = 0.0084 lb/min
ACR Vapor = 0.51 lb/hr

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
}	1	Rate	Rate	
<u></u>	lb/yr	lb/hr	[b/hr	tpy
Total VOC	20070	2.291	2.681	10.035
Chloroprene	14338	1.637	1.915	7.169
Toluene	1950	0.223	0.260	0.975
Total HAPs	16288	1.859	2.176	8.144
Total TAPs	16288	1.859	2.176	8.144



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Solution Makeup Manhole Common Vent

TEMPO ID: GRP0006

Point Source ID No.: 1700-14B

Page

1

Basis:

Common vent for Acetic Acid Make-Up Tank (1700-14B.1/EQT0137), Acetic Acid Hold-Up Tank (1700-14B.2/EQT00138), and Stabilizer & Catalyst Tanks Manholes Vent (1700-14B.3/RLP0013).

Emissions:

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
	1 1	Rate	. Rate	
	lb/yr	lb/hr	lb/hr	tpy
PM-10	131	1.473	9.092	0.066
Total VOC	1119	0.128	0.602	0.559
Chloroprene	738	0.084	0.093	0.369
Toluene	242	0.028	0.494	0.121
Total HAPs	980	0.112	0.586	0.490
Total TAPs	980	0.112	0.586	0.490



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Solution Makeup Manhole Common Vent

TEMPO ID: GRP0006

Point Source ID No.: 1700-14B Page 2 of 4



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Manholes Vent

TEMPO ID: RLP0013

Point Source ID No.: 1700-14B.3

Page

Basis:

Based on 10 hr TWA area data developed between 1999 and 2001, the average concentration of CD in the building air is 0.56 ppmv.

Monitoring data for toluene between February 2001 and September 2002 indicate an average concentration of 0.176 ppm. Toluene is emitted during makeup of toluene based stabilizer when

There is no ACR present in toluene based stabilizer, and no realistic opportunity for ACR to be present in the ambient air around the Stabilizer tanks.

The maximum concentration is estimated to be 10% greater than the maximum measured concentration for CD and toluene.

PTZ, TETD, Lowinox, and Neozone A are added to the makeup tanks through the manholes resulting in particulate emissions.

Estimated that 0.1% of the TETD, Lowinox, PTZ and Neozone A transferred becomes airborne. Estimated that 50% of the airborne dust is captured by exhaust system. Remainder is captured in building.

Calculation basis provided by Mr. P. Offut, DuPont

Rated Capacity of Blower =

11100 cfm

Amount of Time Discharging =

8760 hours/vr

Amount of Time Discharging =

8760 hours/yr while on toluene stabilizer types

Average CD in Air Exhausted =

0.56 ppm CD by volume

Maximum CD in Air Exhausted =

0.62 ppm CD by volume

Avg. Toluene in Air Exhausted =

0.176 ppm toluene by volume 3.1464 ppm toluene by volume

Max. Toluene in Air Exhausted =

Avg. ACR in Air Exhausted =

0 ppm ACR by volume

Max. ACR in Air Exhausted =

0 ppm ACR by volume 88.54 lb/lb-mole

Molecular Weight of CD = Molecular Weight of Toluene =

92.4 lb/lb-mole

122.99 lb/lb-mole

Molecular Weight of ACR =

25 °C

Temperature = Pressure =

14.696 psia

PTZ Used =

2650 lb/vr

Fraction Airborne =

0.1 %



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Manholes Vent

TEMPO ID: RLP0013

Point Source ID No.: 1700-14B.3

Page

TETD Used = 191015 lb/vr Lowinox Used = 21660 lb/yr Neozone A Used = 47184 lb/yr

Fraction Airborne = 0.1 %

Average Solids Addition Time = 89 hours Minimum Solids Addition Time = 14.44 hours

Average VOC Emission Rates

Chloroprene

Using given information,

Average CD Emissions =

0.0062 cfm CD

Using the Ideal Gas Law,

0.000016 moles/minute Average CD Emissions = Average CD Emissions = 0.001404 lbs/minute Average CD Emissions = 0.084 lbs/hour

Average CD Emissions = 738 lbs/vr Average CD Emissions = 0.37 tons/yr

Toluene

Using given information,

Average Toluene Emissions = 0.0020 cfm toluene

Using the Ideal Gas Law,

Average Toluene Emissions = 0.000005 moles/minute Average Toluene Emissions = 0.000460 lbs/minute

Average Toluene Emissions = 0.028 lbs/hour Average Toluene Emissions = 242 lbs/vr Average Toluene Emissions = 0.12 tons/yr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Manholes Vent

TEMPO ID: RLP0013

Point Source ID No.: 1700-14B.3

Page

3

of

4

Maximum VOC Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions =

0.0068 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions =

0.000017 moles CD/minute

Maximum CD Emissions =

0.001544 lbs CD/minute

Maximum CD Emissions =

0.093 lbs CD/hour

Toluene

Using given information,

Maximum Toluene Emissions =

0.0349 cfm toluene

Using the Ideal Gas Law,

Maximum Toluene Emissions =

0.000089 moles/minute

Maximum Toluene Emissions =

0.008231 lbs/minute

Maximum Toluene Emissions =

0.494 lbs/hour



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Manholes Vent

TEMPO ID: RLP0013

Point Source ID No.: 1700-14B.3

Page

4

of

PM/PM-10 Emissions

Capture Efficiency =

50 %

PM/PM-10 Emissions = Process rate, lb/yr x Fraction Airborne x Capture Efficiency / 104 hr/yr

= $(2650 \text{ lb/yr} \times 0.1\% + 259859 \text{ lb/yr} \times 0.1\%) \times 50\% / 89 \text{ hr/yr}$

= 1.473 lb/hr

= 0.0656 tpy

Maximum PM/PM-10 Emission Rates

Capture Efficiency =

50 %

PM/PM-10 Emissions = Process rate, lb/yr x Fract. Airborne x Capture Efficiency / 16.88 hr/yr

= $(2650 \text{ lb/yr} \times 0.1\% + 259859 \text{ lb/yr} \times 0.1\%) \times 50\% / 14.44 \text{ hr/yr}$

9.092 lb/hr

Compound	Total	Average	Maximum	Annual
į	Loss	Emission	Emission	Emissions
		Rate	Rate	
L	lb/yr	ib/hr	lb/hr	tpy
PM-10	131	1.473	9.092	0.066
Total VOC	980	0.112	0.586	0.490
Chloroprene	738	0.084	0.093	0.369
Toluene	242	0.028	0.494	0.121
Total HAPs_	980	0.112	0.586	0.490
Total TAPs	980	0.112	0.586	0.490



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jets Emissions Cap

TEMPO ID: GRP0012

Point Source ID No.: 1700-20 CAP

Page

0

Basis:

Emissions cap for CD Refining Column Jet (1700-20/EQT0139) and CD Refining Column Jet (Spare) (1700-20A/EQT00140).

Emissions:

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
]	Rate	Rate	
	lb/yr_	lb/hr	lb/hr	tpy
NOx	6597	0.753	0.828	3.298
Total VOC	24801	2.831	3.114	12.401
Chloroprene	24794	2.830	3.113	12.397
Toluene	7	0.001	0.001	0.003
Ammonia	0.07	0.000008	0.000009	0.00004
Total HAPs	24801	2.831	3.114	12.401
Total TAPs	24801	2.831	3.114	12.401



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet

TEMPO ID: EQT0139

Point Source ID No.: 1700-20

Page

1

of

5

Basis:

Emissions are based on sampling data on March 12, 2002 and March 21, 2002 by METCO Environmental.

On March 12, 2002 type AD was being produced, which includes toluene.

On March 21, 2002 type WHV was being produced which does not inloude toluene.

The highest vent rate measured is 4.584 dscfm.

The highest NOx concentration measured is 22945.5 ppmv.

The highest chloroprene (CD) concentration measured is 44807 ppmv.

The highest toluene concentration measured is 12 ppmv.

Ammonia was measured at less than 0.68 ppmv. Conservatively assume a concentration of 0.68 ppmv.

The maximum concentrations are estimated to be 10% greater than the maximum measured concentration.

Calculation basis provided by Mr. P. Offut, DuPont

Vent Rate =

4.584 cfm

Amount of Time Venting =

8760 hours/yr

Average NOx in Air Vented =

orou nouisiyi

Maximum NOx in Air Vented =

22945.5 ppm NOx by volume

VIAXIIIIUIII NOX III AII Verited -

25240 ppm NOx by volume

Average CD in Air Vented =

44807 ppm CD by volume

Maximum CD in Air Vented =

49288 ppm CD by volume

Avg. Toluene in Air Vented =

12 ppm toluene by volume

Max. Toluene in Air Vented =

13.2 ppm toluene by volume

Avg. Ammonia in Air Vented =

0.68 ppm ammonia by volume

Max. Ammonia in Air Vented =

0.75 ppm ammonia by volume 46 lb/lb-mole

Molecular Weight of NOx = Molecular Weight of CD =

88.54 lb/lb-mole

Molecular Weight of Toluene =

92.4 lb/lb-mole

Wolcoular Weight of Folderic -

17 lb/lb-mole

Molecular Weight of Ammonia =

20 °C

Temperature = Pressure =

14.696 psia



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet

TEMPO ID: EQT0139

Point Source ID No.: 1700-20 Page 2 of

Average Emission Rates

Nitrogen Dioxide

Using given information,

Average NOx Emissions =

0.11 cfm NOx

Using the Ideal Gas Law,

Average NOx Emissions = 0.000273 moles/minute
Average NOx Emissions = 0.012551 lbs/minute
Average NOx Emissions = 0.753 lbs/hour
Average NOx Emissions = 6597 lbs/yr
Average NOx Emissions = 3.30 tons/yr

Chloroprene

Using given information,

Average CD Emissions = 0.2054 cfm CD

Using the Ideal Gas Law,

Average CD Emissions = 0.000533 moles/minute
Average CD Emissions = 0.047173 lbs/minute
Average CD Emissions = 2.830 lbs/hour
Average CD Emissions = 24794 lbs/yr
Average CD Emissions = 12.40 tons/yr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet

TEMPO ID: EQT0139

Point Source ID No.: 1700-20 Page 3 of 5

Toluene

Using given information,

Average Toluene Emissions = 0.0001 cfm toluene

Using the Ideal Gas Law,

Average Toluene Emissions = 0.0000001 moles/minute
Average Toluene Emissions = 0.000013 lbs/minute
Average Toluene Emissions = 0.0008 lbs/hour
Average Toluene Emissions = 7 lbs/yr
Average Toluene Emissions = 0.0003 tons/yr

Ammonia

Using given information,

Average Ammonia Emissions = 0.000003 cfm ammonia

Using the Ideal Gas Law,

Average Ammonia Emissions = 0.0000001 moles/minute
Average Ammonia Emissions = 0.0000001 lbs/minute
Average Ammonia Emissions = 0.000008 lbs/hour
Average Ammonia Emissions = 0.000004 tons/yr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet

TEMPO ID: EQT0139

Point Source ID No.: 1700-20 Page 4 of

Maximum Emission Rates

NOx

Using given information,

Maximum NOx Emissions =

0.1157 cfm CD

Using the Ideal Gas Law,

Maximum NOx Emissions =
Maximum NOx Emissions =
Maximum NOx Emissions =

0.000300 moles/minute 0.013806 lbs/minute 0.828 lbs/hour

Chloroprene

Using given information,

Maximum CD Emissions =

0.2259 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = Maximum CD Emissions = Maximum CD Emissions =

0.000586 moles CD/minute 0.051891 lbs CD/minute 3.113 lbs CD/hour

Toluene

Using given information,

Maximum Toluene Emissions =

0.0001 cfm toluene

Using the Ideal Gas Law,

Maximum Toluene Emissions = Maximum Toluene Emissions = Maximum Toluene Emissions =

0.0000002 moles/minute 0.00001 lbs/minute 0.0009 lbs/hour



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet

TEMPO ID: EQT0139

Point Source ID No.: 1700-20 Page 5 of

Ammonia

Using given information,

Maximum Ammonia Emissions = 0.000003 cfm ammonia

Using the Ideal Gas Law,

Maximum Ammonia Emissions = 0.0000001 moles/minute
Maximum Ammonia Emissions = 0.0000002 lbs/minute
Maximum Ammonia Emissions = 0.000009 lbs/hour

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
) ·	}	Rate	Rate .	
ļ	l lb/yr	lb/hr	lb/hr	tpy
NOx	6597	0.753	0.828	3.298
Total VOC	24801	2.831	3.114	12.401
Chloroprene	24794	2.830	3.113	12.397
Toluene	7	0.001	0.001	0.003
Ammonia	0.07	0.000008	0.000009	0.00004
Total HAPs	24801	2.831	3.114	12,401
Total TAPs	24801	2.831	3.114	12.401



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet (Spare)

TEMPO ID: EQT0140

Point Source ID No.: 1700-20A of Page

Basis:

Emissions are based on sampling data on March 12, 2002 and March 21, 2002 by METCO

On March 12, 2002 type AD was being produced, which includes toluene.

On March 21, 2002 type WHV was being produced which does not inlcude toluene.

The highest vent rate measured is 4.584 dscfm.

The highest NOx concentration measured is 22945.5 ppmv.

The highest chloroprene (CD) concentration measured is 44807 ppmv.

The highest toluene concentration measured is 12 ppmv.

Ammonia was measured at less than 0.68 ppmv. Conservatively assume a concentration of 0.68 ppmv.

The maximum concentrations are estimated to be 10% greater than the maximum measured concentration.

Calculation basis provided by Mr. P. Offut, DuPont

Vent Rate =

4.584 cfm

Amount of Time Venting =

8760 hours/yr

Average NOx in Air Vented =

22945.5 ppm NOx by volume

Maximum NOx in Air Vented =

25240 ppm NOx by volume

Average CD in Air Vented =

44807 ppm CD by volume

Maximum CD in Air Vented =

49288 ppm CD by volume

Avg. Toluene in Air Vented =

12 ppm toluene by volume

Max. Toluene in Air Vented =

13.2 ppm toluene by volume

Avg. Ammonia in Air Vented =

0.68 ppm ammonia by volume

Max. Ammonia in Air Vented =

0.75 ppm ammonia by volume

Molecular Weight of NOx =

46 lb/lb-mole 88.54 lb/lb-mole

Molecular Weight of CD =

92.4 lb/lb-mole

Molecular Weight of Toluene = Molecular Weight of Ammonia =

17 lb/lb-mole

20 °C

Temperature = Pressure =

14.696 psia



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet (Spare)

TEMPO ID: EQT0140

Point Source ID No.: 1700-20A Page 2 of

Average Emission Rates

NOx

Using given information,

Average NOx Emissions =

0.11 cfm NOx

Using the Ideal Gas Law,

Average NOx Emissions = 0.000273 moles/minute
Average NOx Emissions = 0.012551 lbs/minute
Average NOx Emissions = 0.753 lbs/hour
Average NOx Emissions = 6597 lbs/yr
Average NOx Emissions = 3.30 tons/yr

Chloroprene

Using given information,

Average CD Emissions = 0.2054 cfm CD

Using the Ideal Gas Law,

Average CD Emissions = 0.000533 moles/minute
Average CD Emissions = 0.047173 lbs/minute
Average CD Emissions = 24794 lbs/yr
Average CD Emissions = 12.40 tons/yr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet (Spare)

TEMPO ID: EQT0140

Point Source ID No.: 1700-20A

Page

3

Toluene

Using given information,

Average Toluene Emissions =

0.0001 cfm toluene

Using the Ideal Gas Law,

Average Toluene Emissions =

Average Toluene Emissions = Average Toluene Emissions =

Average Toluene Emissions =

Average Toluene Emissions =

0.0000001 moles/minute

0.000013 lbs/minute

0.0008 lbs/hour

7 lbs/yr

0.003 tons/yr

Ammonia

Using given information,

Average Ammonia Emissions =

0.000003 cfm ammonia

Using the Ideal Gas Law,

Average Ammonia Emissions =

Average Ammonia Emissions =

Average Ammonia Emissions =

Average Ammonia Emissions =

Average Ammonia Emissions =

0.00000001 moles/minute

0.0000001 lbs/minute

0.000008 lbs/hour

0.07 lbs/vr

0.00004 tons/yr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet (Spare)

TEMPO ID: EQT0140

Point Source ID No.: 1700-20A Page 4 of 5

Maximum Emission Rates

NOx

Using given information,

Maximum NOx Emissions =

0.1157 cfm CD

Using the Ideal Gas Law,

Maximum NOx Emissions = Maximum NOx Emissions =

. 0.000300 moles/minute 0.013806 lbs/minute 0.828 lbs/hour

Maximum NOx Emissions =

Chloroprene

Using given information,

Maximum CD Emissions =

0.2259 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = Maximum CD Emissions =

Maximum CD Emissions =

0.000586 moles CD/minute 0.051891 lbs CD/minute 3.113 lbs CD/hour

Toluene

Using given information,

Maximum Toluene Emissions =

0.0001 cfm toluene

Using the Ideal Gas Law,

Maximum Toluene Emissions =

0.000002 moles/minute 0.00001 lbs/minute 0.0009 lbs/hour

Maximum Toluene Emissions = Maximum Toluene Emissions =



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: CD Refining Column Jet (Spare)

TEMPO ID: EQT0140

Point Source ID No.: 1700-20A

Page

·5

of

5

Ammonia

Using given information,

Maximum Ammonia Emissions =

0.000003 cfm ammonia

Using the Ideal Gas Law,

Maximum Ammonia Emissions =

0.00000001 moles/minute

Maximum Ammonia Emissions =

0.0000002 lbs/minute

Maximum Ammonia Emissions =

0.000009 lbs/hour

Compound	Total	Average	Maximum	Annual
·	Loss	Emission	Emission	Emissions
	1	Rate	Rate	,
	lb/yr	lib/hr	lb/hr	tpy
NOx	6597	0.753	0.828	3.298
Total VOC	24801	2.831	3.114	12.401
Chloroprene	24794	2.830	3.113	12.397
Toluene	: 7	0.001	0.001	0.003
Ammonia	0.07	0.000008	0.000009	.0.00004
Total HAPs	24801	2.831	3.114	12.401
Total TAPs	24801	2.831	3,114	12.401



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Product Drying Cap

TEMPO ID: GRP0007

Point Source ID No.: 1700-25A Page 1 of 3

Basis:

For Washbelt and Dryer emissions, use analytical data for CD in stripped emulsion collected for 1996 Title V calculations and lbs of unstripped emulsion to the finishing lines and WD production for chloroprene (CD) and ACR emissions and AD production for toluene emissions.

Cap covers 1700-25, East Wash Belt Dryer, 1700-26, West Wash Belt Dryer, 1700-27, East Dryer Hot Exhaust, 1700-28, West Dryer Hot Exhaust, 1700-45, No. 1 East Dryer Cooling Compartment, 1700-46, No. 1 West Dryer Cooling Compartment, 1700-47, No. 2 East Dryer Cooling Compartment, and 1700-48, No. 2 West Dryer Cooling Compartment.

Calculation basis provided by Mr. P. Offut, DuPont

% VOC Emissions from Washbelt = 16.35 %
% VOC Emissions from Dryer = 83.65 %
Total VOC in Stripped Emulsion = 136416 lbs/yr

CD in Stripped Emulsion = 136416 lbs/yr in worst emitting product

ACR in Stripped Emulsion = 22736 lbs/yr in worst emitting product

Max. Toluene in Stripped Emulsion = 46130 lbs/yr

Operating Hours = 8760 hours/yr

Wash Belt Calculations

Emission Rates

Emissions = Total in Stripped Emulsion / Operating Hours

Calculate total emissions from the washbelts and dryers

CD Emissions = 12.98 lbs/hr ACR Emissions = 2.60 lbs/hr Toluene Emissions = 5.27 lbs/hr

Calculate total emissions from the washbelts

CD Emissions = 2.12 lbs/hr CD Emissions = 18586 lb/yr CD Emissions = 9.29 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Product Drying Cap

TEMPO ID: GRP0007

Point Source ID No.: 1700-25A

Page

2

3

ACR Emissions = 0.42 lbs/hr ACR Emissions = 3717 lb/yr ACR Emissions = 1.86 tpy

Toluene Emissions = 0.86 lbs/hr Toluene Emissions = 7542 ib/yr Toluene Emissions = 3.77 tpy

Dryer Calculations

Emission Rates

Emissions = Total in Stripped Emulsion / Operating Hours

Calculate total emissions from the washbelts and dryers

CD Emissions = 12.98 lbs/hr
ACR Emissions = 2.60 lbs/hr
Toluene Emissions = 5.27 lbs/hr

Calculate total emissions from the dryer vents

CD Emissions = 10.86 lbs/hr CD Emissions = 95093 lb/yr CD Emissions = 47.55 tpy

ACR Emissions = 2.17 lbs/hr ACR Emissions = 19019 lb/yr ACR Emissions = 9.51 tpy

Toluene Emissions = 4.41 lbs/hr
Toluene Emissions = 38588 lb/yr
Toluene Emissions = 19.29 tpy

1,2-Dichlorobenzene Emissions = 0.01 lbs/hr 1,2-Dichlorobenzene Emissions = 60 lb/yr 1,2-Dichlorobenzene Emissions = 0.03 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Product Drying Cap

TEMPO ID: GRP0007

Point Source ID No.: 1700-25A Page 3 of 3

Cooling Compartment Calculations

Effectively all VOC is expected to be removed in the wash belts and dryers. Therefore, VOC emissions from the cooling compartments are expected to be <0.01 tpy.

Summary

Toluene is potentially emitted at a level of 23.36 tpy, although it is not present in the worst case product.

Therefore, toluene totals are not part of the annual VOC emission totals and are calculated only for reference.

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
}	ł	Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	136416	15.573	15.573	68.208
Chloroprene	113680	12.977	12.977	56.840
1,2-Dichlorobenze	60	0.007	0.007	0.030
Toluene	46130	5.266	5.266	23.065
Total HAPs	159870	18.250	18.250	79.935
Total TAPs	159870	18.250	18.250	79.935



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: East Wash Belt Dryer

TEMPO ID: EQT0142

Point Source ID No.: 1700-25

Page

1

of

2

Basis:

For Washbelt and Dryer emissions, use analytical data for CD in stripped emulsion collected for 1996 Title V calculations and lbs of unstripped emulsion to the finishing lines and WD production for chloroprene (CD) and ACR emissions and AD production for toluene emissions. Total emissions for the wash belts are covered under 1700-25A, Product Drying Cap.

Assumes full throughput for each drying line.

Calculation basis provided by Mr. P. Offut, DuPont

% VOC Emissions from Washbelt =

16.35 %

% VOC Emissions from Dryer =

83.65 %

Total VOC in Stripped Emulsion =

136416 lbs/yr

CD in Stripped Emulsion =

113680 lbs/yr in worst emitting product

ACR in Stripped Emulsion =

22736 lbs/yr in worst emitting product

Max. Toluene in Stripped Emulsion =

46130 lbs/yr

Operating Hours =

8760 hours/yr

Average Emission Rates

Average Emissions = Total in Stripped Emulsion / Operating Hours

Calculate total emissions from the washbelts and dryers

Average CD Emissions =

12.98 lbs/hr

Average ACR Emissions =

2.60 lbs/hr

Average Toluene Emissions =

5.27 lbs/hr

Calculate total emissions from the washbelts

Average CD Emissions =

2.12 lbs/hr

Average CD Emissions =

18586 lb/yr

Average CD Emissions =

9.29 tpy

Average ACR Emissions =

0.42 lbs/hr

Average ACR Emissions =

3717 lb/yr

Average ACR Emissions =

1.86 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: East Wash Belt Dryer

TEMPO ID: EQT0142

Point Source ID No.: 1700-25

Page

2

of

2

Average Toluene Emissions = 0.86 lbs/hr Average Toluene Emissions = 7542 lb/yr

Average Toluene Emissions = 3.77 tpy

Maximum Emission Rates

Maximum emission rates are equal to average rates.

Summary

Toluene is potentially emitted at a level of 3.82 tpy, although it is not present in the worst case product.

Therefore, toluene totals are not part of the annual VOC emission totals and are calculated only for reference.

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
	l	Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	22304	2.546	2.546	11.152
Chloroprene	18586	2.122	2.122	9.293
Toluene	7542	0.861	0.861	3.771
Total HAPs	26129	2.983	2.983	13.064
Total TAPs	26129	2.983	2.983	13.064



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: West Wash Belt Dryer

TEMPO ID: EQT0143

Point Source ID No.: 1700-26

Page

2

Basis:

For Washbelt and Dryer emissions, use analytical data for CD in stripped emulsion collected for 1996 Title V calculations and lbs of unstripped emulsion to the finishing lines and WD production for chloroprene (CD) and ACR emissions and AD production for toluene emissions.

Total emissions for the wash belts are covered under 1700-25A. Product Daing Cap.

Total emissions for the wash belts are covered under 1700-25A, Product Drying Cap.

Assumes full throughput for each drying line.

Calculation basis provided by Mr. P. Offut, DuPont

% VOC Emissions from Washbelt = 16.35 %

% VOC Emissions from Dryer = 83.65 %

Total VOC in Stripped Emulsion = 136416 lbs/yr

CD in Stripped Emulsion = 113680 lbs/yr in worst emitting product
ACR in Stripped Emulsion = 22736 lbs/yr in worst emitting product

Max. Toluene in Stripped Emulsion = 46130 lbs/yr

Operating Hours = 8760 hours/yr

Average Emission Rates

Average Emissions = Total in Stripped Emulsion / Operating Hours

Calculate total emissions from the washbelts and dryers

Average CD Emissions = 12.98 lbs/hr Average ACR Emissions = 2.60 lbs/hr Average Toluene Emissions = 5.27 lbs/hr

Calculate total emissions from the washbelts

Average CD Emissions = 2.12 lbs/hr Average CD Emissions = 18586 lb/yr Average CD Emissions = 9.29 tpy

Average ACR Emissions = 0.42 lbs/hr Average ACR Emissions = 3717 lb/yr Average ACR Emissions = 1.86 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: West Wash Belt Dryer

TEMPO ID: EQT0143

Point Source ID No.: 1700-26

Page

2

of

2

Average Toluene Emissions =

0.86 lbs/hr

Average Toluene Emissions =

.7542 lb/yr

Average Toluene Emissions =

3.77 tpy

Maximum Emission Rates

Maximum emission rates are equal to average rates.

Summary

Toluene is potentially emitted at a level of 3.82 tpy, although it is not present in the worst case product.

Therefore, toluene totals are not part of the annual VOC emission totals and are calculated only for reference.

Compound	Total	Average	Maximum	Annual
Į	Loss	Emission	Emission	Emissions
}]]	Rate	Rate	
<u> </u>	lb/yr	_ lb/hr	lb/hr	tpy
Total VOC	22304	2.546	2.546	11.152
Chloroprene	18586	2.122	2.122	9.293
Toluene	7542	0.861	0.861	3.771
Total HAPs	26129	2.983	2.983	13.064
Total TAPs	26129	2.983	2.983	13.064



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: East Hot Dryer Exhaust

TEMPO ID: EQT0144

Point Source ID No.: 1700-27 Page 1 of 2

Basis:

For Washbelt and Dryer emissions, use analytical data for CD in stripped emulsion collected for 1996 Title V calculations and lbs of unstripped emulsion to the finishing lines and WD production for chloroprene (CD) and ACR emissions and AD production for toluene emissions.

Total emissions for the dryer exhausts are covered under 1700-27A, Dryer Exhaust Cap.

Assumes full throughput for each drying line.

Calculation basis provided by Mr. P. Offut, DuPont

Based on mass balances, approximately 60 lb/yr of 1,2-dichlorobenzene is emitted from the driers.

% VOC Emissions from Washbelt = 16.35 %

% VOC Emissions from Dryer = 83.65 %
Total VOC in Stripped Emulsion = 136416 lbs/yr

CD in Stripped Emulsion = 113680 lbs/yr in worst emitting product

ACR in Stripped Emulsion = 22736 lbs/yr in worst emitting product

Max. Toluene in Stripped Emulsion = 46130 lbs/yr

Operating Hours = 8760 hours/yr

Average Emission Rates

Average Emissions = Total in Stripped Emulsion / Operating Hours

Calculate total emissions from the washbelts and dryers

Average CD Emissions = 12.98 lbs/hr Average ACR Emissions = 2.60 lbs/hr Average Toluene Emissions = 5.27 lbs/hr

Calculate total emissions from the dryer vents

Average CD Emissions = 10.86 lbs/hr Average CD Emissions = 95093 lb/yr Average CD Emissions = 47.55 tpy

Average ACR Emissions = 2.17 lbs/hr Average ACR Emissions = 19019 lb/yr Average ACR Emissions = 9.51 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: East Hot Dryer Exhaust

TEMPO ID: EQT0144

Point Source ID No.: 1700-27

Page

2

Average Toluene Emissions =

4.41 lbs/hr

Average Toluene Emissions =

38588 lb/yr

Average Toluene Emissions =

19.29 tpy

Maximum Emission Rates

Maximum emission rates are equal to average rates.

Summary

Toluene is potentially emitted at a level of 19.54 tpy, although it is not present in the worst case product.

Therefore, toluene totals are not part of the annual VOC emission totals and are calculated only for reference.

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
		Rate	Rate	8 8
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	114172	13.033	13.033	57.086
Chloroprene	95093	10.855	10.855	47.547
1,2-Dichlorobenze	60	0.007	0.007	0.030
Toluene	38588	4.405	4.405	19.294
Total HAPs	133741	15.267	15.267	66.871
Total TAPs	133741	15.267	15.267	66.871



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: West Hot Dryer Exhaust

TEMPO ID: EQT0145

Point Source ID No.: 1700-28 Page 1 of 2

Basis:

For Washbelt and Dryer emissions, use analytical data for CD in stripped emulsion collected for 1996 Title V calculations and lbs of unstripped emulsion to the finishing lines and WD production for chloroprene (CD) and ACR emissions and AD production for toluene emissions.

Total emissions for the dryer exhausts are covered under 1700-27A, Dryer Exhaust Cap.

Assumes full throughput for each drying line.

Calculation basis provided by Mr. P. Offut, DuPont

Based on mass balances, approximately 60 lb/yr of 1,2-dichlorobenzene is emitted from the driers.

% VOC Emissions from Washbelt = 16.35 % VOC Emissions from Dryer = 83.65 %

Total VOC in Stripped Emulsion = 136416 lbs/yr

CD in Stripped Emulsion = 113680 lbs/yr in worst emitting product
ACR in Stripped Emulsion = 22736 lbs/yr in worst emitting product

Max. Toluene in Stripped Emulsion = 46130 lbs/yr

Operating Hours = 8760 hours/yr

Average Emission Rates

Average Emissions = Total in Stripped Emulsion / Operating Hours

Calculate total emissions from the washbelts and dryers

Average CD Emissions = 12.98 lbs/hr Average ACR Emissions = 2.60 lbs/hr Average Toluene Emissions = 5.27 lbs/hr

Calculate total emissions from the dryer vents

Average CD Emissions = 10.86 lbs/hr Average CD Emissions = 95093 lb/yr Average CD Emissions = 47.55 tpy

Average ACR Emissions = 2.17 lbs/hr Average ACR Emissions = 19019 lb/yr Average ACR Emissions = 9.51 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: West Hot Dryer Exhaust

TEMPO ID: EQT0145

Average Toluene Emissions =

4.41 lbs/hr

Average Toluene Emissions =

38588 lb/yr

Average Toluene Emissions =

19.29 tpy

Maximum Emission Rates

Maximum emission rates are equal to average rates.

Summary

Toluene is potentially emitted at a level of 20.21 tpy, although it is not present in the worst case product

Therefore, toluene totals are not part of the annual VOC emission totals and are calculated only for reference.

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
	ı	Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	114172	13.033	_ 13.033	57.086
Chioroprene	95093	10.855	10.855	47.547
1,2-Dichlorobenze	60	0.007	0.007	0.030
Toluene	38588	4.405	4.405	19.294
Total HAPs	133741	15.267	15.267	66.871
Total TAPs	133741	15,267	15.267	66.871



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 1 East Dryer Cooling Compartment

TEMPO ID: EQT0146

Point Source ID No.: 1700-45

Page

0

1

Basis:

Effectively all VOC is expected to be removed in the wash belts and dryers. Therefore, VOC emissions from the cooling compartments are expected to be <0.01 tpy.

Compound	Average	Maximum	Annual				
	Emission Rate lb/hr	Emission Rate lb/hr	Emissions tpy				
				Total VOC	<0.01	<0.01	<0.01
				Chloroprene	<0.01	<0.01	<0.01
Toluene	<0.01	<0.01	<0.01				
Total HAPs	<0.01	<0.01	<0.01				
Total TAPs	<0.01	<0.01	<0.01				



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 1 West Dryer Cooling Compartment

TEMPO ID: EQT0147

Point Source ID No.: 1700-46

Page

1

of

Basis:

Effectively all VOC is expected to be removed in the wash belts and dryers. Therefore, VOC emissions from the cooling compartments are expected to be <0.01 tpy.

Compound	Average	Maximum	Annual				
	Emission Rate lb/hr	Emission Rate ' lb/hr	Emissions tpy				
				Total VOC	<0.01	<0.01	<0.01
				Chloroprene	<0.01	<0.01	<0.01
Toluene	<0.01	<0.01	<0.01				
Total HAPs	<0.01	<0.01	<0.01				
Total TAPs	<0.01	< 0.01	<0.01				



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 2 East Dryer Cooling Compartment

TEMPO ID: EQT0148

Point Source ID No.: 1700-47

Page

1

Basis:

Effectively all VOC is expected to be removed in the wash belts and dryers. Therefore, VOC emissions from the cooling compartments are expected to be <0.01 tpy.

Compound	Average	Maximum	Annual				
	Emission Rate lb/hr	Emission Rate lb/hr	Emissions tpy				
				Total VOC	<0.01	<0.01	<0.01
				Chioroprene	<0.01	<0.01	<0.01
Toluene	<0.01	<0.01	<0.01				
Total HAPs	<0.01	<0.01	<0.01				
Total TAPs	<0.01	<0.01	<0.01				



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 2 West Dryer Cooling Compartment

TEMPO ID: EQT0149

Point Source ID No.: 1700-48

Page

Basis:

Effectively all VOC is expected to be removed in the wash belts and dryers. Therefore, VOC emissions from the cooling compartments are expected to be <0.01 tpy.

Compound	Average	Maximum	Annual
	Emission	Emission	Emissions
	Rate	Rate	
	lb/hr	lb/hr	tpy
Total VOC	<0.01	<0.01	<0.01
Chloroprene	<0.01	<0.01	<0.01
Toluene	<0.01	<0.01	<0.01
Total HAPs	<0.01	<0.01	<0.01
Total TAPs	<0.01	<0.01	<0.01



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Vent

TEMPO ID: GRP0009

Point Source ID No.: 1700-50 Page 1 of 3

Basis:

No. 1 Stabilizer Makeup tank is 1070 gallon capacity and used to makeup aqueous dispersion stabilizer which has no VOC emissions.

No. 2 Stabilizer Makeup tank is 1070 gallon capacity and used to makeup any type of stabilizer.

No. 3 and 4 Stabilizer Tanks are 2330 gallon capacity and used to makeup toluene base stabilizer for AD and G types.

No. 3 and 4 Stabilizer Tanks are also used to makeup Emergency Stabilizer for the PK's (about once per quarter).

No. 5 Stabilizer Makeup tank is 1070 gallon capacity and used to makeup dispersion stabilizer which has no VOC emissions but will result in particulate emissions from the manhole vent..

Toluene is used for stabilizers for A-types, G-types, and emergency stabilizer.

Each of the 5 tanks is equipped with a nitrogen blanket regulator set at 1 psig.

All 5 tanks are piped to two common vent systems.

One vent system is equipped with a flame arrestor and vents to atmosphere during preparation of the stabilizers.

The second vent system is equipped with a backpressure regulator set at 2 psig and operates after stabilizer preparation.

The five PK stabilizer tanks are vented back to the second vent system to minimize emissions. Since during operation, the PK stabilizer tanks vent back to the stabilizer makeup tanks there are no emissions when transferring from the makeup tanks to the PK stabilizer tanks.

Solid additives are added to the toluene based and aqueous dispersion stabilizers, resulting in particulate matter emissions.

58.40 hr/yr

When the manhole is open for solids addition, toluene vapors and particulates are captured by the manhole exhaust system (EID No.1700-14B).

Calculation basis provided by Mr. P. Offut, DuPont Performance Polymers.

Maximum Makeup Toluene = 502 lb/batch Temperature = 35 C Toluene Vapor Pressure = 46.77 mm Hq Toluene Liquid Density = 53.21 lbs/ft3 H2O Vapor Pressure = 42.00 mm Hg Toluene Flow Rate = 832 lbs/min Toluene Flow Rate = 15.64 ft3/min Vapor Displacement = 15.64 ft3/min Maximum Toluene Required = 2915575 lb Maximum Toluene Required = 54792 ft3/yr Venting Time = 3504 min/yr

Venting Time =



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Vent

TEMPO ID: GRP0009

Point Source ID No.: 1700-50 Page 2 of

VOC Emissions

Displacement Losses

Assuming worst case - vapor is saturated with toluene and H2O - and using the ideal gas law

Total Vapor = 0.002468 moles/ft3

Toluene Vapor = 0.000152 moles/ft3

Toluene Vapor = 0.014033 lbs toluene/ft3 total vapor

TolueneVapor = 0.219419 lbs toluene/min

H2O Vapor = 0.000136 moles/ft3

H2O Vapor = 0.002455 lbs H2O/ft3 total vapor

H2O Vapor = 0.038382 lbs H2O/min N2 Vapor = 0.002180 moles/ft3

N2 Vapor = 0.061027 lbs N2/ft3 total vapor

Venting from Stabilizer Tanks

Toluene Vapor = 0.22 lb/min
Toluene Vapor = 769 lbs/yr
Toluene Vapor = 13.17 lb/hr
H2O Vapor = 135 lbs/yr
N2 Vapor = 3344 lbs/yr

Type Change Emissions

When a G or AD campaign is complete, the toluene based stabilizer tank is depressured, the heel is drained to drums, and the tank is cleaned.

For the worst case, assume each type change of G type requires tank cleaning, the tank is at 2 psig, and the nitrogen is is saturated with toluene and water, and the entire volume of the tank is discharged to atmosphere.

Assume depressuring occurs within 1 minute.



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Stabilizer Tanks Vent

TEMPO ID: GRP0009

Point Source ID No.: 1700-50

Page

3

of

3

G or AD -type changes/yr =

37

Venting Time =

1 min/type change

Volume of No. 3 or 4 Tank =

311 ft3

Total Volume Vented =

623 ft3 @ 2psig

Total Volume Vented = Toluene Vented =

708 ft3 @ 0 psig 367 lbs/yr

Toluene Vented =

9.93 lb/min

Toluene Vented =

595.89 lb/hr

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
]	Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	1136	19.253	595.885	0.568
Toluene	1136	19.253	595.885	0.568
Total HAPs_	1136	19.253	595.885	0.568
Total TAPs	1136	19.253	595.885	0.568



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Inhibitor Mix Tank

TEMPO ID: EQT0162

Point Source ID No.: 1700-51

Page

1

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Basis:

Inhibitor is made by dissolving PTZ and NDPA in Crude CD

The aim limits are 0.75% PTZ and 0.25% NDPA

Inhibitor is produced in the Inhibitor Makeup Tank (IMUT) located in Poly Building

The batches are pumped to the Final Makeup Tank (FMUT), which is covered under EID No.

1700-63, Vent Header System.

Calculation basis provided by Mr. P. Offut, DuPont

CD Supply Rate = 75 lbs/min

Amount of Inhibitor Produced = 4828384 lbs/yr

Temperature = 1.0 C

Specific Gravity of Inhibitor = 61.655 lbs/ft3

Vapor Pressure of CD = 84.06 mm Hg
Molecular Weight of CD = 88.54 lb/lb-mole

Max. Mole Fraction CD = 1.0 mole/mole

Emission Rates

IMUT Tank data

Total Volume of Tank = 88 ft3
Crude CD in tank at 85% level = 3384 lbs
Crude CD in tank at 85% level = 55 ft3
Vapor space in tank at 85% level = 33 ft3

Tank Charging Time = 63565 min/yr
Tank Charging Rate = 1.22 ft3/min

Number of Sub Batches = 1427 sub batches/yr

Amount of CD per Sub Batch = 3384 lbs CD/sub batch pumped Amount of CD per Sub Batch = 55 ft3 CD/sub batch pumped

Nitrogen supply pressure is controlled at 8 inwg and vent backpressure at 14 inwg.

N2 Supply to Vent = 0.2890 psig

Backpressure Vent Valve Setting = 0.5058 psig



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Inhibitor Mix Tank

TEMPO ID: EQT0162

Point Source ID No.: 1700-51

Page

2

2

For CD saturated nitrogen at 1 C and using the ideal gas law,

Total Vapor = 0.00286909 moles/ft3 0.00030676 moles/ft3 CD Vapor =

CD Vapor = 0.02716085 lbs CD/ft3 total vapor

Total Amount Vented = 55 ft3/sub batch pumped

Venting Rate = 1.22 ft3/min CD Venting Rate = 0.03 lb/min CD Venting Rate = 1.99 lb/hr

> CD vented = 1.49 lbs CD/sub batch

CD vented = 2127 lbs CD/yr CD vented = 1.06 tons CD/yr

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
]]	Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	2127	1.988	1.988	1.064
Chloroprene	2127	1.988	1.988	1.064
Total HAPs	2127	1.988	1.988	1.064
Total TAPs	2127	1.988	1.988	1.064



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Unstripped Storage Tanks Manual Vent

TEMPO ID: RLP0016

Point Source ID No.: 1700-56 Page 1 of 3

Basis:

Unstripped emulsion tanks 6, 7, 8, 10, 13, and 14 are normally vented to the pressure balancing common vent header / tank system.

To prevent backflow to other tanks resulting from venting down during product changes, the tanks are isolated from the common vent system and directed to a bypass vent to atmosphere.

Tanks 6, 7, 8, and 10 store dry type emulsions.

Tanks 13 and 14 store liquid type products.

Venting time is approximately 1 minute.

Vapor pressure of chloroprene (CD) is based on worst case product.

Calculation basis provided by Mr. P. Offut, DuPont

Number of Vent Downs = 25 vent downs/yr/tank for dry types Number of Vent Downs = 50 vent downs/yr/tank for LD types

EST 10 Total Volume = 2400 ft3 EST 7 or 8 Total Volume = 2025 ft3 EST 6, 13, or 14 Total Volume = 1545 ft3

Maximum Pressure = 5 psig

Molecular Weight of CD = 88.54 lb/lb-mole

Molecular Weight of Toluene = 92.14 lb/lb-mole Molecular Weight of ACR = 122.99 lb/lb-mole

> Temperature = 25 °C Atmospheric Pressure = 14.696 psia

Average Emission Rates

Calculate vented volume

No. 10 Vented Volume = 817 ft3/vent down from 5 psig to 0 psig
No. 7 or 8 Vented Volume = 689 ft3/vent down from 5 psig to 0 psig
No. 6, 13 or 14 Vented Volume= 526 ft3/vent down from 5 psig to 0 psig



RTP Environmental Associates, Inc. Kenner, Louisiana

of

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Unstripped Storage Tanks Manual Vent

TEMPO ID: RLP0016

Point Source ID No.: 1700-56 Page

Using worst case of nitrogen saturated with H2O, toluene, ACR and Slocum CD data

Vapor Pressure of Water = 23.6 mm Hg

> Total Vapor = 0.002550 moles/ft3

Vapor Pressure of CD = 189 mm Ha

> CD Vapor = 0.000473 moles/ft3

CD Vapor = 0.041902 lbs CD/ft3 total vapor

Vapor Pressure of Toluene = 28.40 mm Ha

> Toluene Vapor = 0.000071 moles/ft3

Toluene Vapor = 0.006553 lbs toluene/ft3 total vapor

Vapor Pressure of ACR = 42.28 mm Ha

> ACR Vapor = 0.000106 moles/ft3

ACR Vapor = 0.013020 lbs ACR/ft3 total vapor

H2O Vapor = 0.000079 moles/ft3

H2O Vapor = 0.001426 lbs H2O/ft3 total vapor

Nitrogen Vapor = 0.001998 moles/ft3

Nitrogen Vapor = 0.057943 lbs N2/ft3 total vapor

No. 10 EST Vapor Vented = 20414 ft3/yr

No. 10 EST CD Vented = 855 lb/yr

No. 10 EST Toluene Vented = 134 lb/yr

No. 10 EST ACR Vented = 266 lb/yr

No. 7 or 8 EST Vapor Vented = 17224 ft3/vr

No. 7 or 8 EST CD Vented = 722 lb/vr

No. 7 or 8 EST Toluene Vented = 113 lb/yr

No. 7 or 8 EST ACR Vented = 224 lb/vr

No 6 EST Vapor Vented = 13141 ft3/yr

No 6 EST CD Vented = 551 lb/yr

No 6 EST Toluene Vented = 86 lb/vr

No 6 EST ACR Vented = 171 lb/yr

No. 13 & 14 EST Vapor Vented = 52565 ft3 CD/yr

No. 13 & 14 EST CD Vented = 2203 lb/vr

344 lb/yr No. 13 & 14 EST Toluene Vented =

No. 13 & 14 EST ACR Vented = 684 lb/yr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Unstripped Storage Tanks Manual Vent

TEMPO ID: RLP0016

Point Source ID No.: 1700-56

Page

3

of

3

Total CD Emitted = 4330 lb/yr
Total Toluene Emitted = 677 lb/yr
Total ACR Emitted = 1346 lb/yr

Venting Time Per Event = 1 min
Average CD Emission Rate = 1484.69 lb/hr
Average Toluene Emission Rate = 232.18 lb/hr
Average ACR Emission Rate = 461.32 lb/hr

Maximum Emission Rates

Maximum emission rates are equal to the average rates.

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
		Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	6353	2178.189	2178.189	3.177
Chloroprene	4330	1484.685	1484.685	2.165
Toluene	677	232.181	232.181	0.339
Total HAPs	5008	1716.866	1716.866	2.504
Total TAPs	5008	1716.866	1716.866	2.504



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: 1712 Building Common Vent Header System

TEMPO ID: GRP0010

Point Source ID No.: 1700-63 Page 1 of 4

Basis:

The Refined CD Storage Tank, No. 3 Crude CD Storage Tank, CD Inhibitor FMUT, CD Inhibitor HUT, No 1 and No. 2 RCD tanks, CD Refining Column Heels tank, and No. 1 and No. 2 Monomer Solution Tanks all vent into a common vent header, which minimizes emissions as one tank or another fills, venting into the other tanks.

Actual operating data of the common vent system for the past two years show that under normal operating conditions, the system vents very little to none.

Emissions are calculated by estimating and summing up the time for abnormal operations where tank levels will vary significantly and Poly can keep running.

It is conservatively estimated that operating conditions will result in emissions for 10% of the year in addition to maintenance requirements.

Calculation basis provided by Mr. P. Offut, DuPont

Based on mass balances, approximately 2 lb/yr of 1,2-dichlorobenzene is emitted from the Column Heels Tank.

Crude CD Specific Gravity = 60.924 lbs/ft3 Refined CD Pumped = 139871804 lb/yr considering worst case product Recovered CD Pumped = 50529656 lb/yr considering worst case product Vapor Temperature = 5 C 501 R Vapor Temperature = Header Inlet Pressure = 4.5 psig Header Inlet Pressure = 19.196 psia Header Outlet Pressure = 0 psig Header Outlet Pressure = 14.696 psia Gas Cv for Valve (100% open) = 816 Cg/Cv Gas/Liquid Cv for Valve = 36.1 Vapor Pressure of CD = 100.671 mm Hg Molecular Weight of CD = 88.54 lb/lb-mole Max. Mole Fraction CD = 1 mole/mole Vapor Pressure of Toluene = 9.189 mm Ha Molecular Weight of Toluene = 92.14 lb/lb-mole Max. Mole Fraction Toluene = 0.036 mole/mole Vapor Pressure of ACR = 15.538 mm Hg 122.99 lb/lb-mole Molecular Weight of ACR = Max. Mole Fraction ACR = 0.009 mole/mole 6679 hr considering worst case product Operating Time = Unschd Column Maint Down Days = 5 /vr 9 \r Column Water Washes = Other Venting = 668 hrs/yr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: 1712 Building Common Vent Header System

TEMPO ID: GRP0010

Point Source ID No.: 1700-63

Page

2

of

4

Emission Rates

Estimate transfer rates

Total Crude CD Pumped =

95296213 lbs/yr

Hours Flow =

6679 hr

Based on the common vent header design, maximum flow occurs with the backpressure valve fully open and a differential pressure of 4.5 psig and temperature of 5 C Conservatively, assuming nitrogen saturated with CD at 1 C liquid temperature and using the ideal gas law,

Total vapor = 0.001284 moles/ft3 CD vapor = 0.000130 moles/ft3

CD vapor = 0.011525 lbs CD/ft3 total vapor @ 5 psig CD vapor = 0.008823 lbs CD/ft3 total vapor @ 0 psig

Toluene vapor = 0.000000 moles/ft3

Toluene vapor = 0.000022 lbs toluene/ft3 total vapor @ 5 psig
Toluene vapor = 0.000017 lbs toluene/ft3 total vapor @ 0 psig

ACR vapor = 0.000000 moles/ft3

ACR vapor = 0.000021 lbs ACR/ft3 total vapor @ 5 psig ACR vapor = 0.000016 lbs ACR/ft3 total vapor @ 0 psig

Q = $((520 / (1.18 \times \text{Temp}))^{0.5}) \times (\text{Gas Cv x Inlet Pressure}) \times \text{SIN}((\pi/180) \times (3417/\text{Gas/Liquid Cv}) \times (((\text{Inlet Pressure-Outlet Pressure})/\text{Inlet Pressure})^{0.5}))/60$

Gas Flow = 176

176 scfm with 100% valve open



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: 1712 Building Common Vent Header System

TEMPO ID: GRP0010

Point Source ID No.: 1700-63 Page 3 of 4

Equal percentage valve flow characteristics

% open % fu	ll flow	scfm	lbs/hr CD	lbs/hr tol	lbs/hr ACR	lbs/hr VOC
100	100	186	98.46	0.19	0.18	98.83
90	86	160	84.59	0.16	0.15	84.91
80	65	121	63.95	0.12	0.12	64.19
70	43	81	42.80	0.08	0.08	42.96
60	29	54	28.59	0.06	0.05	28.70
50	19	36	19.12	0.04	0.03	19.19
40	13	25	13.20	0.03	0.02	13.25
30	9	17	8.80	0.02	0.02	8.83
20	6	11	5.92	0.01	0.01	5.94
10	4	8	4.06	0.01	0.01	4.08

5 Unschd Column Maint Down Days per Year = 120 hrs/yr 9 Column Water Washes per Year = 216 hrs/yr Other Venting = 668 hrs/yr Total = 1004 hrs/yr

For column down time, assume that Poly continues to run at average rates from the refined CD tank and that refill of the refined tank results in the venting. To be conservative, do not back out amount that would be compressed.

Also assume that during these outages the strippers continue to run at average rate and RCD results in venting. To be conservative, do not back out amount that would be compressed.

Amount Refined CD to Refill = 21024018 lbs/yr

Amount RCD Displacing Vapor = 7595072 lbs/yr

Total Displacement = 28619090 lbs/yr

Total Displacement = 469751 ft3/yr vapor

Total Displacement = 7.80 ft3/min vapor

Total CD = 5414 lbs/yr CD

Total CD = 5.39 lbs/hr CD

Total Toluene = 10 lbs/yr toluene

Total ACR = 10 lbs/yr ACR

Total ACR = 0.01 lbs/hr ACR



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: 1712 Building Common Vent Header System

TEMPO ID: GRP0010

Point Source ID No.: 1700-63

Page

•

Compound	Total	Average Maximum		Annual
	Loss	Emission	Emission	Emissions
		Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	5434	5.413	98.834	2.717
Chloroprene	5414	5.393	98.465	2.707
1,2-Dichlorobenze	2	0.003	0.055	0.001
Toluene	10	0.010	0.190	0.005
Total HAPs	5426	5.406	98.709	2.713
Total TAPs	5426	5.406	98.709	2.713



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Water Solution Exhaust Fan

TEMPO ID: EQT0183

Point Source ID No.: 1700-64 Page

Basis:

Based on 10 hr TWA area data developed between 1999 and 2001, the average concentration of CD in the building air is 0.56 ppmv.

Monitoring data for toluene between February 2001 and September 2002 indicate an average concentration of 0.176 ppm.

3500 lb/yr of dextrose, 203 M lb/yr of sodium sulfite, 4665 lb sodium chloride are added manually from cartons and bags to water solution makeup tank.

Estimated that 0.1% of the material transferred becomes airborne.

Estimated that 50% of the airborne dust is captured by exhaust system. Remainder is captured in building.

Calculation basis provided by Mr. P. Offut, DuPont

Rated Capacity of Blower = 2500 cfm Amount of Time Discharging =

8760 hours/yr

Average CD in Air Exhausted = 0.56 ppm CD by volume Maximum CD in Air Exhausted = 0.67 ppm CD by volume Avg. Toluene in Air Exhausted = 0.176 ppm toluene by volume

3.1464 ppm toluene by volume Max. Toluene in Air Exhausted =

88.54 lb/lb-mole Molecular Weight of CD = Molecular Weight of Toluene = 92.4 lb/lb-mole

> 25 °C Temperature = 14.696 psia Pressure =

3500 lb/yr Dextrose used = 203,000 lb/yr Sodium Sulfite used = Sodium Chloride used = ... 4665 lb/yr Total Addition Time = 66 hours

Average Emission Rates

Chloroprene

Using given information,

0.0014 cfm CD Average CD Emissions =



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Water Solution Exhaust Fan

TEMPO ID: EQT0183

Point Source ID No.: 1700-64

Page

2

Using the Ideal Gas Law,

Average CD Emissions = 0.000004 moles/minute

Average CD Emissions = 0.000316 lbs/minute

Average CD Emissions = 0.019 lbs/hour

Average CD Emissions = 166 lbs/yr

Average CD Emissions = 0.08 tons/yr

Toluene

Using given information,

Average Toluene Emissions = 0.0004 cfm toluene

Using the Ideal Gas Law,

Average Toluene Emissions = 0.000001 moles/minute
Average Toluene Emissions = 0.000104 lbs/minute
Average Toluene Emissions = 0.006 lbs/hour
Average Toluene Emissions = 55 lbs/yr
Average Toluene Emissions = 0.003 tons/yr

Maximum Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions = 0.0017 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = 0.000004 moles CD/minute

Maximum CD Emissions = 0.00379 lbs CD/minute

Maximum CD Emissions = 0.023 lbs CD/hour



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Water Solution Exhaust Fan

TEMPO ID: EQT0183

Point Source ID No.: 1700-64

Page

Toluene

Using given information,

Maximum Toluene Emissions =

0.0079 cfm toluene

Using the Ideal Gas Law,

Maximum Toluene Emissions = 0.000020 moles/minute

0.001854 lbs/minute

Maximum Toluene Emissions = Maximum Toluene Emissions =

0.111 lbs/hour

PM/PM-10 Emissions

Fraction Airborne =

0.1 %

Capture Efficiency =

50 %

PM/PM-10 Emissions = Process rate, lb/yr x Fraction Airborne x Capture Effiency / 8760 hr/yr

= 211165 lb/yr x 0.1% x 50% / 8760 hr/yr

0.0121 lb/hr

0.05 tpy

Maximum Emission Rates

Fraction Airborne =

0.1 %

Capture Efficiency =

50 %

PM/PM-10 Emissions = Process rate, lb/yr x Fraction Airborne x Capture Effiency /40 hr/yr

= 211165 lb/yr x 0.1% x 50% / 66 hr/yr

1.564 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Water Solution Exhaust Fan

TEMPO ID: EQT0183

Point Source ID No.: 1700-64

Page

4

of

4

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
		Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
PM/PM-10	106	0.0121	1.564	0.053
Total VOC	221	0.025	0.134	0.110
Chloroprene	166	0.019	0.023	0.083
Toluene	55	0.006	0.111	0.027
Total HAPs	221	0.025	0.134	0.110
Total TAPs	221	0.025	0.134	0.110



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 10 Emulsion Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65 Page 1 . of 3

Basis:

EST 10 is located outside of the main Poly building. The manway is not ventilated, so any emissions exit to atmosphere from the manway.

Emissions occur when the tank is opened for cleaning or maintenance.

EST 10 is a dry type unstripped emulsion storage tank, which is opened for inspection at every product type change, assume 4 non-compatile type changes / month. This tank requires cleaning once monthly, generally after G campaigns. Inspections last 15 minutes.

When manways opened for inspection, tanks are already vented down via point source

1700-56. Manway will be open for perhaps 15 minutes while tank wall condition is observed for fouling

Assume 1% of tank vapor content is emitted through convection to atmosphere during inspection, since there is no motive force to displace vapor from inside the tank

When vessel entry is required to these tanks for cleaning, an air mover is used to evacuate the vapor contents of the tank, replacing it with an air atmosphere. This can take up to 6 hours.

Calculation basis provided by Mr. D. McCrea DuPont

Formerly under EID No. 1700-1 (EQT0134).

Volume EST 10 = 2400 cub ft ·
Ambient temperature = 25 deg C

Pressure = 14.696 psia

For worst case scenarios, assuming equilibrium in tank before emptying. ACR and toluene not present in > 80% time, but counted as if they were.

Using the Ideal Gas Law, Loss during inspections of EST 10

Vapor content of EST 10 = 6.121 lb moles

EST 10 vapor density = 0.0026 lb moles / cub ft

Inspection of EST 10 = 36 per year Loss to atmosphere = 0.061 lb moles

CD in vapor lost = 0.01522 lb moles per inspection
CD in vapor lost = 1.3478 lb per inspection

CD lost during inspections = 48.521 lb / year

Toluene in vapor lost = 0.00229 lb moles per inspection Toluene in vapor lost = 0.2114 lb per inspection

Toluene lost during inspections = 7.609 lb / year



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 10 Emulsion Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65 Page 2 of 3

ACR in vapor lost = 0.00341 lb moles per inspection ACR in vapor lost = 0.4188 lb per inspection

ACR lost during inspections = 20.320 lb / year

Loss during vessel entry to EST 10

CD in vapor lost = 1.522 lb moles per vessel entry
CD in vapor lost = 134.780 lb per vessel entry

CD lost during vessel entries = 1617 lb / year

Toluene in vapor lost = 0.22875 lb moles per vessel entry
Toluene in vapor lost = 21.137 lb per vessel entry

Toluene lost during inspections = 254 lb / year

ACR in vapor lost = 0.34051 lb moles per vessel entry
ACR in vapor lost = 41.8789 lb per vessel entry

ACR lost during inspections = 503 lb / year

Maximum Emission Rates

Maximum emission rate occurs at the start of tank evaculation using the air mover. Emissions will be at the concentration within the tanks.

Coppus blower capacity 750 cfm CD emission in first minute 42.119 lb/min

assuming no air leakage in occurs in that first minute.

Toluene emission in first minute 6.605 lb/min ACR emission in first minute 13.087 lb/min

Maximum CD Emissions = 42.119 lb/min
Maximum toluene Emissions = 6.605 lb/min
Maximum ACR Emissions = 13.087 lb/min



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 10 Emulsion Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65

Page

3

of

3

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
	1	Rate	Rate	
	lb/yr	. lb/hr	lb/hr	tpy
Total VOC	2450	30.247	4097.575	1.225
Chloroprene	1666	20.566	2527.117	0.833
Toluene	261	3.225	785.229	0.131
Total HAPs	1927	23.792	3312.346	0.964
Total TAPs	1927	23.792	3312.346	0.964



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 13 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65A

Page

.

3

Basis:

EST 13 is located outside of the main Poly building. The manway is not ventilated, so any emissions exit to atmosphere from the manway.

Emissions occur when the tanks are opened for cleaning or maintenance.

EST 13 and 14 are Liquid Dispersion unstripped emulsion storage tanks. These tanks are opened for inspection occasionally, assume once every two months. These tanks require occasional cleaning, assume once every 3 months.

When manways opened for inspection, tanks are already vented down via point source 1700-56. Manway will be open for perhaps 10 minutes while tank wall condition is observed for fouling Assume 1% of tank vapor content is emitted through convection to atmosphere during inspection, since thre is no motive force to displace vapor from inside the tank

When vessel entry is required to these tanks for cleaning, an air mover is used to evacuate the vapor contents of the tank, replacing it with an air atmosphere. This can take up to 6 hours.

Calculation basis provided by Mr. D. McCrea DuPont

Formerly under EID No. 1700-1 (EQT0134).

Volume EST 13 and 14 = 1545 cub ft
Ambient temperature = 25 deg C

Pressure = 14.696 psia

For worst case scenarios, assuming equilibrium in tank before emptying. ACR and toluene not present in > 80% time, but counted as if they were.

Loss during inspections of EST 13

Vapor content of EST 13 or 14 = 3.941 lb moles

EST 13 or 14 vapor density = 0.0026 lb moles / cub ft

Inspection of EST 13 & 14 = 8 per year
Loss to atmosphere = 0.039 lb moles
CD in vapor lost = 0.97995 lb moles

CD in vapor lost = 86.7644 lb

CD lost during inspections = 694.115 lb / year

Toluene in vapor lost = 0.00147 lb moles Toluene in vapor lost = 0.1361 lb

Toluene lost during inspections = 1.089 lb / year



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 13 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65A Page 2 of S

ACR in vapor lost = 0.00219 lb moles per inspection ACR in vapor lost = 0.2696 lb per inspection

ACR lost during inspections = 2.157 lb / year

Loss during vessel entry to EST 13

CD in vapor lost = 0.980 lb moles per vessel entry
CD in vapor lost = 86.764 lb per vessel entry
CD lost during vessel entries = 247.06 lb / vessel

CD lost during vessel entries = .347.06 lb / year

Toluene in vapor lost = 0.14726 lb moles per vessel entry
Toluene in vapor lost = 13.607 lb per vessel entry

Toluene lost during inspections = 54.43 lb / year

ACR in vapor lost = 0.21920 lb moles per vessel entry
ACR in vapor lost = 26.9595 lb per vessel entry

ACR lost during inspections = 107.84 lb / year

Maximum Emission Rates

Maximum emission rate occurs at the start of tank evaculation using the air mover. Emissions will be at the concentration within the tanks.

Coppus blower capacity 750 cfm
CD emission in first minute 42.119 lb/min

assuming no air leakage in occurs in that first minute.

Toluene emission in first minute 6.605 lb/min ACR emission in first minute 13.087 lb/min

Maximum CD Emissions = 42.119 lb/min
Maximum toluene Emissions = 6.605 lb/min
Maximum ACR Emissions = 13.087 lb/min



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 13 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65A

Page

3

· of

3

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
	1	Rate	Rate	Ì
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	1207	46.411	4097.575	0.603
Chloroprene	1041	40.045	2527.117	0.521
Toluene	56	2.135	785.229	0.028
Total HAPs	1097	42.180	3312.346	0.548
Total TAPs	1097	42.180	3312.346	0.548



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 14 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65B

Page

Basis:

EST 14 is located outside of the main Poly building. The manway is not ventilated, so any emissions exit to atmosphere from the manway.

Emissions occur when the tanks are opened for cleaning or maintenance.

EST 13 and 14 are Liquid Dispersion unstripped emulsion storage tanks. These tanks are opened for inspection occasionally, assume once every two months. These tanks require occasional cleaning, assume once every 3 months.

When manways opened for inspection, tanks are already vented down via point source 1700-56. Manway will be open for perhaps 10 minutes while tank wall condition is observed for fouling Assume 1% of tank vapor content is emitted through convection to atmosphere during inspection, since thre is no motive force to displace vapor from inside the tank

When vessel entry is required to these tanks for cleaning, an air mover is used to evacuate the vapor contents of the tank, replacing it with an air atmosphere. This can take up to 6 hours.

Calculation basis provided by Mr. D. McCrea DuPont

Formerly under EID No. 1700-1 (EQT0134).

Volume EST 13 and 14 = 1545 cub ft Ambient temperature = 25 deg C

Pressure = 14.696 psia

For worst case scenarios, assuming equilibrium in tank before emptying. ACR and toluene not present in > 80% time, but counted as if they were.

Loss during inspections of EST 14

Vapor content of EST 13 or 14 = 3.941 lb moles

EST 13 or 14 vapor density = 0.0026 lb moles / cub ft

Inspection of EST 13 & 14 = 8 per year

Loss to atmosphere = 0.039 lb moles

CD in vapor lost = 0.97995 lb moles

CD in vapor lost = 86.7644 lb

CD lost during inspections = 694.115 lb / year

Toluene in vapor lost = 0.00147 lb moles

Toluene in vapor lost = 0.1361 lb

Toluene lost during inspections = 1.089 lb / year



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 14 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65B Page 2 of 3

ACR in vapor lost = 0.00219 lb moles per inspection ACR in vapor lost = 0.2696 lb per inspection

ACR lost during inspections = 2.157 lb / year

Loss during vessel entry to EST 14

CD in vapor lost =	0.980	lb moles	per vessel entry
CD in vapor lost =	86.764	lb	per vessel entry
CD lost during vessel entries =	347.06	lb / year	
Toluene in vapor lost =	0.14726	lb moles	per vessel entry ,
Toluene in vapor lost =	13.607	lb	per vessel entry
Toluene lost during inspections =	54.43	lb / year	
ACR in vapor lost =	0.21920	lb moles	per vessel entry
ACR in vapor lost =	26.9595	lb	per vessel entry

107,84

lb / year

Maximum Emission Rates

ACR lost during inspections =

Maximum ACR Emissions =

Maximum emission rate occurs at the start of tank evaculation using the air mover. Emissions will be at the concentration within the tanks.

13.087

Coppus blower capacity	750 .	cfm
CD emission in first minute	42.119	lb/min

assuming no air leakage in occurs in that first minute.

lb/min

Toluene emission in first minute 6.605 lb/min
ACR emission in first minute 13.087 lb/min

Maximum CD Emissions = 42.119 lb/min

Maximum toluene Emissions = 6.605 lb/min



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 14 Emulsion Storage Tank Manway

TEMPO ID:

Point Source ID No.: 1700-65B Page

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
		Rate	Rate	1
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	1207	46.411	4097.575	0.603
Chloroprene	1041	40.045	2527.117	0.521
Toluene	56	2.135	785.229	0.028
Total HAPs	1097	42.180	3312.346	0.548
Total TAPs	1097	42.180	3312.346	0.548



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Building Wall Fans

TEMPO ID: EQT0185

Point Source ID No.: 1700-66 Page 1 of 4

Basis:

Based on 10 hr TWA area data developed between 1999 and 2001, the average concentration of CD in the building air is 0.56 ppmv.

Monitoring data for toluene between February 2001 and September 2002 indicate an average concentration of 0.176 ppm.

ACR has a vapor pressure similar to that of toluene. Conservatively assume the same concentration in the air.

ACR is present in only 4 out of the 20 Neoprene types manufactured in Poly. Similarly toluene is present in only 6 types Neoprene out of 20

Fans vent fugitive emissions from equipment components located in the building. Calculation basis provided by Mr. P. Offut, DuPont

Rated Capacity of Fans = 4

Amount of Time Discharging =

Average CD in Air Exhausted =

Maximum CD in Air Exhausted = Avg. Toluene in Air Exhausted =

Max. Toluene in Air Exhausted =

Avg. ACR in Air Exhausted = Max. ACR in Air Exhausted =

Molecular Weight of CD = Molecular Weight of Toluene =

Molecular Weight of ACR =

Temperature =

| emperature = | Pressure = 476365 cfm

8760 hours/vr

0.56 ppm CD by volume

0.67 ppm CD by volume

0.176 ppm toluene by volume

3.1464 ppm toluene by volume

0.176 ppm ACR by volume 3.1464 ppm ACR by volume

88.54 lb/lb-mole

92.4 lb/lb-mole 122.99 lb/lb-mole

25 °C 14.696 psia

Average Emission Rates

Chloroprene

Using given information,

Average CD Emissions =

0.2668 cfm CD



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Building Wall Fans

TEMPO ID: EQT0185

Point Source ID No.: 1700-66

Page

2

of

4

Using the Ideal Gas Law,

Average CD Emissions = 0.000680 moles/minute
Average CD Emissions = 0.060241 lbs/minute
Average CD Emissions = 3.614 lbs/hour

Average CD Emissions = 31663 lbs/yr Average CD Emissions = 15.83 tons/yr

Toluene

Using given information,

Average Toluene Emissions = 0.0838 cfm toluene

Using the Ideal Gas Law,

Average Toluene Emissions = 0.000214 moles/minute
Average Toluene Emissions = 0.019758 lbs/minute
Average Toluene Emissions = 1.185 lbs/hour
Average Toluene Emissions = 10385 lbs/yr

Average Toluene Emissions = 5.19 tons/yr

ACR

Using given information,

Average ACR Emissions = 0.0838 cfm ACR

Using the Ideal Gas Law,

Average ACR Emissions = 0.000214 moles/minute
Average ACR Emissions = 0.026299 lbs/minute
Average ACR Emissions = 1.578 lbs/hour
Average ACR Emissions = 13823 lbs/yr
Average ACR Emissions = 6.91 tons/yr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Building Wall Fans

TEMPO ID: EQT0185

Point Source ID No.: 1700-66

Page

3

of

4

Maximum Emission Rates

Chloroprene

Using given information,

Maximum CD Emissions =

0.3201 cfm CD

Using the Ideal Gas Law,

Maximum CD Emissions = Maximum CD Emissions =

=

0.000816 moles CD/minute 0.072289 lbs CD/minute

Maximum CD Emissions =

4.337 lbs CD/hour

Toluene

Using given information,

Maximum Toluene Emissions =

1.4988 cfm toluene

Using the Ideal Gas Law, 1

· Maximum Toluene Emissions =

0.003823 moles/minute

Maximum Toluene Emissions =

0.353225 lbs/minute

Maximum Toluene Emissions =

21.193 lbs/hour

ACR

Using given information,

Maximum ACR Emissions =

1.4988 cfm ACR

Using the Ideal Gas Law,

Maximum ACR Emissions =

0.003823 moles/minute

Maximum ACR Emissions =

0.470163 lbs/minute

Maximum ACR Emissions =

28.210 lbs/hour



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Poly Building Wall Fans

TEMPO ID: EQT0185

Point Source ID No.: 1700-66

Page

4

of

6

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
		Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	55871	6.378	53.741	27.935
Chloroprene	31663	3.614	4.337	15.831
Toluene	10385	1.185	21.193	5.192
Total HAPs	42048	4.800	25.531	21.024
Total TAPs	42048	4.800	25.531	21.024



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Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Finishing Stabilizer Makeup Bag Filter

TEMPO ID: EQT0193

Point Source ID No.: 1700-74

Page

of

Basis:

Keltrol Used = 2521 lb/yr
TETD Used = 150219 lb/yr
Lomar PW = 10212 lb/yr
Total Addition Time = 88 hours

Keltrol, TETD, and Lomar are added manually from bags to finishing stabilizer makeup tanks into an aqueous suspension.

Estimated that 0.25% of the material transferred becomes airborne. This is based on experience with the bag filter, which is almost clean when inspected annually.

Estimated that 50% of the airborne dust is captured by exhaust system. Remainder is captured in building.

Emissions are controlled by a bag filter with 99% control efficiency.

Calculation basis provided by Mr. D.McCrea, DuPont

PM/PM-10 Emissions

Fraction Airborne = 0.25 %
Capture Efficiency = 50 %
Control Efficiency = 99 %

PM/PM-10 Emissions = Process rate, lb/yr x Fraction Airborne x Capture Effiency

x (1 - Control Efficiency) / 214 hr/yr

= 162952 lb/yr x 0.25% x 50% x (1 - 0.99) / 88 hr/yr

= 0.0231 lb/hr = 0.00 tpy

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
		Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
PM/PM-10	2.04	0.023	0.023	0.001



RTP Environmental Associates, Inc. Kenner, Louisiana

5 gal/min

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Emergency Stabilizer Drumming

TEMPO ID: EQT0198

Point Source ID No.: 1700-79 Page

Basis:

Emergency stabilizer is produced 4 times per year.

Emergency stabilizer is drummed out from the stablizer makeup tank.

Emissions are not controlled.

Assume that vapor displaced is saturated with VOC.

Emergency stabilizer is composed of toluene, water and dissolved inhibitors.

Calculation basis provided by Mr. P. Offut, DuPont

Drumming Rate =

Drumming Rate = 0.6685 cfm

Stabilizer Drummed = 20400 lb

Density of Emergency Stabilizer = 7.64 lb/gal

> Volume of Drum = 55 gal

Temperature = 25 C

Vapor Pressure of Toluene = 28.40 mm Hg 92.4 lb/lb-mole

Molecular Weight of Toluene =

Emission Rates

Drumming Time = 534.03 min

Using the Ideal Gas Law,

0.002550 moles/ft3 Total Vapor =

Toluene Vapor = 0.000095 moles/ft3

Toluene Vapor = 0.008807 lbs toluene/ft3 total vapor

Toluene Vapor = 0.005887 lbs toluene/min

Toluene Vapor = 0.353250 lb/hr

Toluene Vapor = 3.14 lb/yr Toluene Vapor = 0.002 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Emergency Stabilizer Drumming

TEMPO ID: EQT0198

Point Source ID No.: 1700-79 Page 2 of 2

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions .
l		Rate	. Rate	
<u> </u>	lb/yr	ib/hr	lb/hr	tpy
Total VOC	3.1	0.353	0.353	0.002
Toluene	3.1	0.353	0.353	0.002
Total HAPs	3.1	0.353	0.353	0.002
Total TAPs	3.1	0.353	0.353	0.002



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Storage Common Vent Header

TEMPO ID: RLP0017

Point Source ID No.: 1700-80

Page

1

of

4

Basis:

Emissions are the total from the Refined ACR Storage Tank (1700-80.1/EQT0199) and Chlorinated ACR Storage Tank (1700-80.2/EQT0200).

Compound	Total Loss	Average Emission	Maximum Emission	Annual Emissions
	lb/yr	Rate lb/hr	Rate lb/hr	tpy
Total VOC	198	0.023	-	0.099
1,2-Dichlorobenze	0.11	0.00001		0.00005
Total HAPs	0.11	0.00001	-	0.00005
Total TAPs	0.11	0.00001	•	0.00005



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Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Refined ACR Storage Tank

TEMPO ID: EQT0199

Point Source ID No.: 1700-80.1

Page

of

4

Basis:

Refined ACR from the ACR Refining Column is pumped into the Refined ACR storage tank. The Refined ACR Storage Tank has an external -18 C brine cooled heat exchanger. The circulating flow from the tank goes to the SMU are to feed the MST and returns to the tank via the cooler. The ACR storage tank is 45,000 gal in size, but the capacity is limited to 172,600 lb by Neovent considerations.

The tank is nitrogen blanketed.

Refined ACR is withdrawn from the ACR supply loop in Poly batchwise at the MST.

The Refined and Chlorinated ACR Storage tanks share a common ven header, but the ACR-solvent blend tank has a separate vent to avoid possible solvent contamination of the Refined ACR Storage Tank.

All inlet streams of ACR tanks enter through droplegs.

The vent stack for the ACR Storage Tank is to be 2° in diameter and approximately 50 ft above grade.

ACR Produced = 2959863 lb/yr

Max Fill Tank = 667 lb/hr

Tank Volume = 45000 gal

Max. Liquid Level in Refined ACR Tank = 17370 gal

Tank Temperature = -10.00 C

263.15 K

Tank Pressure = 6 psig

= 20.7 psia

1070.20 mm Hg

s.g. of ACR at Specified Temp = 1.2



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Refined ACR Storage Tank

TEMPO ID: EQT0199

Point Source ID No.: 1700-80.1 Page 2 of

Emission Rates

Use the working loss equation from Section 7.1.3.1.2 of AP-42, 5th Edition.

 L_W , Working Loss, lb/yr = 0.001 * M_V * P_{VA} * (Q / 42) * K_N * K_P

M_V = vapor molecular weight, lb/lb-mol

= 123.02 lb/lb-mole

P_{VA} = vapor pressure at daily average liquid surface temperature, psia

= 0.1250 psia

Q = throughput, gal/yr

= 295785 gal/yr

Max Level = 173818 lb

N = number of turnovers

= 295785 gal/yr / 17370 gal

= 17.03

 K_N = turnover factor

= 1 for N <= 36

= (180+N)/6N for N>36

:

 K_P = working loss product factor

1 for all liquids except crude oil



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Refined ACR Storage Tank

TEMPO ID: EQT0199

Point Source ID No.: 1700-80.1 Page 3 of

Component	Wt %	Mol Wt	Wt%/MW	Mole	Vapor	Partial
·	in liquid			Fraction	Pressure	Pressure
]		}	in Liquid	(mm Hg)	(mm Hg)
ACR	0.935	122.99	0.760	0.9397	6.66	6.2553
ACR-1	0.046	122.99	0.037	0.0462	4.27	0.1976
ACR-2	0.002	122.99	0.002	0.0020	2.84	0.0057
ACR-3	0.002	122.99	0.002	0.0020	1.89	0.0038
T-1,4 DCB	0	125	0	0.0000	0.01	0
TCB-1	0	159.5	0	0.0000	0.30	0
TCB-2	0	159.5	0.000	0.0000	0.05	0.0000
Meso	0	196	0.000	0.0000	0.03	0.0000
C4Cl4	0.01	196	0.005	0.0063	0.03	0.0002
C4CI5	0	230.5	0	0.0000	0.03	0
C4Cl6	0	265	0	0.0000	0.03	0
1,2-DCB	0.005	166.00	0.003	0.0037	1.11	0.0041
NMP	0	85.1	. 0	0.0000	0.00	0
	1.000		0.809	1		6.4667

Component	Partial	Mole	Mol Weight	Avg. Hourly	Max. Hourly	Annual
	Pressure	Fraction	of Vapor	Emissions	Emissions	Emissions
	(psia)	in Vapor	lb/lb-mol	lb/hr	lb/hr	lb/yr
ACR	0.12096	0.005845	118.97	0.012	0.026	104.793
ACR-1	0.00382	0.000185	3.76	0.0004	0.001	3.310
ACR-2	0.00011	0.000005	0.11	0.0000	0.000	0.096
ACR-3	0.00007	0.000004	0.07	0.0000	0.000	0.064
T-1,4 DCB	0	0	0	0	0	0
TCB-1	0	0	0	0	0	0
TCB-2	0	0	0	0.000000	0.00000	0
Meso	0	0	0	0.0000000	0.000000	Ó
C4Cl4	3.782E-06	1.82757E-07	0.005928087	3.74E-07	1.3E-06	0.003
C4Cl5	0	0	0	0	0	0
C4Cl6	0	0	0	0	0	0
1,2-DCB	0.00008	0.000004	0.11	0.000008	0.00002	0.069
NMP	0	0	0	0	. 0	0
	0.1250	0.0060	123.02	0.012	0.027	108.335



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Refined ACR Storage Tank

TEMPO ID: EQT0199

Point Source ID No.: 1700-80.1

Page

4

of

4

Compound	Total	Average	Maximum	Annual
}	Loss	Emission	Emission	Emissions
l		Raté	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	108	0.012	-	0.054
1,2-Dichlorobenze	0.07	0.000008	•	0.00003
Total HAPs	0.07	0.000008	•	0.00003
Total TAPs	0.07	0.000008	•	0.00003



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Chlorinated ACR Storage Tank

TEMPO ID: EQT0200

Point Source ID No.: 1700-80.2 Page 1 of 4

Basis:

Chlorinated ACR from the Transfer Tank in Monomer is pumped through the 1.5" transfer header to the Chlorinated ACR storage tank in Polly Area. The Chlorinated ACR Storage tank is jacketed with -18 deg C C brine and is nitrogen blanketed. There will be flow in and out of the tank simultaneously. The Chlorinated ACR Storage Tank is the former # 2 Crude CD Storage Tank. Tank is limited to 76.5% inventory by Neovent requirements.

The operating mode of this tank will be to run the level at a constant 50%, by matching the ACR production rate with the ACR refining rate.

Therefore working losses from this tank will be minimal.

However ACR Refining is designed to run at 50% uptime and ACR Synthesis at 80% uptime Therefore for 30% of time chlorinated ACR will run into the tank increasing the level, since ACR Refining is down.

Therefore ACR venting will occur during this period

Assume the tank is refilled for turnarounds twice per year.

ACR Produced = 2921460 lb/yr

Max ACR produced = 13000 lb/day

Chlorinated ACR per Refined ACR Produced = 1.591 lb/lb

Max Chlorinated ACR Produced = 862 lb/hr

Chlorinated ACR Tank Volume = 17600 gal

Max. Liquid Level in Chlorinated ACR Tank = 128040 lb

Tank Temperature = 0.00 C

= 273.15 K

Tank Pressure = 6 psig

= 20.7 psia

= 1070.20 mm Hg

s.g. of Chlorinated ACR at 0 C = 1.22



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Chlorinated ACR Storage Tank

TEMPO ID: EQT0200

Point Source ID No.: 1700-80.2 Page 2

Emission Rates

Use the working loss equation from Section 7.1.3.1.2 of AP-42, 5th Edition.

 L_W , Working Loss, Ib/yr = 0.001 * M_V * P_{VA} * (Q / 42) * K_N * K_P

M_V = vapor molecular weight, lb/lb-mol

= 123.04 lb/lb-mole

P_{VA} = vapor pressure at daily average liquid surface temperature, psia

= 0.1870 psia

Q = throughput, bbl/yr

Since tank is operated as a constant level tank for 70% of the time, the throughput is calculated for the remaining time plus 2 turnarounds

= [2921460 lb ACR/yr x 1.591 lb CACR/lb ACR x 0.3 / (1.22 x 8.34 lb/gal)

+ 17600 gal x 0.765 x 2] / 42 gal/bbl

= 3904 bbl/yr

N = number of turnovers

= 3904 bbl/yr / (17600 gal x 0.765 / 42 bbl/gal)

12.18

 $K_N = turnover factor$

= 1 for N <= 36

= (180+N) / 6N for N > 36

K_P = working loss product factor

= 1 for all liquids except crude oil



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Chlorinated ACR Storage Tank

TEMPO ID: EQT0200

Point Source ID No.: 1700-80.2 Page 3 of

Component	Wt %	Mol Wt	Wt%/MW	Mole	Vapor	Partial
•	in liquid			Fraction	Pressure	Pressure
	1			in Liquid	(mm Hg)	(mm Hg)
ACR	0.720	122.99	0.585	0.7399	11.86	8.7716
ACR-1	0:039	122.99	0.032	0.0399	7.96	0.3174
ACR-2	0.038	122.99	0.031	0.0388	5.37	0.2085
ACR-3	0.099	122.99	0.080	0.1013	3.58	0.3629
T-1,4 DCB	0	125	0	0.0000	. 0.01	0
TCB-1	0	159.5	0	0.0000	0.64	0
TCB-2	0.082	159.5	0.051	0.0647	0.12	0.0076
Meso	0.018	196	0.009	0.0116	0.07	0.0008
C4Cl4	0	196	0	0.0000	0.07	
C4Cl5	0	230.5	0	0.0000	0.07	0
C4Cl6	0	265	0	0.0000	0.07	0
1,2-DCB	0.005	166.00	0.003	0.0038	1.11	0.0042
NMP ⁻	0	85.1	0	0.0000	0.00	0
	1.000		0.791	1		9.6730

Component	Partial	Mole	Mol Weight	Avg. Hourly	Max. Hourly	Annual
	Pressure	Fraction	of Vapor	Emissions	Emissions	Emissions
	(psia)	in Vapor	lb/lb-mol	lb/hr	lb/hr	lb/yr
ACR	0.16961	0.008196	111.53	0.009	0.045	81.479
ACR-1	0.00614	0.000297	4.04	0.0003	0.002	2.949
ACR-2	0.00403	0.000195	2.65	0.0002	0.001	1.937
ACR-3	0.00702	0.000339	4.61	0.0004	0.002	3.371
T-1,4 DCB	0	0	0	0	0	0
TCB-1	0	0	0	0	0	0
TCB-2	0.00015	0.000007	0.13	0.000008	0.00005	0.070
Meso	0.00002	0.000001	0.02	0.0000008	0.000006	0.007
C4Cl4	0	0	0	0	0	_ 0
C4CI5	0	0	0	0	0	0
C4Cl6	0	O	0	0	0	0
1,2-DCB	0.00008	0.000004	0.07	0.000004	0.00003	0.039
NMP	0	0	0	0	0	0
	0.1870	0.0090	123.04	0.010	0.049	89.852



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Chlorinated ACR Storage Tank

TEMPO ID: EQT0200

Point Source ID No.: 1700-80.2

Page

Compound	Total	Average	Maximum	Annual
	Loss	Loss Emission Emission		Emissions
		Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	90	0.010	-	0.045
1,2-Dichlorobenze	0.04	0.000004	•	0.00002
Total HAPs	0.04	0.000004	<u> </u>	0.00002
Total TAPs	0.04	0.000004	-	0.00002



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Refining Vent

TEMPO ID: RLP0018

Point Source ID No.: 1700-81 Page 1 of 1

Basis:

Emissions calculated using an ASPEN simulation.

Compound	Total	Average	Maximum	Annual
'	Loss	Emission	Emission	Emissions
		Rate	Rate	
[lb/yr	lb/hr	lb/hr	tpy
Total VOC	4400	1.00	10.00	2.20
1,2-Dichlorobenze	<20	<0.001	<0.001	<0.01
HCI	1400	0.30	4.50	0.70
Total HAPs	1420	0.30	4.50	0.70
Total TAPs	1420	0.30	4.50	0.70



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR/Solvent Blend Tank

TEMPO ID: EQT0201

Point Source ID No.: 1700-82 Page 1 of 4

Basis:

ACR is sold to customers in drum quantities. To prevent polymerization of the ACR, the ACR is diluted with a solvent and extra polymerization inhibitors are added. The material to be drummed is made up in an ACR-solvent blend tank. Refined ACR from the ACR is added to the blend tank at -5 deg C. Solvent in Blend Tank will be at -10 deg C prior to ACR addition. Mixture temperature and composition when 50% of the ACR has been added represents average conditions during vapor displacement and was used to

Initial solvent added at ambient warehouse temperature (65F). External cooler will cool solvent down as it is added. Assume at mean temperature of -1 deg C.

Assume max rates are 120% of average rates.

	Units	ACR	ACR	ACR
·		Perclene	. DCM	Xylene
Annual Drums Made-up	Drums/yr	2,000	200	500
Drums per Blend Tank Fill	Drums	18	18	18
Refined ACR in ACR / Perclene Drum	lbs Ref. ACR	250	300	200
Amount Solvent per Drum	lbs Solvent	250	200	. 200
Solvent Containers per Batch	Containers	1	6	9
Solvent Container Mass	lbs	4,700	603	400
Solvent Unloading Time	minutes	17.12	15.87	24.57
Spec. Gravity of Solvent at -1 C	g/cc	1.65	1.37	0.88
Annual Blend Tank Fills	Blends/yr	111	11	27
Volume of Blend Tank	gallons	960		
Solvent Fill Rate	gpm	20		
Annual ACR Used in Drum Shipments	рру	660,000		
Tank Pressure at Venting	psig	2.5		
	mm Hg	889		
Avg Tank Temp During Solvent Addition	C	-1		
	K	272		
Adi. Gas Specific Vol. for Solvent Addition	ft ³ /lb mol	306		



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR/Solvent Blend Tank

TEMPO ID: EQT0201

Point Source ID No.: 1700-82

Page

2

of

Emission Rates

Estimation of Losses Due To Solvent Addition to Blend Tank

Component	Mol Wt	Vapor	Solvent Mole	Displaced	Displaced	Displaced
·)	Pressure	Fraction in	Volume in	Total Moles	Moles of
			Vapor	Blend Tank	from Tank	Solvent
	Į			i , ,		from Tank
]	lb/lb-mol	mm Hg		ft ³	lb-mol	lb-mol
Perclene	165.83	4.02	0.005	45.534	0.149	0.0007
Dichloromethane	84.93	137.18	0.154	42.409	0.139	0.0214
Xylene	106.17	1.58	0.002	65.424	0.214	0.0004

Component	Working	Avg. Hourly	Max. Hourly	Annual
	Loss	Loss Emissions E		Emissions
	ſb	lb/hr	lb/hr	lb/yr
Perclene	0.112	0.391	0.470	12.393
Dichloromethane	1.817	6.871	8.246	19.992
Xylene	0.040	0.099	0.118	1.090

Estimation of Losses Due To ACR Addition to Perclene in the Blend Tank

Assume conditions at the 50% ACR addition point, i.e., -10 C.

Average Hourly ACR Fill Rate = 667 pph

Tank Temperature during ACR Addition = -10 C
Tank Temperature during ACR Addition = 263 K

Adjusted Gas Specific Volume for ACR Addition = 296 ft³/lb-mol

Density of ACR at Specific Temperature = 1.20 g/cc

Mass of ACR Added = 4700 ibsVolume Displaced by ACR = 62.74 ft^3

Moles Displaced by ACR = 0.2123 lb-mol

ACR Fill Time = 7.05 hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

, Source Description: ACR/Solvent Blend Tank

TEMPO ID: EQT0201

Point Source ID No.: 1700-82

Page

3

of

4

Component	Wt % in	Mol Wt	Mole Fraction	Vapor	Partial	Mole
	Liquid		in Liquid	Pressure	Pressure	Fraction
						in Vapor
	1 1	lb/lb-mol	·	mm Hg	mm Hg	
ACR	0.3167	122.99	0.257	6.657	1.711	0.0019
ACR-1	0.0167	122.99	0.014	4.274	0.058	0.0001
Perciene	0.6667	165.83	0.729	3.875	2.827	0.0032

Component	Displaced	Working	Avg. Hourly	Max.	Annual
]	Moles from	Loss	Emissions	Hourly	Emissions
1	Tank			Emissions	
l	lb-mol	lb	lb/hr	lb/hr	lb/yr
ACR	0.00041	0.050	0.007	0.009	5.574
ACR-1	0.00001	0.002	0.0002	0.000	0.188
Perciene	0.00067	0.112	0.016	0.019	12.419

Estimation of Losses Due To ACR Addition to Dichloromethane in the Blend Tank

Mass of ACR Added =

5427 lbs

Volume Displaced by ACR = '

72.45 ft³

Moles Displaced by ACR =

0.2451 lb-mol

ACR Fill Time =

8.14 hr

Component	Wt % in Liquid	Mol Wt	Mole Fraction in Liquid	Vapor Pressure	Partial Pressure	Mole Fraction in Vapor
ACR	0.4071	lb/lb-mol 122.99	0.495	mm Hg 6.657	mm Hg 3.292	
ACR-1	0.0214	122.99				0.0001
Dichloromethane	0.5714	. 84.93	0.479	132.230	63.387	0.0713

Component	Displaced Moles from	Working Loss	Avg. Hourly Emissions	Max. Hourly	Annual Emissions
	Tank			Emissions	
	lb-mol	lb	lb/hr	lb/hr	lb/yr
ACR	0.00091	0.112	0.014	0.016	1.228
ACR-1	0.00003	0.004	0.0005	0.001	0.041
Dichloromethane	0.01747	1.484	0.182	0.219	16.321



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR/Solvent Blend Tank

TEMPO ID: EQT0201

Point Source ID No.: 1700-82

Page

4

Estimation of Losses Due To ACR Addition to Xylene in the Blend Tank

Mass of ACR Added =

3600 lbs

Volume Displaced by ACR =

48.06 ft³

Moles Displaced by ACR =

0.1626 lb-mol

ACR Fill Time =

5.40 hr

Component	Wt % in Liquid	Mol Wt	Mole Fraction in Liquid	Vapor Pressure	Partial Pressure	Mole Fraction in Vapor
	}	lb/lb-moi		mm Hg	mm Hg	
ACR	0.3167	122.99	0.348	6.657	2.319	0.0026
ACR-1	0.0167	122.99	0.018	4.274	0.078	0.0001
Xylene	0.6667	106.17	0.633	1.523	0.964	0.0011

Component	Displaced Moles from	. ,		Max. Hourly	Annual Emissions
	Tank			Emissions	
l	lb-mol	lb	lb/hr	lb/hr	lb/yr
ACR	0.00042	0.052	0.010	0.012	1.408
ACR-1	0.00001	0.002	0.0003	0.000	0.048
Xyiene	0.00018	0.019	0.003	0.004	0.505

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
i	, i	Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	10	0.134	0.142	0.005
Dichloromethane	36	7.054	9.895	0.018
Tetrachlorethylens	25	0.407	0.563	0.012
Xylene	2	0.102	0.142	0.001
Total HAPs	63	7.563	9.895	0.031
Total TAPs	63	7.563	9.895	0.031



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Drumming Vent

TEMPO ID: RLP0019

Point Source ID No.: 1700-83 Page 1 of 4

Basis:

ACR- solvent mixtures from the ACR blend tank are added to 55-gallon drums to supply material to customers. Vapors are not recovered from the drumming operation. There is an area ventilation fan in the open drumming shed to minimize operator exposure to vapors during the filling operation. Maximum hourly emissions assume that only 4 pallets (16 drums) of material can be loaded out in one hour, based upon past experience. The max. for ACR/MeCl is 13 drums as this is the largest order experienced. Average hourly emissions was calculated by prorating the hourly emission by type by the annual order quantity by type.

	Units	ACR	ACR	ACR
		Perclene	DCM	Xylene
Vap Press of Solvent @ -5 C	mm Hg	3.1	111.9	1.0
Spec. Grav. Of Solvent @ -5 C		1.66	1.37	0.89
Spec. Gravity of ACR @ -5 C		1.19	1.19	1.19
Wt % ACR in Drum	wt %	50%	60%	50%
s.g of ACR Solvent Blend		1.39	1.26	1.02
Annual No. of Drums Made up	#	2000	200	500
Max No. of Drums Filled	#/hr	16	13	16
Avg No. of Drums Filled	#/hr	12	12	12
ACR Solvent Mixture per Drum	lbs	500	500	400
Drum Temperature	С	-5		
Drum Temperature	K	268		
Drum Pressure	mm Hg	760		
Gas Specific Volume	ft ³ /lb-mol	352		



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Drumming Vent

TEMPO ID: RLP0019

Point Source ID No.: 1700-83

Page

2

of

4

Emission Rates

ACR/Perclene Drum Filling

Component	Wt % in	Mol Wt	Wt%/MW	Mole	Vapor	Partial
	Liquid			Fraction	Pressure	Pressure
				in Liquid		
L	1	lb/lb-mol			mm Hg	mm Hg
ACR	0.4750	122.99	0.386	0.546	8.932	4.8789
ACR-1	0.0180	122.99	0.015	0.021	5.867	0.1215
Others	0.0070	150	0.005	0.007	3.930	0.0259
Perclene	0.5000	165.83	0.302	0.426	3.082	1.3144
	1		0.707	1		

Component	Mole	Working	Avg. Hourly	Max.	Annual
	Fraction	Loss	Emissions	Hourty	Emissions
1	in Vapor			Emissions	
	<u> </u>	lb/drum	lb/hr	lb/hr	lb/yr
ACR	0.0064	0.013	0.155	0.207	25.850
ACR-1	0.0002	0.0003	0.004	0.005	0.644
Others	0.00003	0.00008	0.001	0.001	0.168
Perclene	0.0017	0.005	0.056	0.075	9.390

ACR/Dichloromethane Drum Filling

Component	Wt % in Liquid	Mol Wt	Wt%/MW	Mole Fraction	Vapor Pressure	Partial Pressure
ĺ	· ì		j	in Liquid		
		lb/lb-mol			mm Hg	mm Hg
ACR	0.5700	122.99	0.463	0.484	8.932	4.3227
ACR-1	0.0216	122.99	0.018	0.018	5.867	0.1076
Others	0.0084	150	0.006	0.006	3.930	0.0230
Dichloromethane	0.4000	84.93	0.471	0.492	111.883	55.0273
	1		0.958	1	-	



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Drumming Vent

TEMPO ID: RLP0019

Point Source ID No.: 1700-83 Page 3 of 4

Component	Mole Fraction	Working Loss	Avg. Hourly Emissions	Max. Hourly	Annual Emissions
	in Vapor			Emissions	
[1	lb/drum	lb/hr	lb/hr	lb/yr
ACR	0.0057	0.013	0.151	0.164	2.525
ACR-1	0.0001	0.0003	0.004	0.004	0.063
Others	0.00003	0.00008	0.001	0.001	0.016
Dichloromethane	0.0724	0.111	1.332	1.443	22.194

ACR/Xylene Drum Filling

Component	Wt % in	Mol Wt	Wt%/MW	Mole	Vapor	Partial
	Liquid			Fraction	Pressure	Pressure
			٠,٠	in Liquid		
		lb/lb-mol		·	mm Hg	mm Hg
ACR	0.4750	122.99	0.386	0.441	8.932	3.9356
ACR-1	0.0180	122.99	0.015	0.017	5.867	0.0980
Others	0.0070	150	0.005	0.005	3.930	0.0209
Xylene	0.5000	106.17	0.471	0.537	1.032	0.5544
···	1		0.876	1		

Component	Mole Fraction	Working Loss	Avg. Hourly Emissions	Max. Hourly	Annual Emissions
	in Vapor	2000	2.7110010110	Emissions	21110010110
	. [lb/drum	lb/hr	· lb/hr	lb/yr
ACR	0.0052	0.011	0.136	0.181	5.671
ACR-1	0.0001	0.0003	0.003	0.005	0.141
Others	0.00003	0.00007	0.001	0.001	0.037
Xylene	0.00073	0.001	0.017	0.022	0.690



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: ACR Drumming Vent

TEMPO ID: RLP0019

Point Source ID No.: 1700-83

Page

Ĺ

of

4

Compound	Total	Average	Maximum	Annual
1	Loss	Emission	Emission	Emissions
		Rate	Rate	
[lb/yr	lb/hr	lb/hr	tpy_
Total VOC	45	0.201	0.346	0.023
Dichloromethane	22	0.099	1.443	0.011
Tetrachloroethyle	9	0.042	0.075	0.005
Xylene	1	0.003	0.022	0.0003
Total HAPs	32	0.143	1.443	0.016
Total TAPs	32	0.143	1.443	0.016



RTP Environmental Associates, Inc. ... Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Emulsion Blend Tank

TEMPO ID: EQT0212

Point Source ID No.: 1700-84A Page 1 of 3

Basis:

AFS will purchase up to 32 totes of WRT, GRT, GW emulsion monthly Use 48 totes for calculation

Vented annual volume of ACS tank is that of 48 totes per month

Toluene is emitted from GRT and GW emulsions.

90% of emulsion shipped will contain toluene

AFS Tank Volume = 5772 gal

= 771.72 ft3

Tank filling at ambient temperature = 35 C

Vapor pressure CD at 35 °C is 334.3 mm Hg

Vapor pressure toluene at 35 °C is 52 mm Hg

MW of CD = 88.54 lb/lb-mol

MW of Toluene = 92.14 lb/lb-mol

CD component of emulsion = 0.099 wt % max

Toluene component of emulsion = 0.0165 wt % max Solids component of emulsion = 45 wt %

Tote Contains = 2200 lb emulsion

Emulsion Density = 67.28 lb/ft3

No. of Totes = 48 per month

Specific Volume = 359.7 ft3/mol

Operating Time = 8760 hr

Emission Rates

Convert CD concentration to exclude the solids component

CD component of emulsion = 0.099 / (1 - 0.45)

= 0.180 %

Mole Fraction CD = 0.18 / 88.54 / [0.18 / 88.54 + (100 - 0.18) / 18]

= 0.00037

Partial Pressure CD in Tank = 334.3 x 0.00037

0.123 mm Hg

Mole Fraction CD in Vapor = 0.123 mm Hg / 760

= 0.000161



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Emulsion Blend Tank

TEMPO ID: EQT0212

Point Source ID No.: 1700-84A

Page 2

of

3

Vapor Vented per Tote = 2200 lb/tote / 67.284 lb/cu ft

32.70 ft3/tote

CD Emitted = 48 totes/month x,12 months/yr x 32.7 cu ft/tote x 0.000161

= 3.04 ft3

CD Emitted = 3.04 cu ft x 88.54 lb/lb-mole / [359.7 cu ft/mole x (273 / (273 + 35))]

0.84 lb

= 0.0004 tpy

= 0.0001 lb/hr

Convert toluene concentration to exclude the solids component

Toluene component of emulsion = 0.0165 / (1 - 0.45)

0.030 %

Mole Fraction Toluene = 0.03 / 92.14 / [0.03 / 92.14 + (100 - 0.03) / 18]

= 0.00006

Partial Pressure Toluene in Tank = 52 x 0.00006

0.003 mm Hg

Mole Fraction Toluene in Vapor = 0.003 mm Hg / 760

= 0.000004

Toluene Emitted = 48 totes/month x 12 months/yr x 32.7 cu ft/tote x 0.000004 x 0.9

0.07 ft3

Toluene Emitted = 0.07 cu ft x 92.14 lb/lb-mole / [359.7 cu ft/mole x (273 / (273 + 35))]

e 0.02 lb

= 0.00001 tpy

= 0.000002 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Emulsion Blend Tank

TEMPO ID: EQT0212

Point Source ID No.: 1700-84A Page 3 of

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
	Rate		Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	0.86	0.0001	0.0001	0.0004
Chloroprene	0.84	0.0001	0.0001	0.0004
Toluene	0.02	0.000002	0.000002	0.00001
Total HAPs	0.86	0.0001	0.0001	0.0004
Total TAPs	0.86	0.0001	0.0001	0.0004



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Totes

TEMPO ID: EQT0213

Point Source ID No.: 1700-84B Page 1 of 3

Basis:

AFS will purchase up to 32 totes of WRT, GRT, GW emulsion monthly Use 48 totes for calculation Vented annual volume of ACS tank is that of 48 totes per month Toluene is emitted from GRT and GW emulsions. 90% of emulsion shipped will contain toluene

Tote filling at ambient temperature = 35 C

Vapor pressure CD at 35 °C is 334.3 mm Hg
Vapor pressure toluene at 35 °C is 52 mm Hg

MW of CD = 88.54 lb/lb-mol

MW of Toluene = 92.14 lb/lb-mol

CD component of emulsion = 0.099 wt % max

Toluene component of emulsion = 0.0165 wt % max

Solids component of emulsion = 45 wt %

Tote Contains = 2200 lb emulsion

Emulsion Density = 67.28 lb/ft3

No. of Totes = 48 per month

Specific Volume = 359.7 ft3/mol

Operating Time = 8760 hr

Emission Rates

Convert CD concentration to exclude the solids component

CD component of emulsion = 0.099 / (1 - 0.45)

= 0.180 %

Mole Fraction CD = 0.18 / 88.54 / [0.18 / 88.54 + (100 - 0.18) / 18]

= 0.00037

Partial Pressure CD in Totes = 334.3 x 0.00037

0.123 mm Hg

Mole Fraction CD in Vapor = 0.123 mm Hg / 760

= 0.000161



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Totes

TEMPO ID: EQT0213

Point Source ID No.: 1700-84B

Page

2

of

3

Vapor Vented per Tote = 2200 lb/tote / 67.284 lb/cu ft

= 32.70 ft3/tote

CD Emitted = 48 totes/month x 12 months/yr x 32.7 cu ft/tote x 0.000161

= 3.04 ft3

CD Emitted = 3.04 cu ft x 88.54 lb/lb-mole / [359.7 cu ft/mole x (273 / (273 + 35))]

= 0.84 lb

= 0.0004 tpy

= 0.0001 lb/hr

Convert toluene concentration to exclude the solids component

Toluene component of emulsion = 0.0165 / (1 - 0.45)

0.030 %

Mole Fraction Toluene = 0.03 / 92.14 / [0.03 / 92.14 + (100 - 0.03) / 18]

= 0.00006

Partial Pressure Toluene in Totes = 52 x 0.00006

0.003 mm Hg

Mole Fraction Toluene in Vapor = 0.003 mm Hg / 760

= 0.000004

Toluene Emitted = 48 totes/month x 12 months/yr x 32.7 cu ft/tote x 0.000004 x 0.9

= 0.07 ft3

Toluene Emitted = 0.07 cu ft x 92.14 lb/lb-mole / [359.7 cu ft/mole x (273 / (273 + 35))]

= 0.02 lb

= 0.00001 tpy

= 0.000002 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Advanced Fibres System (AFS) Emulsion Shipping Totes

TEMPO ID: EQT0213

Point Source ID No.: 1700-84B

Page

3

of

3

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
		Rate	Rate Rate	
	lb/yr	lb/hr	lb/hr	tpy_
Total VOC	0.86	0.0001	0.0001	0.0004
Chloroprene	0.84	0.0001	0.0001	0.0004
Toluene	0.02	0.000002	0.000002	0.00001
Total HAPs	0.86	0.0001	0.0001	0.0004
Total TAPs	0.86	0.0001	0.0001	0.0004



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Liquid Dispersion Loading (Truck, Tote, Railcar)

TEMPO ID: EQT0214

Point Source ID No.: 1700-85 Page 1 of 4

Basis:

65% of LD shipments will be by bulk carrier.

LD loaded from Emulsion Storage Tanks # 11, 12, 15,16 into vendor tank trucks

Total LD Shipped = 15 MMlb/yr dry wt

Total LD-750 Shipped = 3.7 MMlb/yr dry wt

Solids component = 50 wt %

Total LD Shipments Bulk = 65 % of total

Loading Temperature = 35 C

Vapor pressure CD at 35 °C = 334.3 mm Hg Vapor pressure toluene at 35 °C = 52 mm Hg

MW of CD = 88.54 lb/lb-mol

MW of Toluene = 92.14 lb/lb-mol ponent of emulsion = 0.099 wt % max

CD component of emulsion = 0.099 wt % max
Toluene component of emulsion = 0.008415 wt % (LD-750)

Weight of LD loaded per truck = 46000 lb wet wt

Weight of LD loaded per tote = 2200 lb wet wt
Weight of LD loaded per Railcar = 180000 lb wet wt

EIGHT OF LD loaded per Hallcar = 160000 lb wet with the loaded per Hallcar = 1600000 lb wet with the loaded pe

Specific Volume = 359.7 ft3/mol

Operating Time = 8760 hr

Emission Rates

Truck Loading

Convert CD concentration to exclude the solids component

CD component of emulsion = 0.099 / (1 - 0.5)

= 0.198 %

Mole Fraction CD = 0.198 / 88.54 / [0.198 / 88.54 + (100 - 0.198) / 18]

= 0.0004

Partial Pressure CD = 334.3 x 0.0004

0.135 mm Hg

Mole Fraction CD in Vapor = 0.135 mm Hg / 760

= 0.000177



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Liquid Dispersion Loading (Truck, Tote, Railcar)

TEMPO ID: EQT0214

Point Source ID No.: 1700-85

Page

2

of

Vapor Vented per Truck = 46000 lb/truck / 68.53 lb/cu ft

671.24 ft3/truck

No. of Trucks = $15 \,\text{MMlb/yr} \,\text{dry} / (1 - 0.5) \times 0.65 \times 1000000 / 46000 \,\text{lb/truck}$

= 424 trucks

CD Emitted = 424 trucks/yr x 671.24 cu ft/truck x 0.000177

= 50.48 ft3

CD Emitted = 50.48 cu ft x 88.54 lb/lb-mole / [359.7 cu ft/mole x (273 / (273 + 35))]

14.02 lb

= 0.007 tpy

= 0.002 lb/hr

Convert toluene concentration to exclude the solids component

Toluene component of emulsion = 0.008415/(1-0.5)

0.017 %

Mole Fraction Toluene = 0.01683 / 92.14 / [0.01683 / 92.14 + (100 - 0.01683) / 18]

= 0.00003

Partial Pressure Toluene in Tank = 52 x 0.00003

0.002 mm Hg

Mole Fraction Toluene in Vapor = 0.002 mm Hg / 760

= 0.000002

No. of Trucks = 3.7 MMib/yr dry / (1 - 0.5) x 0.65 x 1000000 / 46000 ib/truck

= 105 trucks

Toluene Emitted = 105 trucks/vr x 671.24 cu ft/truck x 0.000002

0.16 ft3

Toluene Emitted = 0.16 cu ft x 92.14 lb/lb-mole / [359.7 cu ft/mole x (273 / (273 + 35))]

= 0.05 lb

= 0.00002 tpy

= 0.000005 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Liquid Dispersion Loading (Truck, Tote, Railcar)

TEMPO ID: EQT0214

Point Source ID No.: 1700-85

Page

3

of

Tote Filling

Allow 25% for reworking off spec and returns

Vapor Vented per Tote = 2200 lb/tote / 68.53 lb/cu ft

32.10 ft3/tote

No. of Totes = $15 \text{ MMlb/yr dry / } (1 - 0.5) \times (1 - 0.65) \times 1000000 / 2200 \text{ lb/tote } \times 1.25$

5966 totes

CD Emitted = 5966 totes/yr x 32.1 cu ft/tote x 0.000177

= 33.97 ft3

CD Emitted = 33.97 cu ft x 88.54 lb/lb-mole / [359.7 cu ft/mole x (273 / (273 + 35))]

9.43 lb

= 0.005 tpy

= 0.001 lb/hr

No. of LD-750 Totes = 3.7 MMlb/yr dry / (1 - 0.5) x (1 - 0.65) x 1000000 / 2200 lb/tote x 1.25

1472 totes

Toluene Emitted = 1472 totes/yr x 32.1 cu ft/tote x 0.000002

= 0.11 ft3

Toluene Emitted = 0.11 cu ft x 92.14 lb/lb-mole / [359.7 cu ft/mole x (273 / (273 + 35))]

e 0.03 lb

= 0.00002 tpy

= 0.000004 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Liquid Dispersion Loading (Truck, Tote, Railcar)

TEMPO ID: EQT0214

Point Source ID No.: 1700-85 Page 4 of 4

Railcar Loading

A maximum of 50 railcars will be loaded per year.

No. of Railcars =

50 railcars

Vapor Vented per Truck = 180000 lb/railcar / 68.53 lb/cu ft

= 2626.59 ft3/railcar

CD Emitted = 50 railcars/yr x 2626.59 cu ft/railcar x 0.000177

= 23.29 ft3

CD Emitted = 23.29 cu ft x 88.54 lb/lb-mole / [359.7 cu ft/mole x (273 / (273 + 35))]

6.47 lb

= 0.003 tpy

= 0.001 lb/hr

Toluene Emitted = 50 railcars/yr x 2626.59 cu ft/railcar x 0.000002

= 0.30 ft3

Toluene Emitted = 0.3 cu ft x 92.14 lb/lb-mole / [359.7 cu ft/mole x (273 / (273 + 35))]

= 0.09 lb

= 0.00004 tpy

= 0.00001 lb/hr

Compound	Total	Average	Maximum	Annual
	Loss	Emission	Emission	Emissions
		Rate Rate		
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	30.08	0.0034	0.0034	0.015
Chloroprene	29.92	0.0034	0.0034	0.015
Toluene	0.16	0.00002	0.00002	0.00008
Total HAPs	30.08	0.0034	0.0034	0.015
Total TAPs	30.08	0.0034	0.0034	0.015



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Fugitive Emissions - Neoprene Unt

TEMPO ID: FUG0004

Point Source ID No.: 1-93 Page 1 of

Basis:

Site specific emission factors are based on bagging studies performed at various DuPont-Dow facilities including the Pontchartrain Site and consider historical performance from monitoring.

Emissions are for those components located outside of the Poly Building. Fugitives from equipment components located in the Poly Building are covered by the various manhole vents and Poly Building wall fans.

Calculation basis provided by Ms. D. Grego, DuPont

Summary

Equipment	Service	Total	Average	Total	Total
	·	Component	Emission	Emissions	Emissions
		Count	Rate	1	
			lb/hr	lb/yr	tpy
Valves	Lt. Liquid	314	0.1225	1073	0.54
	Gas	89	0.0320	281	0.14
Pump Seals	Lt. Liquid	14	0.0161	141	0.07
Connectors	All	1780	0.3204	2807	1.40
PRVs	Gas	29	0.0035	30	0.02
		Total:	0.4945	4332	2.17

Maximum Emission Rate =

. 0.4945 lb/hr

Speciation

Chloroprene Emissions = 0.3657 lb/hr Chloroprene Emissions = 3203 lb/yr Chloroprene Emissions = 1.602 tpy

Toluene Emissions = 0.0501 lb/hr
Toluene Emissions = 439 lb/yr
Toluene Emissions = 0.219 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Fugitive Emissions - Neoprene Unt

TEMPO ID: FUG0004

Point Source ID No.: 1-93

Page

2

f

3

Components in Chloroprene Service

Equipment	Service	Component	Dupont-Dow	Emission	Total
	1	Count	Factor	Rate	Emissions
			lb/hr/src	lb/hr	lb/yr
Valves	Lt. Liq./Gas	234	3.90E-04	0.0913	799
	Gas	66	3.60E-04	0.0238	208
Pump Seals	Lt. Liquid	9	1.15E-03	0.0104	91
Connectors	All	1335	1.80E-04	0.2403	2105
PRVs	Gas	21	1.20E-04	0.0025	22
			Total:	0.3657	3203

Components in Toluene Service

Equipment	Service	Component	Dupont-Dow	Emission	Total
		Count	Factor	Rate	Emissions
			lb/hr/src	lb/hr	lb/yr
Valves	Lt. Liq./Gas	32	3.90E-04	0.0125	109
	Gas	9	3.60E-04	0.0032	28
Pump Seals	Lt. Liquid	2	1.15E-03	0.0023	20
Connectors	All·	178	1.80E-04	0.0320	281
PRVs	Gas	3	1.20E-04	0.0004	3
			Total:	0.0501	439

Components in Acetic Acid Service

Equipment	Service	Component	Dupont-Dow	Emission	Total
		Count	Factor	Rate	Emissions
	1.		- lb/hr/src	lb/hr	lb/yr
Valves	Lt. Liq./Gas	16	3.90E-04	0.0062	55
	Gas	5	3.60E-04	0.0018	16
Pump Seals	Lt. Liquid	1	1.15E-03	0.0012	10
Connectors	All	89	1.80E-04	0.0160	140
PRVs	Gas	2	1.20E-04	0.0002	2
			Total:	0.0252	221



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Fugitive Emissions - Neoprene Unt

TEMPO ID: FUG0004

Point Source ID No.: 1-93 Page

Components in Other VOC Service

Equipment	Service	Component	Dupont-Dow	Emission	Total
		Count	Factor	Rate	Emissions
			lb/hr/src	lb/hr	lb/yr
Valves	Lt. Liq./Gas	32	3.90E-04	0.0125	109
	Gas	9	3.60E-04	0.0032	28
Pump Seals	Lt. Liquid	2	1.15E-03	0.0023	20
Connectors	All	178	1.80E-04	0.0320	281
PRVs	Gas	3	1.20E-04	0.0004	3
			Total	0.0501	430



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Diversion Tank

TEMPO ID: EQT0202

Point Source ID No.: 3-95

Page

of

3

Basis:

Calculations are performed using Water 9.

Since ACR is not in the database, emissions of ACR are estimated to be similar to toluene since the two compounds are of similar vapor pressures.

Calculation basis provided by Ms. D. Grego, DuPont

Hours of Operation =

8760 hr

Average Emission Rates

Acetic Acid

Emission Rate = 2.056E-08 g/s Emission Rate = 0.0000002 lb/hr Emission Rate = 0.001 lb/yr Emission Rate = 0.0000007 tpy

Chloroprene

Emission Rate = 3.16E-06 g/s
Emission Rate = 0.00003 lb/hr
Emission Rate = 0.2 lb/yr
Emission Rate = 0.0001 tpy

Toluene

Emission Rate = 1.666E-07 g/s
Emission Rate = 0.000001 lb/hr
Emission Rate = 0.01 lb/yr
Emission Rate = 0.000006 tpy

ACR

Emission Rate = 1.666E-07 g/s
Emission Rate = 0.000001 lb/hr
Emission Rate = 0.01 lb/yr
Emission Rate = 0.000006 tpy



RTP Environmental Associates, Inc.
Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Diversion Tank

TEMPO ID: EQT0202

Point Source ID No.: 3-95

Page

2

of

3

1,2-Dichlorobenzene

Emission Rate = Emission Rate =

Emission Rate = Emission Rate =

0.000001 lb/hr 0.01 lb/yr

1.60E-07 g/s

0.000006 tpy

Maximum Emission Rates

Acetic Acid

Emission Rate =

1.58E-07 g/s

Emission Rate =

0.000001 lb/hr

Chloroprene

Emission Rate =

1.37E-05 g/s

Emission Rate =

0.0001 lb/hr

Toluene

Emission Rate =

1.28E-06 g/s

Emission Rate =

0.00001 lb/hr

ACR

Emission Rate =

1.28E-06 g/s

Emission Rate =

0.00001 lb/hr

1,2-Dichlorobenzene

Emission Rate =

1.23E-06 g/s

Emission Rate =

0.00001 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Diversion Tank

TEMPO ID: EQT0202

Point Source ID No.: 3-95

Page

3

of

3

Compound	Total	Average	Maximum	Annual
}	Loss	Emission	Emission	Emissions
		Rate		
l	lb/yr	lb/hr	lb/hr	tpy
Total VOC	0.3	0.00003	0.0001	0.0001
Chloroprene	0.2	0.00003	0.0001	0.0001
1,2-Dichlorobenze	0.01	0.000001	0.00001	0.000006
Toluene	0.01	0.000001	0.00001	0.000006
Total HAPs	0.2	0.00003	0.0001	0.0001
Total TAPs	0.2	0.00003	0.0001	0.0001



RTP Environmental Associates, Inc. Kenner, Louisiana

3

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 1 Aeration Tank

TEMPO ID: EQT0203

Point Source ID No.: 4-95 Page

Basis:

Calculations are performed using Water 9.

Since ACR is not in the database, emissions of ACR are estimated to be similar to toluene since the two compounds are of similar vapor pressures.

Calculation basis provided by Ms. D. Grego, DuPont

Hours of Operation =

8760 hr

Average Emission Rates

Acetic Acid

Emission Rate = 0.000005233 g/s
Emission Rate = 0.00004 lb/hr
Emission Rate = 0.0002 tpy

Chloroprene

Emission Rate = 0.062409 g/s Emission Rate = 0.495 lb/hr Emission Rate = 4339 lb/yr Emission Rate = 2.170 tpy

Toluene

Emission Rate = 0.001774 g/s
Emission Rate = 0.014 lb/hr
Emission Rate = 123 lb/yr
Emission Rate = 0.062 tpy

ACR

Emission Rate = 0.001774 g/s Emission Rate = 0.014 lb/hr Emission Rate = 123 lb/yr Emission Rate = 0.062 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 1 Aeration Tank

TEMPO ID: EQT0203

Point Source ID No.: 4-95 Page 2 of 3

1,2-Dichlorobenzene

Emission Rate = 0.00184 g/s
Emission Rate = 0.015 lb/hr
Emission Rate = 128 lb/yr
Emission Rate = 0.064 tpy

Maximum Emission Rates

Acetic Acid

Emission Rate = 4.05E-05 g/s Emission Rate = 0.0003 lb/hr

Chloroprene

Emission Rate = 0.27019 g/s Emission Rate = 2.144 lb/hr

Toluene

Emission Rate = 0.013652 g/s Emission Rate = 0.108 lb/hr

ACR

Emission Rate = 0.013652 g/s Emission Rate = 0.108 lb/hr

1.2-Dichlorobenzene

Emission Rate = 0.014244 g/s Emission Rate = 0.113 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 1 Aeration Tank

TEMPO ID: EQT0203

Point Source ID No.: 4-95 Page 3 of 3

Compound	Total	Average	Maximum	Annual
'	Loss	Emission	Emission	Emissions
	ĺ	Rate	Rate	
i	lb/yr	lb/hr	lb/hr	tpy
Total VOC	4586	0.524	2.361	2.293
Chloroprene	4339	0.495	2.144	2.170
1,2-Dichlorobenze	128	0.014	0.113	0.064
Toluene	123	0.014	0.108	0.062
Total HAPs	4590	0.523	2.366	2.295
Total TAPs	4590	0.523	2.366	2.295



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 2 Aeration Tank

TEMPO ID: EQT0204

Point Source ID No.: 5-95 Page 1 of

Basis:

Calculations are performed using Water 9.

Since ACR is not in the database, emissions of ACR are estimated to be similar to toluene since the two compounds are of similar vapor pressures.

Calculation basis provided by Ms. D. Grego, DuPont

Hours of Operation =

8760 hr

Average Emission Rates

Acetic Acid

Emission Rate = 5.58E-07 g/s
Emission Rate = 0.000004 lb/hr
Emission Rate = 0.04 lb/yr
Emission Rate = 0.00002 tpy

Chloroprene

Emission Rate = 0.0007275 g/s
Emission Rate = 0.006 lb/hr
Emission Rate = 51 lb/yr
Emission Rate = 0.025 tpy

Toluene

Emission Rate = 0.00001718 g/s
Emission Rate = 0.0001 lb/hr
Emission Rate = 1 lb/yr
Emission Rate = 0.001 tpy

ACR

Emission Rate = 0.00001718 g/s
Emission Rate = 0.0001 lb/hr
Emission Rate = 1 lb/yr
Emission Rate = 0.001 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 2 Aeration Tank

TEMPO ID: EQT0204

Point Source ID No.: 5-95 Page 2 of 3

1,2-Dichlorobenzene

Emission Rate = 1.12E-04 g/s
Emission Rate = 0.0009 lb/hr
Emission Rate = 8 lb/yr
Emission Rate = 0.004 tpy

Maximum Emission Rates

Acetic Acid

Emission Rate = 4.31E-06 g/s Emission Rate = 0.00003 lb/hr

Chloroprene

Emission Rate = 0.00315 g/s Emission Rate = 0.025 lb/hr

Toluene

Emission Rate = 1.32E-04 g/s Emission Rate = 0.001 lb/hr

ACR

Emission Rate = 1.32E-04 g/s Emission Rate = 0.001 lb/hr

1,2-Dichlorobenzene

Emission Rate = 8.70E-04 g/s Emission Rate = 0.007 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: No. 2 Aeration Tank

TEMPO ID: EQT0204

Point Source ID No.: 5-95

Page

3

of

3

Summary

Compound	Total	Average	Maximum	Annual
]	Loss	Emission	Emission	Emissions
		Rate	Rate	
	lb/yr	lb/hr	lb/hr	tpy
Total VOC	53	0.006	0.027	0.027
Chloroprene	51	0.006	0.025	0.025
1,2-Dichlorobenze	8	0.001	0.007	0.004
Toluene	1	0.000	0.001	0.001
Total HAPs	60	0.007	0.033	0.030
Total TAPs	60	0.007	0.033	0.030



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Clarifier

TEMPO ID:

Point Source ID No.: 6-95

Page

1

of

3

Basis:

Calculations are performed using Water 9.

Since ACR is not in the database, emissions of ACR are estimated to be similar to toluene since the two compounds are of similar vapor pressures.

Calculation basis provided by Ms. D. Grego, DuPont

Hours of Operation =

8760 hr

Average Emission Rates

Acetic Acid

Emission Rate = 4.74E-08 g/s Emission Rate = 0.0000004 lb/hr Emission Rate = 0.0003 lb/yr Emission Rate = 0.000002 tpy

Chloroprene

Emission Rate = 9.316E-06 g/s
Emission Rate = 0.00007 lb/hr
Emission Rate = 0.6 lb/yr
Emission Rate = 0.0003 tpy

Toluene

Emission Rate = 2.346E-07 g/s
Emission Rate = 0.000002 lb/hr
Emission Rate = 0.002 lb/yr
Emission Rate = 0.000008 tpy

ACR

Emission Rate = 2.346E-07 g/s
Emission Rate = 0.000002 lb/hr
Emission Rate = 0.02 lb/yr
Emission Rate = 0.000008 tpy



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Clarifier

TEMPO ID:

Point Source ID No.: 6-95

Page

2

of

3

1,2-Dichlorobenzene

Emission Rate = 2.04E-06 g/s Emission Rate = 0.00002 lb/hr Emission Rate = 0.1 lb/yr

Emission Rate = 0.00007 tpy

Maximum Emission Rates

Acetic Acid

Emission Rate = 3.66E-07 g/s Emission Rate = 0.00000 lb/hr

Chloroprene

Emission Rate = 4.03E-05 g/s Emission Rate = 0.0003 lb/hr

Toluene

Emission Rate = 1.81E-06 g/s Emission Rate = 0.00001 lb/hr

ACR

Emission Rate = 1.81E-06 g/s Emission Rate = 0.00001 lb/hr

1,2-Dichlorobenzene

Emission Rate = 1.58E-05 g/s Emission Rate = 0.0001 lb/hr



RTP Environmental Associates, Inc. Kenner, Louisiana

Client: DUPONT - PONTCHARTRAIN SITE

Source Description: Clarifier

TEMPO ID:

Point Source ID No.: 6-95

Page

3

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3

Summary

Compound	Total	Average	Maximum	Annual
}	Loss	Emission	Emission	Emissions
]		Rate	Rate	
<u>l</u>	lb/yr	lb/hr	lb/hr	tpy
Total VOC	0.7	0.00008	0.0004	0.0003
Chloroprene	0.6	0.00007	0.0003	0.0003
1,2-Dichlorobenze	0.1	0.00002	0.0001	0.00007
Toluene	0.02	0.000002	0.00001	0.000008
Total HAPs	0.8	0.00009	0.0005	0.0004
Total TAPs	0.8	0.00009	0.0005	0.0004

APPENDIX B CERTIFICATION OF GOOD STANDING

Tom Schedler Secretary of State State of Louisiana Secretary of State



COMMERCIAL DIVISION 225.925.4704

<u>Fax Numbers</u> 225.932.5317 (Admin. Services) 225.932.5314 (Corporations) 225.932.5318 (UCC)

Name

Type

City

Status

E. I. DU PONT DE NEMOURS AND COMPANY

Business Corporation (Non-Louisiana)

WILMINGTON

Active

Business:

E. I. DU PONT DE NEMOURS AND COMPANY

Charter Number:

09302090F

Registration Date:

4/24/1919

State Of Origin:

Domicile Address

1007 MARKET STREET

WILMINGTON, DE 19898

Mailing Address

ATTENTION: TAX DIVISION, D-13039

1007 MARKET STREET WILMINGTON, DE 19898

Principal Business Office

1007 MARKET STREET

WILMINGTON, DE 19898

Registered Office in Louisiana

5615 CORPORATE BLVD., STE. 400B

BATON ROUGE, LA 70808

Principal Business Establishment in Louisiana

PONTCHARTRAIN WORKS

LAPLACE, LA 70068

Status

Status:

Active

Annual Report Status:

In Good Standing

Qualified:

4/24/1919

Last Report Filed:

4/4/2012

Type:

Business Corporation (Non-Louisiana)

Registered Agent(s)

Agent:

C T CORPORATION SYSTEM

Address 1:

5615 CORPORATE BLVD., STE. 400B

City, State, Zip:

BATON ROUGE, LA 70808

Appointment Date: 12/12/1955

Officer(s)

Additional Officers: No

Officer:

NICHOLAS C. FANANDAKIS

Title:

Executive Vice-President

Address 1:

1007 MARKET ST.

10 . - L Dataila Drint agny? CharterID

City, State, Zip:	WILMINGTON, DE 19898
Officer:	THOMAS M. CONNELLY, JR.
Title:	Executive Vice-President
Address 1:	1007 MARKET ST.
City, State, Zip:	WILMINGTON, DE 19898
Officer:	MARY E. BOWLER
Title:	Secretary
Address 1:	1007 MARKET ST.
City, State, Zip:	WILMINGTON, DE 19898
Officer:	MARY P. VAN VEEN
Title:	Vice-President
Address 1:	1007 MARKET ST.
City, State, Zip:	WILMINGTON, DE 19898
Officer:	ELLEN J. KULLMAN
Title:	Officer, Director
Address 1:	1007 MARKET ST.
City, State, Zip:	WILMINGTON, DE 19898

Mergers (4)

Filed Date	Effective Date:	Туре	Charter#	Chater Name	Role
1/29/1973	1/29/1973	MERGE	09302090F	E. I. DU PONT DE NEMOURS AND COMPANY	SURVIVOR
6/4/1973	6/4/1973	MERGE	09302090F	E. I. DU PONT DE NEMOURS AND COMPANY	SURVIVOR
10/24/1977	10/24/1977	MERGE	09302090F	E. I. DU PONT DE NEMOURS AND COMPANY	SURVIVOR
4/19/1982	4/19/1982	MERGE	09302090F	E. I. DU PONT DE NEMOURS AND COMPANY	SURVIVOR

Amendments on File (35)

Description	Date
Amendment	6/18/1923
Amendment	7/27/1925
Amendment	11/13/1926
Amendment	2/16/1929
Amendment	5/14/1934
Amendment	8/23/1937
Amendment	10/30/1939
Amendment	5/2/1940
Amendment	4/10/1942
Amendment	6/22/1946
Amendment	5/12/1947
Amendment	5/12/1947
Amendment	6/20/1949
Amendment	7/11/1955
Amendment	7/11/1955
Amendment	7/11/1955
Amendment .	12/5/1957
Amendment	7/19/1963
Amendment	9/26/1966

Amendment	5/6/1968
Amendment	5/14/1970
Merger	1/29/1973
Merger	6/4/1973
Amendment	4/29/1974
Merger	10/24/1977
Amendment	10/24/1977
Amendment	4/20/1979
Amendment	4/20/1979
Amendment	4/25/1980
Amendment	8/21/1981
Merger	4/19/1982
Stmt of Chg or Chg Prin Bus Off	2/22/1985
Stmt of Chg or Chg Prin Bus Off	4/1/1986
Stmt of Chg or Chg Prin Bus Off	2/1/1993
Stmt of Chg or Chg Prin Bus Off	1/29/2008

Print

APPENDIX C FUGITIVE EMISSIONS PROGRAM CONSOLIDATION NOTICE.

Louisiana Fugitive Emission Program Consolidation Source Notice and Agreement DuPont Pontchartrain Site, St. John the Baptist Parish (Agency Interest Numbers 1101 and 38806)

By this notice and agreement, E. I. du Pont de Nemours Co. (DuPont Pontchartrain Site) notifies the Louisiana DEQ (LDEQ) and the United States Environmental Protection Agency (EPA) of the consolidation of fugitive emission programs as indicated below, effective January 1, 2014. Semiannual reports will be submitted on August 15 and February 15, to cover the periods January 1 through June 30 and July 1through December 31, respectively. DuPont Pontchartrain Site agrees to implement the consolidated program in accordance with the Louisiana Fugitive Emission Program Consolidation Guidelines attached, and accepts federal and state enforceability of the consolidated program by EPA and LDEQ. DuPont Pontchartrain Site further acknowledges that compliance with the consolidated program in accordance with the Guidelines will serve to comply with each of the fugitive emission programs being consolidated. In addition, DuPont Pontchartrain Site acknowledges that noncompliance with the consolidated program in accordance with the Guidelines may subject DuPont Pontchartrain Site to enforcement action for one or more of the fugitive emissions programs being consolidated. Unless successfully challenged or otherwise terminated, this agreement remains in effect until revised or replaced upon request by DuPont Pontchartrain Site, LDEQ, or EPA, or until the initial Part 70 permit is issued for DuPont Pontchartrain Site, whichever is earliest. If, at any time, the agreement is not in effect with the State, then it shall not be in effect with EPA.

While several units at the DuPont Pontchartrain Site are only subject to less stringent fugitive emission rules, the entire site will comply with the HON (40 CFR 63 Subpart H) as the most stringent and guiding fugitive rule in each unit at the site per table below. On the effective date the reporting, recordkeeping, and monitoring time period (schedule) will be readjusted for the entire site to coincide with the current Diamines, ACR, and HCL Recovery Unit's schedule which runs as a calendar year from January through December therefore making the entire site applicable to just one time period. Also from the effective date, leak rates will be consolidated and calculated for the entire site per HON guidelines. The DuPont Pontchartrain Site will continue the annual valve and biennial connector monitoring frequency for the plant site until percentage leak rates dictate altering the monitoring frequency.

Unit or Plant Site	Programs being	Stream	Overall Most
	Consolidated	Applicability	Stringent Program
DuPont Pontchartrain Site	63 Sub H – HON 63 Sub FFFF 63 Sub U - P & R I LA Non-HON NSPS RCRA Sub BB LAC 33:III.2121	5% VOHAP 5% VOHAP 5% VOHAP 5% VOTAP 10% VOC 10% VOC 10% VOC	63 Subpart H - HON MACT

Signed

Walter Glenn, Plant Manager

This 18 day of 16 mon, 20 13



DuPont
Pontchartrain Site
560 Highway 44
LaPlace, LA 70068-6908

November 18, 2013

Dept. of Environmental Quality
Office of Environmental Services, Air Permits Division
P. O. Box 4313
Baton Rouge, La 70821-4313

CERTIFIED MAIL NO. 7011 3500 0001 6350 0509

Re: DuPont Pontchartrain Site Fugitive Emissions Program Consolidation Source Notice and Agreement (Al# 1101 and Al# 38806)

The DuPont Pontchartrain Site (DuPont) is requesting consolidation of all applicable site fugitive emission programs in accordance with the Louisiana Fugitive Emission Program Consolidation Guidelines and is hereby submitting the attached Source Notice and Agreement. DuPont will implement the consolidated program beginning January, 1, 2014.

While several units are only subject to less stringent fugitive emission rules, the entire site will comply with the HON (40 CFR 63 Subpart H) as the most stringent and guiding fugitive rule in each unit at the site. According to 40 CFR 63.162(g)(2) and 63.9(i) it is acceptable to adjust time periods upon mutual agreement between owner and Administrator. In addition to being regulatory acceptable, adjusting time periods is in keeping with the spirit of the consolidation agreement recordkeeping and report streamlining intention. DuPont is also requesting that the reporting, recordkeeping, and monitoring time period (schedule) be readjusted for the entire site to coincide with the current Diamines, ACR, and HCL Recovery Unit's schedule which runs as a calendar year from January through December therefore making the entire site applicable to one time period. Each unit at the site currently has a leak rate that allows for annual valve and biennial connector monitoring. From the effective date, leak rates will be consolidated and calculated for the entire site per HON guidelines. The DuPont Pontchartrain Site will continue the annual valve and biennial connector monitoring frequency for the plant site until percentage leak rates dictate altering the monitoring frequency.

The following paragraphs provide additional details relating to the fugitive programs being consolidated and how the fugitive program will be structured after the effective date.

The DuPont Pontchartrain Site currently has five units subject to various fugitive emissions regulations which have multiple overlapping applicable reporting and recordkeeping requirements. The recordkeeping requirements of these various regulations result in the same data being saved and summarized multiple times in the LDAR database. The current reporting requirements result in the submittal

of ten different reports with deadlines for these reports at different times throughout the year. These different reports often result in submitting data already reported in previous reports. In other words, multiple reports are due for different periods with some of these reports requiring and containing the same data or at least some of the same data. The Fugitive Emissions Semi-annual Report Summary Table below summarizes the program report and reporting time period information for each unit.

The following is a list of the units at the site with the most stringent applicable regulation in parenthesis: the Diamines Unit (HON), ACR Unit (MON), Chloroprene Unit (HON), the Neoprene Unit (Polymer & Resins I), and the HCL Recovery Unit (RCRA BB). The Diamines Unit which has always been owned by E. I. du Pont de Nemours Co. has already been consolidated by agreement dated October 15, 1996. The ACR, Chloroprene, HCl Recovery, and Neoprene Units were operated by DuPont Performance Elastomers, a separate entity, before 2013 and are not currently consolidated per Louisiana Fugitive Agreement. The entire facility (DuPont Pontchartrain Site) is now owned by E. I. du Pont de Nemours Co.

Fugitive Emissions Semi-annual Report Summary Table

rugitive Emissions Semi-amuai neport Summary Table				
Unit	Program Report	Reporting Time Period before	Reporting Time Period beginning	
		January 1, 2014	on January 1, 2014	
Diamines	HON -	January through	January through	
	Consolidated	June and July	June and July	
		through December	through December	
Chloroprene	HON	April through	January through	
		September and	June and July	
		October through	through December	
	· ·	March		
Neoprene	Polymers and	August through	January through	
·	Resins I	January and	June and July	
Ì	}	February through	through December	
		July		
ACR	MON	January through	January through	
		June and July	June and July	
		through December	through December	
HCL Recovery	Chapter 21	January through		
		June and July	June and July	
		through December	through December	

Note: Chapter 21 report contains data from Chloroprene, Neoprene, and ACR Units also.

Consolidating all the units at the DuPont Pontchartrain Site and making HON the Guiding Regulation (most stringent rule) throughout the site, will reduce the recordkeeping and reporting requirements without reducing quality of data that was submitted in the multiple reports. All of the monitoring and leak data would still be reported, it will just be reported in two semi-annual reports instead of the current ten reports that result in multiple instances of data duplication. The site will also be complying with an overall more stringent fugitive emissions program

than by complying with various less stringent programs, therefore over time reducing fugitive emissions at the site. The DuPont Pontchartrain Site will continue to submit fugitive reports for the non-HON regulations until all data for the 2013 calendar year has been reported. After all 2013 data has been reported per non-HON fugitive requirements, the DuPont Pontchartrain Site will discontinue these non-HON fugitive reports and will only submit HON semi-annual reports twice a year for the entire site.

Each unit at the site currently has a leak rate that allows for annual valve and biennial connector monitoring. The DuPont Pontchartrain Site will continue this monitoring frequency (skip period frequency) for the plant site until percentage leak rates dictate altering the monitoring frequency. Leak rates will be calculated for the entire site per HON for periods that relate to calendar year of January through December beginning on the effective date.

In summary, on January 1, 2014, the effective date of the consolidated agreement, the DuPont Pontchartrain Site will streamline the recordkeeping, reporting, and monitoring requirements and readjust the recordkeeping, reporting, and monitoring requirements' annual time period to January through December to coincide with the current Diamines, ACR, and HCL Recovery Units' annual time period while keeping the current skip period monitoring frequency intact.

At the next opportunity for renewal or modification of each of the effective permits, DuPont will include a copy of the Fugitive Emissions Program Consolidation Source Notice and Agreement in each of the effective Title V operating permit applications. Current effective Permit Numbers are 3000-V3, 206-V1, 2249-V6, and 2090-V5.

If you have any questions or need additional information you can contact me at (985) 536-5438, or at Anthony. J. Fugarino@dupont.com.

Sincerely,

Anthony Fugarino SHE Consultant

Unthoug Ingarus

Enclosures

cc: US EPA Region 6

Compliance Assurance and Enforcement Division

Mail Number: 6-EN-A

1445 Ross Avenue, Suite 700 Dallas, Texas 75202-2733

CERTIFIED MAIL NO. 7011 3500 0001 6350 0516